

# Optimal control algorithm of fertigation system in greenhouse based on EC model

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**Abstract:** Two new control algorithms based on MSP430 microcontroller unit (MCU) were developed to improve the performance of a fertigation system controlled by the electrical conductivity (EC) value of an irrigation nutrient solution in a greenhouse. The first algorithm is incremental proportional–integral–derivative (PID), and the second one is a two-stage combination algorithm (PID + fuzzy). With an improved multi-line mixing Venturi tube, several sets of experiments were conducted for a fertilizer absorption test under two conditions, namely, various suction lines and different EC target values settings. Under the first condition, with an EC target value of 2.0 mS/cm and opening of various suction pipes, the steady-state times are 186 s, 172 s, 134 s, and 122 s corresponding to the opening of one to four suction pipes, respectively, for PID + fuzzy control. The corresponding values are 220 s, 196 s, 158 s, and 148 s for incremental PID control. Under the second condition, four suction pipes are opened with different target EC values of 1.5 mS/cm, 2.0 mS/cm, and 2.5 mS/cm, and the shortest response time and the minimum overshoot were obtained for PID + fuzzy control when the target EC value is 1.5 mS/cm, which are 96 s and 0.18 mS/cm, respectively. While the corresponding values are 112 s and 0.4 mS/cm, respectively for incremental PID control. The two control strategies can adjust the EC value to the target value for real-time control, but the combination control algorithm can be implemented more rapidly, accurately, and steadily with a small overshoot compared with incremental PID control. The combination algorithm (PID + fuzzy) control strategy also possesses better properties for automatic fertigation control in greenhouses than the incremental PID control strategy, the combination algorithm provides an optimal way of water and fertilizer management for crops in greenhouses which will contribute to water and fertilizer saving.

**Keywords:** fertigation, control algorithm, incremental PID, fuzzy control, irrigation control, greenhouse

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## 1 Introduction

Excessive irrigation and fertilization applied in the conventional soil cultivation will cause wasting of water and nutrient accumulation in the soil of the crops root zone and finally lead to the groundwater pollution<sup>[1-3]</sup>. The establishment of greenhouses (or facility agriculture) is an important direction of modern agriculture in the Internet of Things (IoT) era. And the closed cultivation system of greenhouses as an advanced technology in facility agriculture can save approximately 17.2% of

water and fertilizer compared with traditional cultivation methods and contributes to the promotion of industrial restructuring and facility agriculture development<sup>[4]</sup>. The closed cultivation system uses substrates or nutrient solutions as cultivation bases instead of soil and substitutes several single-element fertilizers for complex ones with real-time proportioning to supply nutrients together with the irrigation water to crops precisely<sup>[5]</sup>, and it usually combines with drip irrigation which can increase water use efficiency and crop yield<sup>[6]</sup>. Fertigation technology is believed to be suitable for the closed cultivation system of greenhouses because this technology provides an optimal combination of water and fertilizer for the nutrient uptake of crops and plays an important role in the efficient using of water and fertilizers for environmental sustainability<sup>[7-9]</sup>. The electrical conductivity (EC) value of the nutrient solution is often used as a key indicator in determining if nutrition regulation reaches the component standard<sup>[10,11]</sup>. Cliff et al.<sup>[12]</sup> reported that greenhouse tomatoes irrigated with a high-EC nutrient solution produce soft, red, and small fruits. Salih et al.<sup>[13]</sup> developed an automatic fertigation control system for rock melon in a greenhouse on the basis of the EC value. The system was fully operated with solar energy and could reduce costs and produce improved yield. However, establishing a precise irrigation nutrition regulation model is difficult due to the time lag and nonlinearity in the process of irrigation nutrient solution proportioning<sup>[14]</sup>.

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Numerous researchers have studied the nutrition regulation model. Samsuri et al.<sup>[15]</sup> studied a control strategy for a drip nutrient solution on the basis of injection time by establishing the relationship between the desired EC value of the nutrient solution and the desired time of fertilizer injection. The measured EC value was close to the desired EC value. Liang et al.<sup>[16]</sup> designed a fuzzy proportional–integral–derivative (PID) control algorithm for a fertigation system and established a mathematical model of a variable-rate fertilization control system according to mechanical dynamics and electrical principles. They also obtained the simulation curve of system performance by tuning the PID parameters and discovered that the system based on fuzzy PID possessed high steady-state precision, fast dynamic response, small overshoot, and strong anti-interface capability. Steidle Neto et al.<sup>[9]</sup> developed an automatic control system based on the Penman–Monteith model and leachate concentration. The developed system was efficient in controlling the prepared nutrient solution concentration, and only 44.42 L of the nutrient solution was necessary to produce 1 kg of tomato fruits. Niu and Zhang<sup>[17]</sup> designed a self-adaptive fertigation control strategy based on artificial neural network–PID, with which the EC value could achieve steady state at the expected value. Yuan<sup>[4]</sup> designed an incremental PID fertigation control algorithm with the improved Smith predictor, but the algorithm was still in the simulation stage.

All of these studies have shown that although many fertigation methods for supplying crops with nutrient solutions have been investigated, the accuracy, time delay, and stability of the fertigation control system still require further research. This study aims to achieve the desired EC value of a nutrient solution accurately, rapidly and steadily. An automatic fertigation control system will be developed, and an EC sensor will be designed. Two control algorithms, namely, incremental PID algorithm and combination algorithm (PID + fuzzy), based on MSP430G2553 microcontroller unit (MCU) will be used in this study. And then the performance of the two algorithms in the fertigation system will be evaluated to determine the ideal control strategy. Several sets of Greenhouse experiments will be also conducted under two conditions to validate the performance of the control strategies.

