

## References

- Adorni, N., Peterlongo, G., Ravetta, R. and Tacconi, F. A., 1964, Large Scale Experiments on Heat Transfer and Hydrodynamics with Steam-water Mixtures, *CISE Report R-91*, Italy.
- Akiyama, M. and Aritomi, M., 2002, *Advanced Numerical Analysis of Two-phase Flow Dynamics –Multi-dimensional Flow Analysis–*, Corona Publishing Co. Ltd., Tokyo, Japan
- Alia, P., Cravarolo, L., Hassid, A. and Pedrocchi, E., 1965, Liquid Volume Fraction in Adiabatic Two-phase Vertical Upflow-round Conduit, *CISE Report-105*, Italy.
- Antal, S. P., Lahey Jr, R. T. and Flaherty, J. E., 1991, Analysis of Phase Distribution in Fully Developed Laminar Bubbly Two-phase Flow, *Int. J. Multiphase Flow* **17**: 635-652.
- Aris, R., 1962, *Vectors, Tensors and the Basic Equations of Fluid Mechanics*, Prentice-Hall, Englewood Cliffs, N.J.
- Arnold, G. S., Drew, D. A. and Lahey Jr., R. T., 1989, Derivation of Constitutive Equations for Interfacial Force and Reynolds Stress for a Suspension of Spheres Using Ensemble Cell Averaging, *Chem. Eng. Comm.* **86**: 43-54.
- Auton, T. R., 1987, The Lift Force on a Spherical Body in a Rotational Flow, *J. Fluid Mech.* **183**: 199-218.
- Azbel, D., 1981, *Two-phase Flows in Chemical Engineering*, Cambridge University Press, Cambridge, UK.
- Azbel, D. and Athanasios, I. L., 1983, A Mechanism of Liquid Entrainment. *Handbook of Fluids in Motion*, Ann Arbor Sci. Pub., Ann Arbor, MI.
- Baker, J. L. L., 1965, Flow-regime Transitions at Elevated Pressure in Vertical Two-phase Flow, *Argonne National Lab. Report*, ANL-7093.
- Bankoff, S. G., 1960, A Variable Density Single-fluid Model for Two-phase Flow with Particular Reference to Steam Water Flow, *J. Heat Transfer* **82**: 265-272.
- Bello, J. K., 1968, *Turbulent Flow in Channel with Parallel Walls*, Moskva, Mir, in Russian.
- Bergonzoli, F. and Halfen, F. J., 1964, Heat Transfer and Void Formation during Forced Circulation Boiling of Organic Coolants, NAA-SR-8906, Atomics International.
- Bilicki, A. and Kestin, J., 1987, Transition Criteria for Two-phase Flow Patterns in Vertical Upward Flow, *Int. J. Multiphase Flow* **13**: 283-294.
- Bird, R. B., Stewart, W. E. and Lightfoot, E. N., 1960, *Transport Phenomena*, John Wiley and Sons, Inc., New York.
- Bornhorst, W. J. and Hatsopoulos, G. N., 1967, Analysis of a Liquid Vapor Phase Change by the Methods of Irreversible Thermodynamics, *J. Applied Mech.* **89**: 847-853.

- Boure, J. and Réocreux, M., 1972, General Equations of Two-phase Flows: Application to Critical Flows and to Non Steady Flows, *4th All Union Heat and Mass Transfer Conference*, Minsk.
- Boure, J., 1973, Dynamique des Écoulements Diphasiques: Propagation des Petites Perturbations, *CEA-R-4456*.
- Bowen, R. M., 1967, Toward a Thermodynamics and Mechanics of Mixtures, *Arch. Rational Mech. Anal.* **24**: 370-403.
- Bridge, A. G., Lapidus, L. and Elgin, J. C., 1964, The Mechanics of Vertical Gas-Liquid Fluidized System I: Counter-current Flow, *AIChE J.* **10**: 819-827.
- Brinkman, H., 1952, The Viscosity of Concentrated Suspensions and Solutions, *J. Chem. Phys.* **20**: 571.
- Brodkey, R. S., 1967, *The Phenomena of Fluid Motion*, Addison-Wesley.
- Brodkey, R. S., 1971, Transport Phenomena at the Liquid-Vapor Interface of Mercury Using a Radioactive Tracer, *International Symposium on Two-phase Systems*, Haifa.
- Burgers, J. M., 1941, On the Influence of the Concentration of a Suspension upon the Sedimentation Velocity (in Particular for a Suspension of Spherical Particles) *Proc. K. Med. Akad. Wet.* **44**: 1045-1051 (1941); **45**: 9-16 (1942)
- Buevich, I., 1969, A Hydrodynamic Model of Disperse Systems, *J. Applied Math. Mech.* **33**: 466-479.
- Buyevich, Y., 1972, Statistical Hydrodynamics of Disperse Systems. Part.I. Physical Background and General Equations, *J. Fluid Mech.* **49**: 489-507.
- Carrier, G. F., 1958, Shock Waves in Dusty Gas, *J. Fluid Mech.* **4**: 376-382.
- Callen, H. B., 1960, *Thermodynamics*, Wiley.
- Chao, B., 1962, Motion of Spherical Gas Bubbles in a Viscous Liquid at Large Reynolds Numbers, *Phys. Fluids* **5**: 69-79.
- Clift, R., Grace, J. R. and Weber, M. E., 1978, *Bubbles, Drops, and Particles*, Academic Press, New York.
- Coleman, B. and Noll, W., 1960, An Approximate Theorem for Functionals with Applications in Continuum Mechanics, *Arch. Rational Mech. Anal.* **6**: 355-370.
- Coleman, B. D., 1964, Thermodynamics of Materials with Memory, *Arch. Rational Mech. Anal.* **17**: 1-46.
- Collier, J., 1972, *Convective Boiling and Condensation*, McGraw Hill, London.
- Coulaloglou, C. A. and Tavlarides, L. L., 1976, Drop Size Distributions and Coalescence Frequencies of Liquid-liquid Dispersion in Flow Vessels, *AIChE J.* **22**: 289-297.
- Coulaloglou, C. A. and Tavlarides, L. L., 1977, Description of Interaction Processes in Agitated Liquid-liquid Dispersions, *Chem. Eng. Sci.* **32**: 1289-1297.
- Cravarolo, L., Giorgini, A., Hassid, A. and Pedrocchi, E., 1964, A Device for the Measurement of Shear Stress on the Wall of a Conduit; Its Application in the Mean Density Determination in Two-phase Flow; Shear Stress Data in Two-phase Adiabatic Vertical Flow, *CISE Report-82*, Italy.
- Culick, F., 1964, Boltzman Equation Applied to a Problem of Two-phase Flow, *Phys. Fluid* **7**: 1898-1904.
- De Groot, S. B. and Mazur, P., 1962, *Non-equilibrium Thermodynamics*, North Holland.
- De Jarlais, G., Ishii and M., Linehan, J., 1986, Hydrodynamic Stability of Inverted Annular Flow in an Adiabatic Simulation, *J. Heat Transfer* **108**: 84-91.
- Delhaye, J. M., 1968, Equations of Fondamentales des Écoulements Diphasiques, Part 1 and 2, *CEA-R-3429*.
- Delhaye, J. M., 1969, General Equations of Two-phase Systems and their Application to Air-water Bubble Flow and to Steam-water Flashing Flow, *ASME Paper 69-HT-63*, *11th Heat Transfer Conference*, Minneapolis.

