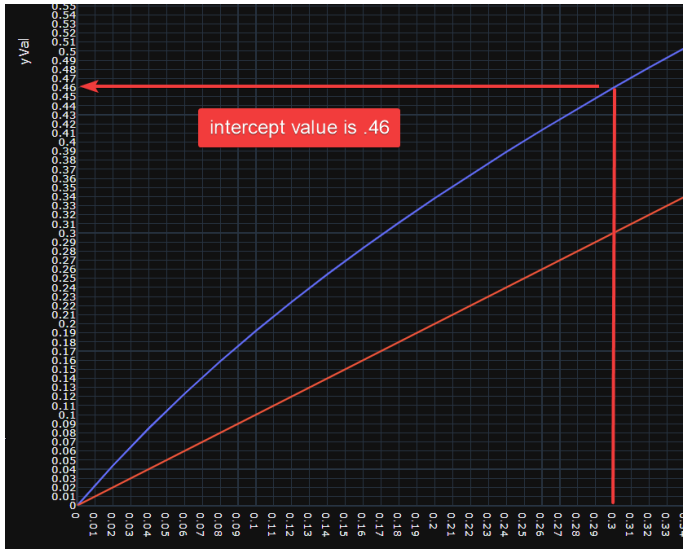
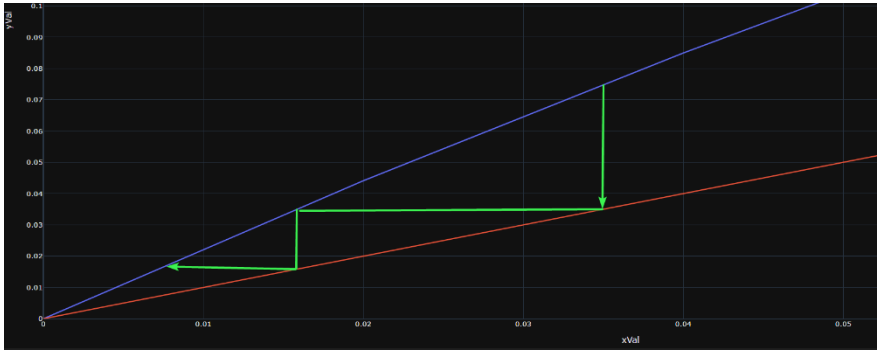
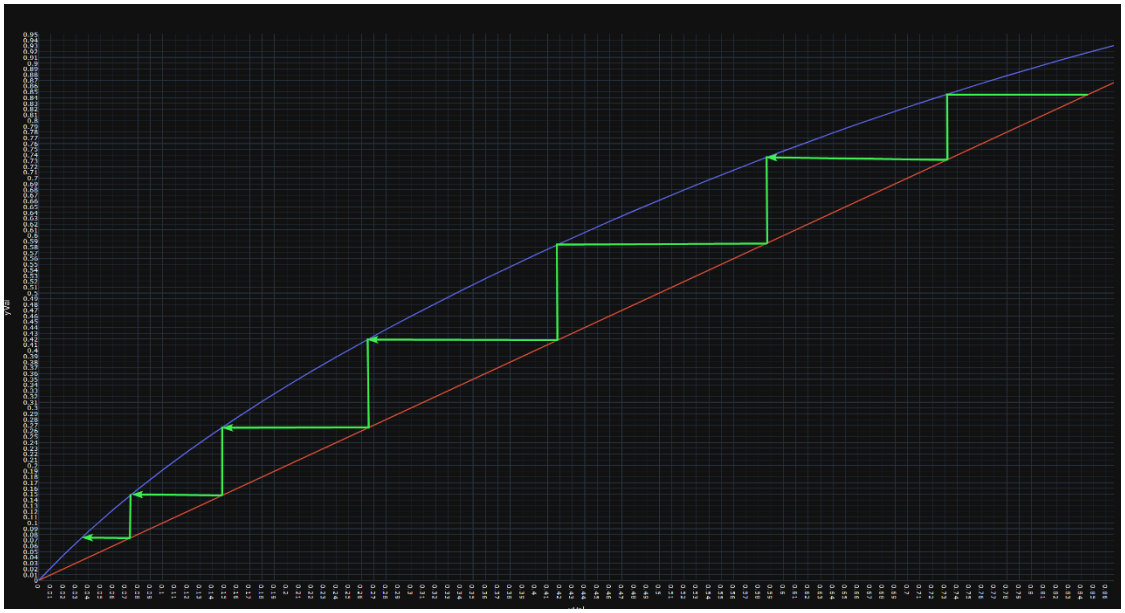
File: https://github.com/hunterviolette/CHE362/blob/master/scripts/hw10.py
Methods: https://github.com/hunterviolette/CHE362/blob/master/scripts/baseFunctions.py

PROBLEM 1 A - 13 TRAYS
PROBLEM 1 B – 13/.75 = 17.3 ~= 18







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```
Flow rates: {B: 352040.816326531*mole/hour, D: 147959.183673469*mole/hour}
Rmin: 3.31250000000000, R: 3.97500000000000
```

```
==== Part C ====
dT Ln, condenser: 131.11700047464612 Δ°F
dT, reboiler: 50 Δ°F
Heat duty, condenser: 24.192792 GJ/h
Heat duty, reboiler: 24.192792 GJ/h
Heat transfer coefficient, condenser: 150 Btu/ft²/h/Δ°F
Heat transfer coefficient, reboilder: 200 Btu/ft²/h/Δ°F
Heat transfer area, condenser: 108.31538326646417 m²
Heat transfer area, reboiler: 213.02982238740688 m²
```

```
==== Part D ====
F_LV: 0.050118242518390 97
kV: 0.38524612240309186 ft/s
uC: 6.01371979633009 ft/s
uO: 4.510289847247567 ft/s
V: 736096.0249999999 mol/h
Vdot: 217.62596106998467 ft³/s
area: 48.25099238417954 ft²
actual area: 60.313740480224425 ft²
diameter: 8.763209427505183 ft
```