



**VIT<sup>®</sup>**  
**Vellore Institute of Technology**  
(Deemed to be University under section 3 of UGC Act, 1956)

## **Optimizing Electrolyser Size for Green Hydrogen Production using Differential Evolution Algorithm**

**Nia Sanjeev(22BRS1205), Aditya Shaw(22BRS1145)**

**School of Computer Science and Engineering, Vellore Institute of  
Technology, Chennai**

**BCSE306L : Artificial Intelligence Dr.**

**Suganya G.**

**April 17<sup>th</sup> 2025**

# 1 Introduction

The Differential Evolution (DE) algorithm is a robust evolutionary optimization technique for solving complex, non-linear, and multi-dimensional problems. It excels at optimizing real-valued parameters by iteratively refining a population of candidate solutions. This report examines a real-world application of DE in optimizing the size and cost of electrolyzers coupled with offshore wind farms (OWFs) for green hydrogen production, as detailed in a 2025 study by Dinh et al. [1] in the *International Journal of Hydrogen Energy*. The study uses DE to minimize the levelised cost of hydrogen (LCOH<sub>2</sub>), supported by mathematical models for wind resources and OWF power output.

## 2 Use Case: Optimizing Electrolyser Size for Green Hydrogen Production

### 2.1 Background

Green hydrogen, produced via electrolysis using renewable sources like offshore wind, is a key solution for reducing CO<sub>2</sub> emissions. Electrolyzers split water into hydrogen and oxygen using electricity, and when powered by renewables, the process is carbon-free. The study focuses on integrating electrolyzers with OWFs, requiring precise sizing to minimize LCOH<sub>2</sub>, the cost per kilogram of hydrogen over the project's lifetime. DE is used to determine the optimal electrolyser capacity for two setups: Offshore Electrolyser (Offshore-EL, electrolyser on an offshore platform) and Onshore Electrolyser (Onshore-EL, electrolyser onshore, powered via HVDC transmission).

### 2.2 Problem Statement

The objective is to minimize LCOH<sub>2</sub> by optimizing the electrolyser capacity relative to the OWF's power output. Key challenges include:

- Balancing electrolyser size, capital costs (e.g., equipment, infrastructure), and hydrogen production efficiency.
- Accounting for variable wind speeds that affect energy availability.
- Managing cost differences between offshore and onshore configurations, such as hydrogen pipelines versus HVDC cables.

### 2.3 Algorithm of Differential Evolution

DE iteratively optimizes the electrolyser capacity, expressed as a percentage of the OWF's 600 MW capacity. The algorithm follows these steps:

1. **Initialization:** A population of candidate electrolyser capacities is generated, each a real-valued ratio (e.g., 0.9 for 90% of OWF capacity).
2. **Mutation:** For each individual  $x_i$  in the population, a mutant vector is created:

$$v_i = x_{r1} + F \cdot (x_{r2} - x_{r3})$$

where  $x_{r1}, x_{r2}, x_{r3}$  are randomly chosen individuals, and  $F$  is the mutation factor (typically 0.5–1), controlling the step size.

3. **Crossover:** A trial vector is formed by combining the mutant vector  $v_i$  with the parent  $x_i$ , using a crossover probability  $CR$  (typically 0.8–1).

4. **Selection:** The trial vector's  $\text{LCOH}_2$  is calculated, and the individual with the lower  $\text{LCOH}_2$  is retained.
5. **Iteration:** The process repeats until  $\text{LCOH}_2$  stabilizes, as shown in the study's convergence graphs (Fig. 8).

## 2.4 Mathematical Models

The DE algorithm operates within a techno-economic framework, using the following equations:

1. **Wind Speed Distribution (Weibull Function):** Wind speed  $v$  is modeled using the Weibull probability density function to capture variability:

$$f_w(k, C) = \frac{k}{C} \left( \frac{v}{C} \right)^{k-1} e^{-\left( \frac{v}{C} \right)^k}$$

where:

- $k$ : Shape parameter (dimensionless), affecting the distribution's shape.
- $C$ : Scale parameter (m/s), related to average wind speed.
- $v$ : Wind speed (m/s).
- $e$ : Base of the natural logarithm ( $\approx 2.718$ ).

This equation determines the likelihood of different wind speeds, influencing OWF energy output.

2. **OWF Power Output:** The power output of the OWF at wind speed  $v$  is calculated using a piecewise function:

$$P_{\text{OWF},w}(v) = \begin{cases} 0, & \text{if } v < v_{\text{ci}} \text{ or } v \geq v_{\text{co}} \\ 0.5 \cdot \rho \cdot c_p \cdot A_{\text{swept}} \cdot v^3 \cdot N_{\text{wt}}, & \text{if } v_{\text{ci}} \leq v < v_r \\ P_r \cdot N_{\text{wt}}, & \text{if } v_r \leq v < v_{\text{co}} \end{cases}$$

where:

- $\rho$ : Air density ( $\text{kg/m}^3$ ).
- $c_p$ : Power coefficient of the turbine (dimensionless, typically 0.4–0.5).
- $A_{\text{swept}}$ : Swept area of the turbine rotor ( $\text{m}^2$ ).
- $v$ : Wind speed (m/s).
- $N_{\text{wt}}$ : Number of turbines (40 in the case study).
- $P_r$ : Rated power per turbine (15 MW).
- $v_{\text{ci}}$ : Cut-in wind speed (m/s).
- $v_{\text{co}}$ : Cut-out wind speed (m/s).
- $v_r$ : Rated wind speed (m/s).

