

Supplementary Material for “Mitigating Electrochemical Degradation in Optimal Vehicle-to-Grid Dispatch via Digital Twin”

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I. EXISTING SEI THICKNESS FOR BATTERY SEI GROWTH

Figures 1(a)–(d) respectively plot the $(S_i^t, I_i^t, \Delta\theta_i^t)$ -spaces under $\theta_i^t = 0$ [nm], $\theta_i^t = 20$ [nm], $\theta_i^t = 40$ [nm], and $\theta_i^t = 80$ [nm], using the same scale for all axes. Intuitively, θ_i^t has a slight shape variation under different θ_i^t . Thus, existing SEI thickness θ_i^t [nm] can be negligible in the SEI growth $\Delta\theta_i^t$ per charge-discharge cycle.

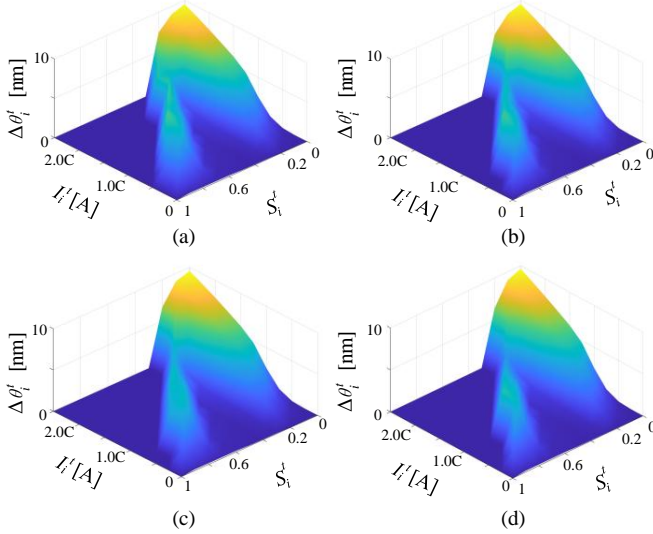


Fig. 1. PDE-based SEI growth surface $\Delta\theta_i^t$: (a) $\theta_i^t = 0$ [nm]; (b) $\theta_i^t = 20$ [nm]; (c) $\theta_i^t = 40$ [nm]; (d) $\theta_i^t = 80$ [nm];

II. DERIVATION OF SECOND-ORDER CONIC CONSTRAINT

We reformulate the constraint $\gamma_i^{t+1} \geq (z_{i,N_I}^{t+1})^2$ with $f = (\gamma_i^{t+1} + 1)^2$ and $g = (\gamma_i^{t+1} - 1)^2 + (2z_{i,N_I}^{t+1})^2$, yielding

$$f - g = 4\gamma_i^{t+1} - 4(z_{i,N_I}^{t+1})^2 \geq 0, \quad (\text{II-1})$$

Rearranging this inequality (II-1), we express

$$(\gamma_i^{t+1} + 1)^2 \geq (\gamma_i^{t+1} - 1)^2 + (2z_{i,N_I}^{t+1})^2, \quad (\text{II-2})$$

This is equivalent to the standard second-order conic constraint

$$\|\gamma_i^{t+1} + 1\|_2^2 \geq \|(\gamma_i^{t+1} - 1, 2z_{i,N_I}^{t+1})^T\|_2^2. \quad (\text{II-3})$$

III. BATTERY CELL PARAMETER VALUES

In this study, we suppose each EV consists of 21700-type battery cells with the capacity of 80 kWh. Each EV battery pack has 96 cells in series and 46 cells in parallel (96S46P), giving it a total of 4416 cells. Each battery cell capacity $I_{b,i} = 5$ Ah, nominal voltage $v_{\text{flat},i} = 3.65$ V with the operating voltage ranging from 2.5 V to 4.2 V, and current rate $C_{r,i}^t \in [0, \bar{C}_{r,i}]$, where the EV aggregator selects $\bar{C}_{r,i} = 2.5$ to avoid sharp charge-discharge cycling. For a battery cell, $\bar{p}_i \approx 3.65 \cdot 0.005 \cdot 2.5 \approx 0.046$ kW. The ambient temperature is 28°C. Other parameters for electrochemical kinetics are given in Table I.

IV. EXISTING BATTERY AGING FORMULATIONS

We revisit the existing linear and nonlinear battery aging methods in [2] and [5]. The linear battery degradation cost F_i^t is defined for each charging and discharging cycle at time period t until the required state of charge (SoC) in the last time period $t = N_t$, i.e., $S_i^{N_t} = \bar{S}$, yielding

$$F_i^t = C_i \frac{\kappa_i}{100} \left(-\frac{1}{\eta_v} p_{d,i}^t \theta t + \bar{S} - S_i^0 \right) \quad (\text{IV-4})$$

where $\kappa_i = 1$ denotes the slope of the linear approximation of the EV i 's battery life as a function of cycles. $C_i = 1$ represents the purchase cost of the EV i 's battery divided by its useful capacity [\$/Ah]. $S_{0,i}$ is the initial SOC value.

