MODEL PREDICTIVE CONTROL

DATA-DRIVEN MPC

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COURSE STRUCTURE

- ✓ Basic concepts of model predictive control (MPC) and linear MPC
- ✓ Linear time-varying and nonlinear MPC
- ✓ MPC computations: quadratic programming (QP), explicit MPC
- ✓ Hybrid MPC
- ✓ Stochastic MPC
 - Data-driven MPC

Course page:

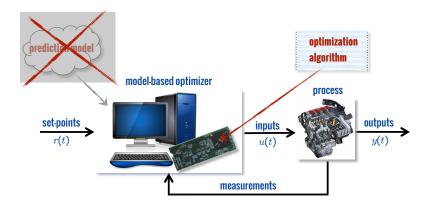
http://cse.lab.imtlucca.it/~bemporad/mpc course.html

LEARNING MPC FROM DATA

- Goal: learn MPC law from data that optimizes a given index
- Reinforcement learning = use data and a performance index to learn an optimal policy
- Q-learning: learn Q-function defining the MPC law from data (Gros, Zanon, 2019) (Zanon, Gros, Bemporad, 2019)
- Policy gradient methods: learn optimal policy coefficients directly from data using stochastic gradient descent (Ferrarotti, Bemporad, 2019)
- Global optimization methods: learn MPC parameters (weights, models, horizon, solver tolerances, ...) by optimizing observed closed-loop performance (Piga, Forgione, Formentin, Bemporad, 2019) (Forgione, Piga, Bemporad, 2020)



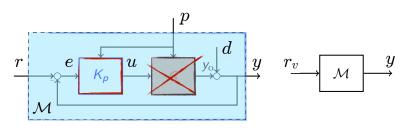
DATA-DRIVEN MPC



 Can we design an MPC controller without first identifying a model of the open-loop process?

DATA-DRIVEN DIRECT CONTROLLER SYNTHESIS

(Campi, Lecchini, Savaresi, 2002) (Formentin et al., 2015)

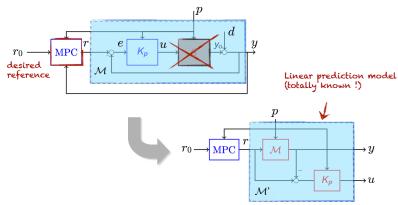


- Collect a set of data $\{u(t), y(t), p(t)\}, t = 1, \dots, N$
- $\bullet \;$ Specify a desired closed-loop linear model ${\mathcal M}$ from r to y
- Compute $r_v(t) = \mathcal{M}^\# y(t)$ from pseudo-inverse model $\mathcal{M}^\#$ of \mathcal{M}
- Identify linear (LPV) model K_p from $e_v = r_v y$ (virtual tracking error) to u

DATA-DRIVEN MPC

ullet Design a linear MPC (reference governor) to generate the reference r

(Bemporad, Mosca, 1994) (Gilbert, Kolmanovsky, Tan, 1994)



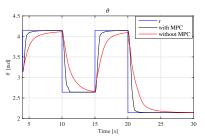
• MPC designed to handle input/output constraints and improve performance

(Piga, Formentin, Bemporad, 2017)

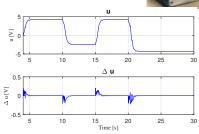
DATA-DRIVEN MPC - AN EXAMPLE

 \bullet Experimental results: MPC handles soft constraints on $u,\Delta u$ and y (motor equipment by courtesy of TU Delft)





desired tracking performance achieved

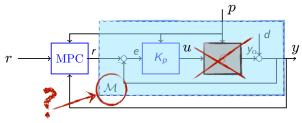


constraints on input increments satisfied

No open-loop process model is identified to design the MPC controller!

OPTIMAL DATA-DRIVEN MPC

• **Question**: How to choose the reference model \mathcal{M} ?



• Can we choose ${\mathcal M}$ from data so that K_p is an optimal controller?

