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Satisficing Infinite-horizon Model Predictive Control Implementation and Simulation

Relatório submetido à Universidade Federal de Santa Catarina
como requisito para a aprovação da disciplina:
DAS 5501: Estágio em Controle e Automação

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Florianópolis, 2017

Satisficing Infinite-horizon Model Predictive Control Implementation and Simulation

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Esta monografia foi julgada no contexto da disciplina

DAS 5501: Estágio em Controle e Automação Industrial

e aprovada na sua forma final pelo

Curso de Engenharia de Controle e Automação

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Abstract

The purpose of this work is to give guidelines for the implementation of Model Predictive Control (MPC) algorithms. MPC is an advanced control technique that is adopted frequently in industry. Different algorithms of MPC are explored here, starting with the basic Generalized Predictive Control (GPC) until the more complex ones with infinite output horizon (IHMPC) and the Distributed Satisficing Predictive Control proposed by Lima [1]. The final algorithm to be developed (S-IHMPC) intends to combine the benefits of the last two approaches: guarantees of nominal stability given by the infinite output horizon and the automatic tunning delivered by the distributed satisficing approach. All implementations and simulations use free software and they are developed with Python. This report shows the initial results of a long-term project and brings as result blocks of reusable code and tools that can be useful both in academia and industry. The code of GPC algorithm is fully developed and presented here and, for the S-IHMPC, the initial code is presented alongside the guidelines for future works.

Keywords: Model Predictive Control, Infinite horizon.

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1 Introduction

Model Predictive Control (MPC) is an advanced control technique that is widely adopted in industry. An MPC algorithm computes control inputs with the solution of a real-time optimization problem that takes into consideration the system's current state, future targets, possible disturbances and constraints that ensure integrity of the system. A lot of advantages are associated with MPC: for multiple input multiple output (MIMO) systems, MPC takes advantage of the subsystems coupling to use it to enhance its performance (rather than deploying multiple single input single output (SISO) PID's that treat other subsystems as disturbances); MPC handles dead-time process intrinsically by its construction, among other benefits [2].

Despite all of MPC advantages, there are some problems regarding practical implementation limitations. The tunning of the controller's parameters and the setting of weights in the cost function (categoric tunning) is not an easy task and can lead to system's instability if not properly tuned. One way to guarantee nominal stability of the system is to consider an infinite output horizon (IHMPC) [3]. For the practical implementation of IHMPC, a scheme based on the Output Prediction Oriented Model (OPOM) developed by Odloak [4] is used here. In addition to the IHMPC, a Distributed Satisficing Predictive Control approach developed by Lima [1] that delivers automatic tuning and dynamically adjusts the weights of each input of cost function (situational tunning) can be considered.

All the algorithms are implemented using free software, the open source programming language Python is the core, optimization libraries are used in order to solve quadratic programming problems and libraries for efficient mathematical operations implementations are adopted.

This work contributed with the development of computational tools for the control of industrial processes. It also produced a framework to implement MPC controllers based on the object oriented paradigm that will be used to continue this work. This report presents the internship activities developed in the first semester of 2017. The work will be continued for the next semester as part of a long-term project. The main activities of the internship include:

- Study MPC and optimization topics.
- Learn and research Python packages for the implementations.
- Study and implement the Generalized Predictive Control (GPC) algorithm.
- Study and implement the OPOM for the IHMPC scheme.

- Apply the algorithms in a case study of a process in the chemical industry.

This work is structured as follows: chapter 2 gives the necessary background on MPC theory to understand the concepts behind the algorithms; chapter 3 presents the case study and shows the algorithm implementations and simulations. First, a GPC algorithm is presented, in order to serve as a standard of comparison for the more complex algorithms to be developed. After that the OPOM implementation for the IHMPC is presented and guidelines for the S-IHMPC are given; chapter 4 gives a conclusion to the work.

2 Model Predictive Control

2.1 MPC Overview

The term model predictive control (MPC) does not designate a specific control strategy but a very ample range of control methods that make explicit use of a model of the process to obtain the control signal by minimizing an objective function. The principal ideas of the predictive control family are [5]:

- Explicit use of a model to predict the process output at future time instants (horizon).
- Calculation of a control sequence minimizing an objective function.
- Receding strategy, so that at each instant the horizon is displaced towards the future, which involves the application of the first control signal of the sequence calculated at each step.

2.1.1 MPC strategy

The methodology of all the controllers belonging to the MPC family is characterized by the following strategy illustrated in Figure 1:

1. The future outputs for a defined horizon N, called the prediction horizon, are predicted at each instant t using the process model. These predicted outputs $\hat{y}(t+k|t)$ for $k = 1, \ldots, N$ depend on the known values up to instant t (past inputs and outputs) and on the future control signals $u(t+k|t), k = 0, \ldots, N-1$, which are to be sent to the system and to be calculated.
2. The set of future control signals is calculated by optimizing a determined criterion in order to keep the process as close as possible to the reference trajectory $w(t+k)$ (which can be the set-point itself or a close approximation of it). This criterion usually takes the form of a quadratic function of the errors between the predicted output signal and the predicted reference trajectory. The control effort is included in the objective function in most cases. An explicit solution can be obtained if the criterion is quadratic, the model is linear and there are no constraints, otherwise an iterative optimization method has to be used. Some assumptions about the structure of the future control law are also made in some cases, such as that it will be constant from a given instant.

3. The control signal $u(t|t)$ is sent to the process whilst, the next control signals calculated are neglected, because at the next sampling instant $y(t+1)$ will already be known, and step 1 will be repeated with this new value and all the sequences will be brought up to date. Thus the $u(t+1|t+1)$ is calculated (which in principle will be different to $u(t+1|t)$ because of the new information available) using the receding horizon concept.

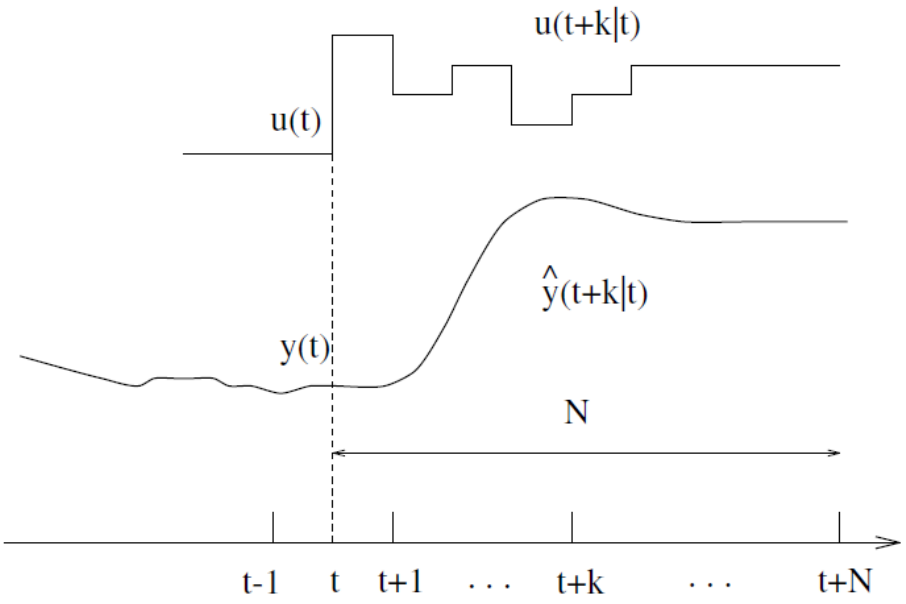


Figure 1 – MPC idea

2.1.2 MPC elements

All the MPC algorithms possess common elements and different options can be chosen for each one of these elements, which gives rise to different algorithms. These elements are

- **the prediction model**

  The process model plays a decisive role in the controller because it is necessary to calculate the predicted output at future instants $\hat{y}(t+k|t)$. The model can be divided into two parts: The actual process model and the disturbances model. Both parts are needed for the prediction.

