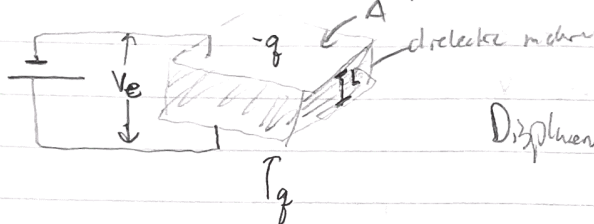


# Thermodynamics in electric & magnetic fields

$$dU = \delta Q - \delta W$$

\* So far we looked at  $\delta W = PdV$ , originates from mechanical work

① dielectric materials, capacitor



$$E = \frac{V_e}{L}$$

$$\text{Displacement field } D = \frac{q}{A}, \quad \vec{\nabla} \cdot \vec{D} = \rho$$

$$\int_{\text{vol}} \vec{\nabla} \cdot \vec{D} d^3r = \oint_{\text{surface}} \vec{D} d^2r = QA \rightarrow \int \rho d^3r = q$$

charge density

• Energy stored in capacitor reduced when means  $W_{\text{cap}} \propto$  done by capacitor

reduce the amount of charge on capacitor

$$W_{\text{cap}} = - \int V_e dq \quad [\text{if } dq < 0, V_e > 0, W_{\text{cap}} > 0]$$

$$\hookrightarrow V_e dq = ELA dD \quad \rightarrow D = \frac{q}{A} \text{ so } dD = \frac{dq}{A}$$

$$V_e dq = V_e E dD \rightarrow W_{\text{cap}} = -V_e \int E dD$$

Use  $D = \epsilon_0 E$ , if no material is present, work still done by changing the field energy (for no material)  $\uparrow$  in the capacitor (vacuum)  $\uparrow$

$$W_{\text{empty cap}} = -V_e \epsilon_0 \int E dE$$

$$\text{do: } W_{\text{sys}} = W_{\text{cap}} - W_{\text{empty cap}} = -V_e \int E dD + V_e \int \epsilon_0 E dE$$

$$W_{\text{sys}} = -V \int E(t) \left( \frac{dD(t)}{dt} - \epsilon_0 \frac{dE(t)}{dt} \right) dt, \quad \vec{D} = \epsilon_0 \vec{E} + \vec{P}$$

Polarization = total dipole moment per volume

$$W_{\text{sys}} = -V_e \int E(t) \frac{dP(t)}{dt} dt, \quad \delta W = -V_e E dP$$

$$\begin{aligned} P &= \gamma E \\ D &= \epsilon_0 E + \gamma E \\ D &= (\epsilon_0 + \gamma) E \\ \epsilon &= \epsilon_0 + \gamma \end{aligned}$$

$$V = \text{const}, P_0/V = 0$$

$$dU = \delta Q - \delta W \Rightarrow dU = \delta Q + E_b dP$$

$$w/ V_n P = P_e$$

$$\hookrightarrow dU = \delta Q + E dP_e$$

1st regime

$$E \leftrightarrow -P$$

$$P_e \leftrightarrow V$$

compare  $\updownarrow$

$$dU = \delta Q - P dV$$

$$dU = T dS + E dP_e$$

2nd Legendre transform

$$dU = T dS + d(E P_e) + P_e dE$$

$$d(U - E P_e) = T dS - P_e dE$$

$$H = H(S, E)$$

$$dH = T dS - P_e dE$$

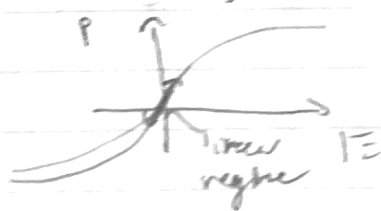
$$dH = d(TS) - S dT - P_e dE \Rightarrow d(H - TS) = -S dT - P_e dE$$

$$G = G(T, E)$$

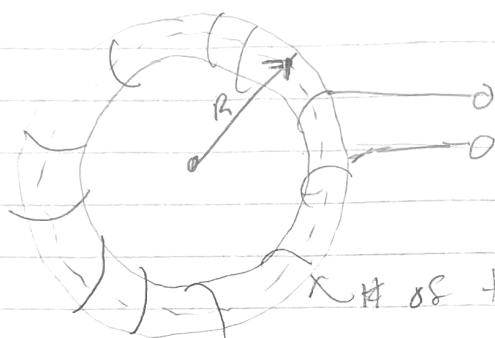
$$dG = -S dT - P_e dE$$

$$S = -\left(\frac{\partial G}{\partial T}\right)_E, \quad P_e = -\left(\frac{\partial G}{\partial E}\right)_T$$