• Idea: parameterize desired closed-loop model $\mathcal{M}(\theta)$ and optimize

$$\min_{\theta} J(\theta) = \frac{1}{N} \sum_{t=0}^{N-1} \underbrace{W_y(r(t) - y_p(\theta, t))^2 + W_{\Delta u} \Delta u_p^2(\theta, t)}_{\text{performance index}} + \underbrace{W_{\text{fit}}(u(t) - u_v(\theta, t))^2}_{\text{identification error}}$$

• Evaluating $J(\theta)$ requires synthesizing $K_p(\theta)$ from data and simulating the nominal model and control law

$$y_p(\theta, t) = \mathcal{M}(\theta)r(t) \qquad u_p(\theta, t) = K_p(\theta)(r(t) - y_p(\theta, t))$$
$$\Delta u_p(\theta, t) = u_p(\theta, t) - u_p(\theta, t - 1)$$

• Optimal θ obtained by solving a (non-convex) nonlinear programming problem

Results: linear process

$$G(z) = \frac{z - 0.4}{z^2 + 0.15z - 0.325}$$

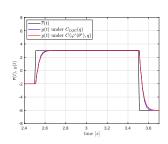
Data-driven controller only 1.3% worse than model-based LQR (=SYS-ID on same data + LQR design)

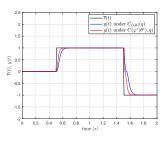
• Results: nonlinear (Wiener) process

$$y_L(t) = G(z)u(t)$$

 $y(t) = |y_L(t)| \arctan(y_L(t))$

The data-driven controller is 24% better than LQR based on identified open-loop model!







Plant + environment dynamics (unknown):

$$s_{t+1} = h(s_t, p_t, u_t, d_t) \\ - s_t \text{ states of plant \& environment} \\ - p_t \text{ exogenous signal (e.g., reference)} \\ - u_t \text{ control input} \\ - d_t \text{ unmeasured disturbances}$$

• Control policy: $\pi: \mathbb{R}^{n_s+n_p} \longrightarrow \mathbb{R}^{n_u}$ deterministic control policy

$$u_t = \pi(s_t, p_t)$$

• Closed-loop performance of an execution is defined as

$$\mathcal{J}_{\infty}(\pi, s_0, \{p_{\ell}, d_{\ell}\}_{\ell=0}^{\infty}) = \sum_{\ell=0}^{\infty} \rho(s_{\ell}, p_{\ell}, \pi(s_{\ell}, p_{\ell}))$$

 $\rho(s_{\ell}, p_{\ell}, \pi(s_{\ell}, p_{\ell})) = \text{stage cost}$

OPTIMAL POLICY SEARCH PROBLEM

• Optimal policy:

$$\pi^* = \arg\min_{\pi} \mathcal{J}(\pi)$$

$$\mathcal{J}(\pi) = \mathbb{E}_{s_0,\{p_\ell,d_\ell\}} \left[\mathcal{J}_{\infty}(\pi,s_0,\{p_\ell,d_\ell\}) \right]$$
 expected performance

• Simplifications:

- Finite parameterization: $\pi=\pi_K(s_t,p_t)$ with K = parameters to optimize
- Finite horizon: $\mathcal{J}_L(\pi,s_0,\{p_\ell,d_\ell\}_{\ell=0}^{L-1}) = \sum_{\ell=0}^{L-1} \rho(s_\ell,p_\ell,\pi(s_\ell,p_\ell))$
- Optimal policy search: use stochastic gradient descent (SGD)

$$K_t \leftarrow K_{t-1} - \alpha_t \mathcal{D}(K_{t-1})$$

with $\mathcal{D}(K_{t-1})$ = descent direction

DESCENT DIRECTION

- The descent direction $\mathcal{D}(K_{t-1})$ is computed by generating:
 - N_s perturbations $s_0^{(i)}$ around the current state s_t
 - N_r random reference signals $r_\ell^{(j)}$ of length L,
 - N_d random disturbance signals $d_\ell^{(h)}$ of length L,

$$\mathcal{D}(K_{t-1}) = \sum_{i=1}^{N_s} \sum_{j=1}^{N_p} \sum_{k=1}^{N_q} \nabla_K \mathcal{J}_L(\pi_{K_{t-1}}, s_0^{(i)}, \{r_\ell^{(j)}, d_\ell^{(k)}\})$$



- SGD step = mini-batch of size $M=N_s\cdot N_r\cdot N_d$
- Computing $\nabla_K \mathcal{J}_L$ requires predicting the effect of π over L future steps
- We use a local linear model just for computing $\nabla_K \mathcal{J}_L$, obtained by running recursive linear system identification

