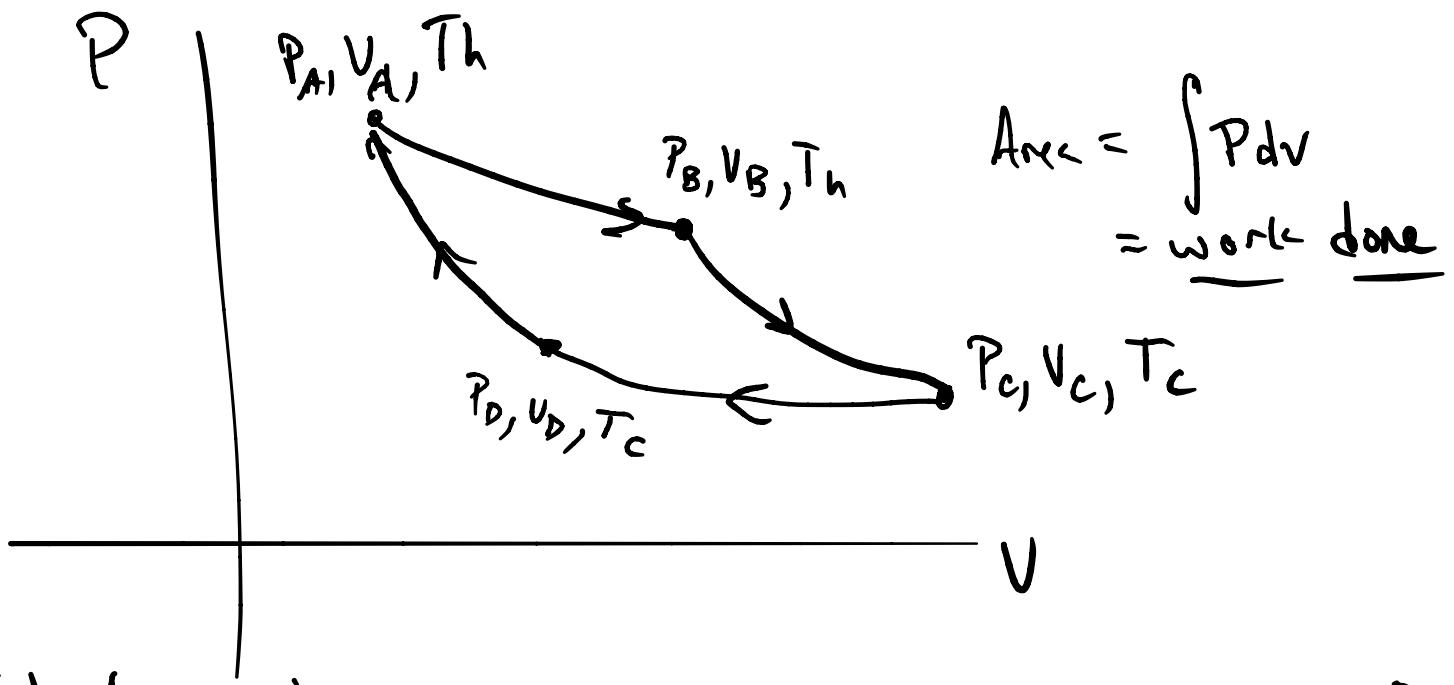


Review of Carnot cycle from last time;  
 2 steps where system does work  
 $(w_{sys} < 0)$  and two where  
 the system has work done on it ( $w_{sys} > 0$ )

Isothermal - adiabatic - Isothermal - adiabatic  
 expansion cooling expansion heating



