

Package ‘methanogenlab’

April 15, 2022

Type Package

Title Methanogenesis Model

Version 0.1.2

Description Evolves a closed system
undergoing methanogenesis.

Imports microbialkitchen,
CHNOSZ,
mathjaxr

Remotes KopfLab/microbialkitchen

RdMacros mathjaxr

License What license is it under?

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alkalinity	<i>Calculates solution alkalinity</i>
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Description

‘alkalinity()’ Uses the calculate_closed_system_alkalinity function from Sebastian Kopf’s micro-bialkitchen R package to calculate media alkalinity

Usage

```
alkalinity(
  pH,
  nDIC,
  VolumeSolution,
  VolumeHeadspace,
  temperature,
  K.CO2HCO3,
  K.HCO3CO3
)
```

Arguments

pH	pH of the system.
nDIC	Moles of dissolved inorganic carbon
VolumeSolution	Volume of liquid in the closed system, in liters.
VolumeHeadspace	Volume of gaseous head space in the closed system, in liters.
temperature	Temperature of the system, in Kelvin.
K.CO2HCO3	Equilibrium constant for the dissociation of CO ₂ (aq) to HCO ₃ ⁻ (aq).
K.HCO3CO3	Equilibrium constant for the dissociation of HCO ₃ ⁻ (aq) to CO ₃ ⁻ (aq).

Value

alkalinity of the solution, in millimolar.

aqueous.step	<i>Uses Henry’s Law to calculate dissolved gas concentrations</i>
--------------	---

Description

‘aqueous.step()’ calculates the aqueous concentration at each step using the current pressure.

Usage

```
aqueous.step(P.step, K)
```

Arguments

P.step	the current pressure in the system.
K	Henry's equilibrium constant of the gas.

Value

Dissolved gas concentration, in molar.

biomass.coefficient	<i>Amount of biomass produced for every DIC consumed</i>
---------------------	--

Description

'biomass.coefficient()' calculates the amount of biomass produced for every mol of DIC consumed

Usage

```
biomass.coefficient(biomass.yield, carbon.fraction)
```

Arguments

biomass.yield	mass of dry biomass produced per mol of product.
carbon.fraction	w/w percent C of biomass, expressed as a decimal.

Value

biomass produced, in mol/mol DIC

calculate.Kgas	<i>Calculates Henry's constant for a gas</i>
----------------	--

Description

'calculate.Kgas()' uses the provided Bunsen coefficient and moles per volume of gas to calculate Henry's constant.

Usage

```
calculate.Kgas(bunsen, temperature, pressure)
```

Arguments

bunsen	The Bunsen coefficient for the gas.
temperature	Temperature of the system, in Kelvin.
pressure	The pressure of the system, in atm.

calculate.KH	<i>Calculates equilibrium constants using CHNOSZ</i>
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Description

‘calculate.KH()’ utilizes the subrt function from Jeffrey Dick’s CHNOSZ R package to calculate equilibrium constants.

Usage

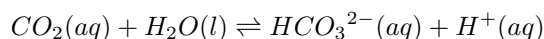
```
calculate.KH(reactants, moles, phases, temperature, pressure)
```

Arguments

reactants	A vector of all components involved in the reaction, both reactants and products.
moles	A vector of the molar coefficients for the reaction, with negative values indicating reactants and positive values indicating products.
phases	A vector of the phases for all components in the reaction, either "aq", "l", or "g".
temperature	Temperature of the system, in Kelvin.
pressure	The pressure of the system, in atm.

Details

For the following chemical equilibrium:



an example can found below

Examples

```
calculate_KH(c("CO2", "H2O", "HCO3-", "H+"), c(-1, -1, 1, 1), c("aq", "l", "aq", "aq"), 273.15+37, 1.7)
```

carbon.yield	<i>Biomass to carbon yield</i>
--------------	--------------------------------

Description

‘carbon.yield()’ converts the known organism-specific biomass yield per mol of product into carbon yield.

Usage

```
carbon.yield(biomass.yield, carbon.fraction)
```

Arguments

biomass.yield mass of dry biomass produced per mol of product.
carbon.fraction w/w percent C of biomass, expressed as a decimal.

Value

carbon yield, in mol C/mol product

CH4.coefficient	<i>Amount of CH4 produced for every DIC consumed</i>
-----------------	--

Description

'CH4.coefficient()' calculates the amount of CH4 produced for every mol of DIC consumed.

Usage

CH4.coefficient(biomass.yield, carbon.fraction)

Arguments

biomass.yield mass of dry biomass produced per mol of product.
carbon.fraction w/w percent C of biomass, expressed as a decimal.

