1 Variables

2 root

| | var | symbol | documentation | type | units | eqs |
|----|----------------------|-------------|--|---------|-------|-----|
| 3 | $F^{source}_{N,I}$ | F_NI_source | incidence matrix NI source | network | | |
| 8 | $F^{sink}_{N,A}$ | F_NA_sink | incidence matrix NA sink | network | | |
| 18 | cz_I | cz_I | interface variable macro -> control | network | | |
| 19 | $A_{N,p,q}$ | A_Npq | mapping from inputs to outputs | network | | |
| 7 | $F^{source}_{N,A}$ | F_NA_source | incidence matrix NA source | network | | |
| 15 | $S_{N,q,t}$ | S_Nqt | selection matrix or splitter | network | | |
| 5 | $F^{source}{}_{A,I}$ | F_AI_source | incidence matrix AI source | network | | |
| 11 | $I_{t,u}$ | I_tu | identity mapping from <t> to <u></u></t> | network | | |
| 2 | $F_{N,A}$ | F | incidence matrix | network | | |
| 13 | $S_{I,q}$ | S_Aq | selection matrix arcs to outputs | network | | |
| 10 | $S_{I,q}$ | S_Iq | selection matrix interface to control output | network | | |
| 9 | $S_{I,p}$ | S_Ip | selection matrix interface to control input | network | | |
| 14 | $S_{N,p,q}$ | S_Npu | selection matrix for stacker | network | | |
| 4 | $F^{sink}{}_{N,I}$ | F_NI_sink | incidence matrix NI sink | network | | |
| 21 | $u_{N,t,u}$ | u_Ntu | input signal in control domain | network | | |
| 6 | $F^{sink}{}_{A,I}$ | F_AI_sink | incidence matrix AI sink | network | | |
| 22 | $y_{N,t,u}$ | y_Ntu | output signal in control domain | network | | |
| 27 | $I_{N,A}$ | I_NA | $ \ identity \ mapping \ from \ < N > \ to \ < A > $ | network | | |
| 20 | $A_{N,t,u}$ | A_Ntu | mapping from input elements to outputs | network | | |
| 12 | $S_{A,p}$ | S_Ap | selection matrix interface species-related measures | network | | |
| 17 | cz_N | cz_N | output from control | network | | |

| | var | symbol | documentation | type | units | eqs |
|-----|------------|------------|-------------------------------------|----------|-------|-----|
| 16 | mv_I | mv_I | interface variable macro -> control | network | | |
| 105 | t^o | to | starting time | frame | s | 4 |
| 106 | t^e | te | end time | frame | s | 5 |
| 107 | Δt | t_interval | time interval | frame | s | 6 |
| 1 | t | t | time | frame | s | |
| 104 | 0.5 | oneHalf | numerical value one half | constant | | 3 |
| 199 | pi | pi | | constant | | 94 |
| 102 | 0 | zero | numerical value zero | constant | | 1 |
| 103 | 1 | one | numerical value one | constant | | 2 |
| 101 | # | value | numerical value | constant | | |

3 physical

| | var | symbol | documentation | type | units | eqs |
|-----|-------------|--------|--------------------------------------|----------------|-------------------------------------|------------|
| 24 | r_{yN} | r_y | y-coordinate | frame | m | |
| 23 | r_{xN} | r_x | x-coordinate | frame | m | |
| 25 | r_{zN} | r_z | z-coordinate | frame | m | |
| 109 | S_N | S | fundamental state – internal entropy | state | $kgm^2K^{-1}s^{-2}$ | |
| 111 | $n_{N,S}$ | n | fundamental state – molar mass | state | mol | 93 |
| 110 | V_N | V | volume | state | m^3 | 7 97 98 |
| 137 | m_N | m | mass | state | kg | 30 |
| 144 | C_N | C | fundamental state – charge | state | A s | |
| 108 | U_N | U | fundamental state – internal energy | state | kgm^2s^{-2} | |
| 123 | R | R | gas constant | constant | $kg m^2 mol^{-1} K^{-1} s^{-2}$ | 17 |
| 122 | k^B | Boltz | Boltzmann constant | constant | $kg m^2 K^{-1} s^{-2}$ | |
| 121 | N^A | Avo | Avogadro constant | constant | mol^{-1} | |
| 132 | λ_S | Mm | molecular masses | constant | $kgmol^{-1}$ | |
| 150 | A_{yzN} | Ayz | cross sectional area yz | secondaryState | m^2 | 42 |
| 148 | A_{xyN} | Axy | cross sectional area xy | secondaryState | m^2 | 40 95 |
| 149 | A_{xzN} | Axz | cross sectional are xz | secondaryState | m^2 | 41 |
| 143 | $ ho_N$ | rho | density | secondaryState | kgm^{-3} | 36 |

