Cascade system using both trough system and dish system for power generation

Nomenclature

 $A_{dishCollector}$ Aperture area of each dish collector, m²

 $A_{stirling,1}$ Heat transfer area of Stirling engine at air side, m²

 $A_{stirling,2}$ Heat transfer area of Stirling engine at water side, m²

 $A_{troughCollector}$ Aperture area of each trough collector, \mathbf{m}^2

 I_{DNI} Direct Normal Irradiance, W/m²

 $k_{stirling}$ Specific heat ratio of the working gas in Stirling engine

n Amount of working gas in each Stirling engine, mol

 n_{se} Speed of Stirling engine, s⁻¹

 $n_{stirlingEngine}$ Number of Stirling engines in the Stirling engine array

 p_c Exhaust pressure of turbine, Pa

 p_s Main steam pressure of turbine, Pa

 p_{amb} Ambient pressure, Pa

 p_{cp} Water pressure after condensate pump, Pa

 $p_{deaerator}$ Outlet pressure of deaerator, Pa

 p_{dish} Air pressure in dish, Pa

 $P_{generator}$ Power of generator, W

 p_{trough} Air pressure in trough, Pa

 $q_{cond,tot}$ Total conduction loss

 $q_{conv,tot}$ Total convection loss

 $q_{dish,air}$ Energy absorbed by air in the dish collector

 q_{in} Solar energy launched into dish receiver aperture, W

 $q_{rad,emit}$ Radiation emitted by dish receiver

 $q_{rad,reflect}$ Reflected radiation

 T_s Main steam temperature of turbine

 $T_{1,after stirling}$ Air temperature after heating Stirling engine

 T_{amb} Ambient temperature, K

 $T_{dish,inlet}$ Dish inlet temperature, K

 $T_{dish,outlet}$ Dish outlet temperature

 $T_{s,d}$ Designed mean steam temperature of turbine

 $T_{trough,outlet}$ Trough outlet temperature

 $U_{stirling,1}$ Overall heat transfer coefficient of Stirling engine at air side,

 $W/(m^2 \cdot K)$

 $U_{stirling,2}$ Overall heat transfer coefficient of Stirling engine at water side,

 $W/(m^2 \cdot K)$

 v_{wind} Ambient wind speed, m/s

x Dryness fraction

Abbreviations

EES Engineering Equation Solver

SAM System Advisor Model

SES Stirling Energy System

Greek Symbols

 α_{eff} Effective absorptance

 $\Delta T_{oil,water,min}$ Minimum temperature difference between oil and water in the

oil-to-water heat exchanger, K

 $\gamma_{stirling}$ Compression ratio of Stirling engine

1 Introduction

- Background Information
 - 1. Why do we need cascade system
 - 2. What is the advantage of cascade system
 - 3. What are others' works
 - 4. What have been done
 - 5. What to be done
 - 6. What can we improve
 - 7. What have we done
- System specification
 - 1. Environment
 - 2. Trough collector
 - 3. Dish collector
 - 4. Steam turbine
 - 5. Stirling engine
 - 1. Air circuit
 - 2. Water circuit
 - 3. Oil circuit
 - 4. System efficiency
- Separate system
- Results

Different types of collectors and different technologies for electricity generation are suitable for different working temperature zones with different costs. An idea of cascade collection and cascade utilisation of solar energy with higher efficiency is presented. Parabolic trough collectors are used to collect lower temperature energy with lower cost and dish collectors are used to collect higher temperature energy with higher efficiency. Rankine cycle is used to work in lower temperature zone and Stirling cycle is used to work in higher temperature zone. Furthermore, effective topological structures are considered to take full advantages of thermodynamic characters of different components of the system. The cold chamber of Stirling engine is cooled by condensed fluid of Rankine cycle to use the heat released by Stirling engine.