Ideal gas:

$$\underline{\text{Isothermal}} \quad \Delta E = 0, \quad f = -w \quad \downarrow$$

$$w_{sys} = - \int_{V_1}^{V_2} P_{sys} dV = - \int_{V_1}^{V_2} \frac{nRT}{V} dV = - nRT \ln(V_2/V_1)$$

$$q = nRT \ln(V_2/V_1), \quad \begin{matrix} \text{heat in work out} \\ \text{if expanding} \end{matrix}$$

$$\underline{\text{Adiabatic}} \quad q = 0, \quad \Delta E = nC_V \Delta T = w$$

$$\text{cool: } T_c - T_h < 0 \Rightarrow w < 0, \text{ does work}$$

- ① isothermal expansion       $\frac{q_f}{nRT_h \ln(v_B/v_A)} = -\frac{\omega_{sys}}{nRT_h \ln(v_B/v_A)}$
- ② adiabatic expansion       $\Delta E = \omega = C_V(T_c - T_h)$
- ③ isothermal compression       $nRT_c \ln(v_D/v_C) = -nRT_c \ln(v_D/v_C)$
- ④ adiabatic compression       $\omega = +C_V(T_h - T_c)$

$$\omega_{total} = -nRT_h \ln(v_B/v_A) - nRT_c \ln(v_D/v_C)$$

$$\omega_{done} = -\omega_{total} = q_1 + q_3$$

$$\epsilon = \frac{-\omega}{q_{in}} = \frac{-\omega}{q_1} = \frac{q_1 + q_3}{q_1} = 1 + \frac{q_3}{q_1}$$

$$\frac{q_3}{q_1} = \frac{nRT_c \ln(v_D/v_C)}{nRT_h \ln(v_B/v_A)}$$

for adiabatic expansion, showed

$$V_f/V_i = \left(\frac{T_f}{T_i}\right)^{-C_V/nR} \Rightarrow \frac{\ln(v_D/v_C)}{\ln(v_B/v_A)} = -1$$

$$\Rightarrow \boxed{\epsilon = 1 - T_c/T_h} \quad \leftarrow \text{more general than ideal gas}$$

as  $T_h \rightarrow \infty$ ,  $\epsilon \rightarrow 1$

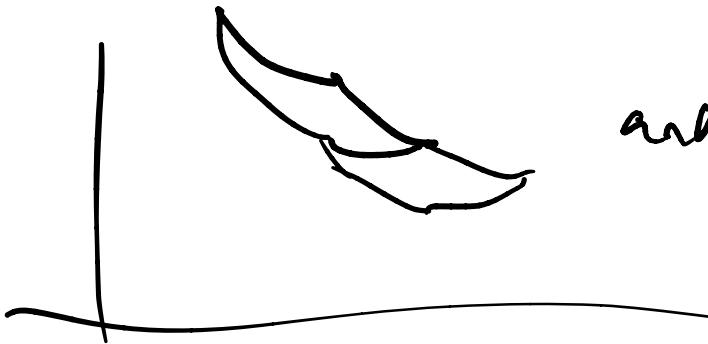
as  $T_c \rightarrow 0$ ,  $\epsilon \rightarrow 1$

Now  $\frac{q_3}{T_1} = -\frac{T_c}{T_h} = -\frac{T_3}{T_1}$

$$\Rightarrow q_1/T_1 + \frac{q_3}{T_3} = 0$$

Suggests a quantity that is a state function, because any path around cycle adds up to zero

Can make many small cannot cycles add up



and take the limit  
to small sides

Any process exchanging  
heat btwn reservoirs  
can look like this

$$\text{so } \sum_{\text{cycle}} q_i^{\text{rev}} / T = 0 \rightarrow \oint dq^{\text{rev}} / T = 0$$

suggests we define  $dS \equiv dq^{\text{rev}} / T$

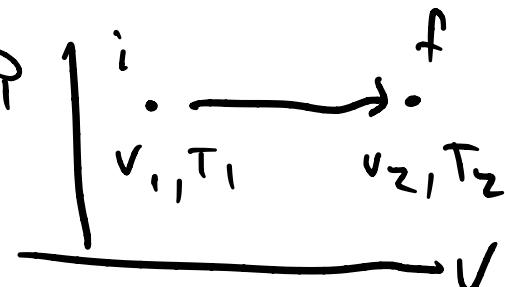
State function &  $\oint dS = 0$

$$\Delta S = \int_i^f dS \quad \text{regardless of path} \star$$

Entropy for some reversible processes

1. Const P expansion

$$\Delta S = \int_i^f \frac{dq^{\text{rev}}}{T} = \int_{T_1}^{T_2} C_P T dT$$



$$dq = C_P dT \quad \underbrace{s_{12}/R}_{\text{ideal gas}} = C_P \ln(T_2/T_1) \text{ if } C_P \text{ const}$$