- Delhaye, J. M., 1970, Contribution à L'étude des Écoulements Diphasiques Eau-air et Eau-vapeur, *Ph.D. Thesis*, University of Grenoble.
- Delhaye, J. M., 1974, Jump Conditions and Entropy Sources in Two-phase Systems. Local Instant Formulation, *Int. J. Multiphase Flow* **1**: 395-409.
- Dinh, T. N., Li, G. J. and Theofanous, T. G., 2003, An Investigation of Droplet Breakup in High Mach, Low Weber Number Regime, *Proc. 41<sup>st</sup> Aerospace Sci. Mtg and Exh.*, Paper AIAA 2003-317, Reno, Nevada.
- Diunin, A. K., 1963, On the Mechanics of Snow Storms, *Siberian Branch, Akademii Nauk SSSR*, Novosibirsk.
- Drew, D. A., 1971, Averaged Field Equations for Two-phase Media, *Studies Appl. Math.* **1**: 133-166.
- Dumitrescu, D. T., 1943, Stomung an einer Luftblase in Senkrechten Rohr, *Z. Angew. Math. Mech.* **23**: 139-149.
- Eilers, H., 1941, The Viscosity of the Emulsion of Highly Viscous Substances as Function of Concentration, *Kolloid Z* **97**: 313-321.
- Ervin, E. A. and Tryggvason, G., 1997, The Rise of Bubbles in a Vertical Shear Flow, *J. Fluids Eng.* **119**: 443-449.
- Fauske, H., 1962, Critical Two-phase, Steam Water Flow, *Proc. Heat Transfer and Fluid Mechanics Institute*, Stanford Univ. Press, pp.78.
- Fick, A., 1855, Über Diffusion, *Ann. Der Phys.* **94**: 59-86.
- Frankl, F. I., 1953, On the Theory of Motion of Sediment Suspensions, *Soviet Physics Doklady, Akademii Nauk SSSR*, **92**: 247-250.
- Frankel, N. A. and Acrivos, A., 1967, On the Viscosity of a Concentrated Suspension of Solid Spheres, *Chem. Eng. Sci.* **22**: 847-853.
- Friedlander, S. K., 1977, *Smoke, Dust and Haze*, Wiley, New York.
- Fu, X. Y. and Ishii, M., 2002a, Two-group Interfacial Area Transport in Vertical Air-water Flow I. Mechanistic Model, *Nucl. Eng. Des.* **219**: 143-168.
- Fu, X. Y. and Ishii, M., 2002b, Two-group Interfacial Area Transport in Vertical Air-water Flow II. Model Evaluation, *Nucl. Eng. Des.* **219**: 169-190.
- Goda, H., Hibiki, T. Kim, S., Ishii, M. and Uhle, J., 2003, Drift-flux Model for Downward Two-phase Flow, *Int. J. Heat Mass Transfer* **46**: 4835-4844.
- Gibbs, J. W., 1948, *Collected Work of J. W. Gibbs*, Yale University Press, Vol.1, New York.
- Goldstein, S., 1938, *Modern Developments in Fluid Dynamics*, Oxford University Press, London.
- Govier G. W. and Aziz, K., 1972, *The Flow of Complex Mixtures in Pipes*, Van Nostrand-Reinhold Co., New York.
- Grace, J. R., Wairegi, T. and Brophy, J., 1978, Break-up of Drops and Bubbles in Stagnant Media, *Can. J. Chem. Eng.* **556**: 3-8.
- Hadamard, J., 1911, Mouvement Permanent Lent d'une Sphere Liquide Visqueuse dans un Liquid Visqueux, *C. R. Acad. Sci. Paris Sér A-B* **152**: 1735-1739.
- Hancox, W. T., and Nicoll, W. B., 1972, Prediction of Time-dependent Diabatic Two-phase Water Flows, *Prog. Heat Mass Transfer* **6**: 119-135.
- Happel, J. and Brfnnner, H., 1965, *Low Reynolds Number Hydrodynamics*, Prentice-Hall.
- Harmathy, T. Z., 1960, Velocity of Large Drops and Bubbles in Media of Infinite and Restricted Extent, *AIChE J.* **6**: 281-288.
- Hawksley, P. G. W., 1951, The Effect of Concentration on the Settling of Suspensions and Flow through Porous Media, *Some Aspect of Fluid Flow*, pp.114, Edward Arnold, London.
- Hayes, W. D., 1970, Kinematic Wave Theory, *Proc. Royal Soc. London Ser. A Math. Phys. Sci.* **320**: 209-226.

- Helmholtz, H., 1868, Über Discontinuirliche Flüssigkeitsbewegungen, *Monatsber. Dtsch. Akad. Wiss. Berlin* pp.215-228.
- Hewitt, G. and Hall Taylor, N. S., 1970, *Annular Two-phase Flow*, Pergamon Press, Oxford.
- Hibiki, T. and Ishii, M., 1999, Experimental Study on Interfacial Area Transport in Bubbly Two-phase Flows, *Int. J. Heat Mass Transfer* **42**: 3019-3035.
- Hibiki, T. and Ishii, M., 2000a, One-group Interfacial Area Transport of Bubbly Flows in Vertical Round Tubes, *Int. J. Heat Mass Transfer* **43**: 2711-2726.
- Hibiki, T. and Ishii, M., 2000b, Two-group Interfacial Area Transport Equations at Bubbly-to-slug Flow Transition, *Nucl. Eng. Des.* **202**: 39-76.
- Hibiki, T., Ishii, M. and Xiao, Z., 2001a, Axial Interfacial Area Transport of Vertical Bubbly Flows, *Int. J. Heat Mass Transfer* **44**: 1869-1888.
- Hibiki, T., Takamasa, T. and Ishii, M., 2001b, Interfacial Area Transport of Bubbly Flow in a Small Diameter Pipe, *J. Nucl. Sci. Technol.* **38**: 614-620.
- Hibiki, T. and Ishii, M., 2002a, Interfacial Area Concentration of Bubbly Flow Systems, *Chem. Eng. Sci.* **57**: 3967-3977.
- Hibiki, T. and Ishii, M., 2002b, Distribution Parameter and Drift Velocity of Drift-flux Model in Bubbly Flow, *Int. J. Heat Mass Transfer* **45**: 707-721.
- Hibiki, T. and Ishii, M., 2002c, Development of One-group Interfacial Area Transport Equation in Bubbly Flow Systems, *Int. J. Heat Mass Transfer* **45**: 2351-2372.
- Hibiki, T. and Ishii, M., 2003a, One-dimensional Drift-flux Model for Two-phase Flow in a Large Diameter Pipe, *Int. J. Heat Mass Transfer* **46**: 1773-1790.
- Hibiki, T. and Ishii, M., 2003b, One-dimensional Drift-flux Model and Constitutive Equations for Relative Motion between Phases in Various Two-phase Flow Regimes, *Int. J. Heat Mass Transfer* **46**: 4935-4948; Erratum, **48**: 1222-1223 (2005).
- Hibiki, T., Situ, R., Mi, Y. and Ishii, M., 2003a, Modeling of Bubble-layer Thickness for Formulation of One-dimensional Interfacial Area Transport Equation in Subcooled Boiling Two-phase Flow, *Int. J. Heat Mass Transfer* **46**: 1409-1423; Erratum, **46**: 3549-3550 (2003).
- Hibiki, T., Situ, R., Mi, Y. and Ishii, M., 2003b, Local Flow Measurements of Vertical Upward Bubbly Flow in an Annulus, *Int. J. Heat Mass Transfer* **46**: 1479-1496.
- Hibiki, T., Takamasa, T. and Ishii, M., 2004, One-dimensional Drift-flux Model and Constitutive Equations for Relative Motion between Phases in Various Two-phase Flow Regimes at Microgravity Conditions, *Proc. 12th Int. Conf. Nucl. Eng., Arlington, VA, USA, ICONE12*-49037.
- Hirschfelder, J. V., Curtiss, C. F. and Bird, R. B., 1954, *Molecular Theory of Gases and Liquids*, John Wiley and Sons, Inc., New York.
- Hinze, J. W., 1959, *Turbulence*, McGraw-Hill, New York.
- Hughes, T. A., 1958, Steam-water Mixture Density Studies in a Natural Circulation High Pressure System, *Babcock and Wilcox, G. Report* No. 5435.
- Ishii, M. and Zuber, N., 1970, Thermally Induced Flow Instabilities in Two-phase Mixtures, *Proc. 4th International Heat Transfer Conference*, Paris.
- Ishii, M., 1971, Thermally Induced Flow Instabilities in Two-phase Mixture in Thermal Equilibrium, *Ph.D. Thesis*, Georgia Institute of Technology.
- Ishii, M., 1975, Thermo-fluid Dynamic Theory of Two-phase Flow, *Collection de la Direction des Etudes et Recherches d'Electricite de France*, Eyrolles, Paris, France, 22.
- Ishii, M. and Grolmes, M. A., 1975, Inception Criteria for Droplet Entrainment in Two-phase Concurrent Film Flow, *AIChE J.* **21**: 308-318.
- Ishii, M., Jones, O. C. and Zuber, N., 1975, Thermal Non-equilibrium Effects in Drift Flux Model of Two-phase Flow, *Trans. Am. Nucl. Soc.* **22**: 263-264.