## 2 Materials and methods

Unlike previous studies that used traditional Venturi tubes with

only one suction channel, this study utilized a redesigned Venturi tube for the fertigation system. The redesigned Venturi tube has multiple suction channels, can suck large amounts of fertilizers at once, saves space, and can be easily controlled<sup>[18]</sup>. An EC sensor based on frequency measurement was also designed to measure the EC value of the nutrient solution, and then a fertigation control system was built for nutrient solution regulation.

### 2.1 Control strategy

Previous studies have revealed that PID controllers have been widely used for automatic control due to their effective mathematical modelling for systems. PID controllers can improve transient and steady-state responses, but most of them still exhibit overshoot and time delay. The incremental PID controller is an improved version and effective for initialization<sup>[19,20]</sup>. Since the proposal of fuzzy inference techniques by Mamdani and Assilian<sup>[21]</sup> and Sugeno<sup>[22]</sup>, fuzzy controllers that reflect the experience of human experts have also been widely studied for the water and fertilizer management<sup>[23-25]</sup>. These controllers can be applied to the systems that are difficult to model by mathematical equations<sup>[26,27]</sup>. On the other hand, a combination control algorithm, which applies PID logic when the error ( $e$ ) value between the measured and target EC values is large and then applies fuzzy logic when  $e$  is small, has rarely been reported, especially for the fertigation nutrient solution regulation. Therefore, we proposed a combination algorithm (PID + fuzzy), based on MSP430G2553 MCU in this study for the fertigation control system, and have it compared to the incremental PID algorithm. Both algorithms were implemented via an analysis of the EC value during the mixing process to determine which of the two was better in controlling the fertigation system.

### 2.2 EC sensor

The EC value of the nutrient solution, similar to that of any conductive medium, has a significant positive correlation with nutrient concentration<sup>[28,29]</sup>. The nutrient solution can serve as an equivalent resistance when current passes through it. The principle of EC measurement is shown in Figure 1. The equivalent resistances measured by the EC sensor changed with the EC value of the nutrient solution, leading to various square-wave output frequencies of the circuit. The EC value of the nutrient solution was determined by measuring the square-wave output frequencies of the circuit.

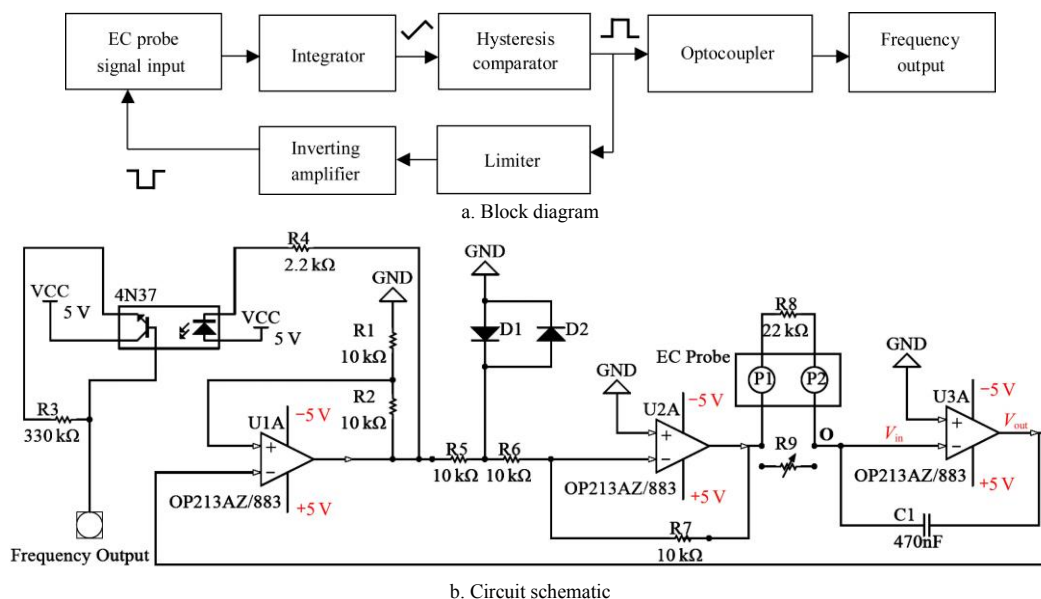


Figure 1 Schematic of EC measurement

In Figure 1b, the three operational amplifiers from left to right are hysteresis comparator U1A, inverting amplifier U2A, and integrating circuit U3A. Two probes of the EC sensor, namely, P1 and P2, were two carbon electrodes made from Shanghai Moyang Electric Carbon Corporation Limited. When the probes are plugged into the irrigation nutrient solutions, there will be an equivalent resistance ( $R$ ) between P1 and P2. And R9 is the equivalent resistance of two parallel resistors, namely R8 and R. The relationship between upper threshold voltage  $U_H$  and lower threshold voltage  $U_L$  of U1A and that between output voltage  $V_{out}$  and input voltage  $V_{in}$  of U3A are as follows:

$$U_H = \frac{R_1}{R_1 + R_2} U_{OM} = -U_L \quad (1)$$

$$V_{out} = -\frac{R_1}{R_3 C_1} \int V_{in} dt \quad (2)$$

where,  $R_3 C_1$  is the time constant, and only two output values of U1A, namely,  $+U_{OM}$  and  $-U_{OM}$ , are available. If  $R_0$  is the equivalent resistance when the EC sensor is placed inside the irrigation nutrient solution, then the output waveform of U3A will be a triangular wave. The slope will be negative if the O point reaches a high level, which would be the input wave of U1A and marked as  $U_{il}$ . When  $U_{il}$  decreased to  $U_L$ , the output voltage of U1A changed from  $-U_{OM}$  to  $+U_{OM}$ . After the level went through U2A, the level of the O point changed from high to low. The situation was exactly the opposite when the O point decreased to a low level. Thus, a square wave was generated, which indicated that P1 and P2 had an AC power supply. The polarization of the two carbon electrodes could then be avoided. The square-wave output frequency of U1A was measured via the digital input of the MCU after isolation by a 4N37 optocoupler.