4 macroscopic

| | var | symbol | documentation | type | units | eqs |
|-----|--------------------------------|-----------|---|------------|--------------------------|-------|
| 157 | d_A | d | flow direction of convective flow | transport | | 49 |
| 194 | $\dot{n}_{N,S}$ | anc | accumulation of molar mass due to convection | transport | $mol s^{-1}$ | 87 |
| 159 | \hat{V}_A | fV | volumetric flow in x-direction | transport | $m^3 s^{-1}$ | 51 |
| 153 | \hat{q}_{zA} | fq_z | heat flow in z-direction | transport | $kg m^2 s^{-3}$ | 45 |
| 152 | \hat{q}_{yA} | fq_y | heat flow in y-direction | transport | $kg m^2 s^{-3}$ | 44 |
| 160 | $\hat{n}_{xA,S}^{c}$ | fnc_x | molar convective flow in x-direction | transport | $mol s^{-1}$ | 52 |
| 154 | $\hat{n}_{xA,S}^d$ | fnd_x | diffusion flow in x-direction | transport | $mol s^{-1}$ | 46 89 |
| 156 | $\hat{n}_{zA,S}^d$ | fnd_z | diffusion flow in z-direction | transport | $mol s^{-1}$ | 48 91 |
| 158 | $c_{A,S}$ | c_AS | concentration in convective event-dynamic flow | transport | $m^{-3} mol$ | 50 |
| 195 | $\dot{n}^{d}{}_{N,S}$ | and_x | accumulation due to diffusion in x-direction | transport | $mol s^{-1}$ | 88 |
| 155 | $\hat{n}_{yA,S}^d$ | fnd_y | diffusion flow in y-direction | transport | $mol s^{-1}$ | 47 90 |
| 151 | \hat{q}_{xA} | fq_x | heat flow in x-direction | transport | kgm^2s^{-3} | 43 |
| 191 | $\hat{k}_{y}^{d,Fick}{}_{A,S}$ | kdAFick_y | Fick diffusivity in arc and y-direction | properties | ms^{-1} | 84 |
| 186 | k_{xA}^q | kqA_x | thermal conductivity in arc and x-direction | properties | $kg K^{-1} s^{-3}$ | 79 |
| 180 | $k_{xA,S}^d$ | kdA_x | diffusivity in arc and x-direction | properties | $kg^{-1} m^{-4} mol^2 s$ | 73 |
| 185 | k_{zA}^c | kcA_z | convecive mass conductivity in arc and y-direction | properties | $m^{-1} s$ | 78 |
| 181 | $k_{yA,S}^d$ | kdA_y | diffusivity in arc and y-direction | properties | $kg^{-1} m^{-4} mol^2 s$ | 74 |
| 190 | $\hat{k}_x^{d,Fick}{}_{A,S}$ | kdAFick_x | Fick's diffusivity in arc and x-direction | properties | ms^{-1} | 83 |
| 187 | k_{yA}^q | kqA_y | thermal conductivity in arc and y-direction | properties | $kg K^{-1} s^{-3}$ | 80 |
| 183 | k_{xA}^c | kcA_x | convective mass conductivity in arc and x diretion | properties | $m^{-1} s$ | 76 |
| 189 | ρ_A | rhoA | density in arc | properties | $kg m^{-3}$ | 82 |
| 188 | k_{zA}^q | kqA_z | thermal conductivity in arc and z-direction | properties | $kg K^{-1} s^{-3}$ | 81 |
| 184 | k_{yA}^c | kcA_y | convective mass conductivity in arc and y-direction | properties | $m^{-1} s$ | 77 |

