Mathemathical Modelling

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Contents

1 Lecture 1

1.1 Practical Information

You need to know

- Separable 1. order equations.
- Linear 1. order equations.
- 2. order linear equations with constant coefficients.

1.2 Dimensional Analysis

Basic facts

- Any physical relation has to make sense dimensionally.
- Any physical relation must be valid for any choice of fundamental units.

Remark.

Make sure remark looks better

- **Forbidden** $3m + 2kg = ?$
- $m = f(x,t)$ is legal
- e^{-t} and $s = 5t^2$, is nonsense
- **Dimension** is length, mass , energy, etc.
- **Unit** is meter, feet, year, etc

Given a variable R, we write $R = \overbrace{v(R)}^{\text{numerical value}} \underbrace{[R]}_{\text{unit}}$.

If we have a physical relation that is dimensionall correct that

$$f(R_1, R_2, \ldots, R_n) = 0 \quad \rightarrow \quad f(v(R_1), v(R_2), \ldots, v(R_n)) = 0$$

1.3 Fundamental Units

Given units $F_1, F_2, \ldots, F_m$ for fundamental if

$$F_1^{\alpha_1}, F_2^{\alpha_2}, \ldots, F_m^{\alpha m} = 0 \quad \rightarrow \quad \alpha_1 = \alpha_2 = \ldots = 0$$

This units are then independent. **Example.** The units kg, m, s are independent.

Example. In a right angle triangle with angle α and hypothenus c. We know the area A is uniquely determined by α and c

$$A = f(c, \alpha)$$

α is dimensialless since $\alpha = \frac{s}{r}$. Since A scales as the square of the length, then is

$$f\left(ac, \alpha\right) = a^2 f\left(c, \alpha\right)$$
$$c = 1 \rightarrow f\left(a, \alpha\right) = a^2 f\left(1, \alpha\right) = a^2 h\left(\alpha\right)$$

Which then ends up with the relation

$$A = a^2 h\left(\alpha\right)$$

Make corollary environmet

Lets derive $A = a^2 h\left(\alpha\right)$ somwhat differently. We know there is a relation $f\left(A, c, \alpha\right) = 0$. We want to introduce new variables.

$$\Pi_1 = \frac{A}{c^2}, \quad c = c_1, \quad \alpha = \alpha_1$$

which means $f\left(c^2\Pi_1, c, \alpha\right) = 0$ and $h\left(\Pi_1, \alpha, c\right) = 0$. h must be dimensially consistent $\rightarrow$ h must be independent of c.

$$h\left(\Pi_1, \alpha\right) = 0 \leftrightarrow \Pi_1 = k\left(\alpha\right)$$
$$\rightarrow \frac{A}{c^2} = k\left(\alpha\right) \quad \leftrightarrow \quad A = c^2 k\left(\alpha\right).$$

1.4 Trinity of the first atomic blast

We assume there is a relation

$$f\left(E, \rho, r, t\right) = 0$$

- Energy: E, $[E] = kgm^2s^{-2}$
- Mass density of air: ρ, $[\rho] = kg^{-3}$
- Radius: r , $[r] = m$
- Time: t, $[t] = s$

We choose 3 independent variables, say r, t, ρ. Also we call r, t, ρ **core variables**. Let is define a dimensionalless number Π_1 such that

$$[\Pi_1] = 0$$

The relation is now given by $h\left(\Pi, t, r, \rho\right) = 0$, where h is independent of t , r and ρ. Which in fact is $h\left(\Pi\right) = 0$, where $\Pi_1 = c$ s.t. $[c] = 1$.

Given by the definitnion is

$$\frac{Et^2}{\rho r^5} = c \quad \rightarrow \quad E = \frac{c\rho r^5}{t^2}$$

Using $\rho = 12kgm^{-3}$, $r = 110m$, $t = 6 \cdot 10^{-3}$ do we end up with the relation

$$E = c \cdot 7.5 \cdot 10^{13} J$$

1.5 Steady-state single phase flow in a uniform straight pipeline

Figure of a pipe

Pipe with flow u, length L and pressure drop Δp Then there is a relation between

- L : length, $[L] = m$
- D: diameter $[D] = m$
- u: flow rate $[u] = ms^{-1}$
- Δp: Pressure drop, $\left[\Delta kgm^{-1}s^{-2}\right]$
- μ: (Shear) viscousity $[\mu] = kgm^{-1}s^{-1}$
- ρ: mass density: $[\rho] = kgm^{-3}$
- E: Wall roughness: $[E] = m$

We have to choose 3 core variables and they are not unique. Since we have 3 independent units ρ, u, D are independent such that it can be a core variable:

$$\Pi_1 = \frac{L}{D} \quad , \quad \Pi_2 = \frac{\Delta p}{\rho u^2} \quad , \quad \Pi_3 = \frac{\rho}{\mu} \quad , \quad \Pi_4 = \frac{E}{D}$$

Then the relation is

$$f\left(\Pi_1, \Pi_2, \Pi_3, \Pi^4, \rho, D, u\right) = 0 \quad \Pi_2 = h\left(\Pi_1, \Pi_3, \Pi_4\right) \leftrightarrow \frac{\Delta p}{\rho u^2} = h\left(\Pi_1, \Pi_3, \Pi_4\right)$$

$$\rightarrow \frac{\Delta p}{u^2 \rho} = \Pi_1 k\left(\Pi_3, \Pi_4\right)$$

$$\Delta p = u^2 \rho \frac{L}{D} k\left(\frac{\rho D u}{\mu}, \frac{E}{D}\right)$$

$$\text{measure} \quad \frac{\rho D \mu}{\mu} \quad , \quad k = \frac{\Delta p D}{u^2 \rho}$$

2 Lecture 2

2.1 Practical Information

Ask for zoom meeting. ola.mahlen@ntnu.no, wednesday 13-14.