2 System description

An EES model was used to study the characteristics of the cascade system. Figure 1 shows the sketch of the cascade system. Dish collectors are used to provide heat for Stirling engines and air-to-water heat exchanger. Trough collectors are used to provide heat for preheating, evaporating and superheating in the Rankine cycle. Water is used as the working fluid of Rankine cycle, which is heated in the cold chamber of Stirling engines, preheater, evaporator, superheater, and air-to-water heat exchanger successively, and then expand in turbine, condense in condenser. Pumps are used to change the pressure of fluids. Stirling engines are used for power generation and cooled by feed water of the Rankine cycle. State number pairs of different fluids are marked on the sketch. The first number of a number pair indicates the fluid type, the second number of a number pair indicates the state point of the fluid. Number pairs with solid circle indicate saturated liquid states (x=0), and with dotted circle indicates saturated gas states (x=1).

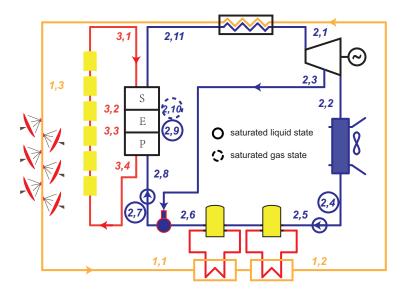


Figure 1: Sketch of the cascade system

To build the cascade system model, several simplifying assumptions are made:

- Steady state at nominal load of the system is analyzed
- Pressure drop due to flow is negligible everywhere
- Same isentropic efficiency of steam turbine with different loads and in different stages

- There is no heat loss to the environment for Stirling engines
- Simple models are used of some processes and equipments
- A symmetrical regenerator behaviour is assumed so that a single effectiveness can be defined as $e=\frac{T_R-T_L}{T_H-T_L}[1,\,2]$
- There is no heat loss to the environment for Stirling engines

3 System specification

Table 1 shows the basic design parameters of the cascade system.

Table 1: Parameters of the cascade system

	Nominal ele	ectric power	
$P_{generator}$	$6\times10^6~\mathrm{W}$		
	Enviro	onment	
I_{DNI}	$700 \mathrm{W/m^2}$	T_{amb}	293 K
p_{amb}	$1 \times 10^{5} \text{ Pa}$	v_{wind}	$4 \mathrm{m/s}$
	Dish co	ollector	
$T_{dish,inlet}$	623K	$T_{dish,outlet}$	1073 K
p_{dish}	$5 \times 10^5 \text{ Pa}$	$A_{dishCollector}$	87.7 m^2
	Trough	collector	
$\Delta T_{oil,water,min}$	15 K	$T_{trough,outlet}$	623 K
p_{trough}	2×10^6 Pa	$A_{troughCollector}$	545 m^2
	Stirling	gengine	
$T_{1,afterstirling}$	673 K	n_{se}	$10 \; {\rm s}^{-1}$
$U_{stirling,1}$	$30 \text{ W/(m}^2 \cdot \text{K})$	$U_{stirling,2}$	$150 \text{ W/(m}^2 \cdot \text{K})$
$A_{stirling,1}$	8 m^2	$A_{stirling,2}$	$8 \mathrm{\ m}^2$
$k_{stirling}$	1.4	$\gamma_{stirling}$	3.375
n	$7.73 \times 10^{-2} \text{ mol}$	$n_{stirlingEngine}$	100
	Steam	turbine	
T_s	340°C	p_s	$2.35 \times 10^6 \text{ Pa}$
p_c	$1.5 \times 10^4 \text{ Pa}$	$T_{s,d}$	$390^{\circ}\mathrm{C}$
$p_{c,p}$	1×10^6 Pa		
	Deae	rator	
$p_{deaerator}$	1×10^6 Pa		

4 System model

The system is built in several blocks. These blocks are made of circuits and efficiency calculations. Two circuits, air circuit and water circuit, are built in some specific states and in some components. Known parameters of the states, we can get the efficiency of the system and the overall efficiency of separated systems.

4.1 Air circuit

In air circuit, efficiency of dish collectors needs to be calculated. Fraser, in his dissertation[3], built a performance prediction model of Stirling dish system, which has detailed description of the dish collector model. The model is also used in the software SAM, which provides performance and financial models for facilitate decision in the renewable energy industry.

