

A. Steady state flux model.

$$N_A = D_{AB} \frac{dc}{dz}$$

$$\frac{\partial N_A}{\partial z} = 0$$

$$N_A = \frac{D_{AB}}{L} [C_{A0} - C_{AS}]$$

B. Average flux across membrane and boundary layer.

$$N_A = K_c (C_{AS} - C_{AX})$$

$$C_{AS} = \frac{N_A}{K_c} + C_{AX}$$

$$N_A = \frac{D_{AE}}{L} [C_{A0} - C_{AS}] = \frac{D_{AE}}{L} [C_{A0} - \frac{N_A}{K_c} - C_{AX}]$$

$$N_A = \frac{[C_{A0} - C_{AX}] \frac{D_{AE}}{L}}{(1 + \frac{D_{AE} L}{K_c})} = \frac{C_{A0} - C_{AX}}{\frac{L}{D_{AE}} + \frac{1}{K_c}}$$

$$N_A = \frac{C_{A0} - C_{AX}}{\frac{L}{D_{AE}} + \frac{1}{K_c}}$$

C. If  $K_c \gg D_{AE}$ , flux would be limited by the flux through the membrane.

D. Flux if transfer resistance is in the membrane.

$$N_A = \frac{D_{Ae}}{L} [C_{A0} - C_{Ax}]$$
$$= \frac{5.54 \times 10^{-7}}{0.1} [1 - 0.4] \times 10^{-5}$$

$$N_A = 3.32 \times 10^{-11} \text{ mol/cm}^2 \cdot \text{s}.$$

E. Flux if transfer resistance is in the boundary layer.

$$N_A = k_c [C_{A0} - C_{Ax}]$$
$$= 1.05 \times 10^{-4} (1 - 0.4) \times 10^{-5}$$

$$N_A = 6.3 \times 10^{-10} \frac{\text{mole}}{\text{cm}^2 \cdot \text{s}}.$$

F. Biot Number  $B_i = \frac{k_e l}{D_e}$

$$B_i = \frac{1.05 \times 10^{-4} \times 0.01}{5.54 \times 10^{-7}}$$

$$B_i = 18.95$$

Most of the resistance to mass transfer is through Membrane.