2.2 Recall

Last time did we consider steady-state single phase in a flow in a pipe.

- Assuming $f(L, \Delta p, u, \mu, D, E, \rho) = 0$ we arrive with this formula

$$\frac{\Delta p D}{u^2 \rho L} = k \left(\overbrace{\frac{\rho u D}{\mu}}^{\text{Reynhold number}}, \underbrace{\frac{E}{D}}_{\text{Relative wall roughness}} \right)$$

- Dimensionless numbers are often called **dimensionless groups**. Such numbers are independent of choice of fundamental units. They have real physical meaning. **Reynholds number** R_e essentially define what type of flow. Usually $R_e < 2000$ is it laminar flow and $R_e > 4000$ turbulent flow.

2.3 Scaling

Let a pipe have diameter D and flow rate u such that $t_v = \frac{D}{u}$. Then can we describe

$$t_\alpha = \frac{D^2}{\frac{\mu}{e}}$$

where μ is the kinematic viscosity. Then is R_e defined such that

$$R_e = \frac{t_\alpha}{t_v}$$

Assume we have the relation

$$R_1 = f(R_2, \ldots, R_m)$$

Such that it exist an

$$\Pi_1 = g(\Pi_2, \Pi_2, \ldots, \Pi_{m-k}).$$

2.4 Buckinghams Pi-Theorem

Assume we have a dimensionally valid relation $f(R_1, \ldots, R_m) = 0$ and a set of fundemental units $F_1, F_2, \ldots, F_n$ such that

$$[R_j] = F_1^{a_{j1}} F_2^{a_{j2}} \ldots F_n^{a_{jn}} \quad j = 1, 2, \ldots, m$$

This then defines the dimension matrix A given by

Table 1:

	F_1	F_2	$\dots$	F_n
R_1	a_{11}	a_{11}		a_{1n}
R_2	a_{21}	a_{21}		a_{2n}
$\vdots$		$\ddots$		
R_n	a_{m1}	$\dots$		a_{mn}

Fix better table environment.

Let $rank\,(A) = dim\,(row\,(A)) = k$. This translates to that we have k dimensionally independent variables. Choosing k linearly independent row vectors, corresponds to choosing core variables. Let this basis be $\mathbf{a}_{i1}, \mathbf{a}_{i2}, \dots, \mathbf{a}_{ik}$. Let the rest of the row vectors be

$$\mathbf{a}_{j_1}, \mathbf{a}_{j_2}, \dots, \mathbf{a}_{j_{m-k}}$$

Then is $\mathbf{a}_{j_r} = \sum_{s=1}^{k} C_{j_r,s} \mathbf{a}_{\mathbf{i_s}}$ where $r = 1, \dots, m-k$. We end up with the equation

$$\Pi_r = \frac{R_{j_r}}{R_{i_1}^{r_{j_r,1}} R_{j_2}^{a_{j_r,2}} \dots R_{j_k}^{a_{j_r,k}}}$$

Are dimensionally numbers.

Our relation becomes

$$g\left(\Pi_1, \dots, \Pi_{m-k}\right) = 0, \qquad \begin{cases} i_1, i_2, \dots, i_k \\ j_1, \dots, j_{m-k} \end{cases}$$

Example. Swinging pendulum
Assume there is a relation

$$f\left(w, \alpha_0, L, M, g,\right) = 0$$

where w is the frequenxy, g gravitational acceleration, M mass, α_0 the swinging angle. We can set L, M, g as core variables such that

$$\left[\frac{L}{g}\right] = s^2 \quad \rightarrow \quad \left[\frac{L}{g} w^2\right] = 1$$

$$f\left(w, \alpha_0, L, M, g\right) = 0 \implies \quad g\left(\alpha_0, \frac{Lw^2}{g}\right) = 0$$

2.5 Scaling

We have a problem at hand, usually differential equations. Then we tru to find representative scales for the various variables, and then write the equation on so-called fimensionless form. This has several advantages

- Our dimensionless variables are of order 1 .
- We get rid of a lot of physical constants.
- It makes us able to see what terms are ”small” in the equation. The idea is to introduce dimensionless variables by introducing appropiate scales. If we have a stick of lenght L, we choose L as length scale i.e

$$x^* = Lx \quad \text{Where} \quad x \quad \text{is dimenionless}$$

Example. Heat flow in a rod with length L. Let $u^*(x^*, t^*)$ be the temperatur with the boundary conditions

$$u^*(0, t^*) = 0 \quad u^*(L, t^*) = 0$$

If we let the model be

$$\frac{\partial u^*}{\partial t^*} = D \cdot \frac{\partial^2 u^*}{\partial {x^*}^2}, \quad u^*(0, t^*) = 0 \quad u^*(L, t^*) = 0$$
$$u^*(x^*, 0) = u_0 \sin\left(\pi \frac{x^*}{L}\right)$$

