

## Numerical Problems

**Illustrative Example 1.1** Consider an impulse gas turbine in which gas enters at pressure = 5.2 bar and leaves at 1.03 bar. The turbine inlet temperature is 1000 K and isentropic efficiency of the turbine is 0.88. If mass flow rate of air is 28 kg/s, nozzle angle at outlet is  $57^\circ$ , and absolute velocity of gas at inlet is 140 m/s, determine the gas velocity at nozzle outlet, whirl component at rotor inlet and turbine work output. Take,  $\gamma = 1.33$ , and  $C_{pg} = 1.147 \text{ kJ/kgK}$ .

### Solution

From isentropic  $p$ – $T$  relation for expansion process

$$\frac{T'_{02}}{T_{01}} = \left( \frac{p_{02}}{p_{01}} \right)^{(\gamma-1)/\gamma}$$

$$\text{or} \quad T'_{02} = T_{01} \left( \frac{p_{02}}{p_{01}} \right)^{(\gamma-1)/\gamma} = 1000 \left( \frac{1.03}{5.2} \right)^{(0.248)} = 669 \text{ K}$$

Using isentropic efficiency of turbine

$$\begin{aligned} T_{02} &= T_{01} - \eta_t (T_{01} - T'_{02}) = 1000 - 0.88(1000 - 669) \\ &= 708.72 \text{ K} \end{aligned}$$

Using steady-flow energy equation

$$\frac{1}{2} (C_2^2 - C_1^2) = C_p (T_{01} - T_{02})$$

$$\text{Therefore, } C_2 = \sqrt{[(2)(1147)(1000 - 708.72) + 19600]} = 829.33 \text{ m/s}$$

From velocity triangle, velocity of whirl at rotor inlet

$$C_{w2} = 829.33 \sin 57^\circ = 695.5 \text{ m/s}$$

Turbine work output is given by

$$\begin{aligned} W_t &= m C_{pg} (T_{01} - T_{02}) = (28)(1.147)(1000 - 708.72) \\ &= 9354.8 \text{ kW} \end{aligned}$$

**Design Example 1.2** In a single-stage gas turbine, gas enters and leaves in axial direction. The nozzle efflux angle is  $68^\circ$ , the stagnation temperature and stagnation pressure at stage inlet are  $800^\circ\text{C}$  and 4 bar, respectively. The exhaust static pressure is 1 bar, total-to-static efficiency is 0.85, and mean blade speed is 480 m/s, determine (1) the work done, (2) the axial velocity which is constant through the stage, (3) the total-to-total efficiency, and (4) the degree of reaction. Assume  $\gamma = 1.33$ , and  $C_{pg} = 1.147 \text{ kJ/kgK}$ .

**Solution**

(1) The specific work output

$$\begin{aligned} W &= C_{pg}(T_{01} - T_{03}) \\ &= \eta_{ts} C_{pg} T_{01} [1 - (1/4)^{0.33/1.33}] \\ &= (0.85)(1.147)(1073) [1 - (0.25)^{0.248}] = 304.42 \text{ kJ/kg} \end{aligned}$$

(2) Since  $\alpha_1 = 0$ ,  $\alpha_3 = 0$ ,  $C_{w1} = 0$  and specific work output is given by

$$W = UC_{w2} \quad \text{or} \quad C_{w2} = \frac{W}{U} = \frac{304.42 \times 1000}{480} = 634.21 \text{ m/s}$$

From velocity triangle

$$\sin \alpha_2 = \frac{C_{w2}}{C_2}$$

or

$$C_2 = \frac{C_{w2}}{\sin \alpha_2} = \frac{634.21}{\sin 68^\circ} = 684 \text{ m/s}$$