### 2.3 EC modeling

On the basis of the studies of Yuan et al.<sup>[4]</sup> and Niu et al.<sup>[17]</sup>, the nutrient solution mixing model was regarded as a first-order lag model to simplify the system model according to real fertilizer mixing conditions. The EC model of the nutrient solution regulation was obtained based on the fertigation system developed in this study (Figure 4). If the nutrient solution volume ( $V_T$ ) inside the mixing tank remained steady when the fertigation equipment was in a working state, then the EC value of the nutrient solution inside the mixing tank would be similar to the EC value of the outlet irrigation nutrient solution. According to the principle of mass conservation, the following equation can be used to show the relationship between the outlet nutrient solution and the inlet water and fertilizers.

$$d(V_T C_{out}(t)) = [\sum_{i=1}^5 C_i Q_{W_i} m_i(t) + Q_I C_0 - Q_O C_{out}(t)] dt \quad (3)$$

where,  $C_{out}(t)$  is the concentration of the nutrient solution inside the mixing tank and outlet pipe,  $C_0$  is the concentration of the nutrient solution inside the inlet fresh water, and  $C_i$  ( $i = 1, 2, 3, 4, 5$ ) is the concentration of the stock solution inside dosage tank  $i$ .  $Q_I$  and  $Q_O$  are the inlet water flow and outlet nutrient solution flow, respectively, which are constant due to the constant power pump.  $m_i(t) Q_{W_i}$  ( $i = 1, 2, 3, 4, 5$ ) is the suction flow of the five input lines from the five dosage tanks connected to the Venturi tube. This flow is implemented by controlling the duty cycle of the solenoid valve control cycle. Therefore, it is a function of the duty cycle.  $Q_W$  is a constant and the suction flow of the Venturi tube when the duty cycle is 100%, which means the solenoid valve is always open. Equation (3) was transformed to the following equation because the concentration of the nutrient solution was proportional to the EC

value of the nutrient solution.

$$d(V_T E_{out}(t)) = [\sum_{i=1}^5 E_i Q_{W_i} m_i(t) + Q_I E_0 - Q_O E_{out}(t)] dt \quad (4)$$

where,  $E_{out}(t)$  is the EC value of the nutrient solution inside the mixing tank and outlet pipe,  $E_0$  is the EC value of the inlet fresh water, and  $E_i$  ( $i = 1, 2, 3, 4, 5$ ) is the EC value of the five types of nutrient solution from the dosage tank.

During the mixing process,  $V_T = 100$  L,  $E_0 = 0$ . If the five EC values and five duty cycles of the five suction lines are the same, then Equation (4) can be transformed to

$$\frac{d(V_T E_{out}(t))}{dt} = 5 E_i Q_{W_i} m(t) - Q_O E_{out}(t) \quad (5)$$

Through Laplace transform, Equation (5) can be rewritten as

$$E_{out}(s) = \frac{5 E_i Q_{W_i}}{V_T s + Q_O} m(s) \quad (6)$$

The response characteristics showed that the fertigation system was a first-order linear system. In an actual experiment, according to the measured data ( $E_i = 20$  mS/cm,  $Q_W = 0.02$  L/s, output pressure = 0.15 MPa, and  $Q_O = 7.47$  L/s), the EC transfer function can be written as

$$H(s) = \frac{2}{100s + 7.47} e^{-10s} = \frac{0.27}{13.39s + 1} e^{-10s} \quad (7)$$

### 2.4 Incremental PID algorithm

The PID control strategy is widely used in the field of control due to its numerous advantages, such as fast response, stable regulation, and easy implementation. As D part of PID control is very sensitive to noise and a very short sampling time, resulting in a severe fluctuation which may cause the overshooting, PID control was cut in this study to PI control to reduce EC overshooting, which might be harmful to crops, due to the lag time of the control system and the crop sensitiveness to the EC value of the irrigation nutrient solution.

An incremental PID algorithm was used, and the output of the PID system was the difference between the former and latter outputs of the positional PID. Unlike positional PID that requires calculation of all errors from the beginning to the present, incremental PID<sup>[30]</sup> only requires calculation of the current and two previous errors, and the output can be written as

$$\Delta u_k = u_k - u_{k-1} = K_p \left[ e_k - e_{k-1} + \frac{T}{T_i} e_k \right] = K_p \left( 1 + \frac{T}{T_i} \right) e_k - K_p e_{k-1} \quad (8)$$

where,  $K_p$  is the proportional gain;  $T$  is the sampling time;  $T_i$  is the integration time;  $e_k$  is the current error ( $e$ ) value between the measured and target EC values, and  $e_{k-1}$  is the previous  $e$ .

MSP430G2553 MCU was used as the core controller of the PID algorithm, with which the suction flows were controlled by controlling the on-off state of the solenoid valves of each suction line to regulate the EC value of the irrigation nutrient solution. The system control flowchart is shown in Figure 2.