Value

CH4 produced, in mol/mol DIC

gibbs.step	<i>Calculates Gibbs free energy</i>
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Description

'gibbs.step()' calculates the Gibbs free energy at each step in the model for a given Q and standard Gibbs free energy.

Usage

gibbs.step(standard.gibbs, Q, temperature)

Arguments

standard.gibbs The standard Gibbs free energy of formation of the reaction in J/mol
Q Current reaction quotient
temperature Temperature of the system, in Kelvin.

growth	<i>Determines the number of new cells generated using Monod kinetics for a given time step size based on the current chemistry of the system.</i>
--------	---

Description

Determines the number of new cells generated using Monod kinetics for a given time step size based on the current chemistry of the system.

Usage

```
growth(
  cells.initial,
  CO2,
  is.CO2.limiting = NA,
  Ks.CO2,
  H2,
  is.H2.limiting = NA,
  Ks.H2,
  umax,
  time.step
)
```

Arguments

cells.initial	Number of cells currently in the system.
CO2	Current dissolved CO2
is.CO2.limiting	Boolean. Determines whether to use the Monod equation for CO2. NA by default (limiting contribution determined by the proportion of current CO2 and Ks.CO2).
Ks.CO2	Half-saturation constant for CO2 (microorganism dependent), in molarity.
H2	Current dissolved H2
is.H2.limiting	Boolean. Determines whether to use the Monod equation for H2. NA by default (limiting contribution determined by the proportion of current H2 and Ks.H2).
Ks.H2	Half-saturation constant for H2 (microorganism dependent), in molarity.
umax	Maximum growth rate for the microorganism, hr^{-1}
time.step	Step size in time, in hours. 0.1 hrs by default.

Value

Number of new cells made

H2.coefficient	<i>Amount of H2 consumed for every DIC consumed</i>
----------------	---

Description

'H2.coefficient()' calculates the amount of H2 consumed for every mol of DIC consumed.

Usage

```
H2.coefficient(biomass.yield, carbon.fraction)
```

Arguments

`biomass.yield` mass of dry biomass produced per mol of product. 2.4 g/mol product by default.
`carbon.fraction` w/w percent C of biomass, expressed as a decimal. 0.44 by default.

Value

H2 consumed, in mol/mol DIC

<code>init</code>	<i>Determines initial conditions from initial inputs</i>
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Description

'init()' sets up the initial environment to be used by the methanogenesis model.

Usage

```
init(
  CH4.initial,
  K.CH4,
  H2.initial,
  K.H2,
  DIC.initial,
  pH.initial,
  K.CO2,
  temperature,
  VolumeSolution,
  VolumeHeadspace,
  inoculum.cell.number,
  biomass.yield,
  carbon.fraction,
  cell.weight,
  K.CO2HCO3,
  K.HCO3CO3
)
```

Arguments

CH4.initial	Concentration of initial dissolved CH ₄ , in molarity.
K.CH4	Henry's constant for CH ₄ . NA by default (calculated by CHNOSZ).
H2.initial	Concentration of initial dissolved H ₂ , in molarity.
K.H2	Henry's constant for H ₂ . NA by default (calculated by CHNOSZ).
DIC.initial	Concentration of initial dissolved inorganic carbon, in molarity.
pH.initial	initial pH.
K.CO2	Henry's constant for CH ₄ . NA by default (calculated by CHNOSZ).
temperature	Temperature of the system, in Kelvin.
VolumeSolution	Volume of liquid in the closed system, in liters.
VolumeHeadspace	Volume of gaseous head space in the closed system, in liters.
inoculum.cell.number	Initial number of cells. 1e6 by default.
biomass.yield	mass of dry biomass produced per mol of product. 2.4 g/mol product by default.
carbon.fraction	w/w percent C of biomass, expressed as a decimal. 0.44 by default.
cell.weight	individual cell mass, in grams. 30e-15 by default.
K.CO2HCO3	Equilibrium constant for the dissociation of CO ₂ (aq) to HCO ₃ ⁻ (aq). NA by default (calculated by CHNOSZ).
K.HCO3CO3	Equilibrium constant for the dissociation of HCO ₃ ⁻ (aq) to CO ₃ ⁻ (aq). NA by default (calculated by CHNOSZ).

Value

A data frame to be used for the methanogenesis function.

methanogenesis.DIC	<i>Steps through DIC consumption during a methanogenesis reaction</i>
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Description

'methanogenesis.DIC()' calculates CH₄ produced, H₂ consumed, CO₂ consumed, pH, and Gibbs free energy changes as dissolved inorganic carbon is consumed.