Axial velocity is given by

$$Ca_2 = 684 \cos 68^\circ = 256.23 \text{ m/s}$$

(3) Total-to-total efficiency,  $\eta_{tt}$ , is

$$\begin{aligned} \eta_{tt} &= \frac{T_{01} - T_{03}}{T_{01} - T'_{03}} \\ &= \frac{w_s}{T_{01} - \left(T_3 + \frac{C_3^2}{2C_{pg}}\right)} = \frac{w_s}{\frac{w_s}{\eta_{ts}} - \frac{C_3^2}{2C_{pg}}} \\ &= \frac{304.42}{\frac{304.42}{0.85} - \frac{(256.23)^2}{2 \times 1147}} = 92.4\% \end{aligned}$$

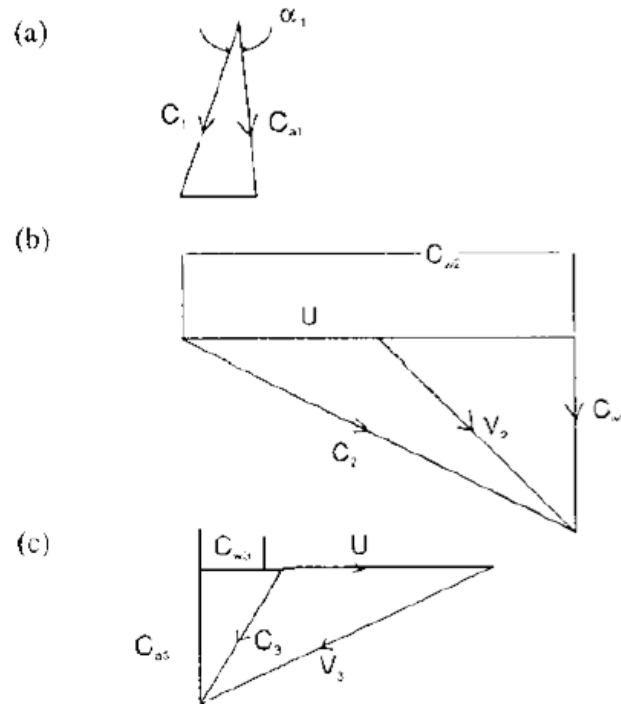
(4) The degree of reaction

$$\begin{aligned}\Lambda &= \frac{Ca}{2U} (\tan \beta_3 - \tan \beta_2) \\ &= \left( \frac{Ca}{2U} \times \frac{U}{Ca} \right) - \left( \frac{Ca}{2U} \tan \alpha_2 \right) + \left( \frac{U}{Ca} \times \frac{Ca}{2U} \right)\end{aligned}$$

(from velocity triangle)

$$\Lambda = 1 - \frac{Ca}{2U} \tan \alpha_2 = 1 - \frac{256.23}{(2)(480)} \tan 68^\circ = 33.94\%$$

**Design Example 1.3** In a single-stage axial flow gas turbine gas enters at stagnation temperature of 1100 K and stagnation pressure of 5 bar. Axial velocity is constant through the stage and equal to 250 m/s. Mean blade speed is 350 m/s. Mass flow rate of gas is 15 kg/s and assume equal inlet and outlet velocities. Nozzle efflux angle is  $63^\circ$ , stage exit swirl angle equal to  $9^\circ$ . Determine the rotor-blade gas angles, degree of reaction, and power output.



### Solution

$$Ca_1 = Ca_2 = Ca_3 = Ca = 250 \text{ m/s}$$

From velocity triangle (b)

$$C_2 = \frac{Ca_2}{\cos \alpha_2} = \frac{250}{\cos 63^\circ} = 550.67 \text{ m/s}$$

From figure (c)

$$C_3 = \frac{Ca_3}{\cos \alpha_3} = \frac{250}{\cos 9^\circ} = 253 \text{ m/s}$$

$$C_{w3} = Ca_3 \tan \alpha_3 = 250 \tan 9^\circ = 39.596 \text{ m/s}$$

$$\tan \beta_3 = \frac{U + C_{w3}}{Ca_3} = \frac{350 + 39.596}{250} = 1.5584$$

$$\text{i.e., } \beta_3 = 57.31^\circ$$

From figure (b)

$$C_{w2} = Ca_2 \tan \alpha_2 = 250 \tan 63^\circ = 490.65 \text{ m/s}$$

and

$$\tan \beta_2 = \frac{C_{w2} - U}{Ca_2} = \frac{490.65 - 350}{250} = 0.5626$$

$$\therefore \beta_2 = 29^\circ 21'$$

Power output

$$\begin{aligned} W &= mUCa(\tan \beta_2 + \tan \beta_3) \\ &= (15)(350)(250)(0.5626 + 1.5584)/1000 \\ &= 2784 \text{ kW} \end{aligned}$$