  - Process model

    Practically every possible form of modeling a process appears in a given MPC formulation, the following being the most commonly used:

    * Impulse response

  - ∗ Step response
  - ∗ Transfer function

  In this work, step response and transfer function will be the main focus.

- **the objective function**

  The objective function sum up the difference between reference and predicted output through all the horizon. Terms including the weighted sum of the squared inputs and input moves along the control horizon are also considered, so one can prioritize one output of the system.

- **the procedure to obtain the control law.**

  As the MPC optimization problem is a quadratic program, it is solved with the interior point method or Newton method for example.

  – Constraints

    Possible constraints that can be applied to the problem can be on the output or the control action and generally, they represent physical constraints. These constraints are typically, Δu, u_{max}, u_{min}, saturation and operation limits for which the model are valid or security constraints.

2.2 Generalized Predictive Control

Generalized Predictive Control (GPC) is a scheme for MPC that has been widely accepted in both industry and academia. It can handle many different control problems for a wide range of plants, including unstable and integrating processes.

2.2.1 Prediction Model

The GPC approach to compute predictions is based on the CARIMA model [6]:

$$A(z^{-1})y(t) = z^{-d}B(z^{-1})u(t-1) + \frac{C(z^{-1})e(t)}{\Delta} \tag{2.1}$$

where $A(z^{-1})$ and $B(z^{-1})$ are polynomials with degrees n_a and n_b, d is the dead time, $\Delta(z^{-1}) = 1 - z^{-1}$, $e(t)$ is a white noise, $C(z^{-1})$ represents the stochastic characteristics of the noise (it is difficult to estimate in practice, a common choice is to set $C(z^{-1}) = 1$).

The output prediction $\hat{y}$ can be obtained from the solution of the following Diophantine Equation:

$$1 = \tilde{A}(z^{-1})E_j(z^{-1}) + z^{-j}F_j(z^{-1}) \tag{2.2}$$

where $\tilde{A}(z^{-1}) = \Delta A(z^{-1})$, $E_j(z^{-1})$ and $F_j(z^{-1})$ are recursively obtained by the polynomial division of 1 by $\tilde{A}(z^{-1})$.

From Equations (2.1) and (2.2), we find a expression to calculate the output predictions:

$$\hat{y}(t+j|t) = E_j B\,\Delta u(t+j-1) + F_j\,y(t) \tag{2.3}$$

The term $E_j B$ contains the coefficients of the step response of the system and it is normally represented by G_j. We can group the terms relative to past inputs and outputs as the free response. The prediction for the horizon $p = N_2 - N_1$ and considering the control horizon equal m is therefore calculated by:

$$\begin{bmatrix} \hat{y}(t+N_1|t) \\ \hat{y}(t+N_1+1|t) \\ \dots \\ \hat{y}(t+N_2|t) \end{bmatrix} = G \begin{bmatrix} \Delta u(t) \\ \Delta u(t+1) \\ \dots \\ \Delta u(t+m-1) \end{bmatrix} + F_u \begin{bmatrix} \Delta u(t-1) \\ \Delta u(t-2) \\ \dots \\ \Delta u(t-n_b) \end{bmatrix} + F_y \begin{bmatrix} \hat{y}(t+N_1-1|t) \\ \hat{y}(t+N_1-2|t) \\ \dots \\ \hat{y}(t+N_1-n_a|t) \end{bmatrix}$$

$$\hat{y} = G\Delta u + f \tag{2.4}$$

2.2.2 Control Algorithm

The objective of a GPC controller is to drive the output as close to the set-point as possible in a least-squares sense with the possibility of the inclusion of a penalty term on the input moves. Therefore, the manipulated variables are selected to minimize a quadratic objective that can consider the minimization of the future errors and the control effort:

$$J = \sum_{j=N_1}^{N_2} \delta(j)[\hat{y}(t+j|t) - \omega(t+j)]^2 + \sum_{j=1}^{N_u} \lambda(j)[\Delta u(t+j-1)]^2 \tag{2.5}$$

$$= (\hat{y}-\omega)^T Q_\delta (\hat{y}-\omega) + \Delta u^T Q_\lambda \Delta u \tag{2.6}$$

where Q_δ and Q_λ are the diagonal weight matrices with values of $\delta(j)$ and $\lambda(j)$, respectively, and ω is the output reference.

If $\hat{y}$ given in Equation (2.4) is introduced in Equation (2.6), then J becomes a function only of the future control increments Δu and the free response f. Rewriting the cost function in the matrix form and introducing $\hat{y}$:

$$J = \frac{1}{2}\Delta u^T H \Delta u + q^T \Delta u + f_0 \tag{2.7}$$

where $H = 2(G^T Q_\delta G + Q_\lambda)$, $q = 2G^T Q_\delta (f-\omega)$, $f_0 = (f-\omega)^T Q_\delta (f-\omega)$.

The algorithm to be implemented consist in minimize Equation (2.7), subject to some constraint, like $A\Delta u \leq b$, and apply only the first Δu to the current control value.

2.3 Infinite-horizon MPC

One frequently debated issue about MPC is the nominal stability of the strategy. It is of great interest an implementation of a stable controller independently of its tuning. In the literature, one can find basically three approaches concerning guarantees of stability [4]:

- state terminal constraints.
- state terminal set constraints.
- infinite output prediction horizon.

The first two approaches are based on the addition of constraints in the optimization problem in such a way that all the states converge to zero. It seems to be the simplest and more intuitive methods, however these strategies hold some issues: they reduce drastically the feasible region of the control problem, the attraction region is very sensitive to disturbances or big changes on the set point and the computational efforts to evaluate the control law at every instant are often impracticable.

The third strategy, considering an infinite output prediction horizon (IHMPC), was proposed by Rawlings and Muske (1993) [3] and the stability of the method was shown for stable and unstable systems subject to control input and state constraints. In general, the IHMPC approach transforms the infinite output horizon in a finite horizon through a weight in the terminal state of the objective function. The weight is obtained solving a Lyapunov equation.

2.3.1 Output Prediction Oriented Model

IHMPC works very well theoretically, however the terminal weight computation is a huge challenge to be performed on-line. Disturbances and big changes on the set point can make the implementation unfeasible. To solve this issue, a different model for the output prediction in the infinite horizon can be used: the Output Prediction Oriented Model (OPOM).