$\uparrow$   
dipole moment  
or polarization



# Magnetic Materials



\$N\$ # of turns of wire

Faradays law:

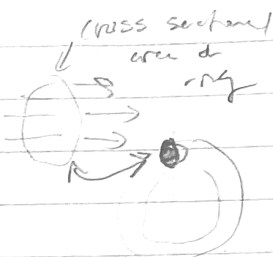
$$\oint \vec{E}(\vec{r}) d\vec{r} = - \frac{d\phi_B}{dt}$$

circle cross section

$$\phi_B = \int \vec{B} d^2\vec{r}$$

$$\phi = A \cdot B$$

area      constant B field



Ampere law:

$$\oint \vec{H} d\vec{r} = I_{tot} \quad \text{where} \quad I_{tot} = NI$$

real circle

Reduction of B field \$\rightarrow\$ work done by Ring \$\rightarrow\$  $V_{ind} = - \frac{d\phi}{dt} = -A \frac{dB}{dt}$

Work done by the ring per the  $\frac{dw_{ring}}{dt} = N V_{ind} I$   $\rightarrow \oint \vec{H} d\vec{r} = 2\pi R H = NI$

$$\frac{dw_{ring}}{dt} = -A 2\pi R \frac{dB}{dt} H = - \underset{\substack{\uparrow \\ \text{volume}}}{V_{ring}} H \frac{dB}{dt}$$

if  $\frac{dB}{dt} < 0$  system does work for us

$$\vec{B} = \mu_0 (\vec{H} + \vec{M})$$

$\vec{M}$  is the magnetization = magnetic dipole moment per volume

no material  $\vec{M} = 0$ ,  $\vec{B} = \mu_0 \vec{H}$ ,  $\frac{dw_{mm}}{dt} = \frac{dw_{ring}}{dt} - (-V_{ring} \mu_0 \frac{dH}{dt})$

$$\frac{dw_{mm}}{dt} = -V_{ring} \mu_0 H \frac{dM}{dt} = -V_{ring} H \left( \frac{dB}{dt} - \mu_0 \frac{dH}{dt} \right)$$

$$dw = -\mu_0 H dM$$

$$d(HM)$$

$$dU = Tds + \mu_0 VM dH$$

$$d(U - \mu_0 VMH) = Tds - \mu_0 VM dH$$

$$H_{\text{ext}} = H_{\text{em}}(S, H)$$

$$d(H_{\text{em}} - TS) = -SdT - \mu_0 VM dH$$

$$G(T, H)$$

$$dG = -SdT - \mu_0 VM dH$$

$$S = -\left(\frac{\partial G}{\partial T}\right)_H \quad \text{and} \quad M = -\frac{1}{\mu_0 V} \left(\frac{\partial G}{\partial H}\right)_T$$

# Basic Concepts of Thermochemistry

• Use minimal gibbs free energy for chemical processes at constant  $T, p$  to derive mass action