The degree of reaction is given by

$$\begin{aligned} \Lambda &= \frac{Ca}{2U} (\tan \beta_3 - \tan \beta_2) \\ &= \frac{250}{2 \times 350} (1.5584 - 0.5626) \\ &= 35.56\% \end{aligned}$$

**Design Example.1.4** Calculate the nozzle throat area for the same data as in the previous question, assuming nozzle loss coefficient,  $T_N = 0.05$ . Take  $\gamma = 1.333$ , and  $C_{pg} = 1.147 \text{ kJ/kgK}$ .

**Solution**

Nozzle throat area,  $A = m/\rho_2 Ca_2$

and  $\rho_2 = \frac{p_2}{RT_2}$

$$T_2 = T_{02} - \frac{C_2^2}{2C_p} = 1100 - \frac{(550.67)^2}{(2)(1.147)(1000)} \quad (T_{01} = T_{02})$$

i.e.,  $T_2 = 967.81 \text{ K}$

From nozzle loss coefficient

$$T_2' = T_2 - \lambda_N \frac{C_2^2}{2C_p} = 967.81 - \frac{0.05 \times (550.67)^2}{(2)(1.147)(1000)} = 961.2 \text{ K}$$

Using isentropic  $p$ - $T$  relation for nozzle expansion

$$p_2 = p_{01} / \left( T_{01} / T_2' \right)^{\gamma/(\gamma-1)} = 5 / (1100/961.2)^4 = 2.915 \text{ bar}$$

Critical pressure ratio

$$p_{01}/p_c = \left( \frac{\gamma+1}{2} \right)^{\gamma/(\gamma-1)} = \left( \frac{2.333}{2} \right)^4 = 1.852$$

or  $p_{01}/p_2 = 5/2.915 = 1.715$

Since  $\frac{p_{01}}{p_2} < \frac{p_{01}}{p_c}$ , and therefore nozzle is unchoked.

Hence nozzle gas velocity at nozzle exit

$$\begin{aligned} C_2 &= \sqrt{[2C_{pg}(T_{01} - T_2)]} \\ &= \sqrt{[(2)(1.147)(1000)(1100 - 967.81)]} = 550.68 \text{ m/s} \end{aligned}$$

Therefore, nozzle throat area

$$A = \frac{m}{\rho_2 C_2}, \text{ and } \rho_2 = \frac{p_2}{RT_2} = \frac{(2.915)(10^2)}{(0.287)(967.81)} = 1.05 \text{ kg/m}^3$$

Thus

$$A = \frac{15}{(1.05)(550.68)} = 0.026 \text{ m}^2$$

**Design Example.1.5** In a single-stage turbine, gas enters and leaves the turbine axially. Inlet stagnation temperature is 1000 K, and pressure ratio is 1.8 bar. Gas leaving the stage with velocity 270 m/s and blade speed at root is 290 m/s. Stage isentropic efficiency is 0.85 and degree of reaction is zero. Find the nozzle efflux angle and blade inlet angle at the root radius.