OPTIMAL POLICY SEARCH ALGORITHM

- At each step t:
 - 1. Acquire current s_t
 - 2. Recursively update the local linear model
 - 3. Estimate the direction of descent $\mathcal{D}(K_{t-1})$
 - 4. Update policy: $K_t \leftarrow K_{t-1} \alpha_t \mathcal{D}(K_{t-1})$
- If policy is learned online and needs to be applied to the process:
 - Compute the nearest policy K_t^{\star} to K_t that stabilizes the local model

$$K_t^\star = \underset{K}{\operatorname{argmin}} \|K - K_t^s\|_2^2$$
 s.t. K stabilizes local linear model Linear matrix inequality

ullet When policy is learned online, **exploration** is guaranteed by the reference r_t

SPECIAL CASE: OUTPUT TRACKING

- $x_t = [y_t, y_{t-1}, \dots, y_{t-n_o}, u_{t-1}, u_{t-2}, \dots, u_{t-n_i}]$ $\Delta u_t = u_t - u_{t-1}$ control input increment
- Integral action dynamics $q_{t+1} = q_t + (y_{t+1} r_t)$

$$s_t = \begin{bmatrix} x_t \\ q_t \end{bmatrix}, \quad p_t = r_t.$$

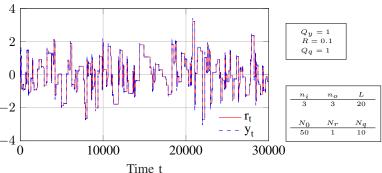
Linear policy parametrization:

$$\pi_K(s_t, r_t) = -K^s \cdot s_t - K^r \cdot r_t, \qquad K = \begin{bmatrix} K^s \\ K^r \end{bmatrix}$$

EXAMPLE: RETRIEVE LQR FROM DATA

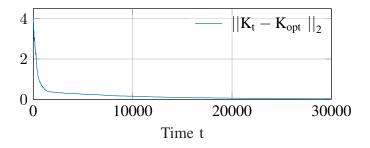
$$\left\{ \begin{array}{ll} x_{t+1} & = & \left[\begin{smallmatrix} -0.669 & 0.378 & 0.233 \\ -0.288 & -0.147 & -0.638 \\ -0.337 & 0.589 & 0.043 \end{smallmatrix} \right] x_t + \left[\begin{smallmatrix} -0.295 \\ -0.325 \\ -0.258 \end{smallmatrix} \right] u_t \\ y_t & = & \left[\begin{smallmatrix} -1.139 & 0.319 & -0.571 \end{smallmatrix} \right] x_t \end{array} \right. \quad \text{model is unknown}$$

Online tracking performance (no disturbance, $d_t = 0$):



EXAMPLE: RETRIEVE LQR FROM DATA

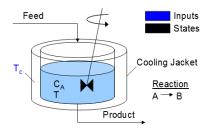
Evolution of the error $||K_t - K_{opt}||_2$:



$$K_{\mathrm{SGD}} = [-1.255, 0.218, 0.652, 0.895, 0.050, 1.115, -2.186]$$

$$K_{\text{opt}} = [-1.257, 0.219, 0.653, 0.898, 0.050, 1.141, -2.196]$$

NONLINEAR EXAMPLE



model is unknown

Feed:

- concentration: 10kg mol/m³
- temperature: 298.15K

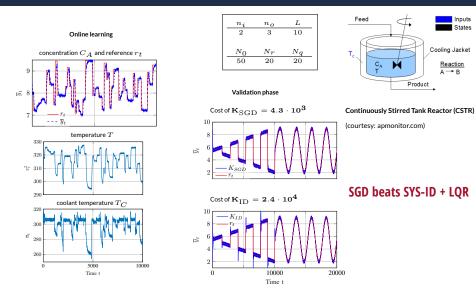
Continuously Stirred Tank Reactor (CSTR)^[1]

$$T = \hat{T} + \eta_T$$
, $C_A = \hat{C_A} + \eta_C$, η_T , $\eta_C \sim \mathcal{N}(0, \sigma^2)$, $\sigma = 0.01$