| | var | symbol | documentation | type | units | eqs |
|-----|------------------------------|-----------------|---|----------------|-----------------------------|-------|
| 182 | $k_{zA,S}^d$ | kdA_z | diffusivity in arc and z-direction | properties | $kg^{-1} m^{-4} mol^2 s$ | 75 |
| 192 | $\hat{k}_z^{d,Fick}{}_{A,S}$ | kdAFick_z | Fick diffusivity in arc and z-direction | properties | ms^{-1} | 85 |
| 193 | $h_{A,S}$ | hA | partial molar enthalpiies in arc | properties | $kg m^2 mol^{-1} s^{-2}$ | 86 |
| 115 | H_N | Н | Enthalpy | state | $kg m^2 s^{-2}$ | 11 |
| 116 | A_N | A | Helmholtz energy | state | $kg m^2 s^{-2}$ | 12 |
| 117 | G_N | G | Gibbs free energy | state | $kg m^2 s^{-2}$ | 13 |
| 197 | d_{xN} | d_x | diameter x | constant | $\mid m \mid$ | |
| 161 | $\mu^{o}{}_{N,S}$ | chemPotStandard | instantiating standard chemical potential | effort | $kg m^2 mol^{-1} s^{-2}$ | 53 |
| 113 | T_N | Т | temperature | effort | K | 9 |
| 114 | $\mu_{N,S}$ | chemPot | chemical potential | effort | $kg m^2 mol^{-1} s^{-2}$ | 10 54 |
| 112 | p_N | p | thermodynamic pressure | effort | $kg m^{-1} s^{-2}$ | 8 |
| 138 | $c_{N,S}$ | С | molar concentration | secondaryState | $m^{-3} mol$ | 31 |
| 141 | c_{pN} | ср | specific heat capacity at constant pressure | secondaryState | $m^2 K^{-1} s^{-2}$ | 34 |
| 125 | CV_N | CV | total heat capacity at constant volume | secondaryState | $kg m^2 K^{-1} s^{-2}$ | 19 |
| 120 | v_{zN} | V_Z | velocity in z-direction | secondaryState | ms^{-1} | 16 |
| 118 | v_{xN} | v_x | velocity in x-direction | secondaryState | ms^{-1} | 14 |
| 139 | $n^t{}_N$ | nt | total number of moles | secondaryState | mol | 32 |
| 124 | Cp_N | Ср | total heat capacity at constant pressure | secondaryState | $kg m^2 K^{-1} s^{-2}$ | 18 |
| 136 | $h_{N,S}$ | h | partial molar enthalpies | secondaryState | $kg m^2 mol^{-1} s^{-2}$ | 29 |
| 140 | $x_{N,S}$ | x | mole fraction | secondaryState | | 33 |
| 200 | h_{LN} | h_L | liquid level cylinder | secondaryState | $\mid m \mid$ | 96 |
| 119 | v_{yN} | v_y | velocity in y-direction | secondaryState | ms^{-1} | 15 |
| 142 | c_{VN} | cV | specific heat capacity at constant volume | secondaryState | $m^2 K^{-1} s^{-2}$ | 35 |
| 196 | $\dot{n}_{N,S}$ | an | differential mass balance without reaction | diffState | $mol s^{-1}$ | 92 |

