# The JHU Turbulence Databases (JHTDB)

#### TURBULENT CHANNEL FLOW DATA SET

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The turbulent channel flow database is produced from a direct numerical simulation (DNS) of wall bounded flow with periodic boundary conditions in the longitudinal and transverse directions, and no-slip conditions at the top and bottom walls. In the simulation, the Navier-Stokes equations are solved using a wall-normal, velocity-vorticity formulation [1]. Solutions to the governing equations are provided using a Fourier-Galerkin pseudo-spectral method for the longitudinal and transverse directions and seventh-order Basis-splines (B-splines) collocation method in the wall normal direction. Dealiasing is performed using the 3/2-rule [3]. Temporal integration is performed using a low-storage, third-order Runge-Kutta method. Initially, the flow is driven using a constant volume flux control (imposing a bulk channel mean velocity of U=1) until stationary conditions are reached. Then the control is changed to a constant applied mean pressure gradient forcing term equivalent to the shear stress resulting from the prior steps. Additional iterations are then performed to further achieve statistical stationarity before outputting fields.

The simulation is performed using the petascale DNS channel flow code (PoongBack) developed at the University of Texas at Austin by Prof. Robert Moser's research group [2]. In the wall-normal, velocity-vorticity formulation, the pressure is eliminated from the governing equations. In order to obtain the pressure field for the database, we subsequently implemented, in PoongBack, the pressure solver which solves the pressure Poisson equation given as

$$\nabla^2 p = -\nabla \cdot [\nabla \cdot (\boldsymbol{u} \otimes \boldsymbol{u})] \tag{1}$$

where p is the pressure and u the velocity. The Neumann boundary condition, expressed as

$$\frac{\partial p}{\partial y} = \nu \frac{\partial^2 v}{\partial y^2} \tag{2}$$

where  $\nu$  is the molecular viscosity and v the wall-normal velocity component, is used at the top and bottom walls. This calculation is performed independently from the velocity field solution only when outputting fields.

The simulation is performed for approximately 1/2 of a flow through time (another 1/2 flow through time will be added in the near future). The 3 component velocity vector and pressure fields are stored every 5 time steps, resulting in 2000 frames of data. Information regarding the simulation setup and resulting statistical quantities are listed below.

Note that the averaging operation for mean and other statistical quantities is applied in time and over x-z planes.

### Simulation parameters

- Domain Length:  $L_x \times L_y \times L_z = 8\pi h \times 2h \times 3\pi h$  where h is the half-channel height (h = 1 in dimensionless units)
- Grid:  $N_x \times N_y \times N_z = 2048 \times 512 \times 1536$  (wavemodes);  $3072 \times 512 \times 2304$  (collocation points); data is stored at the wavemode resolution, i.e.  $N_x \times N_y \times N_z = 2048 \times 512 \times 1536$  at grid point nodes in physical space.
- Viscosity:  $\nu = 5 \times 10^{-5}$  (non-dimensional)
- Mean pressure gradient: dP/dx = 0.0025 (non-dimensional)
- DNS Time step:  $\Delta t = 0.0013$  (non-dimensional)
- Database time step:  $\delta t = 0.0065$  (non-dimensional)
- Time stored: t = [0, 12.993]

## Flow statistics averaged over t = [0, 12.993]

- Bulk velocity:  $U_b = 0.99992$ 

- Centerline velocity:  $U_c = 1.13195$ 

- Friction velocity:  $u_{\tau} = 4.99857 \times 10^{-2}$ 

- Viscous length scale:  $\delta_{\nu} = \nu/u_{\tau} = 1.00029 \times 10^{-3}$ 

- Reynolds number based on bulk velocity and full channel height:  $Re_b = \frac{U_b 2h}{V} = 3.99970 \times 10^4$ 

- Centerline Reynolds number:  $Re_c = U_c h/\nu = 2.26391 \times 10^4$ 

- Friction velocity Reynolds number:  $Re_{\tau} = u_{\tau}h/\nu = 9.99713 \times 10^2$ 

#### Grid spacing in viscous units

- x direction:  $\Delta x^{+} = 12.2683$ 

- y direction at first point:  $\Delta y_1^+ = 1.65259 \times 10^{-2}$ 

- y direction at center:  $\Delta y_c^+ = 6.15728$ 

- z direction:  $\Delta z^{+} = 6.13416$ 

In the following figures several quantities from the simulation are show. Shown in Figure 1 is the computed friction Reynolds for the time interval in the database. In Figure 2 the mean velocity is show along with the standard  $U^+$  profiles in the viscous sublayer and log-layer. The viscous and turblent shear stresses, Reynolds normal stresses, mean pressure, pressure variance, and velocity-pressure covariances are shown in Figures 3–6. In the remaining plots, the power spectral densities of velocity and pressure are shown for various  $y^+$  locations. Streamwise spectra are shown in Figure 7, whereas span wise spectra are shown in Figure 8.

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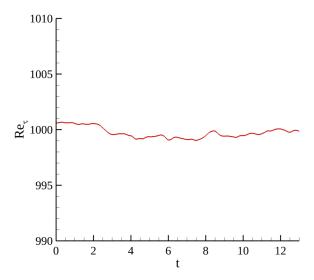


Figure 1: Friction velocity Reynolds number during the channel flow simulation during the database time interval

# References

- [1] J. Kim, P. Moin, and R. Moser. Turbulence statistics in fully developed channel flow at low reynolds number. *J. Fluid Mech.*, 177:133–166, 1987.
- [2] M. Lee, N. Malaya, and R. D. Moser. Petascale direct numerical simulation of turbulent channel flow on up to 786k cores. Supercomputing (SC13), 2013.
- [3] S. A. Orszag. On the elimination of aliasing in finite-difference schemes by filtering high-wavenumber components. *J. Atmos. Sci.*, 28:1074–1074, 1971.