The actuator needed to run at full speed after the output value exceeded the predetermined threshold value to take full advantage of the value of the PID controller. The output value of the PI controller was also limited and transformed to the duty cycle of the solenoid valve control period to control the on-off time ratio of the solenoid valve. The control period was 2 s, and the EC value of the irrigation nutrient solution inside the mixing tank was measured every 1 second, then an average value of two EC measurements was used every control period to calculate the error ( $e$ ) value. According to simulation with MATLAB software (MATLAB

R2017, The MathWorks, Nattick, MA, USA), the proportional and integral coefficients were set to  $K_p = 20$  and  $T_i = 2$ , respectively.

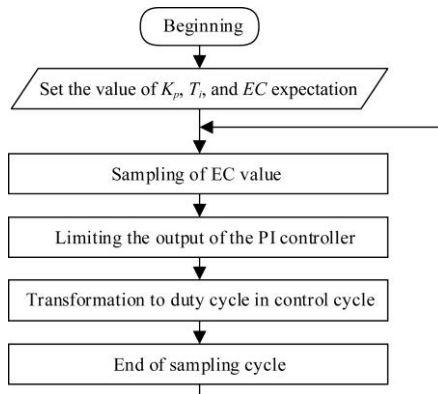


Figure 2 Flowchart of the incremental PID control system

## 2.5 Two-stage combination algorithm

A two-stage control strategy was developed. In the first stage, the PI controller was initialized when the error ( $e$ ) between the measured EC and target EC values was large, which can rapidly control the duty cycle. In the second stage, the fuzzy controller was initialized when  $e$  became smaller than the threshold value  $e_M$  ( $\pm 0.2$  mS/cm) to avoid overshooting and rapidly adjust the EC value to the target value. In this study, the threshold value was set to 0.2 mS/cm for the first time based on our experience in other studies.

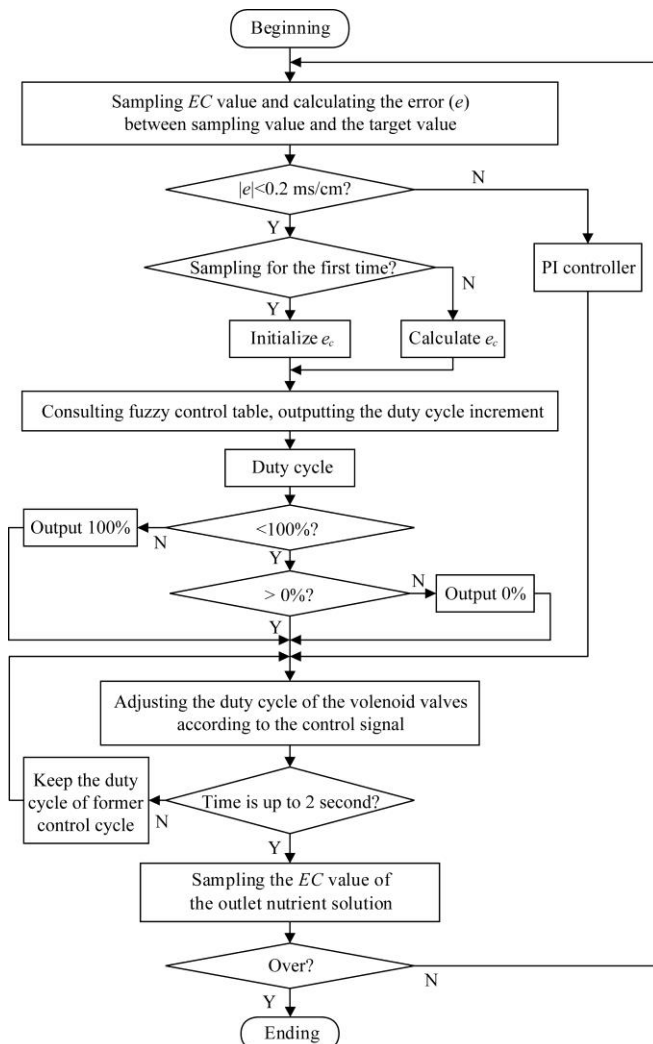


Figure 3 Flowchart of the two-stage combination algorithm control system

For fuzzy stage control, when  $e$  was sufficiently small to meet the condition of ( $|e| < e_M$ ), the PWM driving circuit was connected to the fuzzy controller with inputs of error ( $e$ ) and error rate ( $e_c$ ) and output of solenoid valve duty cycle ( $u$ ). According to actual conditions and simulation with MATLAB software, the range of  $e$  was set from  $-0.2$  mS/cm to  $+0.2$  mS/cm, and its fuzzy language variable was  $E$ , the domain of which was quantified as  $\{-8, -6, -4, -2, 0, 2, 4, 6, 8\}$ . Its fuzzy set was  $\{NBS, NB, NM, NS, Z, PS, PM, PB, PBS\}$ , and its scaling factor was 40. The range of  $e_c$  was set from  $-0.3$  to  $+0.3$ , its fuzzy language variable was  $E_c$ , its domain was quantified as  $\{-6, -4, -2, 0, 2, 4, 6\}$ , its fuzzy set was  $\{NB, NM, NS, Z, PS, PM, PB\}$ , and its scaling factor was 20. The range of output  $u$  was  $[-0.15, +0.15]$ . Its fuzzy language variable was  $U$ , its domain was quantified as  $\{-0.15, -0.125, -0.1, -0.075, -0.05, -0.025, 0, 0.025, 0.05, 0.075, 0.1, 0.125, 0.15\}$ , and its fuzzy set was  $\{N6, N5, N4, N3, N2, N1, Z, P1, P2, P3, P4, P5, P6\}$ . In this stage, the range of the solenoid valve duty cycle could be controlled to  $[-15\%, +15\%]$  relative to the value to the former duty cycle. For example, if input  $E$  was 8 and input  $E_c$  was 6, which means that the error and the error rate were the largest, then output  $U$  would be  $-0.15$ , which means that the fertilizer suction amount would be reduced to 15% of the former suction amount, thereby reducing the latter inputs  $E$  and  $EC$  as much as possible.