5 reactions

| | var | symbol | documentation | type | units | eqs |
|-----|---------------|-------------|--|----------------|---------------|-----|
| 26 | $N_{S,K}$ | N | stoichiometric matrix | constant | | |
| 167 | $T_{N,p}$ | Т | link variable T to interface reactions | effort | K | 60 |
| 171 | ${V}_{N,p}$ | V | link variable V to interface reactions | secondaryState | m^3 | 64 |
| 163 | $c_{N,S,p}$ | С | link variable c to interface reactions | secondaryState | $m^{-3} mol$ | 56 |
| 165 | $x_{N,S,p}$ | x | link variable x to interface reactions | secondaryState | | 58 |
| 169 | $\xi_{N,K,p}$ | probability | probability of reaction to take place | conversion | | 62 |
| 168 | $f_{N,S,K,p}$ | factor | factor for probability computation | conversion | | 61 |

6 macroscopic-reactions

| | var | symbol | documentation | type | units | eqs |
|-----|-------------|--------|---|------|---------------|-----|
| 166 | $_T_I$ | _Т | link variable T to interface macroscopic $\gg>$ reactions with source:node | get | K | 59 |
| 164 | $_x_{I,S}$ | _x | $\begin{array}{c} \mbox{link variable x to interface macroscopic } > \mbox{reactions} \\ \mbox{with source:node} \end{array}$ | get | | 57 |
| 162 | $_c_{I,S}$ | _c | link variable c to interface macroscopic »> reactions with source:node | get | $m^{-3} mol$ | 55 |
| 170 | $_V_I$ | _V | $\begin{array}{c} link\ variable\ V\ to\ interface\ macroscopic\ >> reactions \\ with\ source:node \end{array}$ | get | m^3 | 63 |

7 Equations

8 Generic

| no | equation | documentation | layer |
|----|--|--------------------------|-------------|
| 1 | $0 := \mathbf{Instantiate}(\#, \#)$ | numerical value zero | root |
| 2 | $1 := \mathbf{Instantiate}(\#, \#)$ | numerical value one | root |
| 3 | $0.5 := \mathbf{Instantiate}(\#, \#)$ | numerical value one half | root |
| 4 | $t^o := \mathbf{Instantiate}(t, \#)$ | starting time | root |
| 5 | $t^e := \mathbf{Instantiate}(t, \#)$ | end time | root |
| 6 | $\Delta t := \mathbf{Instantiate}(t, \#)$ | time interval | root |
| 7 | $V_N := r_{xN} \cdot r_{yN} \cdot r_{zN}$ | volume | physical |
| 8 | $p_N := rac{\partial U_N}{\partial V_N}$ | thermodynamic pressure | physical |
| 9 | $T_N := \frac{\partial U_N}{\partial S_N}$ | temperature | macroscopic |
| 10 | $\mu_{N,S} := \frac{\partial U_N}{\partial n_{N,S}}$ | chemical potential | macroscopic |
| 11 | $H_N := U_N - p_N \cdot V_N$ | Enthalpy | macroscopic |
| 12 | $A_N := U_N - T_N \cdot S_N$ | Helmholtz energy | macroscopic |
| 13 | $G_N := U_N + p_N \cdot V_N - T_N \cdot S_N$ | Gibbs free energy | macroscopic |
| 14 | $v_{xN} := \frac{\partial r_{xN}}{\partial t}$ | velocity in x-direction | macroscopic |
| 15 | $v_{yN} := \frac{\partial r_{yN}}{\partial t}$ | velocity in y-direction | macroscopic |
| 16 | $v_{zN} := \frac{\partial r_{zN}}{\partial t}$ | velocity in z-direction | macroscopic |

