



**OREGON STATE UNIVERSITY**  
**CBEE**  
**DEPARTMENT OF CHEMICAL ENGINEERING**  
**CHE 331**  
**Transport Phenomena I**

**Dr. Goran Jovanovic**

**Mechanical Energy Balance Equation II**

**Please turn-off cell phones**

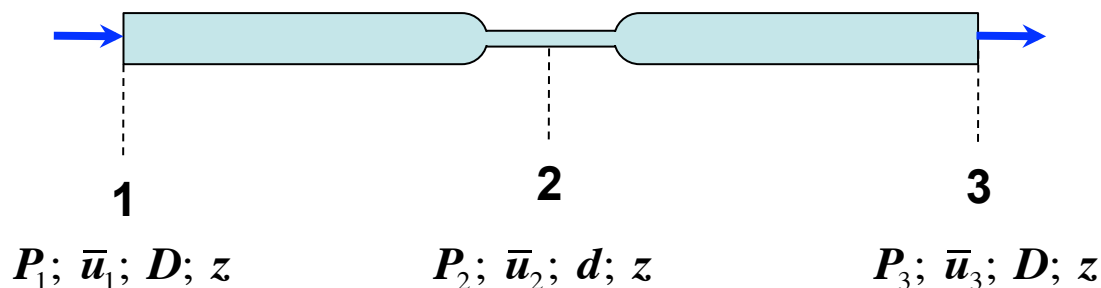
## MECHANICAL ENERGY BALANCE EQUATION

$$g\Delta Z + \frac{\Delta \bar{u}^2}{2} + \frac{\Delta P}{\rho} + \sum F + \dot{W}_{Sout} = 0$$

↑ Potential Energy    ↑ Kinetic Energy    ↑ Flow Work  $\rho = \text{const}$     ↑ Friction Losses    ↑ Shaft Work (out)    ↑ Steady State

## MECHANICAL ENERGY BALANCE EQUATION

$$g\Delta Z + \frac{\Delta \bar{u}^2}{2} + \frac{\Delta P}{\rho} + \sum F + \dot{W}_{Sout} = 0$$



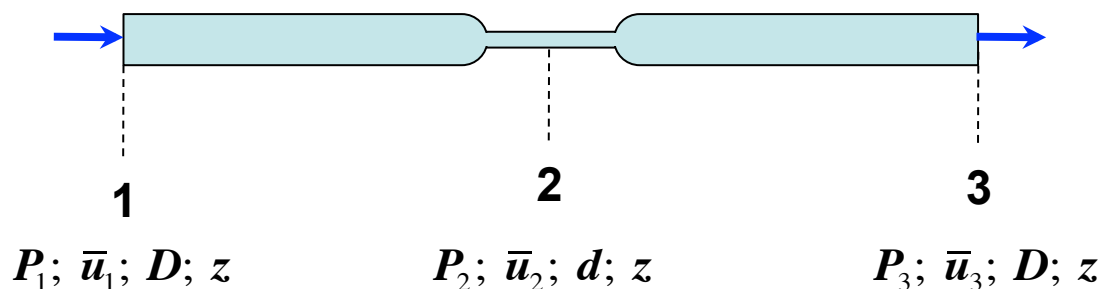
Assumption:

Negligible frictional losses – MEB equation becomes Bernoulli equation !

$$g\Delta Z + \frac{\Delta \bar{u}^2}{2} + \frac{\Delta P}{\rho} + \cancel{\sum F} + \dot{W}_{Sout} = 0$$

## MECHANICAL ENERGY BALANCE EQUATION

$$g\Delta Z + \frac{\Delta \bar{u}^2}{2} + \frac{\Delta P}{\rho} + \dot{W}_{Sout} = 0$$



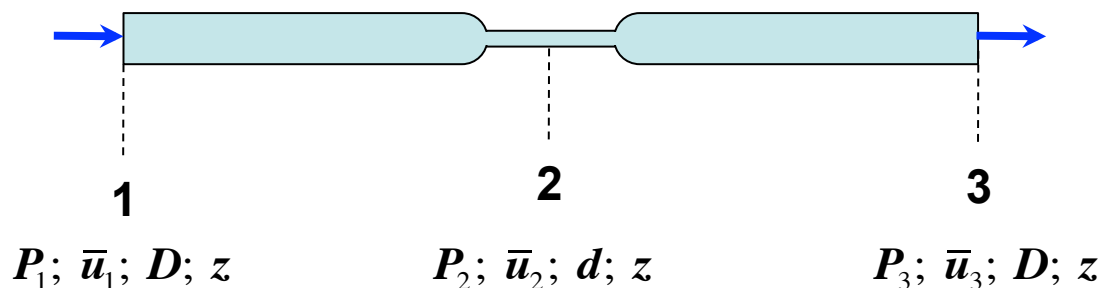
MEB between point 1 and 2:

$$\cancel{g\Delta Z} + \frac{\Delta u^2}{2} + \frac{\Delta P}{\rho} + \cancel{\dot{W}_{Sout}} = 0$$

$$\frac{\Delta u^2}{2} + \frac{\Delta P}{\rho} = 0 \Rightarrow \frac{\bar{u}_2^2 - \bar{u}_1^2}{2} + \frac{P_2 - P_1}{\rho} = 0 \Rightarrow \boxed{\frac{\bar{u}_2^2 - \bar{u}_1^2}{2} = \frac{P_1 - P_2}{\rho}}$$

