

ANSWERS TO EXERCISES

$$1.4^* \quad u_r = \frac{Ur}{2(H_0 - Ut)} \quad u_z = -\frac{Uz}{H_0 - Ut}$$

$$1.5 \quad \text{a) } u_y = \sum_i A_i \sin(k_i x) \cos(k_i y) \quad \text{b) } P = -\frac{1}{4} \rho A^2 [\cos(2kx) + \cos(2ky)]$$

$$1.8 \quad F = \frac{1}{2} \rho g L h (2H - h) \quad \text{a) } T = \frac{1}{6} \rho g L h^2 (3H - h) \quad \text{b) } T = \frac{1}{4} \rho g L^2 h (2H - h)$$

$$1.9 \quad \mathbf{F}_{\text{per unit length}} = -\hat{\mathbf{n}} \frac{g}{2 \sin \theta} H^2 \left(\rho_0 + \frac{\alpha H}{3} \right)$$

$$1.11 \quad dF_{x, \text{per unit length}} = \rho g \frac{R^2}{4} \quad dF_{z, \text{per unit length}} = \frac{5 \rho g R^2}{4}$$

2.2 Note, z_f is continuous at $r = R$

$$z_f = \frac{\Omega^2 r^2}{2g}, \quad r < R$$

$$z_f = -\frac{\Omega^2 R^4}{2gr^2} + \frac{\Omega^2 R^2}{g}, \quad r > R$$

$$\Delta h = \frac{\Omega^2 R^2}{g}$$

1.4** Note, a quasi-stationary flow ($H_0 \gg Ut$), there is a typing error in the preliminary schedule where the problem is given.

$$P = P_{atm} + \frac{\rho U^2}{8H_0^2} (R^2 - r^2) \quad P(r=0) = P_{atm} \frac{\rho U^2 R^2}{8H_0^2} \quad F_{P, flow} = \frac{\rho U^2 \pi R^4}{16H_0^2}$$

$$2.3 \quad Q = US = \frac{\pi}{4} D^2 \sqrt{2(\Theta - 1)gH}$$

$$2.4 \quad \mathbf{F} = (P_1 + \rho U_1^2) S_1 \mathbf{e}_y + (P_1 + \frac{1}{2} \rho U_1^2 (1 + \frac{S_1^2}{S_2^2})) S_2 (\cos \alpha \mathbf{e}_y - \sin \alpha \mathbf{e}_x)$$

The coordinate system has been chosen as $\hat{\mathbf{n}}_1 = -\mathbf{e}_y$ and \mathbf{e}_x points to the right ($\mathbf{e}_x \perp \mathbf{e}_y$).

$$2.6 \quad \mathbf{F}_{xy} = \mathbf{e}_x \sqrt{3} \rho g (h_2 S_2 - h_1 S_1) + \mathbf{e}_y \rho g [h_1 S_1 + h_2 S_2 - \frac{2}{S_3} (\sqrt{h_1} S_1 + \sqrt{h_2} S_2)^2]$$

$$\mathbf{F}_z = -\mathbf{e}_z 2 \rho g \sqrt{h_3} (\sqrt{h_1} S_1 + \sqrt{h_2} S_2)$$

The coordinate system has been chosen as x-axis to the right, y-axis backwards in the direction of the water supply pipe, and z-axis upwards.

$$2.7 \quad a) \quad U = U_2 = \sqrt{\frac{2gL}{S_2^2 - S_3^2}} S_3 \quad b) \quad h = h_\infty + (h_0 - h_\infty) \left(1 - \frac{S_1}{S_0} \sqrt{\frac{gt^2}{2(h_0 - h_\infty)}}\right)^2,$$

where h_0 and h_∞ are the height of the fluid level in the reservoir at the beginning (A) and the height when the flow in the pipe stops after a long time, respectively.