In our cascade system, the structure of the dish receiver is as shown in Figure 2. The dish receiver model concerns the losses includes: collector losses due to mirror reflectivity, receiver intercept losses, losses due to shading, and thermal losses. Thermal losses take the largest portion of all those losses, which are due to conduction, convection and radiation. Figure 3 shows the heat network of dish receiver, which concerns the losses:

- Radiation losses reflected off of the receiver cavity surfaces and out of the receiver through the aperture. $(q_{rad,reflect})$
- Conductive losses through the receiver insulating layer. $(q_{cond,tot})$
- Free convection from the cavity in the absence of wind. $(q_{conv,free})$
- Forced convection in the presence of wind. $(q_{conv.forced})$
- Emission losses due to thermal radiation emitted from the receiver aperture. $(q_{rad,emit})$

4.1.1 Reflected loss of dish receiver

To determine the reflected loss of the cavity surfaces of the dish receiver, the effective absorptance of the cavity receiver α_{eff} is required to determine the fraction of energy reflected out of the receiver. The effective absorptance of a cavity receiver without a receiver aperture cover is given by Equation (1) where α_{cav} is the cavity surface absorptance, A_a is the cavity aperture area, and A_{cav} is the total inner surface area of the cavity [?].

$$\alpha_{eff} = \frac{\alpha_{cav}}{\alpha_{cav} + (1 - \alpha_{cav}) \left(A_{ap} / A_{cav} \right)} \tag{1}$$

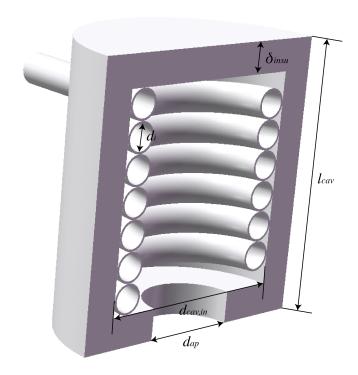


Figure 2: Structure of the dish receiver

4.1.2 Conduction loss of dish receiver

4.1.3 Convection loss of dish receiver

Ma conducted tests to determine the free convection losses from the receiver for six alternative setups, and the data were consistent with Stine and Mc-Donald's free convection correlation[4]. It is assumed that forced convection is independent of free convection in the receiver, so the total convection losses can be represented as the sum of the free and forced convection losses as shown in Figure 3.

$$q_{con,tot} = q_{con,free} + q_{con,forced} \tag{2}$$

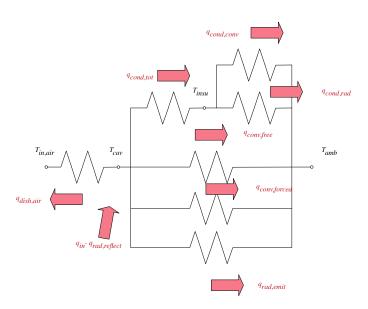


Figure 3: Heat network of dish receiver

$$q_{in} = q_{rad,reflect} + q_{dish,air} + (q_{cond,tot} + q_{conv,tot} + q_{rad,emit})$$
 (3)

A dish collector product of SES used in Fraser's paper, which is also used in this system, and its parameters are listed in Table 2.[3]

 q_{in} can be obtained by

$$q_{in} = DNI \cdot A_{dishCollector} \gamma \eta_{shading} \rho \tag{4}$$

Table 2: Parameters of the dish receiver

Parameters	Value	
d_{cav}	$0.46 \mathrm{\ m}$	
δ_{insu}	$0.075~\mathrm{m}$	
l_{cav}	$0.23 \mathrm{\ m}$	
d_{cav}	$0.184 \mathrm{\ m}$	
λ_{insu}	$0.06 \mathrm{W/(m \cdot K)}$	
ϵ_{insu}	0.6	
α_{cav}	0.87	
δ_a	$0.005 \mathrm{m}$	
$d_{i,air}$	$0.07 \mathrm{\ m}$	
$ heta_{dish}$	45°	
γ	0.97	
$\eta_{shading}$	0.95	
ρ	0.91	

- 4.2 Stirling engine array
- 4.3 Water circuit
- 4.3.1 Oil-Water heat exchangers
- 4.3.2 Steam turbine
- 4.3.3 Condensor
- 4.3.4 deaerator
- 5 Separate system model
- 6 Result and Conclusion

References

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