- Ishii, M., 1976, One-dimensional Drift-flux Modeling: One-dimensional Drift Velocity of Dispersed Flow in Confined Channel, *Argonne National Lab. Report*, ANL-76-49.
- Ishii, M., Chawla, T. C. and Zuber, N., 1976, Constitutive Equation for Vapor Drift Velocity in Two-phase Annular Flow, *AIChE J.* **22**: 283-289.
- Ishii, M. and Chawla, T. C., 1979, Local Drag Laws in Dispersed Two-phase Flow, *Argonne National Lab. Report*, ANL-79-105.
- Ishii, M., 1977, One-dimensional Drift-flux Model and Constitutive Equations for Relative Motion between Phases in Various Two-phase Flow Regimes, *Argonne National Lab. Report*, ANL-77-47.
- Ishii, M. and Zuber, N., 1979, Drag Coefficient and Relative Velocity in Bubbly, Droplet or Particulate Flows, *AIChE J.* **25**: 843-855.
- Ishii, M. and Mishima, K., 1981, Study of Two-fluid Model and Interfacial Area, *Argonne National Lab Report* ANL-80-111.
- Ishii, M. and Mishima, K., 1984, Two-fluid Model and Hydrodynamic Constitutive Relations, *Nucl. Eng. Des.* **82**: 107-126.
- Ishii, M. and De Jarlais, G., 1987, Flow Visualization Study of Inverted Annular Flow of Post Dryout Heat Transfer Region, *Nucl. Eng. Des.* **99**: 187-199.
- Ishii, M., Kim, S. and Uhle, J., 2002, Interfacial Area Transport Equation: Model Development and Benchmark Experiments, *Int. J. Heat Mass Transfer* **45**: 3111-3123.
- Ishii, M. and Kim, S., 2004, Development of One-group and Two-group Interfacial Area Transport Equation, *Nucl. Sci. Eng.* **146**: 257-273.
- Kalinin, A. V., 1970, Derivation of Fluid Mechanics Equations for a Two-phase Medium with Phase Changes, *Heat Transfer Soviet Res.* **2**: 83-96.
- Kataoka, I. and Ishii, M. 1987, Drift Flux Model for Large Diameter Pipe and New Correlation for Pool Void Fraction, *Int. J. Heat Mass Transfer* **30**: 1927-1939.
- Kataoka, I. and Serizawa, A., 1995, Modeling and Prediction of Turbulence in Bubbly Two-phase Flow, *Proc. 2<sup>nd</sup> Int. Conf. Multiphase Flow '95 – Kyoto*, pp. MO2-11-MO2-16.
- Kelly, F. D., 1964, A Reacting Continuum, *Int. J. Engng. Sci.* **2**: 129-153.
- Kelvin, W., 1871, Hydrokinetic Solutions and Observations, *London, Edinburgh and Dublin Philosophical Magazine and Journal of Science Ser.4* **42**: 362-377.
- Kim, W. K. and Lee, K. L., 1987, Coalescence Behavior of two Bubbles in Stagnant Liquids, *J. Chem. Eng. Jpn.* **20**: 449-453.
- Kirkpatrick, R. D. and Lockett, M. J., 1974, The Influence of Approach Velocity on Bubble Coalescence, *Chem. Eng. Sci.* **29**: 2363-2373.
- Kocamustafaogullari, G., 1971, Thermo-fluid Dynamics of Separated Two-phase Flow, *Ph.D. Thesis*, Georgia Institute of Technology.
- Kocamustafaogullari, G., Chen, I. Y. and Ishii, M., 1984, Unified Theory for Predicting Maximum Fluid Particle Size for Drops and Bubbles, *Argonne National Lab. Report*, ANL-84-67.
- Kocamustafaogullari, G. and Ishii, M., 1995, Foundation of the Interfacial Area Transport Equation and its Closure Relations, *Int. J. Heat Mass Transfer* **38**: 481-493.
- Kolev, N., 2002, Multiphase Flow Dynamics 1 Fundamentals, 2: Mechanical and Thermal Interactions, Springer-Verlag.
- Kordyban, E., 1977, Some Characteristics of High Waves in Closed Channels Approaching Kelvin-Helmholtz Instability, *J. Fluids Eng.* **99**: 389-346.
- Kotchine, N. E., 1926, Sur la Théorie des Ondes De-choc dans un Fluide, *Bend. Circ. Mat. Palermo* **50**: 305-344.
- Kutateladze, S. S., 1952, Heat Transfer in Condensation and Boiling, *Moscow, AEC-TR-3770*, USAEC Technical Information Service.
- Kynch, G. J., 1952, A Theory of Sedimentation, *Trans. Faraday Soc.* **48**: 166-176.

- Lackme, C., 1973, Two Regimes of a Spray Column in Counter-current Flow, *AIChE Symp. Heat Transfer R. D.* **70**: 59-63.
- Lahey Jr., R. T., Cheng, L. Y., Drew, D. A. and Flaherty, J. E., 1978, The Effect of Virtual Mass on the Numerical Stability of Accelerating Two-phase Flows, *AIChE 71st Annual Meeting*, Miami Beach, Florida.
- Lahey Jr, R. T., Lopez de Bertodano, M. and Jones Jr., O. C., 1993, Phase Distribution in Complex Geometry Conduits, *Nucl. Eng. Des.* **141**: 117-201.
- Lamb, H., 1945, *Hydrodynamics*, Dover, New York.
- Landau, L. D., 1941, Theory of Super Fluidity of Helium II, *Physical Review* **60**: 166-176.
- Landel, R. F., Moser, B. G. and Bauman, A. J., 1965, Rheology of Concentrated Suspensions: Effects of a Surfactant, *Proc. 4th Int. Congress on Rheology*, Brown University, Part 2, pp.663.
- Letan, R. and Kehat, E., 1967, Mechanics of a Spray Column, *AIChE J.* **13**: 443-449.
- Levich, V. G., 1962, *Physicochemical Hydrodynamics*, Prentice-Hall.
- Levy, S., 1960, Steam Slip-theoretical Prediction from Momentum Model, *J. Heat Transfer* **82**: 113-124.
- Lighthill, M. J. and Whitham, G. B., 1955, On the Kinematic Waves I. Flood Movement in Long Rivers, *Proc. Royal Soc. London* **229**: 281-316.
- Liu, T. J., 1993, Bubble Size and Entrance Length Effects on Void Development in a Vertical Channel, *Int. J. Multiphase Flow* **19**: 99-113.
- Loeb, L. B., 1927, *The Kinetic Theory of Gases*, Dover, New York.
- Lopez de Bertodano, M., Lahey Jr., R. T. and Jones, O. C., 1994, Development of a  $k-\epsilon$  Model for Bubbly Two-phase Flow, *J. Fluids Eng.* **116**: 128-134.
- Loth, E., Taeibi-Rahni, M. and Tryggvason, G., 1997, Deformable Bubbles in a Free Shear Layer, *Int. J. Multiphase Flow* **23**: 977-1001.
- Lumley, J., 1970, Toward a Turbulent Constitutive Relation, *J. Fluid Mech.* **41**: 413-434.
- Marchaterre, J. F., 1956, The Effect of Pressure on Boiling Density in Multiple Rectangular Channels, *Argonne National Lab. Report*, ANL-5522.
- Martinelli, R. C. and Nelson, D. B., 1948, Prediction of Pressure Drop during Forced Circulation Boiling of Water, *Trans. ASME* **70**: 695-702.
- Maurer, G. W., 1956, A Method of Predicting Steady State Boiling Vapour Fractions in Reactor Coolant Channels, WAPD-BT-19.
- Maxwell, J., 1867, On the Dynamical Theory of Gases, *Phil. Trans. Roy. Soc. London* **157**: 49-88.
- McConnell, A. S., 1957, *Application of Tensor Analysis*, Dover.
- Mei, R. and Klausner, J. F., 1994, Shear Lift Force on Spherical Bubbles, *Int. J. Heat Fluid Flow* **15**: 62-65.
- Meyer, J. E., 1960, Conservation Laws in One-dimensional Hydrodynamics, *Bettis Technical Review* **61**: WAPD-BT-20.
- Miles, J. W., 1957, On the Generation of Surface Waves by Shear Flows, I-IV, *J. Fluid Mech.* **3**: 185-204 (1957); **6**: 568-582 (1959); **6**: 583-598 (1959); **13**: 433-448 (1962).
- Mishima, K. and Ishii, M., 1980, Theoretical Prediction of Onset of Slug Flow, *J. Fluid Eng.* **102**: 441-445.
- Mishima, K. and Ishii, M., 1984, Flow Regime Transition Criteria for Upward Two-phase Flow in Vertical Tubes, *Int. J. Heat Mass Transfer* **27**: 723-737.
- Miller, J. W., 1993, An Experimental Analysis of Large Spherical Cap Bubbles Rising in an Extended Liquid, *M. S. Thesis*, Purdue University.
- Mokeyev, Yu. G., 1977, Effect of Particle Concentration on their Drag and Induced Mass, *Fluid Mech.-Soviet Res.* **6**: 161-168.

