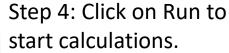


Develop a MATLAB-based software for distillation tower simulation

Hossein Mohammadiarani, Ph.D.

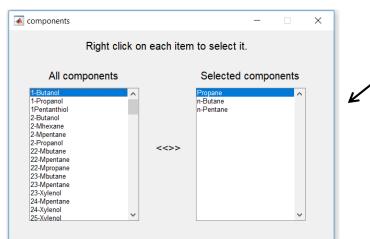
Department of Chemical Engineering
University of New Hampshire, Durham NH
August 2017

Graphical user interface of software

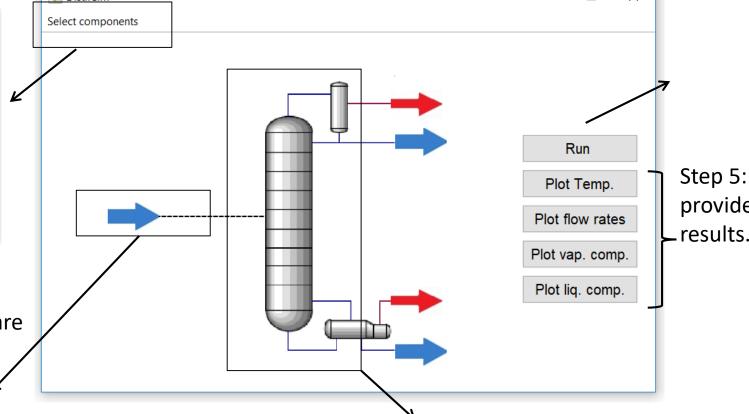


Step 5: These Buttons

provide plots for



Step 1: select components that are used in simulation. In this example Propane, n-Butane, and n-Pentane are selected.

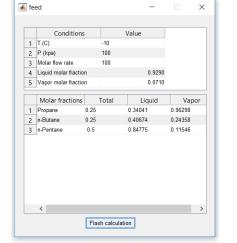


Step 3: Click on column to

Numebr of trays =
Feed tray =
Reflux ratio =
Distillate rate =
Pressure drop (kpa per tray) =

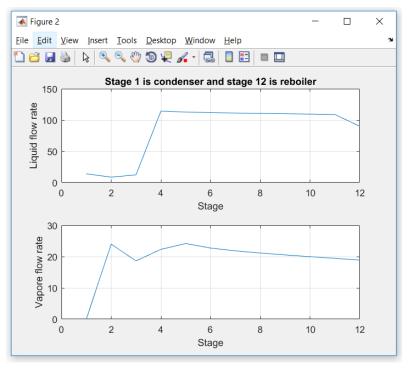
On the top tray is the first.

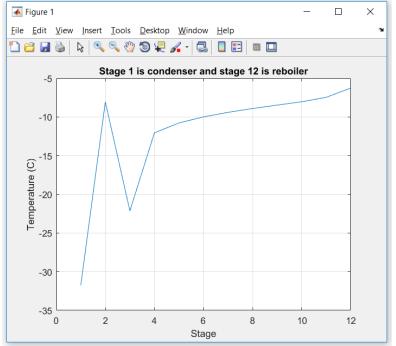
Step 3: Click on column to
enter its specs like number of
tray, reflux ratio.

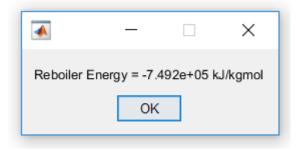


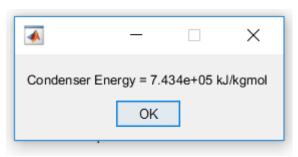
Step 2: Click on feed stream button to open stream window, then enter temperature, pressure, flow rate and the total composition of feed. This window performs flash calculation to compute fraction of vapor and liquid and their compositions.

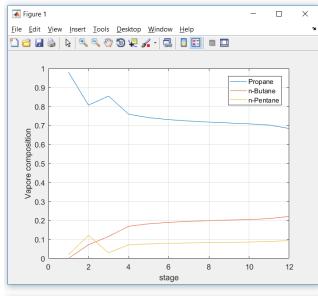
Results: snapshots of temperature, flow rates, compositions, and heat loads.

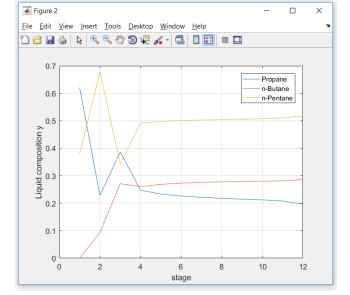












Algorithm

- I coded Wang and Henke algorithm in MATLAB software using GUI toolbox.
- I used PR EOS to compute phase equilibrium ratio and implement bubble point calculation.
- There are 100 components in the software library and include critical properties, Antoine equation coefficients, enthalpy equation coefficients and molecular weights.
 Binary coefficients are supposed zero.

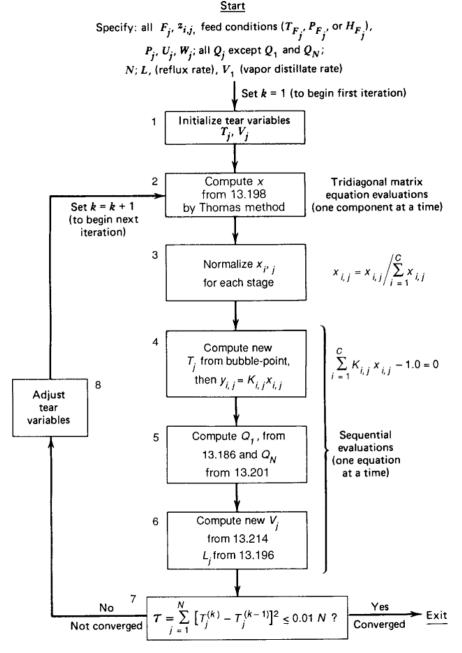


Figure 13.16. Algorithm of the BP (bubble-point) method for distillation separations [Wang and Henke, Hydrocarbon Processing 45(8, 155–166 (1963)); Seader and Henley, 1998].

Movie of a sample simulation of distillation column