| no | equation | documentation | layer |
|----|--|---|-------------|
| 17 | $R := N^A \cdot k^B$ | gas constant | physical |
| 18 | $Cp_N := rac{\partial H_N}{\partial T_N}$ | total heat capacity at constant pressure | macroscopic |
| 19 | $CV_N := \frac{\partial U_N}{\partial T_N}$ | total heat capacity at constant volume | macroscopic |
| 29 | $h_{N,S} := H_N \cdot (n_{N,S})^{-1}$ | partial molar enthalpies | macroscopic |
| 30 | $m_N := \lambda_S \stackrel{S}{\star} n_{N,S}$ | mass | macroscopic |
| 31 | $c_{N,S} := (V_N)^{-1} \cdot n_{N,S}$ | molar concentration | macroscopic |
| 32 | $n^{t}{}_{N} := \mathbf{reduceSum}\left(n_{N,S},S ight)$ | total number of moles | macroscopic |
| 33 | $x_{N,S} := \left(n^t{}_N\right)^{-1} \cdot n_{N,S}$ | mole fraction | macroscopic |
| 34 | $c_{pN} := Cp_N \cdot (m_N)^{-1}$ | specific heat capacity at constant pressure | physical |
| 35 | $c_{VN} := CV_N \cdot \left(m_N\right)^{-1}$ | specific heat capacity at constant volume | macroscopic |
| 36 | $\rho_N := \left(V_N\right)^{-1} . m_N$ | density | physical |
| 40 | $A_{xyN} := r_{xN} \cdot r_{yN}$ | cross sectional area xy | physical |
| 41 | $A_{xzN} := r_{xN} \cdot r_{zN}$ | cross sectional are xz | physical |
| 42 | $A_{yzN} := r_{yN} \cdot r_{zN}$ | cross sectional area yz | physical |
| 43 | $\hat{q}_{xA} := k_{xA}^q \cdot A_{yzN} \cdot F_{N,A} \overset{N}{\star} T_N$ | heat flow in x-direction | macroscopic |
| 44 | $\hat{q}_{yA} := k_{yA}^q \cdot A_{xzN} \cdot F_{N,A} \overset{N}{\star} T_N$ | heat flow in y-direction | macroscopic |
| 45 | $\hat{q}_{zA} := k_{zA}^q \cdot A_{xyN} \cdot F_{N,A} \stackrel{N}{\star} T_N$ | heat flow in z-direction | macroscopic |

| no | equation | documentation | layer |
|----|---|--|-------------|
| 46 | $\hat{n}_{xA,S}^d := \hat{k}_x^{d,Fick}{}_{A,S} \cdot A_{yzN} \cdot F_{N,A} \overset{N}{\star} c_{N,S}$ | Fick diffusion flow in x-direction | macroscopic |
| 47 | $\hat{n}_{yA,S}^d := \hat{k}_y^{d,Fick}{}_{A,S} \cdot A_{xzN} \cdot F_{N,A} \overset{N}{\star} c_{N,S}$ | Fick diffusion flow in y-direction | macroscopic |
| 48 | $\hat{n}_{zA,S}^d := \hat{k}_z^{d,Fick}{}_{A,S} \cdot (A_{xyN} \cdot F_{N,A}) \stackrel{N}{\star} c_{N,S}$ | Fick diffusion flow in z-direction | macroscopic |
| 49 | $d_A := \mathbf{sign}\left(F_{N,A} \stackrel{N}{\star} p_N ight)$ | flow direction of convective flow | macroscopic |
| 50 | $c_{A,S} := (0.5 \cdot (F_{N,A} - d_A \cdot F_{N,A})) \stackrel{N}{\star} c_{N,S}$ | concentration in convective event- dynamic flow | macroscopic |
| 51 | $\hat{V}_A := (\rho_A)^{-1} \cdot k_{xA}^c \cdot A_{yzN} \cdot F_{N,A} \stackrel{N}{\star} p_N$ | volumetric flow in x-direction | macroscopic |
| 52 | $\hat{n}_{xA,S}^c := \hat{V}_A \cdot c_{A,S}$ | molar convective flow in x-direction | macroscopic |
| 53 | $\mu^o{}_{N,S} := \mathbf{Instantiate}(\mu_{N,S},\#)$ | instantiating standard chemical potential | macroscopic |
| 54 | $\mu_{N,S} := \mu^{o}_{N,S} + R \cdot T_{N} \cdot \ln \left(x_{N,S} \right)$ | chemical potential standard model with mole fraction | macroscopic |
| 61 | $f_{N,S,K,p} := x_{N,S,p}((N_{S,K}))$ | factor for probability computation | reactions |
| 62 | $\xi_{N,K,p} := \prod_S f_{N,S,K,p}$ | probability of reaction to take place | reactions |
| 73 | $k_{xA,S}^d := I_{N,A} * \left(\left(\mu_{N,S} \right)^{-1} \cdot \left(v_{xN} \cdot \left(\left(V_N \right)^{-1} \cdot \frac{\partial U_N}{\partial \mu_{N,S}} \right) \right) \right)$ | diffusivity in arc and x-direction | macroscopic |
| 74 | $k_{yA,S}^d := I_{N,A} * \left(\left(\mu_{N,S} \right)^{-1} \cdot \left(v_{yN} \cdot \left(\left(V_N \right)^{-1} \cdot \frac{\partial U_N}{\partial \mu_{N,S}} \right) \right) \right)$ | diffusivity in arc and y-direction | macroscopic |
| 75 | $k_{zA,S}^d := I_{N,A} * \left((\mu_{N,S})^{-1} \cdot \left(v_{zN} \cdot \left((V_N)^{-1} \cdot \frac{\partial U_N}{\partial \mu_{N,S}} \right) \right) \right)$ | diffusivity in arc and z-direction | macroscopic |
| 76 | $k_{xA}^c := I_{N,A} * \left(\left(\lambda_S * (\mu_{N,S})^{-1} \right) \cdot (V_N)^{-1} \cdot \frac{\partial U_N}{\partial p_N} \cdot v_{xN} \right)$ | convective mass conductivity in arc and x diretion | macroscopic |
| 77 | $k_{yA}^c := I_{N,A} * \left(\left(\lambda_S * (\mu_{N,S})^{-1} \right) \cdot (V_N)^{-1} \cdot \frac{\partial U_N}{\partial p_N} \cdot v_{yN} \right)$ | convective mass conductivity in arc and y-direction | macroscopic |