- Muller, I., 1968, A Thermodynamics Theory of Mixtures of Fluids, *Arch. Rational Mech. Anal.* **28**: 1-39.
- Murray, S. O., 1954, On the Mathematics of Fluidization I, Fundamental Equations and Wave Propagation, *J. Fluid Mech.* **21**: 465-493.
- Neal, L. G., 1963, An Analysis of Slip in Gas-liquid Flow Applicable to the Bubble and Slug Flow Regimes, *Kjeller Research Establishment Report, Norway* KR-2.
- Nicklin, D. J., Wilkes, J. O. and Davidson, J. F., 1962, Two-phase Flow in Vertical Tubes, *Trans. Inst. Chem. Eng.* **40**: 61-68.
- Nikuradse, J., 1932, Gesetzmäßigkeit der Turbulenten Strömung in Glatten Rohre, *Forsch. Arb. Ing.-Wes.* pp.356.
- Oolman, T. O. and Blanch, H. W., 1986a, Bubble Coalescence in Air-Sparged Bioreactors, *Biotech. Bioeng.* **28**: 578-584.
- Oolman, T. O. and Blanch, H. W., 1986b, Bubble Coalescence in Stagnant Liquids, *Chem. Eng. Commun.* **43**: 237-261.
- Otake, T., Tone, S., Nakao, K., and Mitsuhashi, Y., 1977, Coalescence and Breakup of Bubbles in Liquids, *Chem. Eng. Sci.* **32**: 377-383.
- Pai, S. I., 1962, *Magnetogasdynamics and Plasma Dynamics*, Wien Springer-Verlag.
- Pai, S. I., 1971, Fundamental Equations of a Mixture of Gas and Small Spherical Solid Particles from Simple Kinetic Theory, *Int. Sym. on Two-phase Systems*, Paper 6-6, Haifa, Israel.
- Pai, S. I., 1972, A New Classification of Two-phase Flows, *J. Mach. Phys. Sci.* **6**: 137-161.
- Panton, R., 1968, Flow Properties for the Continuum View-point of a Non-Equilibrium Gas-Particle Mixture, *J. Fluid Mech.* **31**: 273-303.
- Peebles, F. N. and Garber, H. J., 1953, Studies on the Motion of Gas Bubbles in Liquid, *Chem. Eng. Prog.* **49**: 88-97.
- Petrick, M., 1962, A Study of Vapor Carryunder and Associated Problems, *Argonne National Lab. Report*, ANL-65-81.
- Phillips, M. C. and Riddiford, A. C., 1972, Dynamic Contact Angles 2. Velocity and Relaxation Effects for Various Liquids, *J. Colloid Interface Sci.* **41**: 77-85.
- Pierre, C. C. St., 1965, Frequency-response Analysis of Steam Voids to Sinusoidal Power Modulation in a Thin-walled Boiling Water Coolant Channel, *Argonne National Lab. Report*, ANL-7041.
- Prigogine, I. and Mazur, P., 1951, On Two-phase Hydrodynamic Formulations and the Problem of Liquid Helium II, *Physica* **17**: 661-679.
- Prince, M. J. and Blanch, H. W., 1990, Bubble Coalescence and Break-up in Air-Sparged Bubble Columns, *AIChE J.* **36**: 1485-1497.
- Prosperetti, A., 1999, Some Considerations on the Modeling of Disperse Multiphase Flows by Averaged Equations, *JSME Intl. J.*, Ser. B, **42**: 573-585.
- Réocreux, M., Barriere, G. and Vernay, B., 1973, Etude Expérimentale des Débits Critiques en Écoulement Diphasique Eau-vapeur à Faible Titre sur un Canal à Divergent de 7 Degrés, *Cen. G. Rapport* TT 115.
- Réocreux, M., 1974, Contribution à l'étude des Débits Critiques en Écoulement Diphasique eau Vapeur, *Ph. D. Thesis*, University of Grenoble.
- Richardson, J. F. and Zaki, W. N., 1954, Sedimentation and Fluidization: Part 1, *Trans. Inst. Chem. Eng.* **32**: 35-53.
- Roscoe, R., 1952, The Viscosity of Suspensions of Rigid Spheres, *Br. J. Appl. Phys.* **3**: 267-269.
- Rose, S. C. and Griffith, P., 1965, Flow Properties of Bubbly Mixtures, *ASME Paper* 65-HT-8.
- Rotta, J. C., 1972, *Turbulence Stromungen*, B. G. Teubner, Stuttgart, Germany.

- Rouhani, S. Z. and Becker, K. M., 1963, Measurement of Void Fractions for Flow of Boiling Heavy Water in a Vertical Round Duct, AE-106, Aktiebolaget Atomenergi, Sweden.
- Rybczynski, W., 1911, Über die Fortschreitende Bewegung einer Flüssigen Kugel in einem Zählen Medium, *Bull. Int. Acad. Sci. Cracov.* **1911A**: 40-46.
- Saffman, P. G., 1965, The Lift on a Small Sphere in a Slow Shear Flow, *J. Fluid Mech.* **22**: 385-400.
- Sato, Y., Sadatomi, M. and Sekoguchi, K., 1981, Momentum and Heat Transfer in Two-phase Bubble Flow - 1. Theory, *Int. J. Multiphase Flow* **7**: 167-177.
- Schlichting, H., 1979, *Boundary Layer Theory*, McGraw-Hill Book Co.
- Schwartz, K., 1954, Investigation of Distribution of Density, Water and Steam Velocity and of the Pressure Drop in Vertical Horizontal Tubes, *VDI Forschungsh.* 20, Series B, 445.
- Schwartz, A. M. and Tejada, S. B., 1972, Studies of Dynamic Contact Angles on Solids, *J. Colloid Interface Sci.* **38**: 359-375.
- Scriven, L. E., 1960, Dynamics of Fluid Interface, Equation of Motion for Newtonian Surface Fluids, *Chem. Eng. Sci.* **2**: 98-108.
- Serizawa, A., Kataoka, I. and Michiyoshi, I., 1975, Turbulence Structure of Air-water Bubbly Flow, I, II and III, *Int. J. Multiphase Flow* **2**: 221-259.
- Serizawa, A. and Kataoka, I., 1988, Phase Distribution in Two-phase Flow, *Transient Phenomena in Multiphase Flow*, Hemisphere, Washington DC, pp.179-224.
- Serizawa, A. and Kataoka, I., 1994, Dispersed Flow-I., *Multiphase Science and Technology*, Vol. 8, Begell House Inc., New York, pp.125-194.
- Serrin, J., 1959, *Handbuch der Physik*, Vol.8/I, Springer-Verlag.
- Sevik, M. and Park, S. H., 1973, The Splitting of Drops and Bubbles by Turbulent Fluid Flow, *J. Fluids Eng.* **95**: 53-60.
- Slattery, J. C., 1964, Surface - I. Momentum and Moment-of-momentum Balance for Moving Surfaces, *Chem. Eng. Sci.* **19**: 379-385.
- Slattery, J. C., 1972, *Momentum, Energy and Mass Transfer in Continua*, McGraw-Hill Book Co.
- Smissaert, G. E., 1963, Two-component Two-phase Flow Parameters for Low Circulation Rages, *Argonne National Lab. Report*, ANL-67-55.
- Soo, S. L., 1967, *Fluid Dynamics of Multiphase Systems*, Ginn Blaisdell.
- Sridhar, G. and Katz, J., 1995, Drag and Lift Forces on Microscopic Bubbles Entrained by a Vortex, *Phys. Fluids* **7**: 389-399.
- Standart, G., 1964, The Mass, Momentum and Energy Equations for Heterogeneous Flow Systems, *Chem. Eng. Sci.* **19**: 227-236.
- Standart, G., 1968, The Second Law of Thermodynamics for Heterogeneous Flow Systems III. Effect of Conditions of Mechanical Equilibrium and Electroneutrality on Simultaneous Heat and Mass Transfer and Prigogine Theorem, *Chem. Eng. Sci.* **23**: 279-285.
- Stefan, J., 1871, Über das Gleichgewicht und die Bewegung, Insbesondere die Diffusion von Gasmengen, *Sitzgsber, Akad. Wiss. Wien* **63**: 63-124.
- Stewart, C. W., 1995, Bubble Interaction in Low-viscosity Liquids, *Int. J. Multiphase Flow* **21**: 1037-1046.
- Stokes, G. G., 1851, On the Effect of Internal Friction of Fluids on the Motion of Pendulums, *Trans. Cambr. Phil. Soc.* **9, Part II**: 8-106 or Coll. Papers **III**: 55.
- St. Pierre, C. C., 1965, Frequency-response Analysis of Steam Voids to Sinusoidal Power Modulation in a Thin-walled Boiling Water Coolant Channel, *Argonne National Lab. Report*, ANL-7041.
- Sun, X., Ishii, M. and Kelly, J. M., 2003, Modified Two-fluid Model for the Two-group Interfacial Area Transport Equation, *Annals Nucl. Energy* **30**: 1601-1622.