The fertigation control flowchart is shown in Figure 3. The initial value of  $E_c$  was set to 6, and the control period time was set to 2 seconds. For appropriate control, if the duty cycle was less than 0, then the duty cycle was 0; if the duty cycle was more than 100%, then it was 100%. Based on expert theory and practical experience, a fuzzy control rule table was designed by using the fuzzy reasoning method, as shown in Table 1. A total of 63 rules were derived. The membership functions of inputs and outputs were triangular, and the centroid method was used for defuzzification.

Table 1 Rule table of fuzzy control

EC Rate of error change	E Difference between measured and target values								
	NBS	NB	NM	NS	Z	PS	PM	PB	PBS
NB	P6	P6	P5	P4	P3	P2	P1	Z	Z
NM	P6	P4	P3	P2	P1	P1	Z	Z	Z
NS	P4	P3	P2	P1	P1	Z	Z	N1	N1
Z	P3	P2	P1	P1	Z	Z	N1	N2	N2
PS	P2	P1	P1	Z	Z	N1	N1	N2	N3
PM	P1	Z	Z	Z	N1	N2	N2	N4	N6
PB	Z	Z	N1	N1	N2	N4	N5	N6	N6

## 2.6 Experimental design

The experiment was conducted with a fertigation control system that used the two algorithms. The pipe diameters of the inlet and outlet were 50 mm. The outlet water pressure was 0.15 MPa, and the measured flow was 7.47 L/s. The solution level with a volume of 100 L inside the mixing tank was maintained stable by controlling the inlet and outlet flows, and the EC of the inlet fresh water was 0.7 mS/cm. A potassium nitrate solution with 20 mS/cm of EC value was used as the stock solution and stored in the four dosage tanks (A, B, C, and D). Two EC sensors were utilized to measure the EC values of the mixing irrigation solution, and the average value was adopted as the input value for the controller. The four dosage tanks were connected to the redesigned mixing Venturi tube by using four suction pipes

controlled by solenoid valves, the four dosage tanks are put together in a platform with the same height, and all the pipes between the dosage tanks and the venturi have a same length, so that we can guarantee a same injection rates for all suction pipes, and the suction flow of each pipe was 3.5 L/min.

The EC values were collected by the IO interface of MSP430G2553 MCU and recorded by a computer connected to the MCU by RS-485. The sampling period was 2 s, and the measured time was 350 s. The results were obtained by opening one, two, three, and four suction pipes, respectively, using the two control algorithms. The target EC values of the four pipes were 1.5 mS/cm, 2.0 mS/cm, and 2.5 mS/cm.

### 3 Results and discussion

An automatic fertigation system was developed, incremental PID control algorithm was applied firstly as an example of traditional PID algorithms, then a new combined algorithm was proposed based on the analysis of the EC value of the irrigation nutrient solution during the mixing process. Experiments were then conducted under two different conditions to compare the performance of the two control strategies.

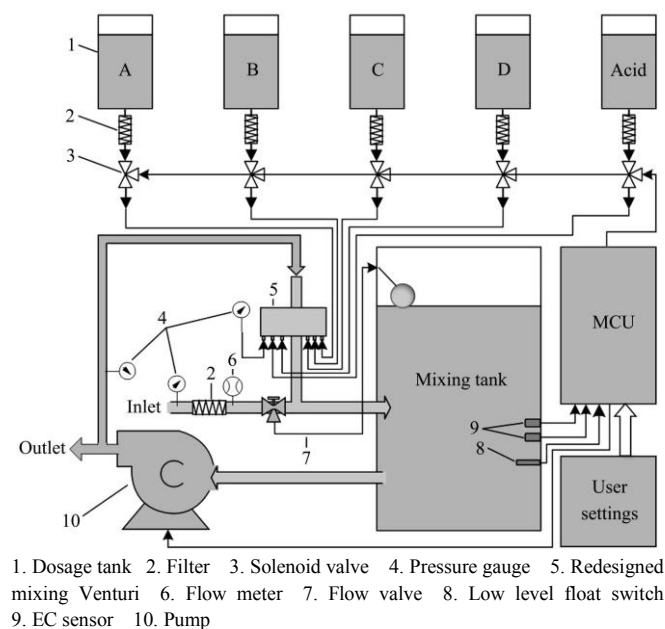


Figure 4 Structure of the automatic fertigation control system



Figure 5 The developed automatic fertigation system

#### 3.1 Automatic fertigation control system

The developed fertigation control system is shown in Figure 4 and Figure 5. The system comprises a mixing tank, several dosage tanks, a Venturi tube, a fertigation pump, and several

solenoid valves, electronic circuits, and sensors (including EC and pH sensors). The mixing tank, with a capacity of approximately 130 L, was used to store the nutrient solution intended for fertigation. Four 500 L dosage tanks were utilized to store the stock solutions (A, B, C, and D), and a 500 L dosage tank was used to store the acid for pH adjustment of the nutrient solution.