**Solution**

Since  $\Lambda = 0$ , therefore

$$\Lambda = \frac{T_2 - T_3}{T_1 - T_3},$$

hence

$$T_2 = T_3$$

From isentropic  $p$ - $T$  relation for expansion

$$T'_{03} = \frac{T_{01}}{(p_{01}/p_{03})^{(\gamma-1)/\gamma}} = \frac{1000}{(1.8)^{0.249}} = 863.558 \text{ K}$$

Using turbine efficiency

$$\begin{aligned} T_{03} &= T_{01} - \eta_t(T_{01} - T'_{03}) \\ &= 1000 - 0.85(1000 - 863.558) = 884 \text{ K} \end{aligned}$$

In order to find static temperature at turbine outlet, using static and stagnation temperature relation

$$T_3 = T_{03} - \frac{C_3^2}{2C_{pg}} = 884 - \frac{270^2}{(2)(1.147)(1000)} = 852 \text{ K} = T_2$$

Dynamic temperature

$$\frac{C_2^2}{2C_{pg}} = 1000 - T_2 = 1000 - 852 = 148 \text{ K}$$

$$C_2 = \sqrt{[(2)(1.147)(148)(1000)]} = 582.677 \text{ m/s}$$

Since,  $C_{pg}\Delta T_{os} = U(C_{w3} + C_{w2}) = UC_{w2}$  ( $C_{w3} = 0$ )

Therefore,  $C_{w2} = \frac{(1.147)(1000)(1000 - 884)}{290} = 458.8 \text{ m/s}$

From velocity triangle

$$\sin \alpha_2 = \frac{C_{w2}}{C_2} = \frac{458.8}{582.677} = 0.787$$



That is,  $\alpha_2 = 51^\circ 54'$

$$\begin{aligned}\tan \beta_2 &= \frac{C_{w2} - U}{C_{a2}} = \frac{458.8 - 290}{C_2 \cos \alpha_2} \\ &= \frac{458.8 - 290}{582.677 \cos 51.90^\circ} = 0.47\end{aligned}$$

i.e.,  $\beta_2 = 25^\circ 9'$

**Design Example 1.6** In a single-stage axial flow gas turbine, gas enters the turbine at a stagnation temperature and pressure of 1150 K and 8 bar, respectively. Isentropic efficiency of stage is equal to 0.88, mean blade speed is 300 m/s, and rotational speed is 240 rps. The gas leaves the stage with velocity 390 m/s. Assuming inlet and outlet velocities are same and axial, find the blade height at the outlet conditions when the mass flow of gas is 34 kg/s, and temperature drop in the stage is 145 K.

**Solution**

Annulus area  $A$  is given by

$$A = 2 \pi r_m h$$

where  $h$  = blade height

$r_m$  = mean radius

As we have to find the blade height from the outlet conditions, in this case annulus area is  $A_3$ .

$$\begin{aligned}\therefore h &= \frac{A_3}{2 \pi r_m} \\ U_m &= \pi D_m N\end{aligned}$$

$$\text{or } D_m = \frac{(U_m)}{\pi N} = \frac{300}{(\pi)(240)} = 0.398$$

$$\text{i.e., } r_m = 0.199 \text{ m}$$

Temperature drop in the stage is given by

$$T_{01} - T_{03} = 145 \text{ K}$$

$$\text{Hence } T_{03} = 1150 - 145 = 1005 \text{ K}$$

$$T_3 = T_{03} - \frac{C_3^2}{2C_{pg}} = 1005 - \frac{390^2}{(2)(1.147)(1000)} = 938.697 \text{ K}$$

Using turbine efficiency to find isentropic temperature drop

$$T'_{03} = 1150 - \frac{145}{0.88} = 985.23 \text{ K}$$

Using isentropic  $p$ - $T$  relation for expansion process

$$p_{03} = \frac{p_{01}}{(T_{01}/T'_{03})^{\gamma/(\gamma-1)}} = \frac{8}{(1150/985.23)^4} = \frac{8}{1.856}$$

i.e.,  $p_{03} = 4.31 \text{ bar}$

Also from isentropic relation

$$p_3 = \frac{p_{03}}{(T'_{03}/T_3)^{\gamma/(\gamma-1)}} = \frac{4.31}{(985.23/938.697)^4} = \frac{4.31}{1.214} = 3.55 \text{ bar}$$

$$\rho_3 = \frac{p_3}{RT_3} = \frac{(3.55)(100)}{(0.287)(938.697)} = 1.32 \text{ kg/m}^3$$