- Sun, X., Kim, S., Ishii, M. and Beus, S. G., 2004a, Modeling of Bubble Coalescence and Disintegration in Confined Upward Two-phase Flow, *Nucl. Eng. Des.* **230**: 3-26.
- Sun, X., Kim, S., Ishii, M. and Beus, S. G., 2004b, Model Evaluation of Two-group Interfacial Area Transport Equation for Confined Upward Flow, *Nucl. Eng. Des.* **230**: 27-47.
- Taylor, G. I., 1932, The Viscosity of a Fluid Containing Small Drops of Another Fluid, *Proc. R. Soc.* **A138**: 41-48.
- Taylor, G. I., 1934, The Formation of Emulsions in Definable Fields of Flow, *Proc. Royal Soc. London* **A146**: 501-523.
- Teletov, S. G., 1945, Fluid Dynamic Equations for Two-phase Fluids, *Soviet Physics Doklady, Akademii Nauk SSSR* **50**: 99-102.
- Teletov, S. G., 1957, On the Problem of Fluid Dynamics of Two-phase Mixtures, I. Hydrodynamic and Energy Equations, *Bull. the Moscow University* **2**: 15.
- Theofanous, T. G., Li, G. J. and Dinh, T. N., 2004, Aerobreakup in Rarefied Supersonic Gas Flows, *J. Fluid Eng.* **126**: 516-527.
- Thomas, D. G., 1965, Transport Characteristics of Suspension: VIII A Note on Viscosity of Newtonian Suspensions of Uniform Spherical Particles, *J. Colloid Sci.* **20**: 267-277.
- Thome, R. J., 1964, Effect of a Transverse Magnetic Field and Vertical Two-phase Flow through a Rectangular Channel, *Argonne National Lab. Report*, ANL-6854.
- Tomiyama, A., Zun, I., Sou, A. and Sakaguchi, T., 1993, Numerical Analysis of Bubble Motion with the VOF method, *Nucl. Eng. Des.* **141**: 69-82.
- Tomiyama, A., Sou, A., Zun, I., Kanami, N. and Sakaguchi, T., 1995, Effects of Eötvös Number and Dimensionless Liquid Volumetric Flux on Lateral Motion of a Bubble in a Laminar Duct Flow, *Advances in Multiphase Flow*, Elsevier, pp.3-15.
- Tomiyama, A., Tamai, H., Zun, I. and Hosokawa, S., 2002, Transverse Migration of Single Bubbles in Simple Shear Flows, *Chem. Eng. Sci.* **57**: 1849-1858.
- Tong, L. S., 1965, *Boiling Heat Transfer and Two-phase Flow*, John Wiley and Sons, Inc., New York.
- Truesdell, C. and Toupin, R., 1960, The Classical Field Theories, *Handbuch der Physik*, Vol.3/I, Springer-Verlag.
- Truesdell, C., 1969, *Rational Thermodynamics*, McGraw-Hill Book Co.
- Tsouris, C. and Tavlarides, L. L., 1994, Breakage and Coalescence Models for Drops in Turbulent Dispersions, *AIChE J.* **40**: 395-406.
- Tsuchiya, K., Miyahara, T. and Fan, L. S., 1989, Visualization of Bubble-wake Interactions for a Stream of Bubbles in a Two-dimensional Liquid-solid Fluidized Bed, *Int. J. Multiphase Flow* **15**: 35-49.
- Vernier, P. and Delhay, J. M., 1968, General Two-phase Flow Equations Applied to the Thermohydrodynamics of Boiling Nuclear Reactors, *Energie Primaire* **4**: No.1.
- Von Karman, 1950, Unpublished Lectures (1950-1951) at Sorbonne and Published by Nachbar et al. in *Quart. Appl. Math.* **7**: 43 (1959).
- Wallis, G. B., Steen, D. A., Brenner, S. N. and Turner T. M., 1964, Joint U. S. – Euratom Research and Development Program, *Quarterly Progress Report*, January, Dartmouth College.
- Wallis, G. B., 1969, *One-dimensional Two-phase Flow*, McGraw-Hill Book Co.
- Wallis, G. B., 1974, The Terminal Speed of Single Drops or Bubbles in an Infinite Medium, *Int. J. Multiphase Flow* **1**: 491-511.
- Wang, S. K., Lee, S. J., Jones Jr., O. C. and Lahey Jr. R. T., 1987, 3-D Turbulence Structure and Phase Distribution Measurements in Bubbly Two-phase Flows, *Int. J. Heat Mass Transfer* **13**: 327-343.

- Weatherburn, C. E., 1927, *Differential Geometry of Three Dimensions*, Cambridge University Press.
- Werther, J., 1974, Influence of the Bed Diameter on the Hydrodynamics of Gas Fluidized Beds, *AIChE Symp. Ser.* No. 141 70: 53.
- Whitaker, S., 1968, *Introduction to Fluid Mechanics*, Prentice-Hall, Inc.
- White, E. T. and Beardmore, R. H., 1962, The Velocity of Rise of Single Cylindrical Air Bubbles through Liquid Contained in Vertical Tubes, *Chem. Eng. Sci.* **17**: 351-361.
- Wu, Q. and Ishii, M., 1996, Interfacial Wave Instability of Co-current Two-phase Flow in Horizontal Channel, *Int. J. Heat Mass Transfer* **39**: 2067-2075.
- Wu, Q., Kim, S., Ishii, M. and Beus, S. G., 1998, One-group Interfacial Area Transport in Vertical Bubbly Flow, *Int. J. Heat Mass Transfer* **41**: 1103-1112.
- Wundt, H., 1967, Basic Relationships in n-components Diabatic Flow, *EUR* 3459e.
- Yoshida, F. and Akita, K., 1965, Performance of Gas Bubble Columns: Volumetric Liquid-phase Mass Transfer Coefficient and Gas Holdup, *AIChE J.* **11**: 9-13.
- Zhang, D. Z., 1993, Ensemble Phase Averaged Equations for Multiphase Flows, *Ph D. Thesis*, Johns Hopkins University.
- Zhang, D. Z., Prosperetti, A., 1994a, Averaged Equations for Inviscid Disperse Two-phase Flow, *J. Fluid Mech.* **267**: 185-219.
- Zhang, D. Z., Prosperetti, A., 1994b, Ensemble Phase-averaged Equations for Bubbly Flows, *Phys. Fluids* **6**: 2956-2970.
- Zuber, N., 1964a, On the Dispersed Flow in the Laminar Flow Regime, *Chem. Eng. Sci.* **19**: 897-917.
- Zuber, N., 1964b, On the Problem of Hydrodynamic Diffusion in Two-phase Flow Media, *Proc. 2nd All Union Conference on Heat and Mass Transfer*, Minsk, USSR, **3**: 351.
- Zuber, N., Staub, F. W. and Bijwaard, G., 1964, Steady state and Transient Void Fraction in Two-phase Flow Systems, Vol.1, *GEAP* 5417.
- Zuber, N. and Findlay, J. A., 1965, Average Volumetric Concentration in Two-phase Flow Systems, *J. Heat Transfer* **87**: 453-468.
- Zuber, N. and Staub, F. W., 1966, Propagation and the Wave Form of the Volumetric Concentration in Boiling Water Forced Convection Systems under Oscillatory Conditions, *Int. J. Heat Mass Transfer* **9**: 871-895.
- Zuber, N., 1967, Flow Excursions and Oscillations in Boiling, Two-phase Flow Systems with Heat Addition, *Proc. Symp. Two-phase Flow Dynamics*, **1**: 1071.
- Zuber, N. and Dougherty, D. E., 1967, Liquid Metals Challenge to the Traditional Methods in Two-phase Flow Investigations, *Proc. EURATOM Symposium on Two-phase Flow Dynamics*, pp.1085.
- Zuber, N., Staub, F. W., Bijwaard, G. and Kroeger, P. G., 1967, Steady State and Transient Void Fraction in Two-phase Flow Systems, *General Electric Co. Report GEAP-5417*, vol.1
- Zuber, N., 1971, Personal Communication at Georgia Institute of Technology.
- Zun, I., 1988, Transition from Wall Void Peaking to Core Void Peaking in Turbulent Bubbly Flow, *Transient Phenomena in Multiphase Flow*, Hemisphere, Washington DC, pp.225-245.