We fund the tune scale T by scales **balancing the equation** .
Let $x^* = Lx$, and $t^* = Tt$, where T is to be determined $u^* = u_0 u$. If we find $u(x, t)$, then the physical temperature is given by

$$u^*(x^*, t^*) = u_0 u\left(\frac{x^*}{L}, \frac{t^*}{T}\right)$$

We have $u(0, t) = u(1, t) = 0$

$$\frac{\partial u^*}{\partial t^*} = D\frac{\partial^2 u^*}{\partial {x^*}^2} \quad \Longrightarrow \quad \frac{u_0}{T}\frac{\partial u}{\partial t} = \frac{u_0}{L^2} D \frac{\partial^2}{\partial x^2}$$
$$\leftrightarrow \frac{\partial u}{\partial t} = \left(\frac{TD}{L^2}\right)\frac{\partial^2 u}{\partial x^2} \quad \text{Balancing the equation}$$
$$\frac{TD}{L^2} = 1 \quad \Longrightarrow T = \frac{L^2}{D}$$
$$u^*(x^*, 0) = u_0 \sin\left(\pi \frac{x^*}{L}\right)$$
$$u(x, 0) = \sin(\pi x)$$

which fulfills the condition

$$\frac{\partial u}{\partial t} = \frac{\partial^2 u}{\partial x^2} \quad , u(0, t) = u(1, t) = 0$$

3 Lecture 3

3.1 Recall

$$\frac{\partial u^*}{\partial t^*} = D\frac{\partial^2 u^*}{\partial x^{*2}}$$
$$0 \le x^* \le L$$
$$x^* = Lx$$
$$t^* = Tt$$
$$u^* = u_0$$

We can also recall

$$u^*\left(x^*, t^*\right) = u_0 u\left(\frac{x^*}{L}, \frac{t^*}{T}\right)$$
$$\frac{u_0}{T}\frac{\partial u}{\partial t} = D\frac{u_0}{L^2} \implies \frac{\partial u}{\partial t} = \frac{TD}{L^2}\frac{\partial^2 u}{\partial x^2}$$
$$\text{Require} \quad \frac{TD}{L^2} = 1 \implies T = \frac{L^2}{D}$$

This can be generelized to

$$\frac{\partial u}{\partial t} = \frac{\partial^2 u}{\partial x^2}, \quad 0 \le x \le 1$$

3.2 Sinking Ball

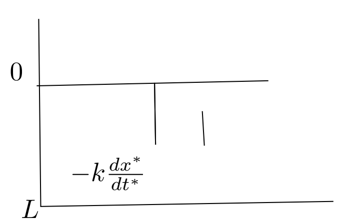

Figure 1: sinkingball

Let

- ρ_b e mass density of ball
- $\rho_f$mass density of fluid
- V Volume of ball

Then is the equation

$$\begin{aligned}\rho_b V g - \rho_f V g &= V g \rho_b \left(1 - \frac{\rho_f}{\rho_b}\right) \\ &= m\hat{g} \implies \hat{g} = g\left(1 - \frac{\rho_f}{\rho_b}\right)\end{aligned}$$

And we then end up with the newtions law

$$m\frac{dx^{*2}}{dt^{*2}} = m\hat{g} - k\frac{dx^*}{dt}, \quad \text{Friction coefficient} \quad k$$

where

$$x^*(0) = 0, \quad \frac{dx^*}{dt^*}(0) = V$$

The cases can be described as follows

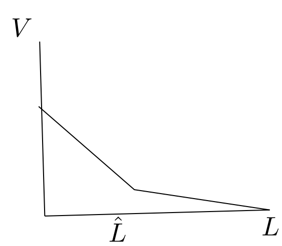

Figure 2: highV

1. High friction, not so high V. Ball will sink at constant speed most of the time.
2. Friction is low, andC not "too high". ("Free fall with V=0")
3. High V, and high friction $m\frac{d^2x^*}{dt^{*2}} = m\hat{g} - k\frac{dx^*}{dt^*}$

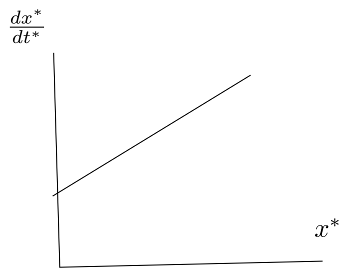

Figure 3: frefall

For this problem there is 3 characteristic speeds

1. V : initial velocity
2. v_0 : equilibrium speed in case A $v_0 = \frac{m\hat{g}}{k}$
3. v_f : free fall $v_f = \sqrt{2\hat{g}L}$

Let us put

$$\begin{aligned} \frac{d^2x^*}{dt^{*2}} = 0 &\implies k\frac{dx^*}{dt} = \hat{g}m \\ &\implies \frac{dx^*}{dt^*} = \hat{g}\frac{m}{k} = v_0 \end{aligned}$$

and put

$$\begin{aligned} x^*(0) &= \frac{dx^*}{dt^*}(0) = 0 \\ k &= 0 \end{aligned}$$

3.2.1 Scaling

1. Case A: The ball sinks at constant speed "most" of the time.
   (a) Length scale L : $x^* = Lx$. Since the ball falls with speed most of the time, a timescale would be $T = \frac{L}{v_0}$. v is not much larger than v_0