In consideration of crop variety, growth stage, and greenhouse environmental factors, the fertigation control system dynamically adjusted the EC value to the expected value in real time according to the data measured by the EC sensors.

A pump with a head of 32 m, speed of 2,900 r/min, flow rate of 25 m<sup>3</sup>/h, and power of 4 kW was connected to the mixing tank to pump the irrigation nutrient solution. The irrigation nutrient solution outputted by the pump flowed through two paths, one was for crop fertigation, and the other was through the mixing Venturi for generating negative pressure to suck fertilizers from the dosage tanks and transport these to the mixing tank, then the fertilizer solution goes directly to the inlet water before going to the mixing tank, which will help for the mixing process. The suction lines were controlled by using solenoid valves with a rated voltage of 24 V DC, power of 4 W, frequency of 1/2 Hz, and orifice of 3 mm. Considering the volume of the mixing tank is relatively not big, and the pump we used is close to mixing tank, it will pump water with pressure which can help to mix the fertilizers with water, no stirring equipment for mixing process is need in our mixing tank for current system.

High-level control of the irrigation nutrient solution inside the mixing tank was performed with a float valve connected to a contact sensor to avoid solution overflow during automatic preparation. Low-level control of the irrigation nutrient solution inside the mixing tank was accomplished with a low-level float switch connected to the electronic circuit of MCU to prevent the solution level from decreasing to below the pipe that was connected to the pump.

#### 3.2 Software simulation and experimental verification for EC sensor

The EC sensor was designed (Figure 6) and by using the Parametric Sweep function of OrCAD Capture and PSpice software<sup>[31]</sup>, the relationship between the output voltage ( $V(out)$ ) of the EC sensor and the equivalent resistor of the irrigation nutrient solution ( $R$ ), as mentioned in section 2.2 and Figure 1, was simulated. Here,  $V(out)$  was the voltage of which the output frequency was measured. The simulation time was set to 200 ms. The result showed that the output frequency changed with  $R$  (Figure 7), which meant that the output frequency of the EC sensor changed when the EC value of the irrigation nutrient solution did.

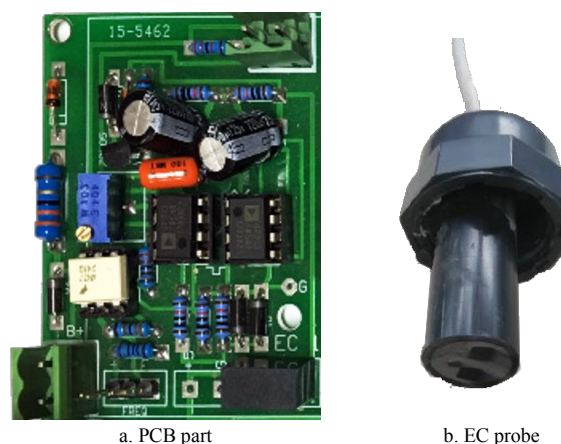


Figure 6 EC sensor



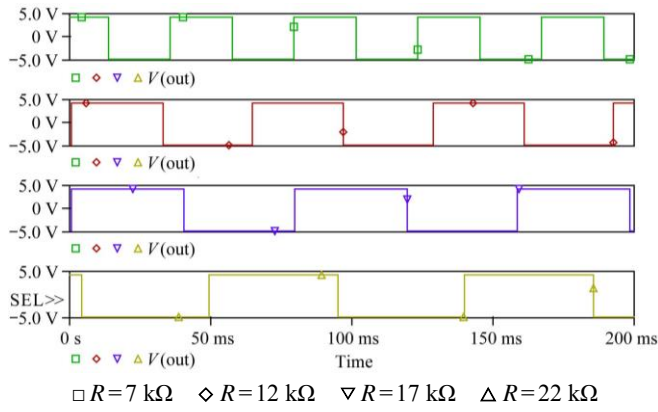


Figure 7 PSpice simulation results of the output voltage with respect to different  $R$  values

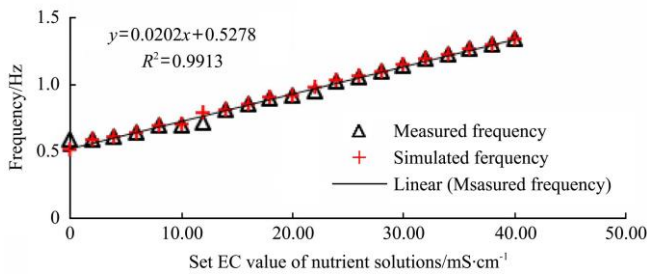


Figure 8 Relationship among simulated frequency, measured frequency and set EC value of the nutrient solution

Moreover, an experiment was conducted to verify the mathematical relationship between the simulated frequency, output frequency of the EC sensor and the EC value of the nutrient solutions. The frequencies were measured by using MSP430 G2553 MCU as the EC values of the nutrient solutions were set to different values. A fitted linear equation was obtained between the output frequency and the EC value of the nutrient solution, and the  $R^2 = 0.9993$  (Figure 8) which meant that there was a significant linear correlation between the output frequency of the EC sensor and the EC value of the nutrient solution. Thus, the EC value of the nutrient solution can be measured precisely, the accuracy of the EC sensor can reach 0.85% according to the measured EC value and set EC value of the nutrient solution (Figure 9), the set EC value was set by using the DDSJ-308F conductivity meter bought from INESA Scientific Instrument Co., Ltd.