Usage

```
methanogenesis.DIC(
  CH4.initial,
  K.CH4 = NA,
  H2.initial,
  K.H2 = NA,
  DIC.initial,
  pH.initial,
  K.CO2 = NA,
  temperature,
```



```

VolumeSolution,
VolumeHeadspace,
K.CO2HCO3 = NA,
K.HCO3CO3 = NA,
delta.DIC = 1e-04,
inoculum.cell.number = 1e+06,
biomass.yield = 2.4,
carbon.fraction = 0.44,
cell.weight = 3e-14
)

```

Arguments

CH4.initial	Concentration of initial dissolved CH ₄ , in molarity.
K.CH4	Henry's constant for CH ₄ . NA by default (calculated by CHNOSZ).
H2.initial	Concentration of initial dissolved H ₂ , in molarity.
K.H2	Henry's constant for H ₂ . NA by default (calculated by CHNOSZ).
DIC.initial	Concentration of initial dissolved inorganic carbon, in molarity.
pH.initial	initial pH.
K.CO2	Henry's constant for CH ₄ . NA by default (calculated by CHNOSZ).
temperature	Temperature of the system, in Kelvin.
VolumeSolution	Volume of liquid in the closed system, in liters.
VolumeHeadspace	Volume of gaseous head space in the closed system, in liters.
K.CO2HCO3	Equilibrium constant for the dissociation of CO ₂ (aq) to HCO ₃ ⁻ (aq). NA by default (calculated by CHNOSZ).
K.HCO3CO3	Equilibrium constant for the dissociation of HCO ₃ ⁻ (aq) to CO ₃ ⁻ (aq). NA by default (calculated by CHNOSZ).
delta.DIC	step size, in millimolar DIC. 0.1 mM by default.
inoculum.cell.number	Initial number of cells. 1e6 by default.
biomass.yield	mass of dry biomass produced per mol of product. 2.4 g/mol product by default.
carbon.fraction	w/w percent C of biomass, expressed as a decimal. 0.44 by default.
cell.weight	individual cell mass, in grams. 30e-15 by default.

Value

A data frame of the model results

Examples

```

methanogenesis(
  CH4.initial = 1e-6,
  H2.initial = 5e-4,
  DIC.initial = 3.2e-3,
  pH.initial = 7.5,
  temperature = 273.15+40,
  VolumeSolution = 80e-3,

```

```
VolumeHeadspace = 20e-3,
delta.DIC = 0.0001)
```

methanogenesis.time	<i>Steps through time during a methanogenesis reaction</i>
---------------------	--

Description

'methanogenesis.time()' calculates CH₄ produced, H₂ consumed, CO₂ consumed, pH, and Gibbs free energy changes as dissolved inorganic carbon is consumed over time.

Usage

```
methanogenesis.time(
  CH4.initial,
  K.CH4 = NA,
  H2.initial,
  K.H2 = NA,
  is.H2.limiting = NA,
  Ks.H2,
  DIC.initial,
  pH.initial,
  K.CO2 = NA,
  is.CO2.limiting = NA,
  Ks.CO2,
  umax,
  temperature,
  VolumeSolution,
  VolumeHeadspace,
  K.CO2HCO3 = NA,
  K.HCO3CO3 = NA,
  time.step = 0.1,
  total.time = 5,
  inoculum.cell.number = 1e+06,
  biomass.yield = 2.4,
  carbon.fraction = 0.44,
  cell.weight = 3e-14
)
```

Arguments

CH4.initial	Concentration of initial dissolved CH ₄ , in molarity.
K.CH4	Henry's constant for CH ₄ . NA by default (calculated by CHNOSZ).
H2.initial	Concentration of initial dissolved H ₂ , in molarity.
K.H2	Henry's constant for H ₂ . NA by default (calculated by CHNOSZ).
is.H2.limiting	Boolean. Determines whether to use the Monod equation for H ₂ . NA by default (limiting contribution determined by the proportion of current H ₂ and Ks.H2).
Ks.H2	Half-saturation constant for H ₂ (microorganism dependent), in molarity.
DIC.initial	Concentration of initial dissolved inorganic carbon, in molarity.

pH.initial	initial pH.
K.CO2	Henry's constant for CH ₄ . NA by default (calculated by CHNOSZ).
is.CO2.limiting	Boolean. Determines whether to use the Monod equation for CO ₂ . NA by default (limiting contribution determined by the proportion of current CO ₂ and Ks.CO ₂).
Ks.CO2	Half-saturation constant for CO ₂ (microorganism dependent), in molarity.
umax	Maximum growth rate for the microorganism, hr^{-1}
temperature	Temperature of the system, in Kelvin.
VolumeSolution	Volume of liquid in the closed system, in liters.
VolumeHeadspace	Volume of gaseous head space in the closed system, in liters.
K.CO2HCO3	Equilibrium constant for the dissociation of CO ₂ (aq) to HCO ₃ -(aq). NA by default (calculated by CHNOSZ).
K.HCO3CO3	Equilibrium constant for the dissociation of HCO ₃ -(aq) to CO ₃ -(aq). NA by default (calculated by CHNOSZ).
time.step	Step size in time, in hours. 0.1 hrs by default.
total.time	Length of time the model will run, in hours. Note: the model may break before the total.time is reached if H ₂ or DIC runs out.
inoculum.cell.number	Initial number of cells. 1e6 by default.
biomass.yield	mass of dry biomass produced per mol of product. 2.4 g/mol product by default.
carbon.fraction	w/w percent C of biomass, expressed as a decimal. 0.44 by default.
cell.weight	individual cell mass, in grams. 30e-15 by default.