| no | equation | documentation | layer |
|----|--|--|-------------|
| 78 | $k_{zA}^c := I_{N,A} * \left(\left(\lambda_S * (\mu_{N,S})^{-1} \right) \cdot (V_N)^{-1} \cdot \frac{\partial U_N}{\partial p_N} \cdot v_{zN} \right)$ | convecive mass conductivity in arc and y-direction | macroscopic |
| 79 | $k_{xA}^q := I_{N,A} * \left((V_N)^{-1} \cdot Cp_N \cdot v_{xN} \right)$ | thermal conductivity in arc and x-direction | macroscopic |
| 80 | $k_{yA}^q := I_{N,A} * \left((V_N)^{-1} . Cp_N . v_{yN} \right)$ | thermal conductivity in arc and y-direction | macroscopic |
| 81 | $k_{zA}^q := I_{N,A} * \left((V_N)^{-1} \cdot Cp_N \cdot v_{zN} \right)$ | thermal conductivity in arc and z-direction | macroscopic |
| 82 | $ ho_A := I_{N,A} \stackrel{N}{\star} ho_N$ | density in arc | macroscopic |
| 83 | $\hat{k}_x^{d,Fick}{}_{A,S} := I_{N,A} \stackrel{N}{\star} \left(v_{xN} \cdot \frac{\partial U_N}{\partial \mu_{N,S}} \cdot (n_{N,S})^{-1} \right)$ | Fick's diffusivity in arc and x-direction | macroscopic |
| 84 | $\hat{k}_{y}^{d,Fick}{}_{A,S} := I_{N,A} * \left(v_{yN} \cdot \frac{\partial U_{N}}{\partial \mu_{N,S}} \cdot (n_{N,S})^{-1} \right)$ | Fick diffusivity in arc and y-direction | macroscopic |
| 85 | $\hat{k}_z^{d,Fick}{}_{A,S} := I_{N,A} \stackrel{N}{\star} \left(v_{zN} \cdot \frac{\partial U_N}{\partial \mu_{N,S}} \cdot (n_{N,S})^{-1} \right)$ | Fick diffusivity in arc and z-direction | macroscopic |
| 86 | $h_{A,S} := I_{N,A} \stackrel{N}{\star} h_{N,S}$ | partial molar enthalpiies in arc | macroscopic |
| 87 | $\dot{n}_{N,S} := F_{N,A} \stackrel{A}{\star} \hat{n}_{xA,S}^c$ | accumulation of molar mass due to convection | macroscopic |
| 88 | $\dot{n}^d{}_{N,S} := F_{N,A} \stackrel{A}{\star} \hat{n}^d_{xA,S}$ | accumulation due to diffusion in x-direction | macroscopic |
| 89 | $\hat{n}_{xA,S}^d := k_{xA,S}^d \cdot (A_{yzN} \cdot F_{N,A}) *^{N} \mu_{N,S}$ | Fick diffusion flow in x-direction | macroscopic |
| 90 | $\hat{n}_{yA,S}^d := k_{yA,S}^d \cdot (A_{yzN} \cdot F_{N,A}) *^{N}_{\star} \mu_{N,S}$ | Fick diffusion flow in y-direction | macroscopic |
| 91 | $\hat{n}_{zA,S}^d := k_{zA,S}^d \cdot (A_{xyN} \cdot F_{N,A}) *^{N} \mu_{N,S}$ | mass diffusion flow in z-direction | macroscopic |
| 92 | $\dot{n}_{N,S} := \dot{n}_{N,S} + \dot{n}^d{}_{N,S}$ | differential mass balance without reaction | macroscopic |