$$A_3 = \frac{m}{\rho_3 C a_3} = \frac{34}{(1.32)(390)} = 0.066 \text{ m}^2$$

Finally,

$$h = \frac{A_3}{2 \pi r_m} = \frac{0.066}{(2 \pi)(0.199)} = 0.053 \text{ m}$$

**Design Example 1.7** The following data refer to a single-stage axial flow gas turbine with convergent nozzle:

Inlet stagnation temperature, $T_{01}$	1100 K
Inlet stagnation pressure, $p_{01}$	4 bar
Pressure ratio, $p_{01}/p_{03}$	1.9
Stagnation temperature drop	145 K
Mean blade speed	345 m/s
Mass flow, $m$	24 kg/s
Rotational speed	14,500 rpm
Flow coefficient, $\Phi$	0.75
Angle of gas leaving the stage	$12^\circ$
$C_{pg} = 1147 \text{ J/kg K}$ , $\gamma = 1.333$ , $\lambda_N = 0.05$	

Assuming the axial velocity remains constant and the gas velocity at inlet and outlet are the same, determine the following quantities at the mean radius:

- (1) The blade loading coefficient and degree of reaction
- (2) The gas angles
- (3) The nozzle throat area



**Solution**

$$(1) \quad \Psi = \frac{C_{pg}(T_{01} - T_{03})}{U^2} = \frac{(1147)(145)}{345^2} = 1.4$$

Using velocity diagram

$$U/Ca = \tan \beta_3 - \tan \alpha_3$$

$$\begin{aligned} \text{or} \quad \tan \beta_3 &= \frac{1}{\Phi} + \tan \alpha_3 \\ &= \frac{1}{0.75} + \tan 12^\circ \\ \beta_3 &= 57.1^\circ \end{aligned}$$

From Equations (7.14) and (7.15), we have

$$\Psi = \Phi(\tan \beta_2 + \tan \beta_3)$$

and

$$\Lambda = \frac{\Phi}{2}(\tan \beta_3 - \tan \beta_2)$$

From which

$$\tan \beta_3 = \frac{1}{2\Phi}(\Psi + 2\Lambda)$$

Therefore

$$\tan 57.1^\circ = \frac{1}{2 \times 0.75}(1.4 + 2\Lambda)$$

Hence

$$\Lambda = 0.4595$$

$$\begin{aligned} (2) \quad \tan \beta_2 &= \frac{1}{2\Phi}(\Psi - 2\Lambda) \\ &= \frac{1}{2 \times 0.75}(1.4 - [2][0.459]) \\ \beta_2 &= 17.8^\circ \end{aligned}$$

$$\begin{aligned} \tan \alpha_2 &= \tan \beta_2 + \frac{1}{\Phi} \\ &= \tan 17.8^\circ + \frac{1}{0.75} = 0.321 + 1.33 = 1.654 \\ \alpha_2 &= 58.8^\circ \end{aligned}$$

$$(3) \quad Ca_1 = U\Phi$$

$$= (345)(0.75) = 258.75 \text{ m/s}$$

$$C_2 = \frac{Ca_1}{\cos \alpha_2} = \frac{258.75}{\cos 58.8^\circ} = 499.49 \text{ m/s}$$

$$T_{02} - T_2 = \frac{C_2^2}{2C_p} = \frac{499.49^2}{(2)(1147)} = 108.76 \text{ K}$$

$$T_2 - T_{2s} = \frac{(T_N)(499.49^2)}{(2)(1147)} = \frac{(0.05)(499.49^2)}{(2)(1147)} = 5.438 \text{ K}$$

$$T_{2s} = T_2 - 5.438$$

$$T_2 = 1100 - 108.76 = 991.24 \text{ K}$$

$$T_{2s} = 991.24 - 5.438 = 985.8 \text{ K}$$

$$\frac{p_{01}}{p_2} = \left( \frac{T_{01}}{T_{2s}} \right)^{\gamma/(\gamma-1)}$$