## Nomenclature

### *Latin*

$A$	surface of a volume
$A$	frontal area of bubble
$A^{\alpha\beta}$	surface metric tensor (Aris, 1962)
$\mathcal{A}$	turbulence anisotropy tensor
$A_d$	projected area of a typical particle
$A_i$	mathematical surface between $A_1$ and $A_2$
$A_i$	surface area
$A_k$	surface bounding the interfacial region and adjacent to phase $k$
$A_m$	surface of fixed mass volume
$A_p$	projected area of a particle
$a$	cross sectional radius of cap or slug bubble
$a_c^i$	mobility of the fluid at the interface
$a_i$	interfacial area concentration
$a_{sk}, a_{tk}$	isentropic and isothermal sound velocities based on the average thermodynamic properties
$B_d$	volume of a typical particle
$B_S$	balance at an interface
$B_V$	balance in each phase
$b_k^F, b_k^M, b_k^E$	Transport coefficients associated with interfacial

	transfer of mass, momentum and energy
$C$	wave velocity
$C$	constant
$C_D$	drag coefficient
$C_{D\infty}$	ideal drag coefficient
$C_g$	variable defined by $\sqrt{2g\Delta\rho/\rho_f}$
$C_{hk}$	distribution parameter
$C_{hm}$	mixture-enthalpy-distribution parameter
$C_i$	closed curve on an interface
$C_K$	kinematic wave velocity
$C_{LW}$	coefficient of lift force caused by slanted wake
$C_M$	virtual mass constant
$C_T$	adjustable parameter
$C_{vk}$	distribution parameter
$C_{vm}$	virtual volume coefficient
$C_{vm}$	mixture-momentum-distribution parameter
$C_\tau$	distribution parameter
$C_{\psi k}$	distribution parameter for flux
$C^i$	shape factor
$C_0$	distribution parameter
$C_\infty$	propagation velocity
$C_\infty$	asymptotic value of distribution parameter
$c_k$	mass concentration of phase $k$
$c_{pk}, c_{vk}$	specific heat at constant pressure and density based on averaged properties
$D$	hydraulic-equivalent diameter
$D^*$	length scale ratio
$D_b$	bubble diameter
$D_{bc}$	critical bubble size
$D_{cl}^*$	ratio of $D_{crit}$ to $D_{Sm1}$
$D_{c,maz}$	maximum diameter of stable bubble
$D_{crit}$	volume-equivalent diameter of a bubble at boundary between groups 1 and 2
$D_{d,maz}$	maximum distorted bubble limit

$D_d^*$	ratio of bubble diameter to bubble diameter at distorted bubble limit
$D_e$	volume-equivalent diameter of a fluid particle
$D_e$	eddy diameter
$D_E$	effective diameter of mixture volume that contains one bubble
$D_H$	hydraulic-equivalent diameter
$D_H^*$	non-dimensional hydraulic-equivalent diameter
$D_k$	diffusion coefficient
$D_k$	total deformation tensor of phase $k$
$D_{kb}$	bulk deformation tensor
$D_{ki}$	interfacial extra deformation tensor
$D_k^\alpha$	drift coefficient
$D_{Sm}$	Sauter mean diameter
$D_s$	surface-equivalent diameter of a fluid particle
$d_B$	bubble diameter
$\widehat{d}_B$	cross-sectional mean diameter of bubbles
$E_B$	average energy required for bubble breakup
$E_d$	area fraction of liquid entrained in gas core from total liquid area at any cross section
$E_e$	average energy of a single eddy
$E_k$	total energy gain through interfaces for phase $k$
$E_m$	mixture total energy source from interfaces
$E_m^H$	mixture energy gain due to changes in mean curvature
$Eu$	Eötvös number
$\widehat{e}_k, \widehat{e}_{ki}$	weighted mean virtual internal energy (with turbulent kinetic energy included) at the bulk phase and at the interfaces
$F(x, t)$	general function
$\mathbf{F}^B$	Basset force
$\mathbf{F}^D$	standard drag force
$\mathbf{F}^L$	lift force
$\mathbf{F}^T$	turbulent dispersion force
$\mathbf{F}^V$	virtual mass force

$\mathbf{F}^W$	wall lift force
$F_D$	drag force
$F_k, \mathcal{F}_k$	general function associated with phase $k$
$f(\mathbf{x}, t)$	function for interface position
$f(\mathbf{x}, t, \boldsymbol{\xi})$	molecular density function
$f$	collision frequency
$f$	friction factor
$f^*$	correction factor for drag coefficient
$f_i$	interfacial friction factor
$f_k$	Helmholtz potential
$f_{kn}(\mathbf{x}, t, \boldsymbol{\xi})$	particle density function of the $n^{\text{th}}$ -kind particles
$f_{TW}$	two-phase friction factor
$G$	mass velocity
$G$	cap bubble thickness
$G_s$	non-dimensional velocity gradient
$g$	gravity field
$g_k$	body force field
$g_k, \widehat{g}_k, \widehat{g}_{ki}$	Gibbs free energy: local instant, bulk mean and interfacial mean values
$g_{ln}$	space metric tensor (Aris, 1962)
$g_N$	normal gravitational acceleration
$H_{21}, \overline{\overline{H}}_{21}$	local instant and averaged mean curvature ( $\overline{\overline{H}}_{21} > 0$ if phase 2 is the dispersed phase)
$h$	bubble height
$h_1, h_2$	average thickness of upper (1) and lower (2) fluid layers
$\widehat{h}_k, \widehat{h}_{ki}$	weighted mean virtual enthalpy (with turbulent kinetic energy included) at the bulk phase and at the interfaces
$h_m$	mixture virtual enthalpy
$\mathcal{I}$	unit tensor
$I_k$	interfacial source term in the balance equations for phase $k$
$I_m$	interfacial source term for mixture balance equations
$I_{ka}, I_{ma}$	interfacial source terms in the shock conditions for

	phase $k$ and for mixture
$\dot{v}_k, \hat{v}_k$	local instant and mean enthalpies
$\hat{v}_{ki}$	mean enthalpy of phase $k$ at interfaces
$\dot{v}_m$	mixture enthalpy
$\dot{v}_a$	local instant surface enthalpy per area
$J$	flux
$J^D$	drift flux
$J_a$	line flux for interface
$J_k$	surface flux for phase $k$
$J_k^T, J^T$	turbulent fluxes
$J_k, J_m$	Jacobians based on macroscopic field
$\dot{j}_k, \dot{j}$	volumetric fluxes of phase $k$ and mixture
$\dot{j}^*$	non-dimensional mixture volumetric flux
$\dot{j}^+$	non-dimensional mixture volumetric flux
$K$	constant
$K_k$	thermal conductivity
$\mathbb{K}_k$	thermal conductivity tensor
$K_k^T$	turbulent conductivity
$K_k^{T*}$	thermal mixing length coefficient
$k$	wave number
$k^{SI}$	turbulent kinetic energy due to shear-induced turbulence
$k_e$	wave number of eddy
$L$	pitch of slug unit
$L_b$	cylindrical bubble length
$1/L_j$	area concentration of $j^{\text{th}}$ -interface
$1/L_s$	total area concentration
$L_T$	mean traveling distance between two bubbles for one collision
$L_W$	effective wake length
$l$	mixing length
$l_B$	mixing length due to bubble-induced turbulence
$l_{SP}$	mixing length of single-phase flow
$l_{TP}$	mixing length of two-phase flow
$m_e$	mass per a single eddy