$$2.10 \quad a) \quad S_1 = \frac{S_0}{2}(1 + \cos \theta), \quad S_2 = \frac{S_0}{2}(1 - \cos \theta) \\ b) \quad \mathbf{F}_p = \hat{\mathbf{n}}_p \rho S_0 (U_0 - U_p)^2 \sin \theta, \text{ where the unit normal of the plate } (\hat{\mathbf{n}}_p) \text{ has been defined that it has a component in the direction of the } U_p. \\ c) \quad W_{max} = \frac{4}{27} \rho S_0 U_0^3 \sin^2 \theta \text{ when } U_p = \frac{U_0}{3}$$

$$2.13 \quad \phi = \frac{Ar^2}{4} - \frac{Az^2}{2} \quad u_r = \frac{Ar}{2} \quad u_z = -Az, \text{ A is a constant}$$

$$zr^2 = C, \text{ (C is a constant) for stream lines} \quad P = P_s - \frac{\rho A^2}{2} \left(z^2 + \frac{r^2}{4}\right)$$

2.14 Note, in a) we calculate only the pressure difference between the pressure exerted on the plate from the left and the pressure at a location far away from the plate in the stagnation zone.

$$a) \quad \Delta P = \frac{\rho U^2}{2} \frac{S_t^2}{(S_t - S_p)^2} \quad b) \quad F = \frac{\rho U^2}{2} \frac{S_t S_p^2}{(S_t - S_p)^2}$$

$$2.15 \quad F_{lift}/L_z \text{ straightforward, } F_{drag}/L_z = -\rho U \Gamma \tan \alpha$$

$$5.1 \quad a) \quad U_m = \frac{2}{3} U_0 \quad b) \quad F_0 = 0.27 F_m$$

$$5.3 \quad T \propto \mu \Omega R^3$$

$$5.4 \quad F \propto \sqrt{\frac{\mu^3 U S}{\rho L}}$$

$$5.7 \quad R \propto t^{2/5}$$

$$5.10 \quad u_x = \frac{\rho g}{2\mu} \sin \alpha (R - y)y, \quad \text{discharge per unit length } \frac{Q}{L_z} = \frac{\rho g}{12\mu} \sin \alpha R^3$$

5.11 Note, we find u_x , $u_{x,max}$ and the viscous stress acting on the lower plate. In the selected coordinate system x axis is to the right along the lower plate.

$$u_x = \frac{\rho g \sin \alpha}{2 \mu} (2R - y)y \quad u_{x,max} = \frac{\rho g \sin \alpha}{2 \mu} R^2 \quad \text{Viscous stress } \frac{F}{S} = \rho g R \sin \alpha$$

$$5.12 \quad U = \frac{Rg \sin \alpha}{\mu S} (M + \rho R S / 2)$$

$$5.13 \quad u = u_2 = \frac{\Delta P}{4\mu L}(r^2 - R_2^2) + [U + \frac{\Delta P}{4\mu L}(R_2^2 - R_1^2)] \frac{\ln(r/R_2)}{\ln(R_1/R_2)}$$

$$5.14 \quad h = h_\infty + (h_0 - h_\infty)\exp(-t/\tau), \quad \text{where typical time scale } \tau = \frac{8\mu LS_0}{\pi\rho g R^4}$$

$$5.15 \quad u_{max} = \frac{3}{2}U \frac{x}{H}$$

$$5.24 \quad u_x = U \exp(-\sqrt{\frac{\omega}{2\nu}}y) \sin(\omega t - \sqrt{\frac{\omega}{2\nu}}y)$$

$$E1 \quad U = (1 - \alpha)g\tau[1 - \exp(-\frac{t}{\tau})], \quad \text{where } \tau = \frac{M}{6\pi\mu R}$$

$$6.1 \quad F_{drag}/L_z = 1.32\rho\nu U \sqrt{\frac{UL}{\nu}}$$

$$7.3 \quad T = T_0 + \Theta \exp(-\alpha x) \sin(\pi y/R) \sin(\pi y/R)$$

$$7.4 \quad T = T_0 + \Theta \frac{x}{R} \quad u_z = \frac{g\alpha\Theta}{6R\nu}(R^2 - x^2)x$$