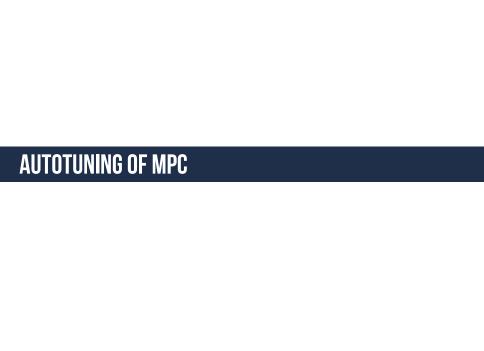
$$Q_y = \begin{bmatrix} 1 & 0 \\ 0 & 0 \end{bmatrix}$$
 $R = 0.1$ $Q_q = \begin{bmatrix} 0.01 & 0 \\ 0 & 0 \end{bmatrix}$

[1] figure retrived from apmonitor.com

NONLINEAR EXAMPLE



Approach currently extended to multiple-linear and nonlinear policies



MPC CALIBRATION PROBLEM

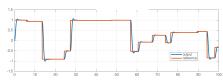
- Controller depends on a vector x of parameters
- Parameters can be many things:
 - MPC weights, prediction model coefficients, horizons
 - Entries of covariance matrices in Kalman filter
 - Tolerances used in numerical solvers

- ...



Define a performance index f over a closed-loop simulation or real experiment.
 For example:

$$f(x) = \sum_{t=0}^{T} \|y(t) - r(t)\|^2$$
(tracking quality)



 Auto-tuning = find the best combination of parameters that solves the global optimization problem

$$\min_{x} f(x)$$

GLOBAL OPTIMIZATION ALGORITHMS FOR AUTO-TUNING

What is a good optimization algorithm to solve $\min f(x)$?

• The algorithm should not require the gradient ∇f of f(x) (derivative-free or black-box optimization)

The algorithm should not get stuck on local minima (global optimization)

The algorithm should make the fewest evaluations of the cost function f
(which is expensive to evaluate)

AUTO-TUNING - GLOBAL OPTIMIZATION ALGORITHMS

- Several derivative-free global optimization algorithms exist: (Rios, Sahidinis, 2013)
 - Lipschitzian-based partitioning techniques:
 - DIRECT (Divide in RECTangles) (Jones, 2001)
 - Multilevel Coordinate Search (MCS) (Huyer, Neumaier, 1999)
 - Response surface methods
 - Kriging (Matheron, 1967), DACE (Sacks et al., 1989)
 - Efficient global optimization (EGO) (Jones, Schonlau, Welch, 1998)
 - Bayesian optimization (Brochu, Cora, De Freitas, 2010)
 - Genetic algorithms (GA) (Holland, 1975)
 - Particle swarm optimization (PSO) (Kennedy, 2010)
 - ..
- New method: radial basis function surrogates + inverse distance weighting
 - (GLIS) (Bemporad, 2019)

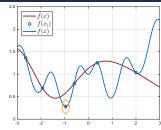
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AUTO-TUNING - GLIS

• Goal: solve the global optimization problem

$$\min_{x} f(x)
s.t. \ell \le x \le u
 g(x) \le 0$$





• Step #1: given N samples of f at x_1, \ldots, x_N , build the surrogate function

$$\hat{f}(x) = \sum_{i=1}^{N} \beta_i \phi(\epsilon ||x - x_i||_2)$$

 $\phi=$ radial basis function

Example:
$$\phi(\epsilon d) = \frac{1}{1 + (\epsilon d)^2}$$
 (inverse quadratic)

Vector eta solves $\hat{f}(x_i) = f(x_i)$ for all $i = 1, \dots, N$ (=linear system)

• CAVEAT: build and minimize $\hat{f}(x_i)$ iteratively may easily miss global optimum!

AUTO-TUNING - GLIS

• Step #2: construct the IDW exploration function

$$\begin{array}{rcl} z(x) & = & \frac{2}{\pi} \Delta F \tan^{-1} \left(\frac{1}{\sum_{i=1}^N w_i(x)} \right) \\ & \text{ or 0 if } x \in \{x_1, \dots, x_N\} \end{array}$$

where
$$w_i(x) = \frac{e^{-\|x - x_i\|^2}}{\|x - x_i\|^2}$$

 ΔF = observed range of $f(x_i)$

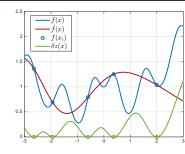
• Step #3: optimize the acquisition function