$\dot{m}_k, \overline{\dot{m}_k}$	local instant and mean mass transfer rates per unit area (mass loss)
$M$	Morton number
$M_F$	frictional pressure gradient in multi-particle system
$M_{F\infty}$	frictional pressure gradient in single particle system
$M_{ik}$	generalized interfacial drag
$M_k, M_s$	state density functions for phase $k$ and interface
$M_k, M_m$	momentum sources for phase $k$ and mixture
$M_m^H$	force due to changes in mean curvature
$M_k^n, M_k^t, M_k^d$	form, skin and total drag forces
$M_{\tau m}$	force associated with mixture transverse stress gradient
$N$	unit normal vector to a curve on an interface
$N$	number of samples
$N_b$	number of bubbles
$N_D$	drift number
$N_{drag}$	drag number
$N_e$	number of eddies of wave number $k_e$ per volume of fluid
$N_{Ec}$	Eckert number
$N_{Eu}$	Euler number
$N_{Fr}$	Froude number
$N_i$	converted enthalpy ratio
$N_{Jk}$	Jakob number
$N_{pch}$	phase change number
$N_{pch}^i$	interfacial phase change effect number
$N_{Pe}$	Peclet number
$N_{Prk}^T$	turbulent Prandtl number
$N_q$	interface heating number
$N_{Re}$	Reynolds number
$N_{Re}^i$	interfacial Reynolds number
$N_{Sl}$	Strouhal number
$N_{We}$	Weber number
$N_\sigma$	surface tension number



$N_{Pr}$	Prandtl number
$N_W$	number of bubbles inside effective volume
$N_\mu$	viscosity number
$N_\rho$	density ratio
$n$	fluid particle number per unit mixture volume
$\mathbf{n}$	unit normal vector
$n_b$	bubble number density
$n_e$	number of eddies of wave number per volume of two-phase mixture
$\mathbf{n}_k$	outward unit normal vector for phase k
$P^{SI}$	production of shear-induced turbulence
$P_C$	probability for a bubble to move toward neighboring bubble
$\overline{P}_k$	partial pressure tensor
$P_i$	interfacial wetted perimeter
$P_{wf}$	wall wetted perimeter
$p$	pressure
$p_c$	critical pressure
$p_k, \overline{\overline{p}}_k, \overline{\overline{p}}_{ki}$	partial, bulk mean and interfacial mean pressure
$p_m$	mixture pressure
$q$	heat flux
$q^D$	diffusion (drift) heat flux
$\overline{\overline{q}}_k, \overline{\overline{q}}_k^T$	mean conduction and turbulent heat fluxes
$\overline{\overline{q}}, \overline{\overline{q}}_k^T$	mixture conduction and turbulent heat fluxes
$\dot{q}_k$	local instant body heating
$\overline{\overline{q}}_k''$	average heat transfer per interfacial area (energy gain)
$q_k^C$	mean conduction heat flux
$R$	ideal gas constant
$R$	radius of a pipe
$R$	radius of curvature
$R^+$	variable defined by $Rv_f^*/\nu_f$
$\overline{\overline{R}}_d$	mean radius of fluid particles
$R_j$	particle number source and sink rate

$R_w$	tube radius
$Re$	Reynolds number
$(Re)_d$	particle Reynolds number
$r$	radial coordinate
$r_d^*$	non-dimensional radius
$S_B, S_C$	surface available to collision
$S_j$	particle source and sink rates per unit mixture volume due to $j$ -th particle interactions such as disintegration or coalescence
$S_{ph}$	particle source and sink rates per unit mixture volume due to phase change
$s$	entropy
$s_a$	surface entropy per area
$\widehat{s}_k, \widehat{s}_{ki}$	weighted mean entropy at bulk phase and at interfaces
$s_m$	mixture entropy
$T$	temperature
$T_i, \overline{\overline{T}}_i$	instant and mean interface temperature
$\overline{\overline{T}}_k, \overline{\overline{T}}_{ki}$	mean temperature at bulk phase and at interface
$\mathcal{T}_k$	stress tensor
$t$	time
$t_C$	time required for bubble coalescence
$t_j$	time when the $j^{\text{th}}$ -interface passes the point
$t_\alpha^m$ (or $t_\alpha$ )	hybrid tensor of interface, see Aris (1962)
$U$	velocity of shock in mixture
$U_0$	velocity of stream
$U_B, U_C$	volume available to collision
$u$	internal energy
$u_a$	surface energy per area
$u_b$	mean fluctuation velocity
$u_B, u_C$	bubble velocity
$u_e$	eddy velocity
$\widehat{u}_k, \widehat{u}_{ki}$	weighted mean internal energy at bulk phase and at interfaces
$u_m$	mixture internal energy

$u_{rW}$	averaged relative velocity between leading bubble and bubble in wake region
$u_t$	root-mean-square approaching velocity of two bubbles
$u_{t,crit}$	critical fluctuation velocity
$V$	volume
$\dot{V}$	time derivative of volume $V$
$V_c$	critical bubble volume
$V_{gi}^+$	non-dimensional drift velocity
$V_i$	interfacial region
$V_{kj}$	drift velocity
$V_{km}$	diffusion velocity
$V_m$	fixed mass volume
$V_s^*$	ratio of $V_{s,min}$ to $V_{s,max}$
$V_W$	effective wake volume
$V_{1p}$	peak bubble volume in group 1
$v$	velocity
$v'_f$	liquid velocity fluctuation independent of bubble agitation
$v''_f$	liquid velocity fluctuation dependent on bubble agitation
$v_f^*$	friction velocity
$v_g$	average center-of-volume velocity of dispersed phase
$v_i$	velocity of interface
$\widehat{v}_k, \widehat{v}_{ki}$	weighted mean velocity at bulk phase and at interfaces
$\widehat{(v'_k)^2}/2$	mean turbulent kinetic energy
$v_m$	mixture center of mass velocity
$v_{pm}$	average local particle velocity weighted by particle number
$v_r$	relative velocity
$\overline{v_r}$	difference between area averaged mean velocities of phases
$v_{r\infty}$	relative velocity of a single particle in an infinite medium

$v_s$	velocity of interfacial particles
$W_{ki}^T$	work due to fluctuations in drag forces
$We$	Weber number
$We_{crit}$	critical Weber number
$\mathbf{X}$	convective coordinates
$\mathbf{x}$	spatial coordinates
$x$	spatial coordinate
$y$	spatial coordinate
$y^+$	variable defined by $yv_f^*/\nu_f$
$z$	spatial coordinate