OPOM defines a prediction strategy based on a state-space model obtained from the step response of the system. In terms of computational effort, IHMPC with OPOM as prediction model, offers an equivalent solution comparing to terminal state constrained MPC, however one does not need to choose a prediction horizon. Besides ensuring nominal stability independently of tuning the matrix weights and parameters in the objective function.

The main ideas of the model of OPOM are:

- Divide the system in three parts according to its step response: steady state, poles dynamics and the integrating part. A state for each part of the system is created and its evolution along time is considered. Dividing the system, one can easily propose constraints directly on each state.

- Create a continuous output prediction model that can be analytically integrated.

  To clarify how OPOM is built, consider the following example:

- First order system. The system is represented by the transfer function $G(s) = \frac{k}{\tau s+1}$. The corresponding step response is giving by $s_p(t) = k - ke^{-t/\tau} = c_0 + c_1 e^{-t/\tau}$. And the Output Prediction Oriented Model of the system is giving by:

$$x_{k+1} = A\,x_k + B\,\Delta u_k \tag{2.8}$$

$$y_k(t) = C(t)x_k \tag{2.9}$$

  where $A = \begin{bmatrix} 1 & 0 \\ 0 & e^{-T/\tau} \end{bmatrix}$, $B = \begin{bmatrix} c_0 \\ c_1 e^{-T/\tau} \end{bmatrix}$, $C(t) = \begin{bmatrix} 1 & e^{-t/\tau} \end{bmatrix}$, $x = \begin{bmatrix} x^s \\ x^d \end{bmatrix}$, T is the sample time.

  Observe that, in Equation (2.9), $C(t)$ is not constant and depends on the prediction instant t, which is now a continuous variable. One can also observe that x^s and x^d represent the steady state and the pole dynamic evolution, respectively.

The previously example was just a small case were OPOM can be applied. A generalization of the model is made on [4], [7] and [8] for MIMO systems with multiple poles, integrator and dead time considerations.

2.4 Summary

In this chapter, it was presented a brief review of model predictive control. All the concepts required to fully understand the implementations of the algorithms in this work were shown. A general intuition on MPC, with the main idea of the strategy and its elements. Followed by specific strategies inside the context of MPC: GPC, an algorithm that can handle unstable and integrating systems; and the IHMPC (using OPOM to compute the predicted output) approach that guarantees stability for MPC.

3 Implementation, Simulation and Results

3.1 Implementation

All the implementations of MPC algorithms in this work are written in Python 3.6 (code can be found in the Appendix). The object oriented paradigm is used to produce a modular piece of software, where all the classes and their methods can be easily reused for different applications. Here we define a framework that defines how the code must be structured.

The framework consists in the construction of three main classes: one to represent the system, one to represent the controller and one to represent the simulation environment. Each class has its own attributes and methods as described below:

- Classes:

  1. **System model representation:** this class is built from the transfer function of a SISO system or a matrix of transfer functions of a MIMO system.

SystemModel
+ H: matrix of transfer functions + ny: number of system outputs + nu: number of system inputs
+ step_response(): return step responses of H

Table 1 – Class diagram representation of SystemModel

  2. **Controller:** this class represent the digital controller to be implemented. Its attributes contain the parameters to be tunned and its methods compute the control action. A class controller for each MPC algorithm is implemented.

Controller
+ system_model: SystemModel in wich the controller will be based on + Ts: sample time + p: output prediction horizon + m: control horizon + weights + constraints
+ calculate_control(): return next control action

Table 2 – Class diagram representation of Controller

3. **Simulation:** this class creates an environment for simulation. It is built giving the following inputs: one object of controller and one optional object of real system model for robustness analysis (if not passed, the model used by the controller is considered the same as the real model). A method is created for simulation running, passing the time of simulation as argument.

Simulation
+ controller: Controller + real_system: SystemModel
+ run(tsim): run simulation

Table 3 – Class diagram representation of Simulation

The following packages, available in the Python community, are required as dependencies of the implementation:

- Python packages

1. **Numpy:** the fundamental package for scientific computing with Python. It contains an efficient data structure (numpy.array) to handle mathematical operations with N-dimensional data.
2. **Scipy:** it offers a toolbox for engineering. In this work. the module of the library called *signal* is used for signal processing and operations with transfer functions.
3. **Cvxopt:** this package offers solvers for optimization problems. In particular, the quadratic programming solver is used for the MPC algorithms.
4. **Matplotlib:** it is used for visual analysis of the simulations.

3.2 Case Study

In this section, we illustrate an application of the algorithms proposed in this work. This case study is based on the ethylene oxide reactor system (Figure 2), presented by [4]. This is a typical example of the chemical process industry that exhibits stable and integrating poles.

The production of ethylene-oxide (EO) is based on the exothermic reaction

$$C_2H_4 + \frac{1}{2}O_2 \rightarrow C_2H_4O \tag{3.1}$$

The complete combustion of ethylene occurs through the undesirable secondary reaction