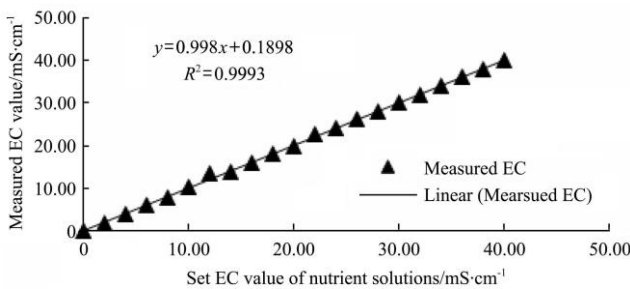


Figure 9 Relationship between measured EC value and set EC value of the nutrient solution.

### 3.3 Experiment under the first condition using the two algorithms

An experiment was conducted under the first condition, in which various suction pipes were opened with a target EC value of 2 mS/cm. The EC response curves over time when the four suction pipes were opened are shown in Figures 10-13.

According to all four figures, the system could reach the steady state by using both control algorithms. When the combination

control algorithm was used, the steady-state response time was 186 s (Figure 10), 172 s (Figure 11), 134 s (Figure 12), and 122 s (Figure 13) corresponding to the opening of suction pipes 1, 2, 3, and 4, respectively. By contrast, the response time was 220 s (Figure 10), 196 s (Figure 11), 158 s (Figure 12), and 148 s (Figure 13) when incremental PID control was used. The response time was shortened when the suction flow was high, and the response time of the combination algorithm control was shorter than that of incremental PID control.

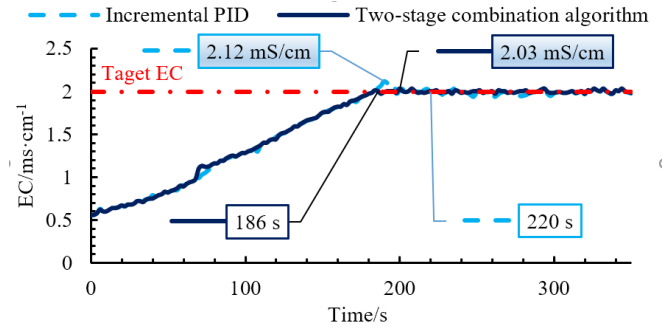


Figure 10 EC response using the two control algorithms when opening one suction pipe

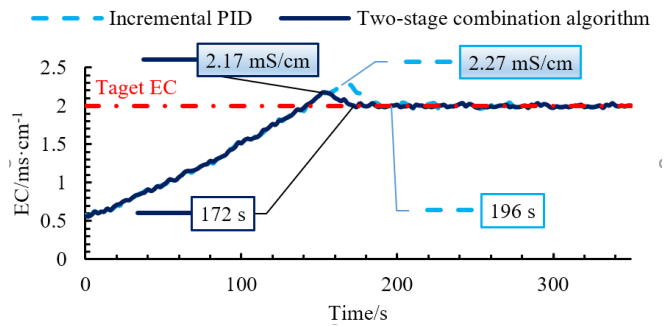


Figure 11 EC response using the two control algorithms when opening two suction pipes

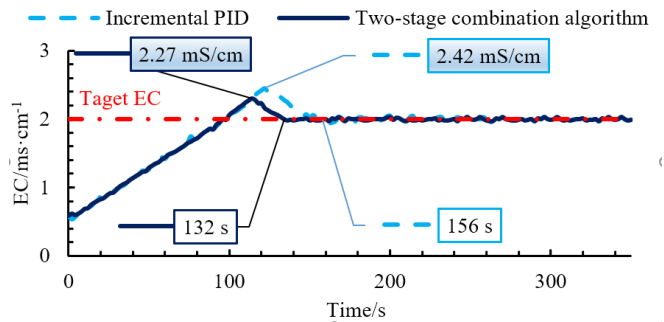


Figure 12 EC response using the two control algorithms when opening three suction pipes

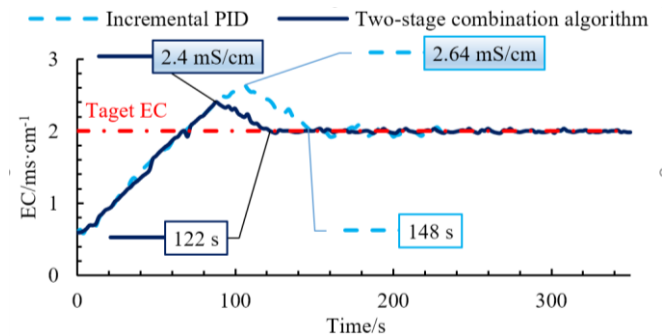


Figure 13 EC response using the two control algorithms when opening four suction pipes

Overshoot phenomena were observed in both control strategies when various suction pipes were opened, but no such phenomena were observed when only one suction pipe was opened using the combination algorithm control strategy. The maximum EC values obtained by opening suction pipes 1, 2, 3, and 4 using the combination algorithm were 2.03 mS/cm (Figure 10), 2.17 mS/cm (Figure 11), 2.3 mS/cm (Figure 12), and 2.4 mS/cm (Figure 13), respectively. Whereas the obtained values were 2.12 mS/cm (Figure 10), 2.27 mS/cm (Figure 11), 2.45 mS/cm (Figure 12), and 2.64 mS/cm (Figure 13), respectively, by using incremental PID control. The overshoot was evidently higher for incremental PID control than for the combination algorithm control.