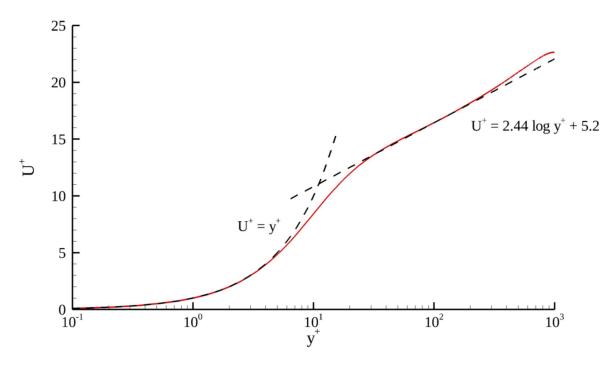


Figure 2: Mean velocity profile in viscous units. Standard values of  $\kappa=0.41$  and B=5.2 are used in the log-law (dashed line) for reference.

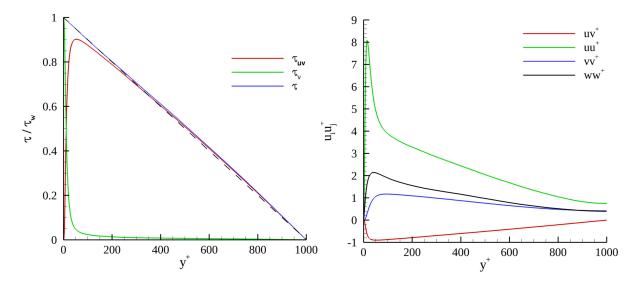


Figure 3: Mean viscous, turbulent, and total shear stress normalized by the wall stress

Figure 4: Velocity covariances in viscous units

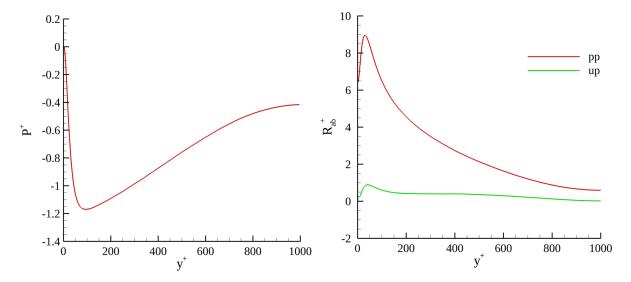


Figure 5: Mean pressure profile in viscous units

Figure 6: Pressure variance and pressure-velocity covariance in viscous units

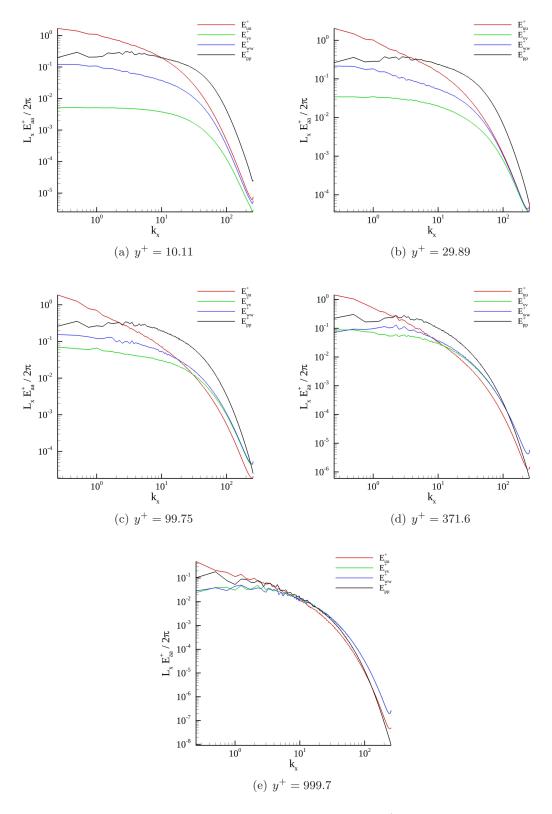


Figure 7: Streamwise power spectral densities at various  $y^+$  locations as function of  $k_x$ 

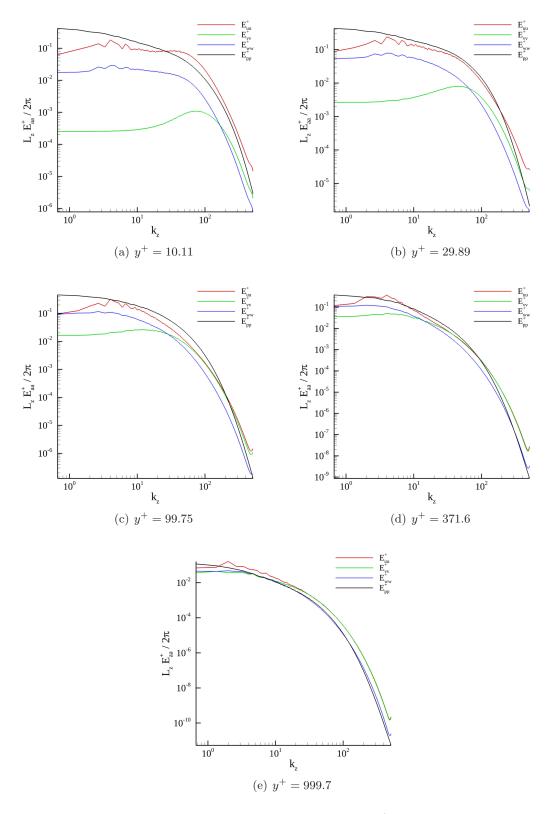


Figure 8: Spanwise power spectral densities at various  $y^+$  locations as function of  $k_z$