$$C_2H_4 + 3\,O_2 \rightarrow 2\,CO_2 + 2\,H_2O \tag{3.2}$$

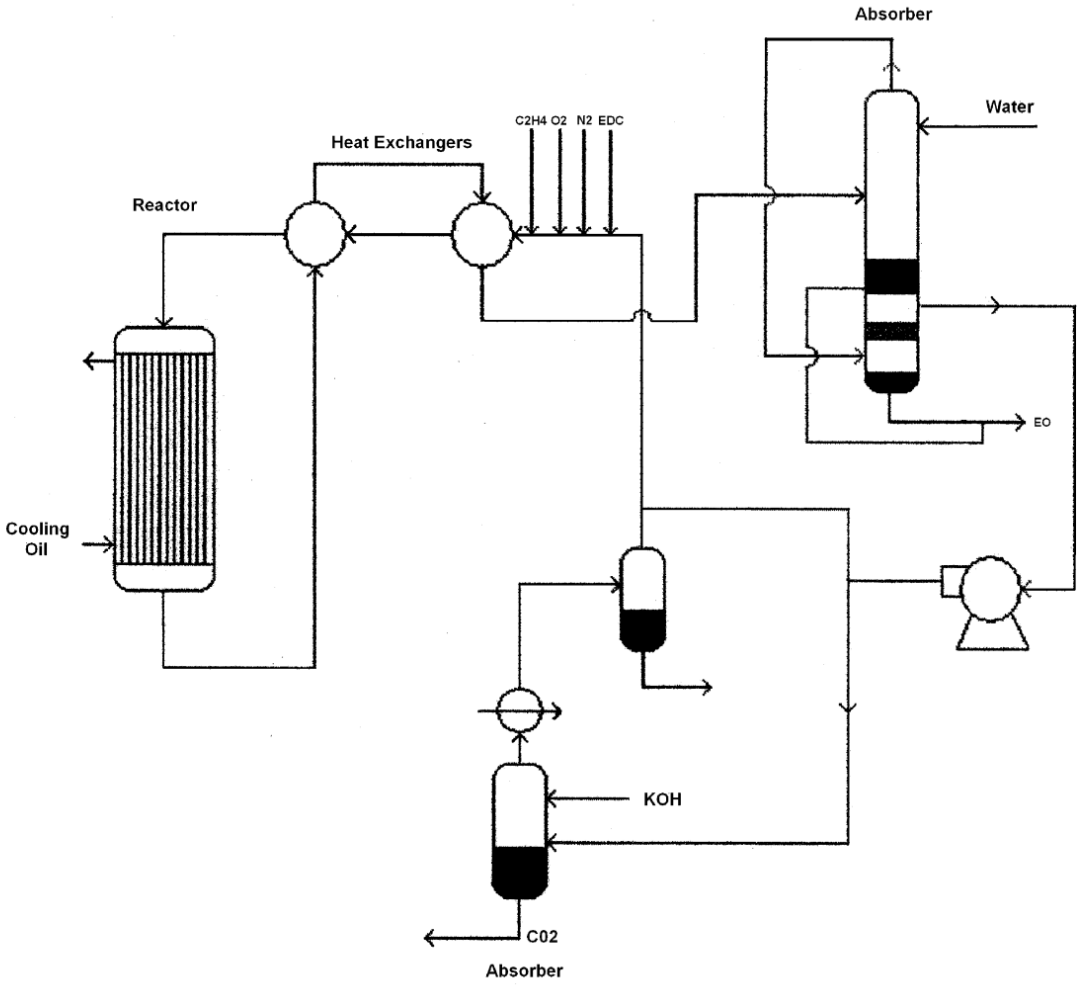


Figure 2 – Schematic representation of an industrial ethylene-oxide plant.

The gaseous mixture that leaves the reactor is sent to an absorber where the ethylene-oxide is extracted. The remaining gas is recycled through other chemical processes and it is mixed with the feed stream. One can observe that this procedure of recycling the gas introduces an integrating dynamic, since the introduction of a feed component in excess tends to increase the concentration of this component in the recycle gas continuously.

Typical process variables considered in the problem are:

- Manipulated variables (inputs)
  - the pure oxygen (O_2) feed flow rate
  - the ethylene (C_2H_4) feed flow rate
  - the nitrogen (N_2) feed flow rate
  - the temperature of cooling oil used in the reactor
  - the combustion inhibitor (EDC) feed flow rate
  - the potassium hydroxide flow rate, introduced in the second absorber

- Process variables (outputs)
  - the reaction selectivity, which is defined as the percentage of the reacted ethylene that is converted to ethylene-oxide
  - the molar fraction of ethylene in the gas stream at the entrance of the reactor
  - the temperature of reaction products in reactor
  - the system pressure
  - the molar fraction of oxygen in the gas stream at the entrance of the reactor

For simplicity and to compare results with published articles [7], we consider a small example of the ethylene-oxide system represented by the following matrix of transfer function:

$$H(s) = \begin{bmatrix} \frac{-0.19}{s} & \frac{-1.7}{19.5\,s+1} \\ \frac{-0.763}{31.8\,s+1} & \frac{0.235}{s} \end{bmatrix} \tag{3.3}$$

where each element $H_{i,j}$ of $H(s)$ represents the transfer function of the output/input pair (y_i, u_j).

3.3 GPC Implementation

In this section, we will present all the steps for the implementation of an MPC algorithm based on the GPC scheme. First, the construction of the GPC controller is presented, then a simulation for the case study is shown.

3.3.1 Controller Parameters

The controller implemented deals with both SISO and MIMO systems. It calculates actions for the nu inputs to control the ny outputs of the system. It uses an output prediction horizon of p samples and a control horizon of m samples. Two matrices of weights Q and R are used for the prediction error and control increment effort terms of the cost function, respectively. The constraint du_{max} in the magnitude of control increment is also passed to the controller. To sum up, Table 4 shows the GPC controller parameters:

Table 4 – Parameters of GPC controller

Parameter	**Description**
ny	number of system outputs
nu	number of system inputs
p	output prediction horizon
m	control action horizon
Q_δ	matrix of weights for the prediction error
Q_λ	matrix of weights for the control increment effort
Δu_{max}	maximum increment on the control input

3.3.2 Prediction Model

The construction of the prediction model starts with the creation of the *SystemModel* class. As stated before, this class stores the matrix of transfer functions of the system and it has a method to compute the step response of each transfer function. This method will be used to build the matrix G (Equation (2.4)).

The next step is to implement the controller's code, the *GPCController* class is built upon the *SystemModel*. In the controllers initialization all the parameters and weights passed by the user are all set up. Moreover, as the matrix G never changes, it can also be initiated, using the *SystemModel* to obtain the step response coefficients.

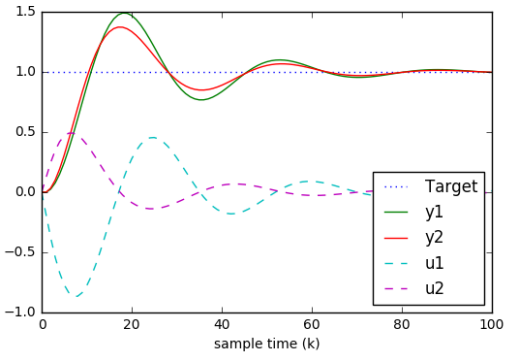
Finally, to complete the Equation (2.4) to become possible the output prediction calculation, the free response can be obtained recursively as described in the previous chapter.

3.3.3 Control Algorithm

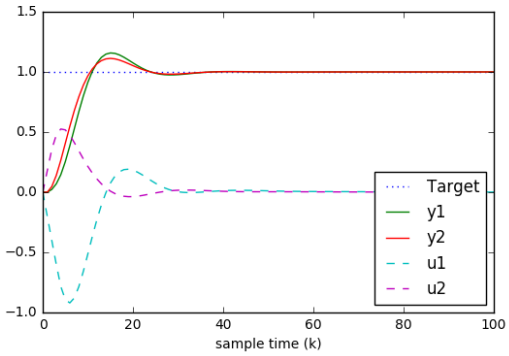
The control algorithm returns the next control action given as inputs the actual and the past inputs/outputs and the future set-points. This function is implemented as a method of the class *GPCController*. This method builds the matrices in equation (2.7) and gives them as input for the quadratic programming solver, which returns the next control actions.