Value

A data frame of the model results

Examples

```
methanogenesis.time(
  CH4.initial= 1e-6,
  H2.initial= 5e-4,
  is.H2.limiting=FALSE,
  Ks.H2=10e-6,
  DIC.initial= 3.2e-3,
  pH.initial= 7.5,
  is.CO2.limiting=TRUE,
  Ks.CO2=20e-6,
  umax=0.6,
  temperature= 273.15+40,
  VolumeSolution = 80e-3,
  VolumeHeadspace = 20e-3,
  time.step=0.1,
  total.time=50,
  inoculum.cell.number = 1e6,
  biomass.yield=2.4,
  carbon.fraction=0.44,
  cell.weight=30e-15)
```

PCO2

*Calculates CO2 pressure in the head space of the closed system.***Description**

‘PCO2()’ Uses the calculate_closed_system_pCO2 function from Sebastian Kopf’s microbialkitchen R package to calculate pressure of CO2 gas.

Usage

```
PCO2(
  pH,
  nDIC,
  VolumeSolution,
  VolumeHeadspace,
  temperature,
  K.CO2HCO3,
  K.HCO3CO3
)
```

Arguments

pH	pH of the system.
nDIC	Moles of dissolved inorganic carbon
VolumeSolution	Volume of liquid in the closed system, in liters.
VolumeHeadspace	Volume of gaseous head space in the closed system, in liters.
temperature	Temperature of the system, in Kelvin.
K.CO2HCO3	Equilibrium constant for the dissociation of CO2(aq) to HCO3-(aq).
K.HCO3CO3	Equilibrium constant for the dissociation of HCO3- (aq) to CO3- (aq).

Value

CO2 pressure in the head space, in atm.

pH

*Calculates pH of the solution***Description**

‘pH()’ Uses the calculate_closed_system_pH function from Sebastian Kopf’s microbialkitchen R package to calculate pH.

Usage

```
pH(
  nDIC,
  VolumeSolution,
  VolumeHeadspace,
  temperature,
  alkalinity,
  K.CO2HCO3,
  K.HCO3CO3
)
```

Arguments

nDIC	Moles of dissolved inorganic carbon
VolumeSolution	Volume of liquid in the closed system, in liters.
VolumeHeadspace	Volume of gaseous head space in the closed system, in liters.
temperature	Temperature of the system, in Kelvin.
alkalinity	initial alkalinity of the system, in millimolar.
K.CO2HCO3	Equilibrium constant for the dissociation of CO ₂ (aq) to HCO ₃ ⁻ (aq).
K.HCO3CO3	Equilibrium constant for the dissociation of HCO ₃ ⁻ (aq) to CO ₃ ⁻ (aq).

Value

pH of the solution.

pressure.step	<i>Calculates head space pressure</i>
---------------	---------------------------------------

Description

‘pressure.step()’ calculates head space partial pressure from the total moles of a particular gas in the system using Henry’s law and the Ideal Gas law.

Usage

```
pressure.step(n.total.step, K, VolumeSolution, VolumeHeadspace, temperature)
```

Arguments

n.total.step	The total number of moles of a gas in the system.
K	Henry’s constant of the gas.
VolumeSolution	Volume of liquid in the closed system, in liters.
VolumeHeadspace	Volume of gaseous head space in the closed system, in liters.
temperature	Temperature of the system, in Kelvin.

Value

Partial pressure of the head space.

standard.gibbs	<i>Calculates standard Gibbs free energy for a given temperature and pressure</i>
----------------	---

Description

'standard.gibbs()' determines the standard Gibbs free energy to be used in 'gibbs.step()'

Usage

```
standard.gibbs(reactants, moles, phases, temperature, pressure = 1)
```

Arguments

reactants	A vector of all components involved in the reaction, both reactants and products.
moles	A vector of the molar coefficients for the reaction, with negative values indicating reactants and positive values indicating products.
phases	A vector of the phases for all components in the reaction, either "aq", "l", or "g".
temperature	Temperature of the system, in Kelvin.
pressure	The pressure of the system, in atm.

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