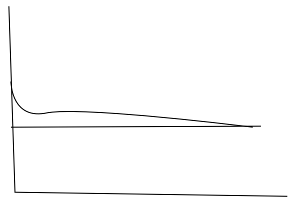

Figure 4: sinking

$\Longrightarrow$ it is not so that $v \gg v_0$

$$
\begin{aligned}
m\frac{L}{T^2}x^{''} &= m\hat{g} - k\frac{L}{T}x^{'} \quad \text{Divide by } L \\
\Longrightarrow m\frac{1}{kT}x^{''} &= \frac{Tm\hat{g}}{KL} - x^{'} \\
\frac{m}{k\frac{L}{v_0}}x^{''} &= \frac{\frac{k}{v_0}m\hat{g}}{kL} - x^{'} \\
\Longrightarrow \frac{mv_0}{Lk}x^{''} &= \frac{Lm\hat{g}}{KLv_0} - x^{'}
\end{aligned}
$$

We can then derive

$$
\begin{aligned}
\frac{m\frac{m\hat{g}}{k}}{Lk}x^{''} &= 1 - x^{'} \\
\Longrightarrow \frac{m^2\hat{g}}{Lk^2}x^{''} &= 1 - x^{'} \\
\Longrightarrow \frac{m^2\hat{g}^2}{\hat{g}Lk^2}x^{''} &= 1 - x^{'} \\
\epsilon x^{''} &= 1 - x^{'} \quad \text{Where} \quad \epsilon = 2\left(\frac{v_0}{v_f}\right)^2
\end{aligned}
$$

The condition are $x(0) = 0$, $\frac{L}{T}x^{'}(0) = V$ which can be rewritten to

$$
x^{'}(0) = \frac{TV}{L}) \frac{\frac{L}{v_0 V}}{L} = \frac{V}{v_0} = \mu
$$

3.3 Let Analyze The equation

In case A is the

$$\epsilon \ddot{x} = 1 - \dot{x}$$

An approximation we can do is to put $\epsilon = 0$ such that

$$0 = 1 - \dot{x} \quad x(0) = 0, \quad \dot{x}(0) = \mu \quad \dot{x} = 0$$

unless $\mu = 1$, we cant find a solution.

3.3.1 Case B

Small friction, V is not too high. Let the lengthscale be L.

$$\frac{d^2}{dt^{*2}} x^{*2} = \hat{g}, \quad x^*(0) = \frac{dx^*}{dt^*}(0) = 0$$
$$x^*(t^*) = \frac{1}{2}\hat{g}(t^*)^2$$

Hit the bottom with speed V_f . We can choose time scale T such that

$$T = \frac{L}{v_f}$$

So gain

$$\frac{mL}{T^2}\ddot{x} = m\hat{g} - \frac{kL}{T}\dot{x}$$

What you can observe is that gravity dominates so we modify the equation to be

$$\frac{L}{\hat{g}T^2}\ddot{x} = 1 - \frac{kL}{gmT}\dot{x}$$
$$\implies 2\ddot{x} = 1 - \left(\frac{v_F}{v_0}\right), \quad \frac{K}{T}\dot{x}(0) = 0$$
$$2\ddot{x} = 1 - \epsilon\dot{x} \quad \dot{x}(0) = \frac{V}{v_f} = \mu$$

3.3.2 Case C: High V and high friction

Let us consider

$$m\frac{d^2x^*}{dt^{*2}} = -kV \quad \frac{dx^*}{dt^*} = V - \frac{kV}{m}t^* = 0$$

Where we choose the scales $t^* = \frac{m}{k} = T$, $L = \frac{Vm}{k}$, where $TV = L$.

$$\implies \ddot{x} = \epsilon - \dot{x}, \quad x(0) = 1, \quad \dot{x} = 1, \quad \epsilon = \frac{v_0}{V}$$

Example. Let

$$a\frac{d^2x^*}{dt^{*2}} + b\frac{dx^*}{dt^*} + cx^* = 0$$
$$x^*(0) = x_0, \quad \frac{dx^*}{dt^*}(0) = 0$$

Three waus to scale by balancing the equation. Last term ”small”

$$x^* = x_0 x, \quad t^* = Tt$$

Where T is to be determined.

$$a\frac{x_0}{T^2}\ddot{x} + b\frac{x_0}{T}\dot{x} + cx_0 = 0$$

$$\ddot{x} + \frac{bT}{a}\dot{x} + \frac{cT^2}{a} = 0$$

If we are smart can we choose the timescale $T = \frac{a}{b}$ then we get

$$\ddot{x} + \dot{x} + \frac{ca^2}{b^2a} = 0.$$
$$\implies \ddot{x} + \dot{x} + \left(\frac{ca}{b^2}\right)x = 0$$

3.4 Turbulence

Reynold number

$$R_e = \frac{u\rho L}{\mu} = \frac{uL}{\frac{mu}{\rho}} = \frac{uL}{\mathcal{V}}$$

Then we have

$$\frac{\partial v}{\partial t} = \mathcal{V}\frac{\partial^2 v}{\partial x^2}$$

4 Lecture 31/08

4.1 Turbulence

Kolmogorvs Microscales .

$$\rho \frac{du}{dt} = \mu \frac{\partial^2 u}{\partial x^2}$$

Time svale for convitive flow over a distance L

$$t_c = \frac{L}{U}, \quad U \quad \text{is velocity.}$$

This can be rearranged such that

$$\frac{\partial u}{\partial t} = \left(\frac{\mu}{\rho} \frac{\partial^2 u}{\partial x^2} \right).$$

We also define $\mathcal{V} = \frac{\mu}{\rho}$ where $[\mathcal{V}] = m^2 s^{-1}$, which is the time for dispersion of velocity.