$G = \mu N$  and  $dG = -SdT + Vdp + \mu dN$

We want to go from multicomponent systems to single component

*(We need to generalize to single component systems)*

# We also only do single phase systems for simplicity

↳ Specifically looking at reactions



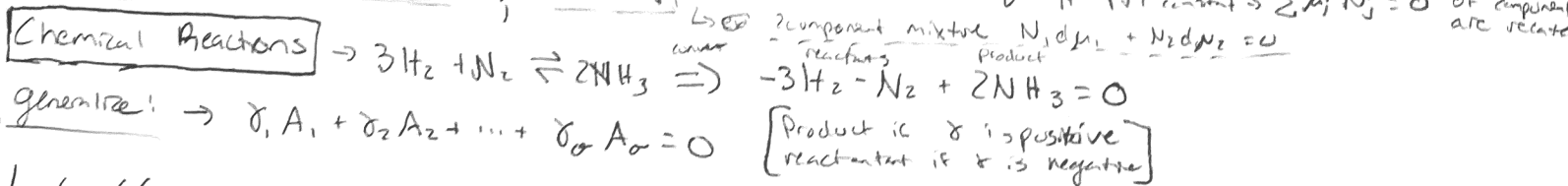
Gibbs of a multicomponent system

$G = G(N_1, \dots, N_j, T, p)$  *(w/  $N_j$  among)*

$G = \sum_i \left( \frac{\partial G}{\partial N_i} \right) N_i = \sum_i \mu_i N_i$  *(what you'd expect as a generalization of  $G = \mu N$ )*  
 $dG = \sum_i \mu_i dN_i$

$dG = -SdT + Vdp + \sum_i \mu_i dN_i$  *(we can make a relation)*  
 $dG - dG = -SdT + Vdp + \sum_i \mu_i dN_i - \sum_i \mu_i dN_i$

$0 = -SdT + Vdp - \sum_i d\mu_i N_i$  *Gibbs-Duhem eq*



$G = G(N_1, \dots, N_j, T, p) \rightarrow \min dG = 0$  w/  $T, p$  constant,  $\sum_i \mu_i dN_i = 0$  (in equilibrium)

$dN_i$  is a single particle element  $= \delta_i \rightarrow \sum_i \mu_i \delta_i = 0$

**Chemical Potentials for an ideal gas**  $\rightarrow G = \mu N \rightarrow \left( \frac{\partial G}{\partial p} \right)_T = N \left( \frac{\partial \mu}{\partial p} \right)_T \rightarrow \frac{V}{N} = \left( \frac{\partial \mu}{\partial p} \right)_T = \frac{k_B T}{p}$   
 $\mu = k_B T \ln \frac{p}{p_r} + k_B T \phi(T)$

For each reactant & product:

$\sum_i \mu_i \delta_i = 0$ , where  $\mu_i = k_B T \ln \left( \frac{p_i}{p_r} \right) + k_B T \phi_i(T)$ ,  $[A_i]$  is the concentration of component  $i$

$\rightarrow k_B T \sum_i \delta_i \left( \ln p \frac{[A_i]}{p_r} + \phi_i(T) \right) = 0$

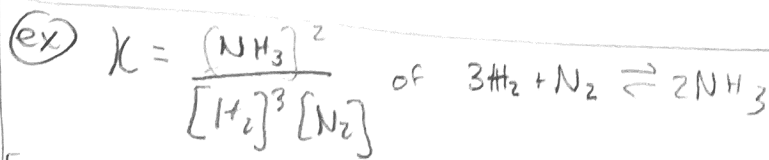
$\rightarrow \sum_i \delta_i \left[ \ln \frac{p}{p_r} + \ln [A_i] + \phi_i(T) \right] = 0$

$\rightarrow \sum_i \ln [A_i]^{\delta_i} = - \sum_i \delta_i \left[ \ln \left( \frac{p}{p_r} + \phi_i(T) \right) \right]$

$\rightarrow \sum_i \ln [A_i]^{\delta_i} = - \sum_i \delta_i \left[ \ln \left( \frac{p}{p_r} + \phi_i(T) \right) \right]$

$e^{\ln(x) + \ln(y)} = x \cdot y$

$\prod_i [A_i]^{\delta_i} = K(p, T)$  *law of mass action*



if  $K$  is big:  $[A_i]$  large w/  $\delta_i > 0$ ; product concentration large  
 if  $K$  is big:  $[A_i]$  small w/  $\delta_i < 0$ ; reactant conc low  
 if  $K$  is small:  $[A_i]$  small w/  $\delta_i > 0$ ; product conc low  
 if  $K$  is small:  $[A_i]$  big w/  $\delta_i < 0$ ; reactant conc large