3.3.4 Case Study Simulation

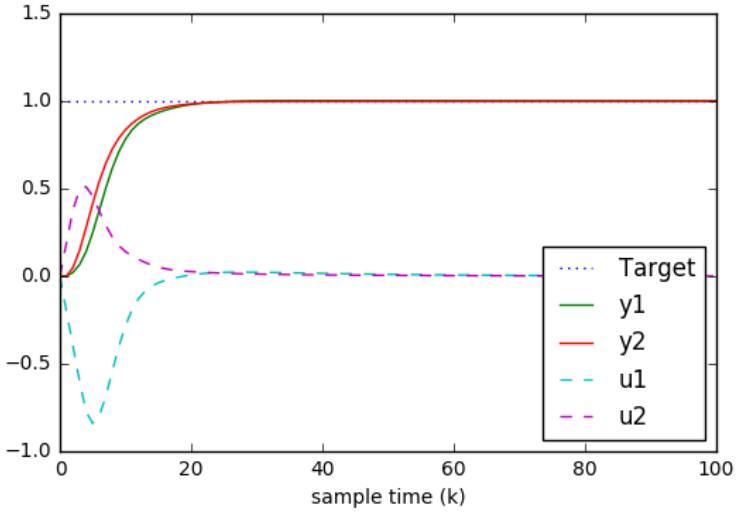
Different scenarios are simulated for the case study. First, the weight matrices are chosen and the prediction horizon p and the control horizon m are adjusted based on the response of a unit step in both output set-points. Once the horizon parameters are obtained, different changes in the set-point and different initial conditions are tested. Lastly, a robustness analysis varying the real gains of the system is done.



(a) Horizons: $m = 3$, $p = 5$. Overshoot = 50%



(b) Horizons: $m = 3$, $p = 7$. Overshoot = 15%



(c) Horizons: $m = 3$, $p = 10$. No overshoot

Figure 3 – Controller tuning - simulation of GPC algorithm

The simulations illustrated in Figure 3 show the process of tuning the controller until the system response does not exhibit overshoot. The adjusted controller parameters are presented in Table 5.

Table 5 – Parameters of Controller

ny	nu	p	m	Ts	Q_δ	Q_λ	Δu_{max}
2	2	10	3	1min	diag(1,...,1)	diag(10,...,10)	0.2

For the simulation in Figure 3c, the graphic in Figure 4 reveals the evolution of the primal objective value of the optimization problem along each sample.

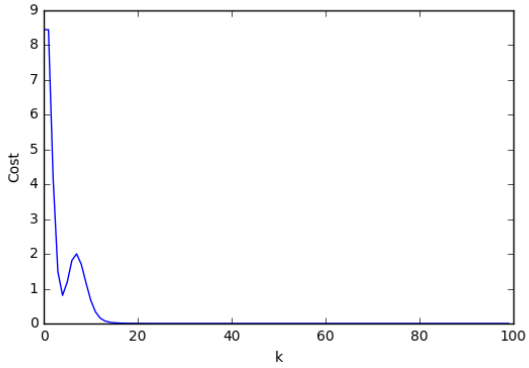
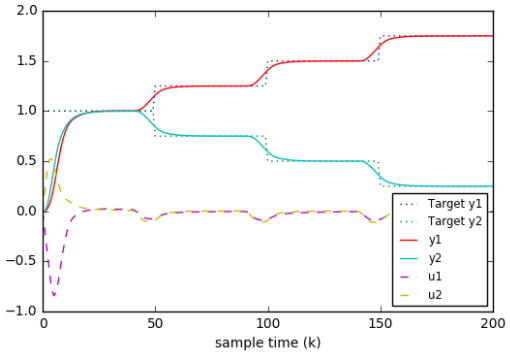
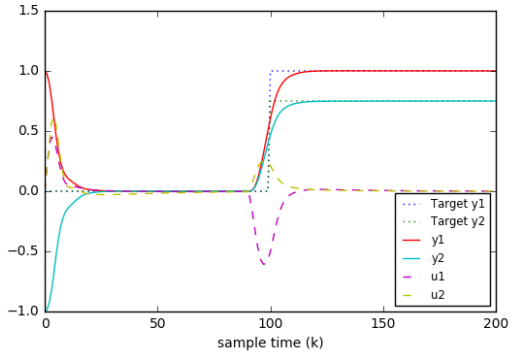


Figure 4 – Primal objective value

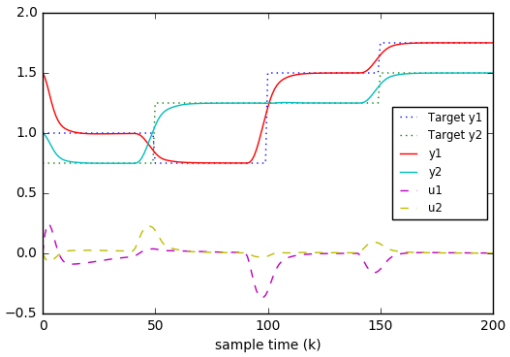
After the process of tunning the controller, other simulations were performed (Figure 5) in order to test different scenarios of the case study. First, a sequence of steps on the set-points was applied with output states initially null. Then, the initial states were set with different values for the next simulations. At last, a ramp signal was applied on the set-points.



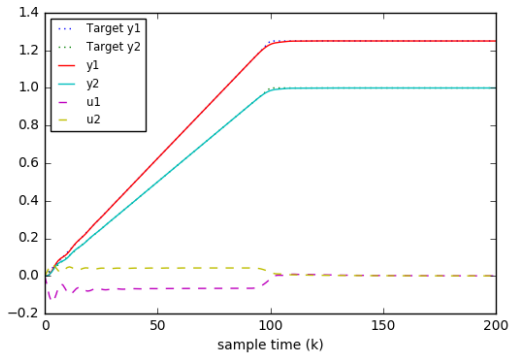
(a) Steps, with $y_1(0) = y_2(0) = 0$



(b) Steps, with $y_1(0) = 1$ and $y_2(0) = -1$



(c) Steps, with $y_1(0) = 1.5$ and $y_2(0) = 1$



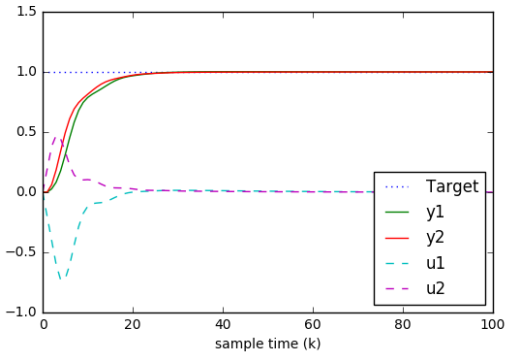
(d) Ramp, with $y_1(0) = y_2(0) = 0$

Figure 5 – Simulations for different changes on set-point

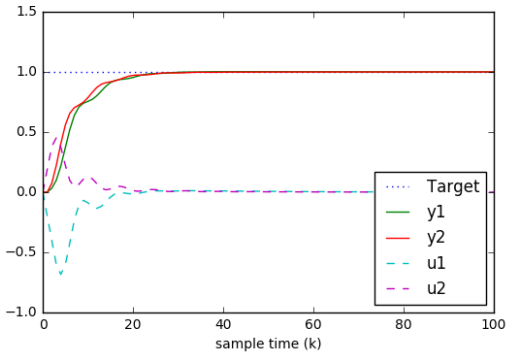
A robustness analysis is performed for the case where the gains of the system used as model for the controller and the real system are different. Errors of 25%, 50%, 75% and 100% in systems model gains are imposed. The results are shown in Figure 6.

We can conclude that the controller responds well to variations in the gain of the system. The response changes minimally till the 50% of gain error. From the 75% of gain error, the response starts to oscillate till the appearance of a limit cycle when the error reaches 100%.