Let $t_d = \frac{L^2}{\mathcal{V}}$ such that the Reynolds number can be written

$$R_e = \frac{v \rho L}{\mu} = \frac{UL}{\left(\frac{\mu}{\rho}\right)} = \frac{UL}{\mathcal{V}} = \frac{t_d}{t_0}$$

For water is $\mathcal{V} = 10^{-6} m^2 s^{-1}$. So for a river , put $L = 100m$ with $U = 1ms^{-1}$

$$R_e = \frac{1ms^{-1} \cdot 100m}{10^{-6} m^2 s^{-1}} = 10^8$$

Assume the generation of new whrils stops when $t_d \approx t_c \to R_e \approx 1$. Let

$$E = \frac{\text{Energy}}{\text{time per unit mass}}$$
$$[E] = kgm^2 s^{-2} s^{-1} kg$$

Let l be bthe scale of the smallest whirls and u the unit velocity then is

$$E = E\left(l, u, \mathcal{V}\right).$$

We assume that E is proportional to u^2.

$$f\left(\frac{E}{u^2}, l, \mathcal{V}\right) = 0$$

Table 2:

	m	s
$\frac{E}{n^2}$	1	0
l	1	0
v	2	-2

$$\left[\frac{\frac{E}{u^2}}{\mathcal{V}}\right] = m^{-2}$$

$$\Pi = \frac{\frac{E}{u^2}}{\mathcal{V}} l^2$$

$$\text{choose } \Pi = 1$$

$$\rightarrow E = \mathcal{V}(\frac{u^2}{l})^2$$

$$ul = \mathcal{V}$$

$$\implies k = \left(\mathcal{V}^3 \frac{1}{E}\right)^{\frac{1}{4}}, \quad u = (VE)^{\frac{1}{4}}$$

Example . Let us have $1kg$ what in a mixmaster and apply $100W$ power. then is

$$l = \left(\frac{\left(10^{-6} m^2 s^{-1}\right)^3}{100 m^2 s^{-3}}\right)^{\frac{1}{4}} = 0.01mm$$

4.2 Regular Perturbation Theory

Assume we have an equation s.t.

$$D(x,\varepsilon) = 0 \quad \text{where} \quad \varepsilon \ll 1$$

meaning that ε is small.

We have a solution $x(\varepsilon)$ to the problem $D(x,\varepsilon)$. The perturbation problem is regular if $\lim_{\varepsilon\to 0} x(\varepsilon)$ is a solution to $D(x,0) = 0$. The idea is

1. Put $x(\varepsilon) = x_0 + \varepsilon x_1 + \varepsilon^2 x_2 + \ldots$

$$\begin{aligned} x(\varepsilon) &\approx x_0 && \text{in 0. order} \\ x(\varepsilon) &\approx x_0 + \varepsilon x_1 && \text{to 1. order} \end{aligned}$$

2. Insert $x(\varepsilon) = x_0 + \varepsilon x_1 + \ldots$ into $D(x,\varepsilon)$.

3. Collect all terms of order 0, all terms of order 1 so that

$$D(x,\varepsilon) = 0 \leftrightarrow \overbrace{()}^{=0} + \overbrace{()}^{=0}\varepsilon^2 + \ldots = 0$$

Example. Let

$$x^3 + x^2 + \varepsilon x - 2 = 0, \quad \varepsilon \ll 1$$

For $\varepsilon = 0$ we have $x = 1$ as a solution. To find a solution "close to" 1 when $\varepsilon \neq 0$ we put

$$x = 1 + \varepsilon x_1 + \varepsilon^2 x_2 + O(\varepsilon)$$

Want an approximation to 2. order. We get

$$\begin{aligned} \left(1 + \varepsilon x_1 + \varepsilon^2 x_2\right)^3 + \left(1 + \varepsilon x_1 + \varepsilon^2 x_2\right)^2 + \varepsilon\left(1 + \varepsilon x_1 + \varepsilon^2 x_2\right) - 2 = 0 \\ \implies \varepsilon(5x_1 + 1) + \varepsilon^2(\ldots) = 0 \end{aligned}$$

$$x(\varepsilon) \approx 1 - \frac{\varepsilon}{5} + \frac{\varepsilon^2}{125}$$

4.3 The Projectile Problem

Let v_0 be the vertical velocity and v_e be escape velocity such that $v_0 \ll v_e$.

Newton gravitational law

$$\mathbf{F} = -m\frac{R^2 g}{(R + x^*)^2}$$

Where g is the gravitational constand at $x^* = 0$.

