# EE2703 - Applied Programming Lab Final Exam

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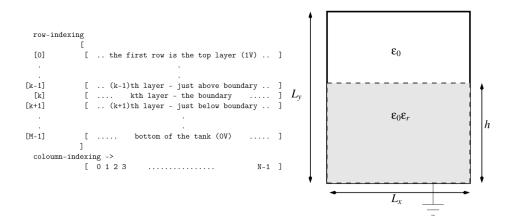
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#### Overview

In this assignment, we try to calculate the potential, electric field, and the charge distribution of a capacitor partially filled with a dielectric fluid. We analyse the system for different amounts of the fluid. We compute the distributions using Laplace's equations, some continuity equations and the given boundary conditions. We then move on to verify the continuity of  $D_n$  at the boundary and also see if the system obeys Snell's law.

#### (a) Setting up Parameters and Conventions used

Since, the exact indexing and the parameters to be used have not been mentioned in the problem statement, I would like to list out all of them used in the program here. A 100x200 mesh (M=200 and N=100) is used throughout and so, the step size is 0.1cm/step. The maximum number of iterations has been set to Niter=15000 and an accuracy of  $\delta=10^{-7}$  is desired. The following diagram shows how the matrix used in the program maps to the tank in question.



The index *k* in the matrix is calculated as :

$$k = \frac{L_y - h}{L_y} * M = (1 - \frac{h}{L_y}) * M$$

So, for example, for  $h/L_y=0.1$  and  $h/L_y=0.8$ ,  $k_{0.1}=180$  and  $k_{0.8}=40$  respectively. Also, whenever the center point of the mesh is in question, the point (M/2,N/2) is considered. Since center point can also be taken as the point next to it, there may be slight variations from the original field at the center.

#### (b) Algorithm to determine h from the observed resonant frequency f

We know that the resonant frequency is given by  $2\pi f = 1/\sqrt{LC}$ . Also for the given setup, the capacitance *C* can be calculated as the series combination of

$$C_1 = rac{A\epsilon_o}{L_v - h}$$
 and  $C_2 = rac{A\epsilon_o\epsilon_r}{h}$ 

which gives us:

$$\frac{1}{C} = \frac{1}{A\epsilon_0} (L_y - h + \frac{h}{\epsilon_r}) \dots (1)$$

where,

A=B as a area of the tank h=H eight till which fluid is filled  $L_y=T$  ot al height of the tank  $\epsilon_r=R$  elative permittivity of the fluid

So, given the above variables and the inductance of the inductor used in RLC circuit, the h required for the resonant frequency can be found out, using the expression mentioned above.

### (c) Parallelizing the computation

The central part of the computations done involve updating very huge matrices using their old values. Using for-loops for doing this would lead python to a crawl and thus would slow down the process. To parallelize these operations, we use **vectorization**. We splice different parts of the matrices required for updation and perform the update with these, in a single line. For example the following for-loop:

can be converted to a single line in python by:

Once these updates are done, the boundary conditions have to be separately updated. In our case, the boundary condition is the continuity of  $D_n$  at the fluid's surface, for which the update equation is:

$$\phi_{k,n} = \frac{\epsilon_r \phi_{k-1,n} + \phi_{k+1,n}}{(1+\epsilon r)} ,$$

where *k* denotes the row corresponding to the boundary in the potential distribution matrix.

#### (d) Calculating the potential distribution in the given system

To do so, we use Laplace's equations and the continuity of  $D_n$  at the boundary to iteratively build the distribution. The update equation for the latter has been mentioned above. For Laplace's equations, we have :

$$\phi_{m,n} = \frac{\phi_{m-1,n} + \phi_{m+1,n} + \phi_{m,n+1} + \phi_{m,n-1}}{4},$$

Apart from these, we also should take care of the given boundary conditions, i.e the top part of the tank is maintained at 1V and the other sides are grounded. The following code snippet shows the mentioned updates:

Apart from the updates, we also keep track the error by making a copy of the previous iteration and take the maximum of the absolute error between them. This is done so that when the desired accuracy is reached, we could break and not waste any more time.

```
for _ in range(Niter):
    # Copy of previous iteration
    old_phi = phi.copy()
    ... update
    # Calculation of error
    errors[_] = (abs(old_phi-phi).max())
```

Putting all the things above, the following function returns the potential distribution given the size of the mesh  $(M \times N)$ , K (the dielectric constant of the fluid), dx (the step-size of the x and y axes), hbyL (ratio of h and  $L_y$ ), acc (the required accuracy) and Niter (the maximum number of iterations).

```
def potential(M,N,K,dx,hbyL,acc,Niter):
    k = int(M*(1-hbyL))
    phi = zeros((M,N))
    phi[0] = np.ones((1,N))
    errors = ndarray((Niter,1))
    for _ in range(Niter):
```