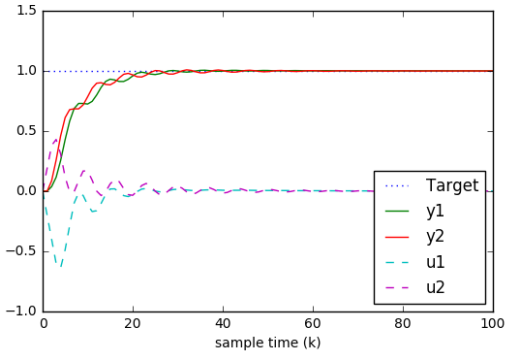
The controller can still be re-tuned in order to obtain better responses for large gain errors and remove the limit cycle. The simulations in Figure 7 show the processes of re-tuning the controller's parameters.



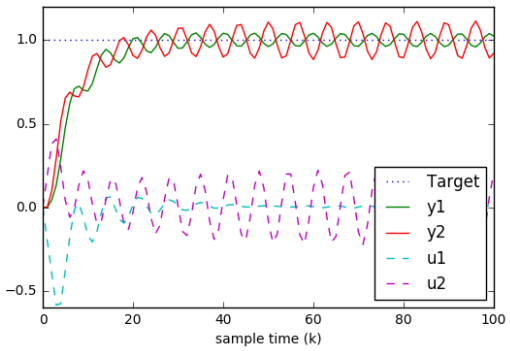
(a) $m = 3$, $p = 10$ and gain error = 25%



(b) $m = 3$, $p = 10$ and gain error = 50%

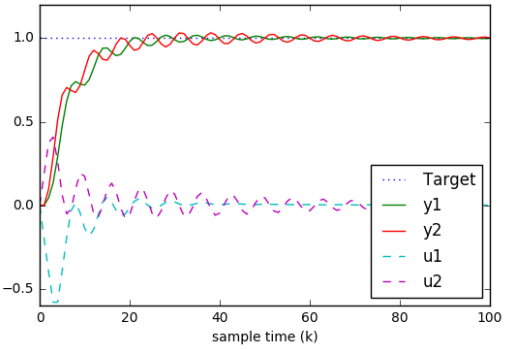


(c) $m = 3$, $p = 10$ and gain error = 75%

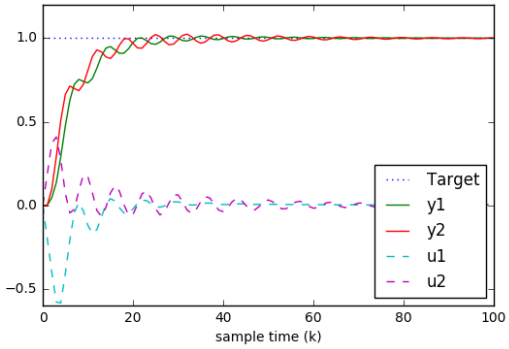


(d) $m = 3$, $p = 10$ and gain error = 100%

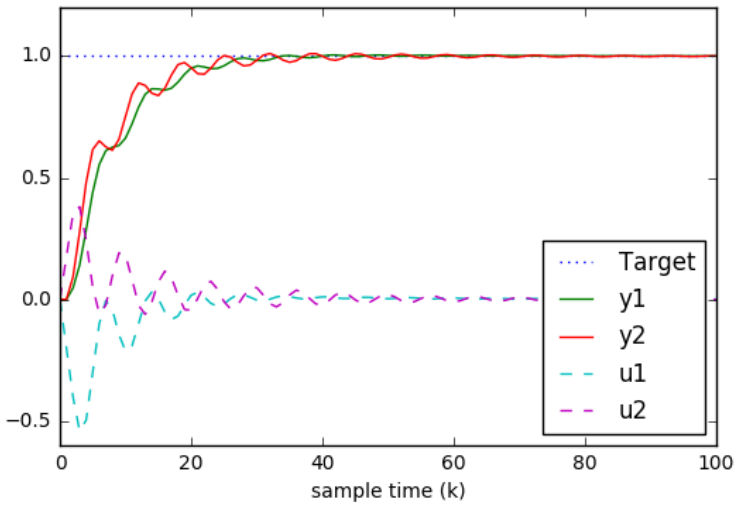
Figure 6 – Robust analysis - simulation of GPC algorithm with gain errors



(a) $m = 4$, $p = 10$ and gain error = 100%



(b) $m = 5$, $p = 10$ and gain error = 100%



(c) $m = 5$, $p = 15$ and gain error = 100%

Figure 7 – Controller re-tuning - simulation of GPC algorithm with 100% of gain error

3.4 IHMPC Implementation

3.4.1 Prediction Model: OPOM

$$A = \begin{bmatrix} 1 & 0 & 0 & 0 & 0 & 0 & 1 & 0 \\ 0 & 1 & 0 & 0 & 0 & 0 & 0 & 1 \\ 0 & 0 & 1 & 0 & 0 & 0 & 0 & 0 \\ 0 & 0 & 0 & 0.950 & 0 & 0 & 0 & 0 \\ 0 & 0 & 0 & 0 & 0.969 & 0 & 0 & 0 \\ 0 & 0 & 0 & 0 & 0 & 1 & 0 & 0 \\ 0 & 0 & 0 & 0 & 0 & 0 & 1 & 0 \\ 0 & 0 & 0 & 0 & 0 & 0 & 0 & 1 \end{bmatrix} \quad B = \begin{bmatrix} -0.190 & -1.700 \\ -0.763 & 0.235 \\ 0 & 0 \\ 0 & 1.615 \\ 0.739 & 0 \\ 0 & 0 \\ -0.190 & 0 \\ 0 & 0.235 \end{bmatrix} \quad C = \begin{bmatrix} 1 & 0 & 1 & 1 & 0 & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 & 1 & 1 & 0 & 0 \end{bmatrix}$$