### 3.4 Experiment under the second condition using the two algorithms

Another experiment was conducted under the second condition, in which four suction pipes were opened with different target EC settings. The EC values under steady state, minimum bias, response time, and maximum overshoot are presented in Table 2, with target EC value settings of 1.5 mS/cm, 2.0 mS/cm, and

2.5 mS/cm, respectively. The results showed that the EC values remained more stable after reaching the steady state when the combination algorithm control was used compared with incremental PID control with the three types of target EC value settings. Using the combination algorithm control resulted in a short response time and low maximum overshoot. The combination algorithm control also showed better performance than incremental PID control. The shortest response time and the minimum overshoot were 96 s and 0.18 mS/cm, respectively, when the target EC value was 1.5 mS/cm.

The results also showed that the response was fast, and the control strategy obtained low overshoot when the target EC value was low.

Most greenhouses in China are located in more than 1 mu (666.67 m<sup>2</sup>), and the time for irrigation nutrient solutions to move from the fertigation system to the farthest irrigation area is more than 2 min. Therefore, the response time of the combination control algorithm (such as 96 s, 122 s, and 135 s) is suitable for fertigation control in a greenhouse.

**Table 2 Comparison of the two control algorithms with different target EC values**

Target EC values /mS·cm <sup>-1</sup>	Control strategy	EC under steady-state /mS·cm <sup>-1</sup>	Minimum bias /%	Response time /s	Maximum overshoot /mS·cm <sup>-1</sup>
1.5	Two-stage Combination algorithm	1.48–1.53	1.67	96.00	+0.18
	Incremental PID algorithm	1.40–1.59	6.30	112.00	+0.40
2.0	Two-stage Combination algorithm	1.97–2.02	1.25	122.00	+0.40
	Incremental PID	1.92–2.08	4.00	148.00	+0.64
2.5	Two-stage Combination algorithm	2.48–2.53	0.80	135.00	+0.46
	Incremental PID algorithm	2.41–2.60	3.80	166.00	+0.69

### 3.5 Discussion

The fertigation control system developed in this study can automatically regulate the EC values of the irrigation nutrient solutions. With a good control algorithm, it will provide an optimal way of water and fertilizer management to meet the nutritional requirements of crops in greenhouses, thus the automatic fertigation control system can contribute to precise cultivation of crops in greenhouses and save water and fertilizers. The results of the experiments in this study under the two conditions showed that the fertigation system with the combination algorithm can operate rapidly, accurately, and steadily with a small overshoot. Therefore, the fertigation system controlled fertilizer concentration of the irrigation nutrient solution precisely and effectively, which means that the fertigation system can provide a precise quality control of the irrigation and fertilization for greenhouse crops. Fertigating crops in greenhouses based on the two-stage combination algorithm that can provide the nutrient solution that has the most suitable EC value is economical due to the following two reasons.

First, the mixing process of the nutrient solution was simplified to obtain a mathematical model of the fertigation system. The transfer function for incremental PID controller, which might be inaccurate, was then obtained. The mixing process of the nutrient solution is highly complicated, and fuzzy control logic, which can be used for complex nonlinear systems<sup>[32]</sup>, is suitable for the fertigation system.

Second, a two-stage combination control algorithm was proposed and showed better performance than a single one. In the first stage, the fertigation system could rapidly regulate the EC value of the nutrient solution to the desired EC value with the PI controller, and in the second stage, the fuzzy controller could help

the system avoid a large overshoot and maintain stability.

Although the two-stage combination control algorithm was suitable for the fertigation system, overshooting still existed, it might be because the threshold value (+0.2 mS/cm) for  $e$  was set too low, or the accuracy of fuzzy logic was insufficiently high. Moreover, only EC control of the irrigation nutrient solution was studied, however, the pH value of the nutrient solution is also a key parameter of the nutrient solution<sup>[33]</sup> which was under control in this study but not presented in this paper. Thus, we will continue to carry out some experiments for the threshold value adjusting to achieve a better performance in future study, also the pH value regulation of the irrigation nutrient solution will be the topic of our next paper.

## 4 Conclusions

Two control strategies for automatic fertigation control, namely, incremental PID control and combination control algorithm, were analyzed. Both could effectively adjust the EC value of the nutrient solution to the target EC value.

When the fertigation system was operated with four opened suction pipes and the target EC value was set to 2.0 mS/cm, the response time and maximum overshoot were 148 s and 0.64 mS/cm, respectively, for incremental PID control and 122 s and 0.4 mS/cm, respectively, for the combination control algorithm. When the target EC value was 2.5 mS/cm with four opened suction pipes, the response time and maximum overshoot were 166 s and 0.69 mS/cm, respectively, for incremental PID control and 135 s and 0.46 mS/cm, respectively, for the combination control algorithm. The combination control algorithm had a shorter response time and lower overshoot than incremental PID control. Overshoot, which can lead to a high EC value of the nutrient solution, might be

harmful to crops.

For the combination control algorithm, when the target EC values were set to 1.5 mS/cm, 2.0 mS/cm, and 2.5 mS/cm with four opened suction pipes, the minimum bias data were 1.67%, 1.25%, and 0.80%, respectively. The bias decreased when the target EC was set to a large value.

The present study showed that the combination control strategy had better properties than the incremental PID control strategy for automatic fertigation management, and it will provide a scientific basis for precise irrigation and fertilization control for crops in greenhouses. While due to the limitation of the study, the quantitative estimation is not carried out to verify that the developed control algorithm could significantly decrease the water and fertilizer usage, we do have our fertigation system using in several greenhouses, we will continue to do more greenhouse experiments to verify it.

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