Energy to move to $x^* = \infty$

$$
\begin{aligned}
-\int_0^\infty \mathbf{F} dx^* &= mgR^2 \int_0^\infty \frac{dx^*}{(R+x^*)^2} \\
&= mgR^2 \left[-\frac{1}{(R+x^2)} \right]_0^\infty \\
&= mgR = \frac{1}{2} m v_e^2 \\
\implies v_e &= \sqrt{2gR}
\end{aligned}
$$

We have

$$
m \frac{d^2 x^*}{dt^{*2}} = -m \frac{gR^2}{(R+x^*)^2}
$$

Such that

$$
\frac{d^2}{dt^{*2}} = -\frac{R^2 g}{(R\ x^*)^2}, \quad x^*(0) = 0, \quad \frac{dx^*}{dt^*}(0) = v_0
$$

and $v_0 \ll v_e$, when $x^* \ll R$ (a consequence of $v_0 \ll v_e$)

$$
\frac{d^2 x^*}{dt^{*2}} \approx -g \quad \frac{dx^*}{dt^*} = v_0 - t^* g = 0 \quad \leftrightarrow t^* = \frac{v_0}{g} = T = \text{timescale}
$$

$$
X^* = v_0 t^* - \frac{1}{2} t^* g \quad x^*(T) = \frac{v_0^2}{g} - \frac{1}{2} \frac{v_0^2}{g} = \frac{1}{2} \frac{v_0^2}{g}
$$

Let $L = \frac{v_0^2}{g}$ and scale the equation $\left(\frac{L}{T}\right) = v_0$ and $x^* = Lx$.

$$
\begin{aligned}
\frac{L}{T^2} \ddot{x} &= \frac{-gR^2}{(R+Lx)^2} \leftrightarrow \frac{L}{T^2} \ddot{x} = -\frac{gR^2}{R^2 \left(1 + \frac{L}{R} x\right)^2} \\
\to \ddot{x} &= \frac{-T^2 \frac{g}{L}}{\left(1 + \frac{L}{R} x^2\right)} \to \ddot{x} = \frac{-1}{(1+\varepsilon x)^2}
\end{aligned}
$$

Where

$$
\varepsilon = \frac{L}{R} = \frac{v_0^2}{Rg} = 2 \frac{2 v_0^2}{v_e^2}
$$

Following problem

$$
\ddot{x} = \frac{-1}{(1+\varepsilon x)^2}, \quad x(0) = 0, \quad \dot{x}(0) = 1
$$

> Recall that
>
> $$
> \begin{aligned}
> f(u) = \frac{1}{(1+u)^2} \to \int f(u) &= \frac{1}{1+u} + C \\
> &= C - \left(1 - u + u^2 - u^3 + \dots\right) \\
> \implies f(u) &= 1 - 2u03u^2 + O\left(u^3\right)
> \end{aligned}
> $$

Then to second order

$$\ddot{x} = -\left(1 - 2\varepsilon x + 3\varepsilon x^2\right), \quad x(0) = 0, \quad \dot{x}(0) = q$$

Next et

$$x(t) = x_0(t) + \varepsilon x_1(t) + \varepsilon x_2(t) + O(\varepsilon)$$

So let

$$x_j(0) = 0 \quad \text{for} \quad j = 0, 1, 2$$
$$\ddot{x_0}(0) = 1, \quad \dot{x_1}(0) = \dot{x_2}(0) = 0$$
$$\rightarrow \ddot{x_0} + \varepsilon \ddot{x_1} + \varepsilon^2 \ddot{x_2} = -1 + 2\varepsilon (x_0 0 \varepsilon x_1) - 3\varepsilon^2 x_0^2$$
$$\rightarrow (\ddot{x_0} + 1) + \varepsilon (\ddot{x_1} - 2x_0) + \varepsilon^2 \left(\ddot{x_2} + 2x_1 + 3x_0^2\right) = 0$$
$$\ddot{x_0} = -1 \quad x_0(0) = 0, \quad \dot{x_0} = 1$$
$$\ddot{x_1} = 2x_0, \quad \dot{x1}(0) = \dot{x_i}(0) = 0$$
$$\ddot{x_2} = 2x_1 - 3x_0^2, \quad x_2(0) = \dot{x_2}(0) = 0$$

$$\rightarrow x_0(t) = t - \frac{1}{2} tst$$
$$\ddot{x_1}(t) = 2t - t^2$$
$$\dot{x_1}(t) = t^2 - \frac{1}{3} t^3$$
$$x_1(t) = \frac{1}{3} t^3 - \frac{1}{12} t^4$$

Where

$$\ddot{x_2} = \frac{2}{3} t^3 - \frac{1}{6} t^4 - 3\left(t^2 - t^3 + \frac{1}{4} t^4\right)$$
$$x_2 = -\frac{1}{4} t^4 + \frac{11}{60} t^5 - \frac{11}{360} t^6$$

Which end up with

$$x(t) = t - \frac{1}{2} t^2 0 \varepsilon \left(\frac{1}{3} t^3 - \frac{1}{12}\right) + \varepsilon^2 \left(-\frac{t^4}{4} 0 \frac{11}{60} t^5 - \frac{11}{360} t^6\right)$$

Gives the diea of how to approx the time to the macimum height. $\dot{x}(t) = 0$ is a 5. degree equation containing ε .