The nonlinear battery degradation cost G_i^t is an approximation function with respect to depth of discharge by $1 - S_i^t$ and cell current I_i^t (denoted in C-rate) based on the experimental data [5]. We have

$$G_i^t = \frac{1}{f_c(I_i^t) \cdot f_d(S_i^t)}, \quad (\text{IV-5})$$

where f_c and f_d respectively represent battery life loss under different DoDs and cell currents.

$$f_d = \begin{cases} 4000, & \text{if } S_i^t > 0.95 \\ 946.1 \cdot (1 - S_i^t)^{-1.079}, & \text{if } S_i^t \leq 0.95 \end{cases} \quad (\text{IV-6a})$$

$$f_c = \begin{cases} 4, & \text{if } I_i^t < 0.2 \\ 1.041 \cdot (I_i^t)^{-0.445}, & \text{if } 0.2 \leq I_i^t \leq 2.5 \end{cases} \quad (\text{IV-6b})$$

Subsequently, we express

$$G_i^t = \begin{cases} 0.6 \cdot 10^{-4}, & \text{if } S_i^t > 0.95, I_i^t < 0.2 \\ 0.2 \cdot 10^{-3} \cdot (I_i^t)^{0.445}, & \text{if } S_i^t > 0.95, 0.2 \leq I_i^t \leq 2.5 \\ 0.2 \cdot 10^{-3} \cdot (1 - S_i^t)^{1.079}, & \text{if } S_i^t \leq 0.95, I_i^t < 0.2 \\ 10^{-3} \cdot (1 - S_i^t)^{1.079} \cdot (I_i^t)^{0.445}, & \text{if } S_i^t \leq 0.95, 0.2 \leq I_i^t \leq 2.5 \end{cases} \quad (\text{IV-7a})$$

V. COMPARISON OF RESULTING DEGRADATION

We further compare the electrochemical degradation costs between the nonlinear method [5] and the ICNNs-based formulation (2b)–(2d) under a random set of 66 SoC values. We normalize the electrochemical degradation costs in a continuous range $[0, 1]$ and present their solutions on the normalized PDE-based degradation surface $\Delta\theta_1^{t+1}$ in Fig. 2. This figure shows that blue square markers by the ICNNs-based approach are closer to the PDE-based degradation surface than the yellow circle markers. As compared, the 84.8% and 19.7% of markers have only with less than 1% error for the ICNNs-based and the nonlinear degradation cost methods, respectively. And the ICNNs-based electrochemical degradation cost method has less than 2% error across the domain, and is thus accurate for the optimal V2G model.

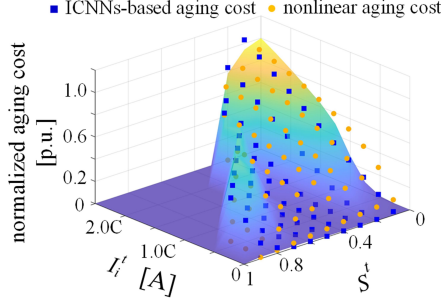


Fig. 2. Comparison between nonlinear and ICNNs-based degradation costs.

TABLE I
PARAMETERS FOR ELECTROCHEMICAL KINETICS

Parameter	Negative electrode	Separator	Positive electrode
electrode plate area (m^2)	0.163	0.163	0.163
electrode thickness (m)	$78 \cdot 10^{-6}$	$20 \cdot 10^{-6}$	$45 \cdot 10^{-6}$
Li^+ diffusion coefficient (m^2/s)	$3.9 \cdot 10^{-5}$	-	$1.8 \cdot 10^{-8}$
active electrode volume fraction (%)	0.6	-	0.6
electrolyte phase volume fraction (%)	0.3	-	0.3
max solid phase concentration (mol/m^3)	31507	-	49000
particle radius (m)	$6 \cdot 10^{-6}$	-	$5 \cdot 10^{-6}$
reaction rate efficiency (A/m^2)	$9.77 \cdot 10^{-2}$	-	$1.19 \cdot 10^{-2}$
exchange current density of side reaction (A/m^2)	10	-	10
initial electrolyte concentration (mol/m^3)	$1.25 \cdot 10^4$	$1.25 \cdot 10^4$	$1.25 \cdot 10^4$
Binder volume fraction(%)	0.1	-	0.1
Separator volume fraction(%)	-	0.4	-
Thickness of current collectors (m)	$10 \cdot 10^{-6}$	-	$10 \cdot 10^{-6}$