$$p_2 = 4 \times \left( \frac{985.8}{1100} \right)^4 = 2.58$$

$$\rho_2 = \frac{p_2}{RT_2} = \frac{(2.58)(100)}{(0.287)(991.24)} = 0.911 \text{ kg/m}^3$$

$$(4) \quad \text{Nozzle throat area} = \frac{m}{\rho_1 C_1} = \frac{24}{(0.907)(499.49)} = 0.053 \text{ m}^2$$

$$A_1 = \frac{m}{\rho_1 Ca_1} = \frac{24}{(0.907)(258.75)} = 0.102 \text{ m}^2$$

**Design Example 1.8** A single-stage axial flow gas turbine with equal stage inlet and outlet velocities has the following design data based on the mean diameter:

Mass flow	20 kg/s
Inlet temperature, $T_{01}$	1150K
Inlet pressure	4 bar
Axial flow velocity constant through the stage	255 m/s
Blade speed, $U$	345 m/s
Nozzle efflux angle, $\alpha_2$	60°
Gas-stage exit angle	12°

Calculate (1) the rotor-blade gas angles, (2) the degree of reaction, blade-loading coefficient, and power output and (3) the total nozzle throat area if the throat is situated at the nozzle outlet and the nozzle loss coefficient is 0.05.

**Solution**

(1) From the velocity triangles

$$C_{w2} = Ca \tan \alpha_2$$

$$= 255 \tan 60^\circ = 441.67 \text{ m/s}$$

$$C_{w3} = Ca \tan \alpha_3 = 255 \tan 12^\circ = 55.2 \text{ m/s}$$

$$V_{w2} = C_{w2} - U = 441.67 - 345 = 96.67 \text{ m/s}$$

$$\beta_2 = \tan^{-1} \frac{V_{w2}}{Ca} = \tan^{-1} \frac{96.67}{255} = 20.8^\circ$$

Also  $V_{w3} = C_{w3} + U = 345 + 55.2 = 400.2 \text{ m/s}$

$$\therefore \beta_3 = \tan^{-1} \frac{V_{w3}}{Ca} = \tan^{-1} \frac{400.2}{255} = 57.5^\circ$$

$$(2) \quad \Lambda = \frac{\Phi}{2} (\tan \beta_3 - \tan \beta_2)$$

$$= \frac{255}{2 \times 345} (\tan 57.5^\circ - \tan 20.8^\circ) = 0.44$$

$$\Psi = \frac{Ca}{U} (\tan \beta_2 + \tan \beta_3)$$

$$= \frac{255}{345} (\tan 20.8^\circ + \tan 57.5^\circ) = 1.44$$

Power  $W = mU(C_{w2} + C_{w3})$

$$= (20)(345)(441.67 + 54.2) = 3421.5 \text{ kW}$$

$$(3) \quad \lambda_N = \frac{C_p(T_2 - T_2')}{\frac{1}{2}C_2^2}, C_2 = Ca \sec \alpha_2 = 255 \sec 60^\circ = 510 \text{ m/s}$$

$$\text{or } T_2 - T_2' = \frac{(0.05)(0.5)(510^2)}{1147} = 5.67$$

$$T_2 = T_{02} - \frac{C_2^2}{2C_p} = 1150 - \frac{510^2}{(2)(1147)} = 1036.6 \text{ K}$$

$$T_2' = 1036.6 - 5.67 = 1030.93 \text{ K}$$

$$\frac{p_{01}}{p_2} = \left( \frac{T_{01}}{T_2} \right)^{\gamma/(\gamma-1)} = \left( \frac{1150}{1030.93} \right)^4 = 1.548$$

$$p_2 = \frac{4}{1.548} = 2.584 \text{ bar}$$

$$\rho_2 = \frac{p_2}{RT_2} = \frac{2.584 \times 100}{0.287 \times 1036.6} = 0.869 \text{ kg/m}^3$$

$$m = \rho_2 A_2 C_2$$

$$A_2 = \frac{20}{0.869 \times 510} = 0.045 \text{ m}^2$$