$$\text{ideal gas} = C_P \ln(v_2/v_1) \text{ b/c } v \propto T$$

## ② Const Volume

$$\Delta S = C_V \ln(T_2/T_1) \text{ for same reason}$$

$$= \frac{3}{2} R \ln(T_2/T_1) \leftarrow \text{more ideal gas}$$

## ③ Const T, $dE = 0$ , $df = -\omega = PdV$

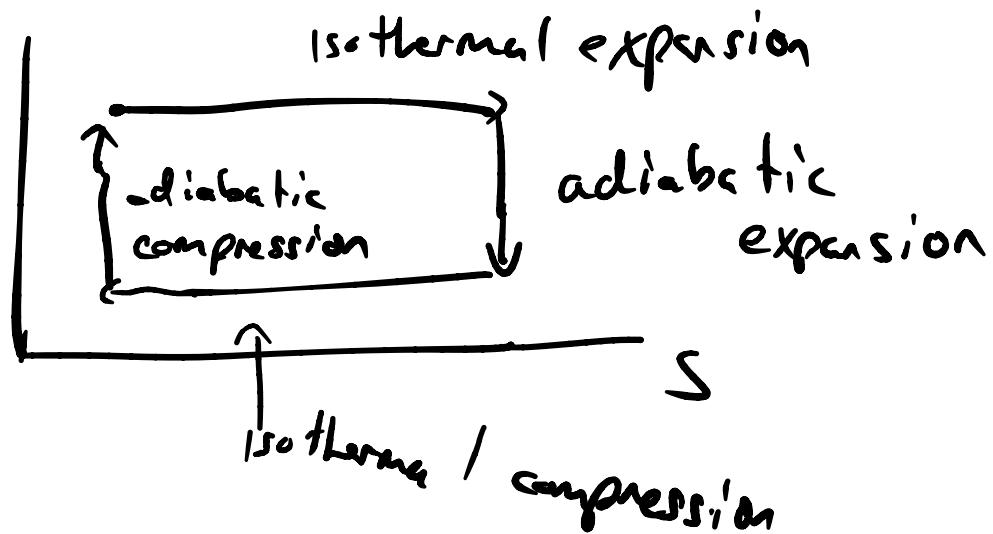
$$\Delta S = \int_i^f \frac{df_{rw}}{T} = \int_{V_1}^{V_2} \frac{P}{T} dV = nR \ln(V_2/V_1)$$

$\leftarrow \text{ideal gas}$

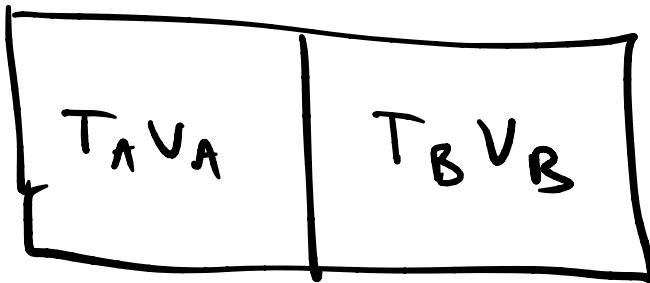
in these two, have only  $T$  or  $V$   
because other is constant

## ④ adiabatic - $df = 0 \Rightarrow \Delta S = 0$

Carnot cycle  $T$



lets look at heat flow instead of cycles



isolated  
 $V_A$  fixed  $V_B$  fixed  
heat flows until  $T_L = T_R$

$$\mathcal{E} = \mathcal{E}_A + \mathcal{E}_B$$

$$d\mathcal{E} = d\mathcal{E}_A + d\mathcal{E}_B$$

$$dq^{\text{rev}} = T dS$$

$$d\mathcal{E} = \underbrace{dq}_{0, \text{ constant}} + \underbrace{d\omega}_{0}$$

$$\text{So } dS = dS_A + dS_B = \frac{d\mathcal{E}_A}{T_A} + \frac{d\mathcal{E}_B}{T_B}$$

$$\text{But here } d\mathcal{E}_A = -d\mathcal{E}_B$$

$$\Rightarrow dS = d\mathcal{E}_A \cdot \left( \frac{1}{T_A} - \frac{1}{T_B} \right)$$

$$\text{If } T_A > T_B, d\mathcal{E}_A < 0$$

$$\text{and } \frac{1}{T_A} - \frac{1}{T_B} < 0$$

Entropy increases!