| no | equation | documentation | layer |
|----|---|--------------------------------|-------------|
| 93 | $n_{N,S} := \int_{t^o}^{t^e} \dot{n}_{N,S} \ dt$ | fundamental state – molar mass | macroscopic |
| 94 | $pi := \mathbf{Instantiate}(\#, \#)$ | | root |
| 95 | $A_{xyN} := pi \cdot (0.5 \cdot d_{xN}) \cdot (0.5 \cdot d_{xN})$ | cross sectional area xy | macroscopic |
| 96 | $h_{LN} := V_N \cdot \left(A_{xyN} \right)^{-1}$ | liquid level cylinder | macroscopic |
| 97 | ${V}_N := \mathbf{Root}\left(ho_N ight)$ | volume | macroscopic |
| 98 | $V_N := m_N \cdot (\rho_N)^{-1}$ | volume | macroscopic |

9 Interface Link Equation

| no | equation | documentation | layer |
|----|---|--------------------|-------------------------------|
| 55 | $_c_{I,S} := F^{source}{}_{N,I} \stackrel{N}{\star} c_{N,S}$ | interface equation | macroscopic -> reactions |
| 56 | $c_{N,S,p} := \left(F^{sink}_{N,I} \cdot _c_{I,S}\right) \overset{I}{\star} S_{I,p}$ | interface equation | reactions |
| 57 | $_x_{I,S} := F^{source}_{N,I} \overset{N}{\star} x_{N,S}$ | interface equation | macroscopic -> re- actions |
| 58 | $x_{N,S,p} := (F^{sink}_{N,I} \cdot _x_{I,S}) \overset{I}{\star} S_{I,p}$ | interface equation | reactions |
| 59 | $_T_I := F^{source}{}_{N,I} \stackrel{N}{\star} T_N$ | interface equation | macroscopic -> re- actions |
| 60 | $T_{N,p} := \left(F^{sink}_{N,I} \cdot _T_I\right) \overset{I}{\star} S_{I,p}$ | interface equation | reactions |
| 63 | $_V_I := F^{source}{}_{N,I} \stackrel{N}{\star} V_N$ | interface equation | macroscopic -> re- actions |
| 64 | $V_{N,p} := \left(F^{sink}_{N,I} \cdot _V_I\right) \stackrel{I}{\star} S_{I,p}$ | interface equation | reactions |