$K = \frac{\text{product}}{\text{reactant}}$

$K$  is a function of  $P$ , thus we can use it to change the amount of product

$$K = e^{-\sum_j \nu_j \left( \ln \frac{P}{P_r} + \phi_j(T) \right)} = e^{-\ln \left( \frac{P}{P_r} \sum_j \nu_j - \sum_j \nu_j \phi_j(T) \right)} = \left( \frac{P}{P_r} \right)^{-\sum_j \nu_j} e^{-\sum_j \nu_j \phi_j(T)} = K$$

if  $\sum \nu_j > 0$   $\uparrow P$  <sup>in denominator now</sup> decreases  $K$ , equilibrium shifts towards reactants  
 if  $\sum \nu_j < 0$   $\uparrow P$  <sup>in numerator now</sup> increases  $K$ , equilibrium shifts towards products

$K$  is a function of  $T$ , thus we can use it to change the amount of product

$$\ln(K) = \ln \left( \frac{P}{P_r} \right)^{-\sum_j \nu_j} - \sum_j \nu_j \phi_j(T) \rightarrow \left( \frac{\partial \ln(K)}{\partial T} \right)_P = - \sum_j \nu_j \frac{d\phi_j}{dT}$$

Go back to:

$$\mu_j = k_B T \ln \left( \frac{P_j}{P_r} \right) + k_B T \phi_j(T) \rightarrow \left( \frac{\partial \mu_j}{\partial T} \right)_P = k_B \ln \left( \frac{P_j}{P_r} \right) + k_B \phi_j(T) + k_B T \frac{d\phi_j}{dT} = \mu_j + k_B T \frac{d\phi_j}{dT}$$

Now look at Gibbs:

$$G = H - TS \rightarrow \mu_j = h_j - TS_j \quad \text{and} \quad dG = -SdT + VdP + \sum \mu_j dN_j, \quad \left( \frac{\partial \mu_j}{\partial T} \right)_P = -S_j$$

$$\hookrightarrow \mu_j = h_j + T \left( \frac{\partial \mu_j}{\partial T} \right)_P \rightarrow \text{combine} \quad \boxed{h_j = -k_B T^2 \frac{d\phi_j}{dT}}$$

$$\text{Now look at } \left( \frac{\partial \ln K}{\partial T} \right)_P = - \sum_j \nu_j \frac{d\phi_j}{dT} \rightarrow \left( \frac{\partial \ln K}{\partial T} \right)_P = \frac{\sum_j \nu_j h_j}{k_B T^2} = \Delta h = \frac{\Delta h}{k_B T^2}$$

(we can integrate)

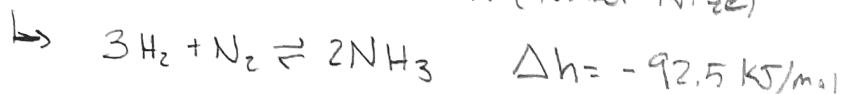
$$\ln \frac{K(T_2)}{K(T_1)} = \int_{T_1}^{T_2} \frac{\Delta h}{k_B T^2} dT \Rightarrow K(T_2) = K(T_1) e^{-\frac{\Delta h}{k_B} \left( \frac{1}{T_2} - \frac{1}{T_1} \right)}$$

if  $\Delta h < 0$ : heat leaves the system, reaction is exothermic,  $K$  decreases w/ increasing  $T$ , yield goes down

if  $\Delta h > 0$ : the reaction is endothermic,  $K$  increases w/ increasing  $T$ , yield goes up

# Haber Bosch Process

industrial route to ammonia (Nobel Prize)



even though its a good idea to increase T in a reaction (from intuition of molecules) you better not over do it. We know this from our law of mass action.

Since  $\Delta h < 0$ , reaction is exothermic, K decreases w/ increasing T, yield goes down

$$(K(T_2) = K(T_1) e^{\frac{-\Delta h}{R} (\frac{1}{T_2} - \frac{1}{T_1})})$$

Can't go further w/ Temperature, but we can use pressure:  $-3H_2 - N_2 + 2NH_3 = 0$   
 $\delta(NH_3) = 2, \delta(H_2) = -3, \delta(N_2) = -1$

$$K = \left(\frac{P}{P_r}\right)^{-\sum \delta_i} e^{-\sum \delta_i \phi_i(T)}$$

$$\rightarrow K = \left(\frac{P}{P_r}\right)^2 \cdot \text{constant}$$

sum it up,  $-3-1+2 = -2 < 0$

increase pressure to get more yield.