Not conserved for closed sys.

In fact = 0 for equilibrium

and spontaneous processes occur until entropy is Maximized

$dS > 0$  (spont process, isolated system)

$dS = 0$  (rev process isolated system)

For an irreversible process, entropy is produced in the system

Now, if we are not in an isolated system  $dS = dS_{prod} + dS_{exch}$

$$= dS_{prod} + \frac{dq_f}{T}$$

For reversible,  $dS = \frac{dq^{rev}}{T}$

For irreversible,  $dS_{prod} > 0$

$$\Rightarrow dS > \frac{dq^{irr}}{T}$$

$dS \geq \frac{dq}{T}$  any process (equal for rev)

$\Delta S \geq \int \frac{dq}{T} \leftarrow \text{2nd law eqn}$

Note, Universe is closed system

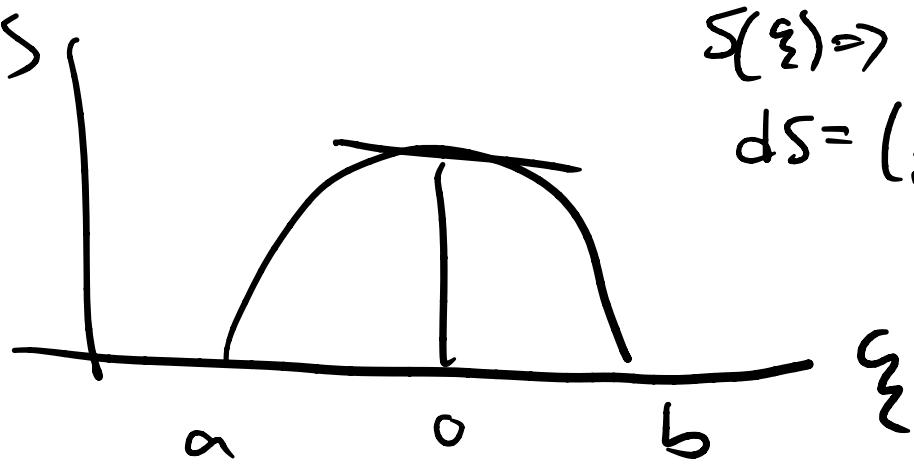
$$\text{so } dQ=0 \text{ &}$$

$dS > 0$  for any spontaneous process!

Entropy as a thermodynamic potential

Suppose  $\xi$  says how far we are from eq (like  $[A] - [A_{eq}]$ )

Then  $S$



$$S(\xi) \Rightarrow$$

$$dS = \left( \frac{\partial S}{\partial \xi} \right) d\xi$$

$$\frac{\partial S}{\partial \xi} = 0 \text{ @ eq,}$$

$$\frac{\partial S}{\partial \xi} > 0 \text{ if } \xi < 0$$

$$\frac{\partial S}{\partial \xi} < 0 \text{ if } \xi > 0$$

Acts like a potential

Ex: heat flow btwn two bodies

$$T_f = \frac{T_A + T_B}{2}$$

Entropy is state func so although irreversible, can do const volume reversible cooling so

$$\Delta S_A = C_V \ln \left( \frac{T_f}{T_A} \right) \quad (\text{some substance})$$

$$\Delta S_B = C_V \ln \left( \frac{T_f}{T_B} \right)$$

$$\begin{aligned}\Delta S &= \Delta S_A + \Delta S_B \\ &= C_V \ln \left( \frac{(T_A + T_B)^2}{4 T_A T_B} \right)\end{aligned}$$

$$\text{if } T_A = T_B = 0$$

otherwise always positive

$$\begin{aligned}\text{b/c } T_A^2 + 2 T_A T_B + T_B^2 - 4 T_A T_B \\ = (T_A - T_B)^2 > 0\end{aligned} \quad \checkmark$$