This equation calculates the energy available for electrolysis, critical for hydrogen production.

3. **Levelised Cost of Hydrogen ( $\text{LCOH}_2$ ):** The objective function,  $\text{LCOH}_2$ , is:

$$\text{LCOH}_2 = \frac{\text{Total Discounted Costs}}{\text{Total Hydrogen Production}}$$

where:

- **Total Discounted Costs:** Sum of capital costs (electrolyser, turbines, foundations, pipelines/HVDC) and operational costs, discounted at 8% over the project lifetime (€).
- **Total Hydrogen Production:** Annual hydrogen output (kg), based on electrolyser capacity, efficiency, and OWF power output.

DE minimizes  $\text{LCOH}_2$  by adjusting the electrolyser capacity.

4. **Water Consumption for Electrolysis:** Water needed for hydrogen production is:

$$V_{\text{H}_2} = V_{\text{H}_2\text{O}} \cdot \frac{P_{\text{EL, rated}} \cdot \eta}{\text{LHV}_{\text{H}_2}}$$

where:

- $V_{\text{H}_2\text{O}}$ : Water consumption per kg of hydrogen ( $0.015 \text{ m}^3/\text{kg}$ ).
- $P_{\text{EL, rated}}$ : Rated power of the electrolyser (MW).
- $\eta$ : Stack efficiency of the electrolyser (dimensionless, typically 0.6–0.8).
- $\text{LHV}_{\text{H}_2}$ : Lower heating value of hydrogen ( $33.3 \text{ kWh/kg}$ ).

This ensures water requirements are included in the cost model.

## 2.5 Population Features in DE

The population consists of candidate electrolyser capacities with these features:

1. **Electrolyser Capacity Ratio:**

- Each individual is a real-valued ratio of electrolyser capacity to OWF capacity (e.g., 0.9141 for 548.46 MW).
- Range: 0% to 100%, with optimal ratios of 91.41% (Offshore-EL) and 94.54% (Onshore-EL).

2. **Population Size:**

- Typically 10–100 individuals (not specified in the study), balancing exploration and computational efficiency.

3. **Fitness Evaluation:**

- Fitness is  $\text{LCOH}_2$ , calculated using the techno-economic model and the above equations.

4. **Diversity and Evolution:**

- Mutation and crossover generate new capacities, ensuring diverse exploration.
- The population evolves over iterations, converging to optimal capacities (Fig. 8).

## 3 Case Study Details

The study optimizes a 600 MW OWF near Cork, Ireland ( $51^\circ 38' 24.0''\text{N}$ ,  $7^\circ 42' 36.0''\text{W}$ ), with 40 turbines (15 MW each) in a  $4 \times 10$  layout. Proton Exchange Membrane (PEM) electrolysers are used for their fast response to variable wind energy. Costs are projected for 2030, with an 8% discount rate. DE optimizes capacities for Offshore-EL and Onshore-EL configurations.

## 4 Results

DE yielded:

- **Optimal Electrolyser Capacity:**
  - Offshore-EL: 91.41% (548.46 MW),  $\text{LCOH}_2 = \text{€}3.7901/\text{kg}$ , hydrogen production = 57.55 kt/year.
  - Onshore-EL: 94.54% (567.24 MW),  $\text{LCOH}_2 = \text{€}4.292/\text{kg}$ , hydrogen production = 55.5 kt/year.
- **Cost Comparison** (Table 4):
  - Offshore-EL had lower  $\text{LCOH}_2$  than Onshore-EL due to reduced transmission losses, despite higher capital costs (€1764M vs. €1974M).
  - Non-optimal ratios (e.g., 60%, 100%) increased  $\text{LCOH}_2$ , showing DE’s precision.
- **Sensitivity Analysis** (Table 5):
  - Discount rate was most influential ( $\pm 1\%$  change  $\rightarrow$  0.65%  $\text{LCOH}_2$  change).
  - Turbine costs ( $\pm 1\% \rightarrow$  0.37–0.41%  $\text{LCOH}_2$  change) and wind resources also mattered.
- **Spatial Insights:**
  - $\text{LCOH}_2$  maps for Ireland’s offshore areas, based on wind, depth, and port proximity, aid project planning.

## 5 Impact and Significance

DE’s application shows its power in complex energy optimization. By minimizing  $\text{LCOH}_2$ , it enhances green hydrogen’s viability. Implications include:

- **Policy:** Low-interest loans can reduce discount rates, lowering  $\text{LCOH}_2$ .
- **Site Selection:** Strong wind resources cut costs.
- **Technology:** PEM electrolyzers suit offshore variability.

## 6 Comparison with Other Methods

DE surpasses gradient-based methods because:

- It handles non-linear, non-differentiable functions like  $\text{LCOH}_2$ .
- It avoids local optima via population diversity.
- It’s efficient for multi-parameter problems.

## 7 Conclusion

The DE application in optimizing electrolyser size for green hydrogen, as shown by Dinh et al. [1] (2025), is a strong real-world case. Supported by clear equations like the Weibull distribution and OWF power output, DE minimizes  $\text{LCOH}_2$ , finding optimal capacities (91.41% for Offshore-EL, 94.54% for Onshore-EL). This highlights DE’s role in renewable energy optimization, offering a blueprint for AI-driven sustainable energy solutions.

## References

- [1] Dinh, et al. (2025). Optimizing Electrolyser Size for Green Hydrogen Production Using Differential Evolution. *International Journal of Hydrogen Energy*. .