you can also remove ammonia so more stuff reacts to try to get it to equilibrium.  
 $K = \frac{[NH_3]^2}{[H_2]^3 [N_2]}$  ← removing  $[NH_3]$ , increases yield

## 3<sup>rd</sup> Law of Thermodynamics

Nernst Heat Theorem: In the neighborhood of abs 0, all reactions in a liquid or solid in internal equilibrium take place w/ no change in entropy

$$\rightarrow \lim_{T \rightarrow 0} (S_1 - S_2) = 0$$

We know at  $P, T = \text{constant}$  equilibrium is determined by  $G \Rightarrow \min$ ,  $\Delta G = G_2 - G_1$

$$G = H - TS \quad \text{and} \quad dG = -SdT + VdP$$

$$G = H + T \left(\frac{\partial G}{\partial T}\right)_P \rightarrow \Delta G = \Delta H + T \left(\frac{\partial \Delta G}{\partial T}\right)_P$$

$$\text{as } T \rightarrow 0, \Delta G \rightarrow \Delta H, \left(\frac{\partial \Delta G}{\partial T}\right)_P \rightarrow 0$$

$$\text{From } \lim_{T \rightarrow 0} \left(\frac{\partial \Delta G}{\partial T}\right)_P = 0 \rightarrow \lim_{T \rightarrow 0} (S_1 - S_2) = 0$$

Planck's  
 Further  
 generalization  
 of 3<sup>rd</sup> Law

### 3rd Law

[Entropy of every solid or liquid substance in internal equilibrium at absolute 0 is itself 0]

$$\lim_{T \rightarrow 0} S = 0$$

$$ds = \frac{\delta Q}{T} \rightarrow dS(V=\text{const}) = \int_0^T C_V \frac{dT}{T}, \quad dS(P=\text{const}) = \int_0^T C_P \frac{dT}{T}$$

↳ you can't have sol'n at  $T=0$  thus  $C_V$  and  $C_P \rightarrow 0$  at  $T=0$ .

$$\lim_{T \rightarrow 0} C_V = \lim_{T \rightarrow 0} C_P = 0 \quad \text{* requires QM to derive in terms of statistical mechanics}$$

↳ Nernst:  $\lim_{T \rightarrow 0} (S_1 - S_2) = 0 \rightarrow \lim_{T \rightarrow 0} \left( \frac{\partial S}{\partial P} \right)_T = \lim_{T \rightarrow 0} \left( \frac{\partial S}{\partial V} \right)_T = 0$

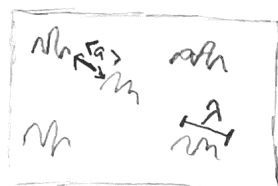
Use Maxwell relation  $\rightarrow \left( \frac{\partial S}{\partial P} \right)_T = - \left( \frac{\partial V}{\partial T} \right)_P \rightarrow \lim_{T \rightarrow 0} \left( \frac{\partial V}{\partial T} \right)_P = 0$ ,  $\alpha_V = \lim_{T \rightarrow 0} \frac{1}{V} \left( \frac{\partial V}{\partial T} \right)_P = 0$



# Kinetic Theory

consider a dilute gas of  $N$  atoms in a box

$$E_k = \frac{p^2}{2m}$$

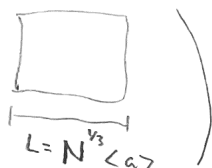


Classical limit  $\rightarrow \lambda \ll \langle a \rangle$

$$p = \frac{h}{\lambda} \rightarrow \lambda = \frac{h}{p} = \frac{h}{\sqrt{2m E_{kinetic}}} \approx \frac{h}{\sqrt{2m k_B T}}$$

derived on bulk

$$\hookrightarrow \frac{h}{\sqrt{2m k_B T}} \ll \left( \frac{L}{N^{1/3}} = \langle a \rangle \right) \rightarrow$$

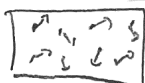


and w/ density  $n = \frac{N}{L^3}$

$$\left[ \frac{h n^{1/3}}{\sqrt{2m k_B T}} \ll 1 \quad \text{classical limit} \right]$$

Assumes on average every spread out system, think of a letter  $N^{1/3}$  we are on one side thus their average distance is  $L$