Lets put

$$t = 1 + \varepsilon t_2 \varepsilon^2 t_2$$

Into the 5. degree edition and to regular perturabation

$$\rightarrow t = 1 + \frac{2}{3}\varepsilon + 2/5 \varepsilon^2 + O(\varepsilon)$$

such that

$$\ddot{x} = \frac{-1}{(1+\varepsilon x)^2} \rightarrow \ddot{x}\dot{x} = \frac{\dot{x}}{(1+\varepsilon x)^2}$$

$$\rightarrow \frac{d}{dt}\left(\frac{1}{2}\dot{x}^2\right) = \frac{d}{dt}\left(\frac{-1}{\varepsilon}\frac{1}{1+\varepsilon x}\right)$$

$$\frac{1}{2}\dot{x}^2 = \frac{-1}{\varepsilon}\frac{1}{1+\varepsilon x} + C$$

$$\frac{1}{2} = \frac{-1}{\varepsilon}$$

$$C = \frac{1}{2} + \frac{1}{\varepsilon}$$

where

$$\frac{1}{2}\dot{x}^2 = \frac{-1}{\varepsilon}\frac{1}{1+\varepsilon x} + \frac{1}{2} + \frac{1}{\varepsilon}$$

At maximum height $\dot{x} = 0$

$$0 = -\frac{1}{\varepsilon}.$$

5 Lecture 02/09

Let Newtons Law be

$$\frac{d^2 s^*}{dt^{*2}} = g\sin\left(\alpha^*\right) \implies \frac{d^2\alpha^*}{dt^{*2}} = -\frac{g}{L}\sin\left(\alpha^*\right)$$

scaling:

$$\begin{aligned}
\alpha^* = \varepsilon\alpha, \quad t^* = Tt \\
\frac{\varepsilon}{T^2}\ddot{\alpha} = \frac{-g}{L}\sin\left(\varepsilon\alpha\right) \implies \ddot{\alpha} = -\left(T^2 g\frac{1}{L}\right)\frac{\sin\left(\varepsilon\alpha\right)}{\varepsilon} \\
T = \sqrt{\frac{L}{g}} \implies \ddot{\alpha} = -\frac{\sin\left(\varepsilon\alpha\right)}{\varepsilon} \\
\alpha\left(0\right) = 1 \quad \dot{\alpha}\left(0\right) = 0
\end{aligned}$$

Let put $\alpha = \alpha_0\left(t\right) + \varepsilon^2\alpha_2\left(t\right) + O\left(\varepsilon^4\right)$. where $\alpha\left(t\right)$ is an even function of ε due to symmetry.

$$\alpha_0\left(0\right) = 1, \quad \dot{\alpha}_0\left(0\right) = 0, \quad \alpha_2\left(0\right) = \dot{\alpha_2}\left(0\right) = 0$$

Inserted into the equation

$$\begin{aligned}
\ddot{\alpha_0} + \varepsilon^2\ddot{\alpha}_2 = -\frac{\sin\left(\varepsilon\left(\alpha_0 + \varepsilon^2\alpha_2\right)\right)}{\varepsilon} \implies \quad \ddot{\alpha_0} + \varepsilon^2\ddot{\alpha_2} \\
= \frac{-1}{3}\left(\varepsilon\underbrace{\left(\alpha_0 + \varepsilon^2\alpha_2\right)}_{u}\frac{\varepsilon^2}{6}\left(\alpha_0 + \alpha\varepsilon^2\right)\right)
\end{aligned}$$

Let

$$\begin{aligned}
\alpha_0\left(t\right) &= A\cos t + B\sin t \\
\alpha_0\left(0\right) &= 1, \quad \dot{\alpha}\left(0\right) = 0 \quad \implies \alpha_0\left(t\right) = \cos t \\
\alpha_2\left(t\right) &= A\cos t + B\sin t + \alpha_{2,f}\left(t\right) \\
\cos^3 t &= \left(\frac{1}{2}\left(e^{it} - e^{it}\right)\right)^3 = \frac{1}{8}\left(e^{i3t} + 3e^{it}03e^{-i3t}\right) \\
&= \frac{1}{4}\left(\cos 3t + 3\cos t\right) \\
\alpha_{20}\left(t\right) &= A\cos 3t + B\sin 3t + Ct\cos t + Dt\sin t \\
\alpha_2\left(t\right) &= \frac{1}{192}\left(\cos t + \cos 3t\right) + \frac{1}{16}t\sin t \\
\alpha\left(t\right) &= \alpha_0\left(t\right) + \varepsilon_2^2\left(t\right) \quad \text{is not periodic}
\end{aligned}$$

Poincare-Lin Stel Method . Instead let

$$\alpha(t) = \alpha_0(\omega(\varepsilon)t) + \alpha_2(\omega(\varepsilon)t)\varepsilon^2 + O(\varepsilon^4)$$

Where $\omega(\varepsilon) = 1 + \omega_2\varepsilon^2\ O(\varepsilon^4)$. See exercise.

5.1 Modelling how the kidney disposes salt and water.

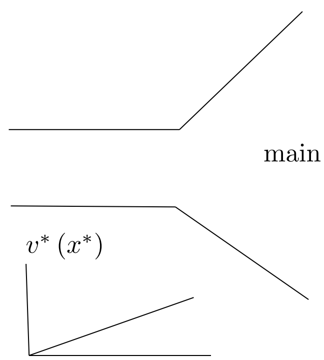

Figure 5: watermodell

Assumptions

1. Secondary channel is fed water by osmosis from the sorrouinding tissue.
2. Ions are transported down the channel by connection and diffusion.
3. Ions are fed into the channel be a chemical ppump-

We want the steady-state profiles of ion concenstration $C^*(x^*)$ and the velocity $v^*(x^*)$ of the ion water solution.