#### (e) Charge accumulated in different parts of the tank

To calculate charge we use Gauss' law, for which we would require the electric fields distribution, which can be easily obtained from the potential distribution (*phi*) by differentiation.

$$ec{E} = -
abla \phi$$
 , which can be vectorized as

$$E_{x,(i,j)} = \frac{\phi_{i,j-1} - \phi_{i,j+1}}{\Delta x}$$
 ,  $E_{y,(i,j)} = \frac{\phi_{i-1,j} - \phi_{i+1,j}}{\Delta y}$ 

Once we have found electric field at all points, we know that :  $\int Eds = q/\epsilon$ . For the top part, we have ds = W.dx, where W is the width of the tank (the unknown dimension of the tank). So, we now have

$$\frac{q}{W} = \epsilon_o \int E dx \approx \epsilon_o . \Delta x. \sum_{x=0}^{N-1} E_{y(1,x)}$$

Essentially, we take the summation of the electric field's normal components just inside the tank, to get the charge per unit width at the top. Similarly, we can get the charge on the portion of the wall touching the dielectric fluid as the sum of :

Charge at bottom surface 
$$\approx \epsilon_0 \epsilon_r . \Delta x. \sum_{x=0}^{N-1} E_{y(-2,x)}$$
 and

Charge at walls inside fluid 
$$\approx 2 * \epsilon_0 \epsilon_r . \Delta y. \sum_{y=0}^{M-1} E_{x(y,1)}$$

The second equation is multiplied by 2 to take into account the charge on both sides, rather than computing it separately, due to symmetry. The following code snippet shows the above computations:

```
# $phi$ for field calculation
phi = potential(M,N,2,1,hbyL,10**(-7),15000)

# initialising Ex, Ey arrays
Ex = zeros((M, N)); Ey = zeros((M, N))

# filling Ex, Ey arrays with fields
Ex[1:-1, 1:-1] = (phi[1:-1, 2:] - phi[1:-1, 0:-2])/delta
Ey[1:-1, 1:-1] = (phi[2:, 1:-1] - phi[0:-2, 1:-1])/delta
```

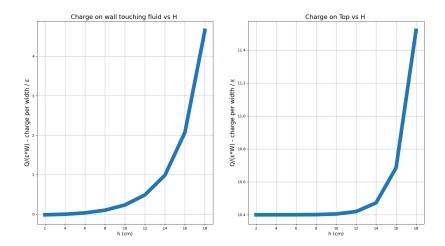
```
# Charge at top
q_top.append(-sum(Ey[1])*delta)

# Charge on tank inside fluid
q_fluid_bottom = 2*(sum(Ey[-2]))*delta
q_fluid_wall = 4*(sum(Ex[k:,1]))*delta
q_fluid.append(q_fluid_bottom+q_fluid_wall)
```

The charges were computed for different values of  $h/L_y$ . From equation (1), substituting  $\epsilon_r = 2$ , we get the following relation :

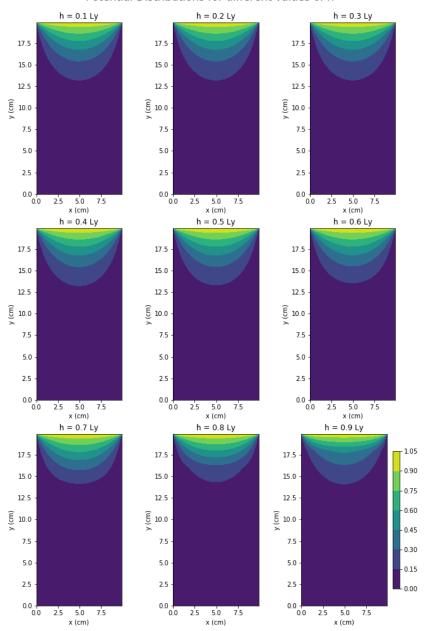
$$C \propto \frac{1}{L_y - h/2}$$

So, as h increases, C increases inversely and we expect a hyperbolic relation between C and h. Since the charge  $q \propto C$  for a capacitor, we can tell that q would approximately follow the same relation with h as that of C. So we expect it not to be linear, rather expect it to be hyperbolic. The generated plots of  $q_{top}$  vs  $h/L_y$  and and  $q_{fluid}$  vs  $h/L_y$  are shown below.