Identical gas



Momentum change when hitting the wall!

$$\Delta \vec{p} = \int_t^{t+\Delta t} \frac{d\vec{p}}{dt'} dt' = \int_t^{t+\Delta t} \vec{F}(t') dt'$$

divide each side by  $\Delta t$

$$\vec{F}_{x, atom}^{av} = \frac{1}{\Delta t} \int_t^{t+\Delta t} F_x(t') dt'$$

$$p_i = m v_x$$

$$p_f = m v_x(t + \Delta t)$$

(X-component of the momentum change)

$$\Delta p_x =$$

$$m v_x(t + \Delta t) - m v_x(t) = -2 m v_x(t) = F_{x, atom}^{av} \Delta t$$

all that happens before and after is change of sign but magnitude stays the same

what's  $\Delta t$ ?

(e)

hits wall hits opposite wall & comes back & hits wall, the time it takes to do that is the time we average over

We can't choose when the force is turned off & when it's on, so we choose  $\Delta t$  to be time between 2 successive collisions

$$F_{x, wall}^{av} \Delta t = 2 m v_x(t) \quad , \quad w/ \quad \Delta t = \frac{2 L_x}{v_x}$$

twice the time it takes for it to reach the wall at speed  $v_x$

$$\hookrightarrow F_{x, wall}^{av} = \frac{m v_x^2}{L_x}$$

total force on back

$$F_{x, \text{wall}}^* = \frac{m v_x^2}{L_x}$$

[Total Force by N particles]  $\rightarrow F_x^{\text{tot}} = \sum_{i=1}^N \frac{m_i v_{x,i}^2}{L_x}$  and  $A = L_y L_z$   $P = \frac{F}{A}$  so;

$$P = \frac{F_x^{\text{tot}}}{L_y L_z} = \frac{1}{L_y L_z L_x} \sum_{i=1}^N m_i v_{x,i}^2 = \frac{1}{V} \sum_{i=1}^N m_i v_{x,i}^2 \quad \text{now do for each direction}$$

$$3P = \frac{1}{V} \sum_{i=1}^N m_i (v_{x,i}^2 + v_{y,i}^2 + v_{z,i}^2) \Rightarrow \boxed{P = \frac{1}{3V} \sum_{i=1}^N m_i v_i^2}$$

To further simplify look at the time average:

$$\frac{K^{\text{tot}}}{N} = K^{\text{av}} \rightarrow \frac{\frac{1}{2} \sum_{i=1}^N m_i v_i^2}{N} = \frac{1}{2} \overline{m_i v_i^2} \xrightarrow{\text{average}} \text{for all } m_i \text{ the same} \rightarrow \frac{1}{2} \overline{m v^2} = \frac{1}{2} m \overline{v^2}$$

(adding up + dividing by how many there are)

$$\hookrightarrow PV = N \frac{2}{3} \left( \frac{1}{2} m \overline{v^2} \right)$$

$$\frac{1}{2} m \overline{v^2} = \frac{3}{2} k_B T$$

[compare w/ ideal gas eqn]  $\rightarrow PV = N k_B T$

$$* V_{\text{rms}} = \sqrt{\overline{v^2}} = \sqrt{\frac{3 k_B T}{m}}$$

Calculating the statistical average of  $\overline{v^2}$ :

To do so we use a distribution function.

Specifically, we use one of the form  $f(\vec{r}, \vec{p}, t) d^3 \vec{r} d^3 \vec{p} \propto$  [ # of molecules at a given time  $t$  within a volume element  $d^3 r$  located at  $r$  and momentum element  $d^3 p$  around  $\vec{p} = m \vec{v}$  ]

To do an average:


$$\overline{v^2} = \frac{\int v^2 f(\vec{r}, \vec{p}, t) d^3 \vec{r} d^3 \vec{p}}{\int f(\vec{r}, \vec{p}, t) d^3 \vec{r} d^3 \vec{p}} \quad \xrightarrow{\text{integrate over } \vec{r}} \quad \frac{1}{T} \int_0^T f(t) dt$$

Next trick  $\rightarrow$  if  $f(\vec{r}, \vec{p}, t) = f(\vec{r}, \vec{p}) = f_1(\vec{p}) f_2(\vec{r})$  then

$$\overline{v^2} = \frac{\int v^2 f_1(\vec{p}) d^3 \vec{p}}{\int f_1(\vec{p}) d^3 \vec{p}} \cdot \frac{\int f_2(\vec{r}) d^3 \vec{r}}{\int f_2(\vec{r}) d^3 \vec{r}} = \frac{\int v^2 f_1(\vec{p}) d^3 \vec{p}}{\int f_1(\vec{p}) d^3 \vec{p}}$$

this will be important once we show that we can separate it like this.