The ion concentration is written as

$$[C^*] = \frac{ions}{m^3} = \frac{osmol}{m^3}$$

One mole salt give two moles ions
Osomosis :

$$J^* = P(c^* - c_0)$$

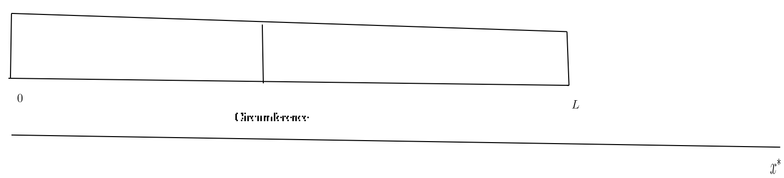

Figure 6: molefig

Is flux density of water entering the secondary channel. J^* is volume water in per area per time. c_0 ion concentration is tissue and main channel. P is called membrance permeability.

$$[P] = \frac{[J^*]}{[c^*]} = \frac{ms^{-1}}{osmol \cdot m^{-3}} = \frac{m^4}{s \cdot osmol}$$

Ion flux density

$$N^* = \begin{cases} N_0, & 0 \leq x^* \leq \delta \\ 0, & \delta \leq x^* \leq L \end{cases}$$

Where $[N_0] = \frac{osmol}{m^2 \cdot s}$. The toal rate of salt entering the channel

$$N_0 \cdot c \cdot \delta$$

Where c is the area of pump.

- The flux density of ions in the secondary channel

$$F^* = F_c^* + F_\alpha^*$$

$$[F^*] = \frac{osmol}{m^2 \cdot s}$$

- Convective flow

$$F_c^* = c^* v^*$$

- Diffusion: **Ficus law**

$$F_1^* = -D\frac{dc^*}{dx^*}.$$

where D is the diffusion of salt in water.

Conservation of water

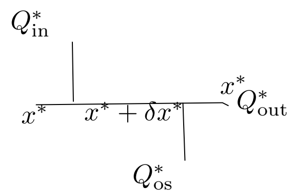

Figure 7: conssswater

$$
\begin{aligned}
Q^*_{\text{out}} &= Q^*_{\text{in}} + Q^*_{\text{os}} \\
v^*\left(x^*+\Delta x^*\right) &= v^* A + P\left(c^*\left(\hat{x}\right)-c_0\right) c\Delta x^* \quad \text{where} \quad \hat{x^*} \in \left\langle x^*, x^*+\Delta x^*\right\rangle \\
\implies \frac{v^*\left(x^*+\Delta x^*\right)-v^*\left(x^*\right)}{\Delta x^*} &= \frac{c}{A} P\left(c^*\left(\hat{x^*}\right)-c_0\right) \\
\Delta x^* \to 0 \quad \implies \frac{dv^*}{dx^*} &= \left(\frac{cP}{A}\right)\left(c^*-c_0\right)
\end{aligned}
$$

COnservation of salt

$$
F^*\left(x^*+\Delta x^*\right) A = F^*\left(x^*\right) A + N^*\left(\hat{x^*}\right) c\Delta x^*
$$

This ends up with

$$
\begin{aligned}
\implies \frac{dF^*}{dx^*} &= \frac{c}{A} N^*(x^*) \\
\text{or} \quad \frac{dF^*}{dx^*} &= \frac{c}{A} \cdot \begin{cases} N_0, & 0 < x^* < \delta \\ 0, & \delta < x^* < L \end{cases} \\
F^*(0) = 0 \quad \implies F(x^*) &= \begin{cases} \frac{N_0 c}{A} x^*, & 0 < x^* < \delta \\ \frac{N_0 \delta c}{A}, & \delta < x^* < L \end{cases} \\
\implies v^* c^* - D \frac{dc^*}{dx^*} &= F^*(x^*) \\
\frac{dv^*}{dt^*} &= \frac{cP}{A}(c^* - c_0) \\
v^*(0) &= 0 \\
c^*(L) &= c_0
\end{aligned}
$$

Also same that v^* and c^* are continious at $x^* = \delta$.

5.1.1 Scaling the model

Two length scales δ and L. Choose δ as length svale. Natural to use c_0 as scale for c^*. The rate salt supplied is

$$N_0 \delta c = c_0 U A$$

Ions supplied is convectiv flux with c^* such that $U = \frac{N_0 \delta c}{c_0 A}$.

$$
\begin{aligned}
x^* &= \delta, \\
c^* &= c_0 c \\
v^* &= U v
\end{aligned}
$$

1. $(Uc_0)\, cv - \frac{Dc_0}{\delta} \dot{c} = F^*$ such that

$$\implies vc - \frac{Dc}{\delta U c_0} \dot{c} = \frac{1}{Uc} \cdot \begin{cases} \frac{N_0 c \delta x}{A U c_0}, & 0 < x\delta < \delta \\ \frac{N_0 c \delta}{A u c_0}, & \delta < x\delta < L \end{cases}$$

$$vc - \varepsilon \dot{c} = \begin{cases} x & 0 < x < 1 \\ 1 & 1 < x < \lambda \end{cases}$$

where $\varepsilon = \frac{D}{\delta u}$, and $\lambda = \frac{L}{\delta}$

$$\implies U = \frac{N_0 \delta c}{c_0 A}$$

2. $\frac{U}{\delta} \dot{v} = \frac{cP}{A} c_0 (c - 1)$

6 References