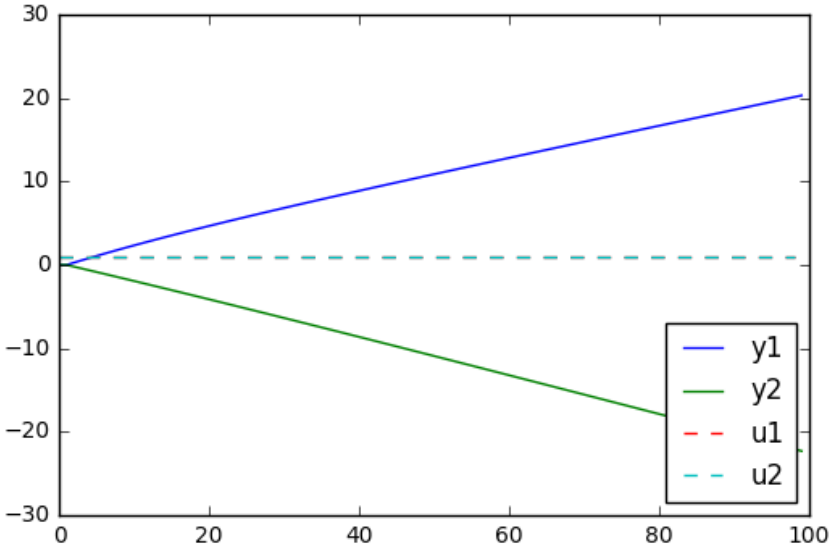


Figure 8 – Simulation to validate the OPOM

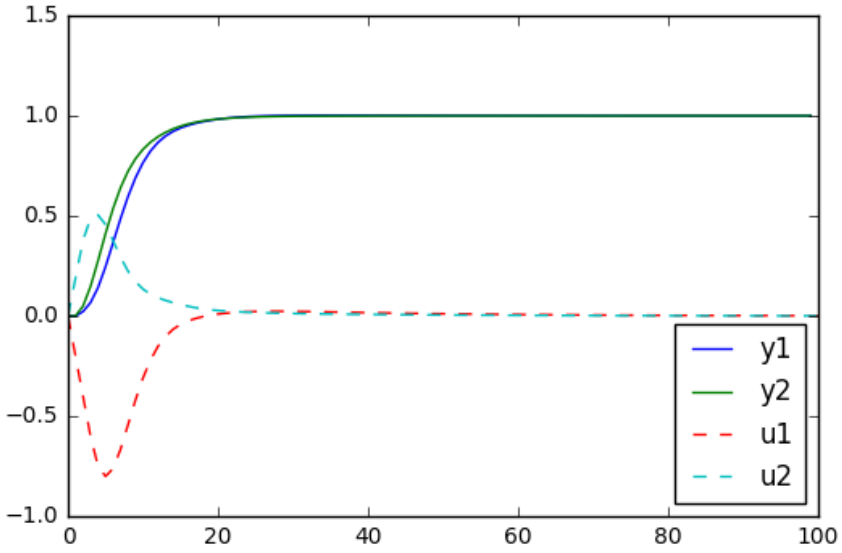


Figure 9 – Simulation to validate the OPOM

3.5 S-IHMPC Implementation

give guidelines to implement S-IHMPC

3.6 Summary

4 Conclusion

In this report, we presented guidelines for MPC algorithms implementation. First, we created a programming framework to implement the code in Python. Following this framework, we designed a GPC controller and tested it for the case study, represented by a real problem in the chemical industry. Next, we implemented the OPOM in Python and reproduced the results found in [7]. At last, we discuss the future continuation of the algorithms (IHMPC and S-IHMPC) implementation.

The Python code produced here was designed to be modular and, consequently, easy to implement in real applications. The implementation intends to suit the general case even though the code developed till this point have some parts specifically designed for the case study. The process to build the algorithm is iterative and as the implementation is still in an early version, new features need to be added and code optimizations must be implemented.

In the near future, the implementation of the IHMPC will be continued and the development of the S-IHMPC will begin afterward. Suggestions for future works are the inclusion dead time in OPOM [8] and simulations for different processes.

Bibliography

1 LIMA, M. L. de et al. Distributed satisficing MPC. *IEEE Transactions on Control Systems Technology*, v. 23, n. 1, p. 305–312, 2015. Citado 2 vezes nas páginas 2 and 5.

2 CAMACHO, E.; BORDONS, C. *Model Predictive Control*. Springer London, 2004. (Advanced Textbooks in Control and Signal Processing). ISBN 9781852336943. Disponível em: <https://books.google.com.br/books?id=Sc1H3f3E8CQC>. Citado na página 5.

3 RAWLINGS, J. B.; MUSKE, K. R. The stability of constrained receding horizon control. *IEEE Transactions on Automatic Control*, v. 38, n. 10, p. 1512–1516, Oct 1993. ISSN 0018-9286. Citado 2 vezes nas páginas 5 and 11.

4 RODRIGUES, M. A.; ODLOAK, D. An infinite horizon model predictive control for stable and integrating processes. *Computers and Chemical Engineering*, v. 27, 2003. Citado 4 vezes nas páginas 5, 11, 12, and 14.

5 CAMACHO, C. B. E. F. *Model Predictive Control*. [S.l.]: Springer, 1999. (Advanced textbooks in control and signal processing). ISBN 9783540762416,3-540-76241-8. Citado na página 7.

6 NORMEY-RICO, J. E.; CAMACHO, E. *Control of Dead-time Processes*. [S.l.]: Springer, 2007. (Advanced textbooks in control and signal processing). Citado na página 9.

7 CARRAPICO, O. L.; ODLOAK, D. A stable model predictive control for integrating processes. *Computers and Chemical Engineering*, v. 29, 2005. Citado 3 vezes nas páginas 12, 16, and 23.

8 SANTORO, B. F.; ODLOAK, D. Closed-loop stable model predictive control of integrating systems with dead time. *Journal of Process Control*, v. 22, 2012. Citado 2 vezes nas páginas 12 and 23.