### ***Greek***

$\alpha_b$	void fraction in slug bubble section
$\alpha_{core}$	ratio of liquid-film cross-sectional area to total cross-sectional area
$\alpha_d$	average overall void fraction
$\alpha_{drop}$	ratio of cross-sectional area of drops to cross-sectional area of core
$\alpha_{g,crit}$	critical void fraction when center bubble cannot pass through free space among neighboring bubbles
$\alpha_{g,max}$	maximum void fraction
$\alpha_k$	time (void) fraction of phase $k$
$\beta$	ratio of mixing length and width of wake
$\beta_C$	variable to take account of overlap of excluded volume
$\beta_k$	thermal expansivity based on averaged properties
$\Gamma$	constant
$\Gamma_k$	mass generation for phase $k$
$\gamma$	constant
$\gamma_k$	ratio of specific heats
$\Delta_a$	interfacial entropy generation per area
$\Delta_k$	entropy generation for phase $k$
$\Delta\dot{m}_{12}$	inter-group mass transfer rates from group 1 to group 2
$\Delta t$	time interval of averaging
$\Delta t_B$	time interval to drive daughter bubble apart with

	characteristic length of $D_b$
$\Delta t_C$	time interval for one collision
$\Delta t_k, \Delta t_s$	time intervals associated with phase $k$ and interfaces
$\Delta t_W$	average time interval for a bubble in wake region to catch up with preceding bubble
$\delta$	thickness of interface
$\delta$	film thickness
$\delta'$	collective parameter
$\delta_{crit}$	critical film thickness where rapture occurs
$\delta_{init}$	initial film thickness
$\delta p_k$	pressure deviation from saturation pressure
$\delta\mu$	volume element in $\mu$ space
$\varepsilon$	energy dissipation rate per unit mass
$2\varepsilon$ (or $2\varepsilon_j$ )	time associated with the $j^{\text{th}}$ -interface
$\varepsilon^{SI}$	dissipation of shear-induced turbulence
$\varepsilon', \varepsilon''$	eddy diffusivity
$\eta_{ph}$	rate of volume generated by nucleation source per unit mixture volume
$\eta_0$	amplitude
$\Theta$	contact angle
$\theta$	angle in cylindrical coordinates
$\theta_w$	wake angle
$\kappa_{fr}$	variable defined by $1 - \exp(-C_{fr} V_s^{*1/2} / D^{1/2})$
$\kappa_{Sk}, \kappa_{Tk}$	isentropic and isothermal compressibilities of phase $k$
$\Lambda_k$	interfacial thermal energy transfer term in the averaged equation
$\lambda$	wavelength
$\lambda$	constant
$\lambda_B$	breakup efficiency
$\lambda_C$	coalescence efficiency
$\lambda_c$	critical wavelength
$\lambda_k$	bulk viscosity
$\mu$	viscosity
$\overline{\mu}_k, \mu_k^T$	mean molecular and turbulent viscosities

$\mu_k^{T*}$	mixing length coefficient
$\mu_m$	mixture viscosity
$\nu$	kinematic viscosity
$\nu_t$	turbulent kinematic viscosity
$\xi$	particle (phase) velocity in Boltzmann statistical average
$\xi$	ratio of $V_{1p}$ to $V_c$
$\xi$	variable defined by $2(1 - 0.2894D_{cl}^{*3})^2$
$\xi$	variable defined by $P_i/P_{wf}$
$\rho$	density
$\rho_a$	surface mass per area
$\overline{\rho_k}, \overline{\overline{\rho_k}}$	partial and mean densities
$\rho_k'$	modified density defined by $\rho_k \coth(kh_k)$
$\rho_m$	mixture density
$\sigma$	surface tension
$\mathcal{T}$	viscous stress tensor
$\mathcal{T}^D$	diffusion (or drift) stress tensor
$\mathcal{T}_f^{BI}$	bubble-induced turbulent stress tensor
$\mathcal{T}_f^{SI}$	shear-induced turbulent stress tensor
$\overline{\mathcal{T}}, \mathcal{T}^T$	mixture viscous and turbulent stress tensors
$\overline{\overline{\mathcal{T}_k}}, \mathcal{T}_k^T$	average viscous and turbulent stress tensor
$\mathcal{T}_k^\mu$	average viscous stress
$\overline{\overline{\mathcal{T}_{ki}}}, \mathcal{T}_{ki}$	interfacial shear stress
$\tau_C$	contact time for two bubbles
$\tau_i$	interfacial shear stress
$\tau_o$	reference time constant
$\tau_{tk}, \tau_{nk}$	tangential and normal stresses at interface
$\tau_{wf}$	wall shear
$\Phi$	velocity potential
$\Phi_k^T$	turbulent work effect in enthalpy energy equation
$\Phi_m^i$	interfacial mechanical energy exchange effect in the mixture thermal energy equation
$\Phi_k^\mu$	viscous dissipation

$\Phi_m^\mu$	mixture viscous dissipation
$\Phi_m^\sigma$	surface tension effect in the mixture thermal energy equation
$\phi$	source term
$\phi_a$	interfacial source per area
$\phi_j$	source and sink rate for interfacial area concentration
$\phi_k$	velocity potential
$\chi$	coefficient accounting for contribution from inter-group transfer
$\psi$	property of extensive characteristics
$\psi$	shape factor
$\widehat{\psi}, \widehat{\psi}_k$	mass weighted mean values for mixture and phase k
$\psi_a$	property per interfacial area
$\Omega$	potential function

### ***Subscripts and Superscripts***

$a$	surface (property per area)
$c$	continuous phase
$d$	dispersed phase
$f$	liquid phase
$g$	vapor phase
$i$	interface
$j$	$j^{\text{th}}$ -interface
$k$	each phase : ( $k=1$ & $2$ ), ( $k=c$ & $d$ ), ( $k=f$ & $g$ )
$ki$	$k^{\text{th}}$ -phase at interfaces
$m$	<div style="display: flex; align-items: center;"> <div style="font-size: 3em; margin-right: 5px;">{</div> <div> mixture (in macroscopic formulation)  fixed mass (in local instant formulation) </div> </div>
$n$	normal to interface
$o$	reference
RC	random collision
$r, \theta, z$	cylindrical coordinate
$sat$	saturation
$s$	<div style="display: flex; align-items: center;"> <div style="font-size: 3em; margin-right: 5px;">{</div> <div> surface (surface property per mass)  solid phase </div> </div>

$SI$	surface instability
$SO$	shearing off
$TI$	turbulent impact
$WE$	wake entrainment
$t$	tangential to interface
$w$	wall
$x, y, z$	rectangular coordinate
$+, -$	$+$ and $-$ side of shock in macroscopic field
$1, 2$	phase 1 and phase 2

### ***Symbols and Operators***

$\mathcal{A}$	tensor
$\mathbf{A}$	vector
$A$	scalar
$\mathbf{A} \cdot \mathbf{B}$	dot product
$\mathbf{AB}$	dyadic product of two vectors (=tensor)
$\mathbf{A}:\mathbf{B}$	double dot product of two tensors (=scalar)
$\nabla \cdot$	divergence operator
$\nabla$	gradient operator
$\nabla_s \cdot$	surface divergence operator (Aris, 1962)
$(\mathcal{A})^+$	transposed tensor
$\frac{D_k}{Dt}$	$= \frac{\partial}{\partial t} + \widehat{\mathbf{v}}_k \cdot \nabla$
$\frac{D}{Dt}$	$= \frac{\partial}{\partial t} + \mathbf{v}_m \cdot \nabla$
$\frac{D_c}{Dt}$	$= \frac{\partial}{\partial t} + \mathbf{C}_k \cdot \nabla$
$\frac{D_i}{Dt}$	$= \frac{\partial}{\partial t} + \widehat{\mathbf{v}}_i \cdot \nabla$
$\frac{d_s}{dt}$	surface convective derivative with $\widehat{\mathbf{v}}_s$ (Aris, 1962)
$\overline{F}$	time average
$\overline{F}^w$	weighted mean value
$\overline{F}^{w_k}$	$k^{\text{th}}$ -phase weighted mean value
$\overline{\overline{F}}$	phase average



$\widehat{\psi}_k$	$k^{\text{th}}$ -phase mass weighted mean value
$\widehat{\psi}$	mixture mass weighted mean value
$F'_k$	fluctuating component with respect to mean value
$F'_{ki}$	fluctuation component with respect to surface mean value
$\overline{\overline{F_{(i)}}}, \overline{\overline{F_{ki}}}$	surface average
$\widehat{F_{ki}}$	mass flux weighted mean value at interfaces
$(\ )_{,\beta}$	surface covariant derivative (Aris, 1962)
$[\Delta t]_k$	with $(k=T,S,1,2)$ ; sets of time intervals
$\sum_k$	summation on both phases
$\sum_j$	summation on the interfaces passing in $\Delta t$ at $\boldsymbol{x}$

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