$$x_{N+1} = \underset{\text{arg min}}{\operatorname{arg min}} \quad \hat{f}(x) - \delta z(x)$$

s.t. $\ell \le x \le u, g(x) \le 0$

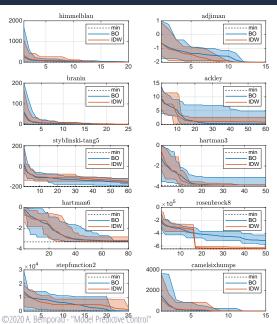
to get new sample x_{N+1}

• Iterate the procedure to get new samples $x_{N+2},\dots,x_{N_{ ext{max}}}$



 δ = exploitation vs exploration tradeoff

GLIS VS BAYESIAN OPTIMIZATION



problem	n	BO[s]	IDW[s]
ackley	2	26.42	3.24
adjiman	2	3.39	0.66
branin	2	9.58	1.27
camelsixhumps	2	4.49	0.62
hartman3	3	23.19	3.58
hartman6	6	52.73	10.08
himmelblau	2	7.15	0.92
rosenbrock8	8	58.31	11.45
stepfunction2	4	10.52	1.72
styblinski-tang5	5	33.30	5.80

Results computed on 20 runs per test

BO = MATLAB's **bayesopt** fcn

AUTO-TUNING: MPC EXAMPLE

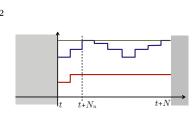
• We want to auto-tune the linear MPC controller

min
$$\sum_{k=0}^{50-1} (y_{k+1} - r(t))^2 + (W^{\Delta u}(u_k - u_{k-1}))^2$$
s.t.
$$x_{k+1} = Ax_k + Bu_k$$

$$y_c = Cx_k$$

$$-1.5 \le u_k \le 1.5$$

$$u_k \equiv u_{N_u}, \ \forall k = N_u, \dots, N-1$$

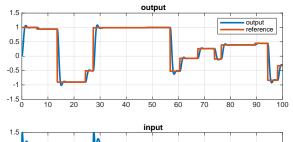


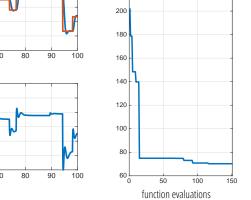
• Calibration parameters: $x = [\log_{10} W^{\Delta u}, N_u]$

- Range: $-5 \le x_1 \le 3$ and $1 \le x_2 \le 50$
- Closed-loop performance objective:

$$f(x) = \sum_{t=0}^{T} \underbrace{(y(t) - r(t))^2}_{\text{track well}} + \underbrace{\frac{1}{2}(u(t) - u(t-1))^2}_{\text{smooth control}} + \underbrace{\frac{2N_u}{\text{small Q}}}_{\text{small Q}}$$
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AUTO-TUNING: EXAMPLE





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best function value

• Result:
$$x^* = [-0.2341, 2.3007]$$



$$W^{\Delta u} = 0.5833, N_u = 2$$

AUTO-TUNING: PROS AND CONS

- Pros:

 - Applicable to any calibration parameter (weights, horizons, solver tolerances, ...)
 (Piga, Forgione, Formentin, Bemporad, 2019) (Forgione, Piga, Bemporad, 2020)
 - $\, \blacksquare \,$ Rather arbitrary performance index f(x) (tracking performance, response time, worst-case number of flops, ...)
- Cons:
 - \P Need to **quantify** an objective function f(x)
 - No room for qualitative assessments of closed-loop performance
 - Often objectives are multiple, not clear how to blend them in a single one
- Current research: preference-based optimization (GLISp), having human assessments in the loop (semi-automatic tuning)

(Bemporad, Piga, 2019) (Zhu, Bemporad, Piga, 202

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LEARNING MPC FROM DATA - LESSON LEARNED SO FAR

- Model/policy structure includes real plant/optimal policy:
 - Sys-id + model-based synthesis = model-free reinforcement learning
 - Reinforcement learning may require more data (model-based can instead "extrapolate" optimal actions)

- Model/policy structure does not include real plant/optimal policy:
 - optimal policy learned from data may be better than model-based optimal policy
 - when open-loop model is used as a tuning parameter, learned model can be quite different from best open-loop model that can be identified from the same data