As expected, both the plots are not linear, and increase rapidly after some h like the function mentioned in equation (1). Though, Q does not vary linearly with C ideally, it was a good approximation for us to arrive at this result. The potential distributions for different hs were also plotted while calculating the charges :

#### Potential Distributions for different values of h



## (f) $\vec{E}$ Calculation at center and continuity of $D_n$

The electric field can be calculated at all points using the method described above. After doing so, we take the  $E_x$  and  $E_y$  at the index N/2 in the  $M/2^{th}$  row, which describes the boundary in the matrix, to get the electric field exactly at the center. By doing so, the electric field was found to be:

```
Ex at center :
```

 $<sup>-0.0003512403176645501 \</sup>text{ V} / \text{cm}$ 

Ey at center :

 $<sup>-0.03376457217756437\</sup> V\ /\ cm$ 

Now, to prove the continuity of  $D_n$  at the boundary, we have to prove :

$$D_{n(air)} = D_{n(fluid)} ... (at boundary)$$
  
 $\implies \epsilon_{air} E_{y(air)} = \epsilon_{fluid} E_{y(fluid)} ... (2)$ 

Here,  $E_{y(air)}$  is the electric field just above the boundary, which can be taken from the row just above the boundary row in the electric field distribution matrix. Similarly, for  $E_{y(fluid)}$ , we take the row just below it. and for any point in the boundary equation (2) must be satisfied. In other words,

$$\frac{E_{y(k+1,i)}}{E_{y(k-1,i)}} = \frac{\epsilon_{air}}{\epsilon_{fluid}} \ \forall \ 0 \leqslant i < N \ ,$$

where k refers to the index of the row representing the boundary in the matrix. So, by taking the  $(k-1)^{th}$  row and  $(k+1)^{th}$  row of  $E_y$  and performing element-wise division, we got the following array as output :

```
E_fluid/E_air at all points in boundary:
```

```
[0.48782275 0.48782328 0.48782416 0.4878254 0.48782698 0.48782889
0.48783113 0.4878337 0.48783657 0.48783975 0.4878432
                                                     0.48784693
0.48785091 0.48785514 0.48785958 0.48786423 0.48786906 0.48787406
0.4878792  0.48788447  0.48788984  0.48789529  0.48790079  0.48790634
0.4879443 0.48794934 0.48795423 0.48795893 0.48796344 0.48796773
0.4879718 \quad 0.48797561 \quad 0.48797916 \quad 0.48798244 \quad 0.48798542 \quad 0.48798811
0.48799048 0.48799253 0.48799426 0.48799564 0.48799669 0.48799738
0.48799773 0.48799773 0.48799738 0.48799669 0.48799564 0.48799426
0.48799253 0.48799048 0.48798811 0.48798542 0.48798244 0.48797916
0.48797561 0.4879718 0.48796773 0.48796344 0.48795893 0.48795423
0.48794934 0.4879443 0.48793912 0.48793383 0.48792844 0.48792297
0.48791745 0.4879119 0.48790634 0.48790079 0.48789529 0.48788984
0.48788447 0.4878792 0.48787406 0.48786906 0.48786423 0.48785958
0.48785514 0.48785091 0.48784693 0.4878432 0.48783975 0.48783657
          0.48783113 0.48782889 0.48782698 0.4878254
0.48782328 0.48782275]
```

Average value of the ratio is 0.48791123630262306

Since  $\epsilon_{fluid} = 2$ , as expected, the value of  $\frac{E_{y(k+1,i)}}{E_{y(k-1,i)}}$  at all points of the boundary is close to  $\frac{\epsilon_{air}}{\epsilon_{fluid}}$  (0.5 in our case). Hence, the continuity of  $D_n$  has been verified.

### (g) Is Snell's Law agreed here?

The change in angle at the boundary can be found by taking difference of the angle of the electric field just above the boundary and below the boundary. The angle is found taking  $tan^{-1}(E_x/E_y)$ . So,

$$\Delta\theta = tan^{-1}(E_{x(k+1,n/2)}/E_{y(k+1,n/2)} - tan^{-1}(E_{x(k-1,n/2)}/E_{y(k-1,n/2)}),$$

where (k, n/2) refers to the center of the mesh, for  $h/L_Y = 0.5$ . By doing so, the following output was obtained :

```
Incident Angle:
0.471 degrees
Transmitted Angle:
0.879 degrees
Change in Angle:
0.408 degrees
```

To check Snell's Law, we have to check if  $\frac{\sin(i)}{\sin(r)} = \frac{1}{\sqrt{\varepsilon_{fluid}}}$  From the obtained i and r,  $\frac{\sin(i)}{\sin(r)}$  comes out to be approximately 0.53. But  $\frac{1}{\sqrt{\varepsilon_{fluid}}} \approx 0.7$ . So, Snell's law is not obeyed here. It is because Snell's law is valid only for propagating electromagnetic waves. The electric field in analysis is static, so there is no varying magnetic field which could cause propagation. Another reason might be that the field is almost normally incident at the boundary, as it evident from the very small angles found out.

#### Conclusion

We successfully calculated the potential distributions for different amounts of fluid in the tank and also found the electric field and charge accumulations. We verified the continuity of  $D_n$  at the boundary and found that, at the boundary, the electric field didn't obey Snell's law, as it is static in nature, and almost normally incident.