Appendix

APPENDIX A – Implementation Codes

A.1 GPC

```
# -*- coding: utf-8 -*-
"""
Created on Thu Mar 31 17:03 2017

@author: Igor Yamamoto
"""
import numpy as np
import matplotlib.pyplot as plt
import scipy.signal as signal
from cvxopt import matrix, solvers


class SystemModel(object):
    def __init__(self, ny, nu, *args):
        self.ny = ny
        self.nu = nu
        self.H = list(*args)

    def step_response(self, X0=None, T=None, N=None):
        def fun(X02=None, T2=None, N2=None):
            def fun2(sys):
                return signal.step(sys, X02, T2, N2)
            return fun2
        fun3 = fun(X0, T, N)
        step_with_time = list(map(fun3, self.H))
        return [s[1] for s in step_with_time]

class GPCController(object):
    def __init__(self, system, p, m, Q, R, du_min, du_max):
        self.system = system
        self.nu = system.nu
        self.ny = system.ny
        self.p = p
```

```
        self.m = m
        self.Q = Q
        self.R = R
        self.du_min = du_min
        self.du_max = du_max
        self.G = self.initialize_G()
        AB = self.create_AB()
        self.A_til = AB[0]
        self.B = AB[1]

    def create_matrix_G(self, g, p, m):
        g = np.append(g[:p],np.zeros(m-1))
        G = np.array([])
        for i in range(p):
            G = np.append(G,[g[i-j] for j in range(m)])
        return np.resize(G,(p,m))

    def initialize_G(self):
        Ts = 1
        T = np.array(range(1, 200, Ts))
        g11, g12, g21, g22 = ethylene.step_response(T=T)
        G11 = self.create_matrix_G(g11,p,m)
        G12 = self.create_matrix_G(g12,p,m)
        G21 = self.create_matrix_G(g21,p,m)
        G22 = self.create_matrix_G(g22,p,m)
        G1 = np.hstack((G11,G12))
        G2 = np.hstack((G21,G22))
        G = np.vstack((G1,G2))
        return G

    def create_AB(self):
        Bm11 = np.array([-0.19])
        Am11 = np.array([1, -1])
        Am11_til = np.convolve(Am11, [1,-1])

        Bm12 = np.array([-0.08498])
        Am12 = np.array([1, -0.95])
        Am12_til = np.convolve(Am12, [1,-1])
```

```
        Bm21 = np.array([-0.02362])
        Am21 = np.array([1,  -0.969])
        Am21_til = np.convolve(Am21, [1,-1])

        Bm22 = np.array([0.235])
        Am22 = np.array([1,  -1])
        Am22_til = np.convolve(Am22, [1,-1])
        return [[Am11_til, Am12_til, Am21_til, Am22_til],
                [Bm11, Bm12, Bm21, Bm22]]

    def calculate_control(self, w, **kwargs):
        dm = 0
        y11_f = np.zeros(self.p)
        y12_f = np.zeros(self.p)
        y21_f = np.zeros(self.p)
        y22_f = np.zeros(self.p)
        # Free Response
        du1, du2 = kwargs['current_du']
        du1_f, du2_f = kwargs['du_past']
        y11_aux, y12_aux, y21_aux, y22_aux = kwargs['y_past']
        for j in range(p):
            if j <= dm:
                du1_f = du1
                du2_f = du2
            else:
                du1_f = du2_f = np.array(0)
            y11_f[j] = -y11_aux.dot(self.A_til[0][1:]) + du1_f.dot(self.B
            y12_f[j] = -y12_aux.dot(self.A_til[1][1:]) + du2_f.dot(self.B
            y21_f[j] = -y21_aux.dot(self.A_til[2][1:]) + du1_f.dot(self.B
            y22_f[j] = -y22_aux.dot(self.A_til[3][1:]) + du2_f.dot(self.B
            y11_aux = np.append(y11_f[j], y11_aux[:-1])
            y12_aux = np.append(y12_f[j], y12_aux[:-1])
            y21_aux = np.append(y21_f[j], y21_aux[:-1])
            y22_aux = np.append(y22_f[j], y22_aux[:-1])
        f = np.append(y11_f+y12_f, y21_f+y22_f)
        # Solver Inputs
        H = matrix((2*(self.G.T.dot(self.Q).dot(self.G)+self.R)).tolist()
        q = matrix((2*self.G.T.dot(self.Q).dot(f-w)).tolist())
        A = matrix(np.hstack((np.eye(self.nu*self.m),-1*np.eye(self.nu*se
```

```
        b = matrix([self.du_max]*self.nu*self.m+[-self.du_min]*self.nu*se
        # Solve
        sol = solvers.qp(P=H,q=q,G=A,h=b)
        dup = list(sol['x'])
        return dup

class Simulation(object):
    def __init__(self, system, controller, real_system=None):
        if real_system:
            self.real_system = real_system
        else:
            self.real_system = system
        self.system = system
        self.controller = controller

    def run(self, tsim):
        # Real Process
        Br11 = np.array([-0.19])
        Ar11 = np.array([1, -1])
        Br12 = np.array([-0.08498])
        Ar12 = np.array([1, -0.95])
        Br21 = np.array([-0.02362])
        Ar21 = np.array([1, -0.969])
        Br22 = np.array([0.235])
        Ar22 = np.array([1, -1])
        na11 = len(Ar11)
        na12 = len(Ar12)
        na21 = len(Ar21)
        na22 = len(Ar22)
        nb = 1
        # Reference and Disturbance Signals
        w1 = np.array([1]*(tsim+p))
        w2 = np.array([1]*(tsim+p))
        # Initialization
        y11 = np.zeros(tsim+1)
        y12 = np.zeros(tsim+1)
        y21 = np.zeros(tsim+1)
        y22 = np.zeros(tsim+1)
        u1 = np.zeros(tsim+1)
```

```
u2 = np.zeros(tsim+1)
du1 = np.zeros(tsim+1)
du2 = np.zeros(tsim+1)
y11_past = np.zeros(na11)
y12_past = np.zeros(na12)
y21_past = np.zeros(na21)
y22_past = np.zeros(na22)
u1_past = np.zeros(nb)
u2_past = np.zeros(nb)

# Control Loop
for k in range(1,tsim+1):
    y11[k] = -Ar11[1:].dot(y11_past[:-1]) + Br11.dot(u1_past)
    y12[k] = -Ar12[1:].dot(y12_past[:-1]) + Br12.dot(u2_past)
    y21[k] = -Ar21[1:].dot(y21_past[:-1]) + Br21.dot(u1_past)
    y22[k] = -Ar22[1:].dot(y22_past[:-1]) + Br22.dot(u2_past)

    # Select references for the current horizon
    w = np.append(w1[k:k+p], w2[k:k+p])

    du_past = np.array([du1[k-1], du2[k-1]])
    y_past = [y11_past, y12_past, y21_past, y22_past]
    current_du = [np.array([du1[k]]), np.array([du2[k]])]
    dup = self.controller.calculate_control(w,
                                            du_past=du_past,
                                            y_past=y_past,
                                            current_du=current_du


    du1[k] = dup[0]
    du2[k] = dup[m]
    u1[k] = u1[k-1] + du1[k]
    u2[k] = u2[k-1] + du2[k]

    u1_past = np.append(u1[k],u1_past[:-1])
    u2_past = np.append(u2[k],u2_past[:-1])
    y11_past = np.append(y11[k],y11_past[:-1])
    y12_past = np.append(y12[k],y12_past[:-1])
    y21_past = np.append(y21[k],y21_past[:-1])
    y22_past = np.append(y22[k],y22_past[:-1])
```

```
        #%% Teste
        plt.clf()
        plt.plot([1]*(tsim+1),':', label='Target')
        plt.plot(y11+y12, label='y1')
        plt.plot(y21+y22, label='y2')
        plt.plot(u1,'--', label='u1')
        plt.plot(u2,'--', label='u2')
        plt.legend(loc=4)
        plt.xlabel('sample time (k)')

if __name__ == '__main__':
    nu = 2    # number of inputs
    ny = 2    # number of outputs
    h11 = signal.TransferFunction([-0.19],[1, 0])
    h12 = signal.TransferFunction([-1.7],[19.5, 0])
    h21 = signal.TransferFunction([-0.763],[31.8, 1])
    h22 = signal.TransferFunction([0.235],[1, 0])
    ethylene = SystemModel(2, 2, [h11, h12, h21, h22])

    p = 15    # prediction horizon
    m = 3     # control horizon
    Q = np.eye(p*ny)
    R = 10**1*np.eye(m*nu)
    du_max = 0.2
    du_min = -0.2
    controller = GPCController(ethylene, p, m, Q, R, du_min, du_max)

    real_h11 = signal.TransferFunction([-0.19],[1, -1])
    real_h12 = signal.TransferFunction([-1.7],[19.5, 0])
    real_h21 = signal.TransferFunction([-0.763],[31.8, 1])
    real_h22 = signal.TransferFunction([0.235],[1, 0])
    real_ethylene = SystemModel(2, 2, [real_h11, real_h12, real_h21, real

    solvers.options['show_progress'] = False
    tsim = 100
    sim = Simulation(ethylene, controller)
    sim.run(tsim)
```

A.2 IHMPC