How do we get  $f$ ?  $\rightarrow$  Turns out to be the Maxwell-Boltzmann dist.  
 To get a feel for it recall the following example.



$$P(h) = P(h+\Delta h) + \frac{Mg}{A} = P(h+\Delta h) + \frac{P(h) A \Delta h g}{A} = P(h+\Delta h) + P(h) \Delta h g$$

$[Air is \text{ ideal gas}] \rightarrow PV = nRT \rightarrow P \frac{V}{M} = \frac{n}{M} RT \rightarrow P = \frac{M}{n} \frac{P}{RT}$

$$\hookrightarrow \frac{P(h+\Delta h) - P(h)}{\Delta h} = -\frac{M}{n} \frac{g P(h)}{RT(h)} \rightarrow \frac{dP}{dh} = -\frac{M}{n} \frac{g P(h)}{RT(h)}$$

In case  $T = \text{const.}$  ( $M = n N_A m$  and  $R = N_A k_B$ )

$$\frac{dP}{dh} = -\frac{mg}{k_B T} P(h) \rightarrow \int_{P_0}^P \frac{dP}{P} = -\frac{mg}{k_B T} \int_0^h dh' \rightarrow$$

$$P(h) = P_0 e^{-\frac{mgh}{k_B T}}$$

$$p(h) = p_0 e^{-\frac{mgh}{k_B T}}$$

$p(\vec{r}) d^3\vec{r} = \# \text{ of particles in } d^3\vec{r} \propto \text{probability of finding a particle in } d^3\vec{r}$

$$\int f(\vec{r}, \vec{p}) d^3\vec{p} = p(\vec{r}) = p(x) = p_0 e^{-\frac{mgh}{k_B T}} = p_0 e^{-\frac{E_{pot}(x)}{k_B T}}$$

$[Assume \vec{r}, \vec{p} \text{ contribute to the energy}] \rightarrow f(\vec{r}, \vec{p}) = f(E = \frac{p^2}{2m} + E_{pot}(\vec{r})) \rightarrow \int d^3\vec{p} f(E) = p_0 e^{-\frac{E_{pot}}{k_B T}}$

$$[Take \text{ derivative of } dE_{pot} \text{ of both sides}] \frac{d}{dE_{pot}} \left( \int f(E) d^3\vec{p} \right) = \frac{d}{dE_{pot}} (p(\vec{r})) = \int d^3\vec{p} \frac{df(E)}{dE} \frac{dE}{dE_{pot}} = -\frac{1}{k_B T} p_0 e^{-\frac{E_{pot}}{k_B T}}$$

$$\hookrightarrow \int d^3\vec{p} \frac{df(E)}{dE} = -\frac{1}{k_B T} \int d^3\vec{p} f(E)$$

$$\hookrightarrow \int d^3\vec{p} \left( \frac{df(E)}{dE} + \frac{1}{k_B T} f(E) \right) = 0 \rightarrow \frac{df(E)}{dE} + \frac{1}{k_B T} f(E) = 0 \rightarrow \int \frac{1}{f} df \propto -\frac{E}{k_B T}$$

$$\hookrightarrow f \propto e^{-E/k_B T} \propto e^{-\frac{1}{k_B T} \left( \frac{p^2}{2m} + E_{pot}(\vec{r}) \right)} = e^{-\frac{1}{k_B T} \left( \frac{p^2}{2m} \right)} e^{-\frac{1}{k_B T} E_{pot}(\vec{r})} = f_1(\vec{p}^2) f_2(\vec{r})$$

$$\hookrightarrow N = \int_{-\infty}^{\infty} d^3\vec{p} e^{-\frac{1}{k_B T} \frac{p^2}{2m}}$$