## MECHANICAL ENERGY BALANCE EQUATION

$$g\Delta Z + \frac{\Delta \bar{u}^2}{2} + \frac{\Delta P}{\rho} + \dot{W}_{Sout} = 0$$



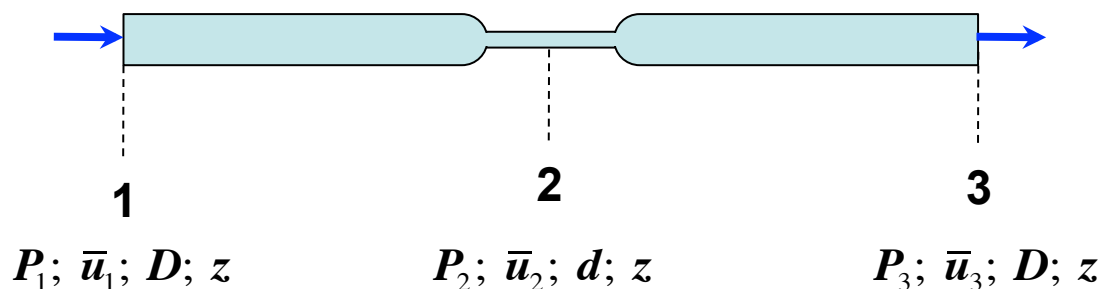
MEB between point 2 and 3:

$$\cancel{g\Delta Z} + \frac{\Delta u^2}{2} + \frac{\Delta P}{\rho} + \cancel{\dot{W}_{Sout}} = 0$$

$$\frac{\Delta u^2}{2} + \frac{\Delta P}{\rho} = 0 \Rightarrow \frac{u_3^2 - u_2^2}{2} + \frac{P_3 - P_2}{\rho} = 0 \Rightarrow \boxed{\frac{u_3^2 - u_2^2}{2} = \frac{P_2 - P_3}{\rho}}$$

## MECHANICAL ENERGY BALANCE EQUATION

$$g\Delta Z + \frac{\Delta \bar{u}^2}{2} + \frac{\Delta P}{\rho} + \dot{W}_{Sout} = 0$$



MEB between point 1 and 3:

$$\cancel{g\Delta Z} + \frac{\Delta \bar{u}^2}{2} + \frac{\Delta P}{\rho} + \cancel{\dot{W}_{Sout}} = 0$$

$$\frac{\Delta \bar{u}^2}{2} + \frac{\Delta P}{\rho} = 0 \Rightarrow \frac{\bar{u}_3^2 - \bar{u}_1^2}{2} + \frac{P_3 - P_1}{\rho} = 0 \Rightarrow \frac{\bar{u}_3^2 - \bar{u}_1^2}{2} = \frac{P_1 - P_3}{\rho}$$

$$P_1 = P_3$$



## MECHANICAL ENERGY BALANCE EQUATION

Consider a simple case where fluid flows in a horizontal tube. This time we **will not ignore** the energy loss due to the friction of fluid on tube walls (assume liquid fluid  $\rho = \text{const}$ ).



$$\cancel{g\Delta Z} + \cancel{\frac{\Delta \bar{u}^2}{2}} + \frac{\Delta P}{\rho} + \sum F + \cancel{\dot{W}_{Sout}} = 0$$

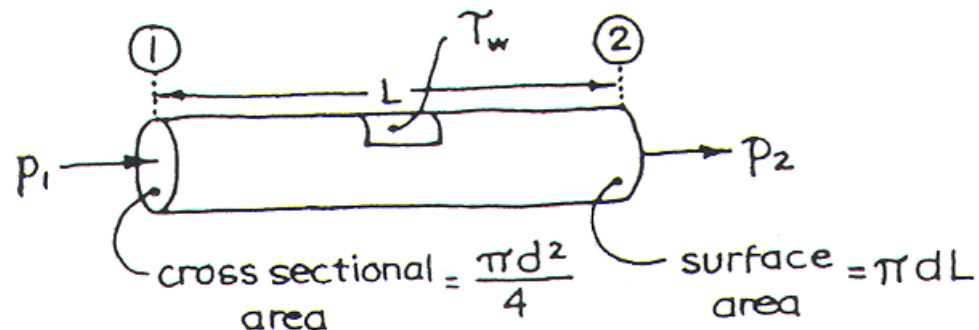
$$\sum F = -\frac{P_2 - P_1}{\rho} \Rightarrow \rho \sum F = P_1 - P_2 = \Delta P_{friction}$$

$$\rho \sum F = \Delta P_{friction}$$

## MECHANICAL ENERGY BALANCE EQUATION

In order to account for the friction losses we may conveniently define a Friction Factor,  $f_F$ , as:

$$f_F = \frac{\left( \frac{\text{Frictional Drag Force}}{\text{Area of Pipe Surface}} \right)}{\text{Kinetic Energy of Fluid}} = \frac{\left( \frac{F_{\text{Drag}}}{A_{\text{pipe}}} \right)}{\frac{\rho u^2}{2}}$$





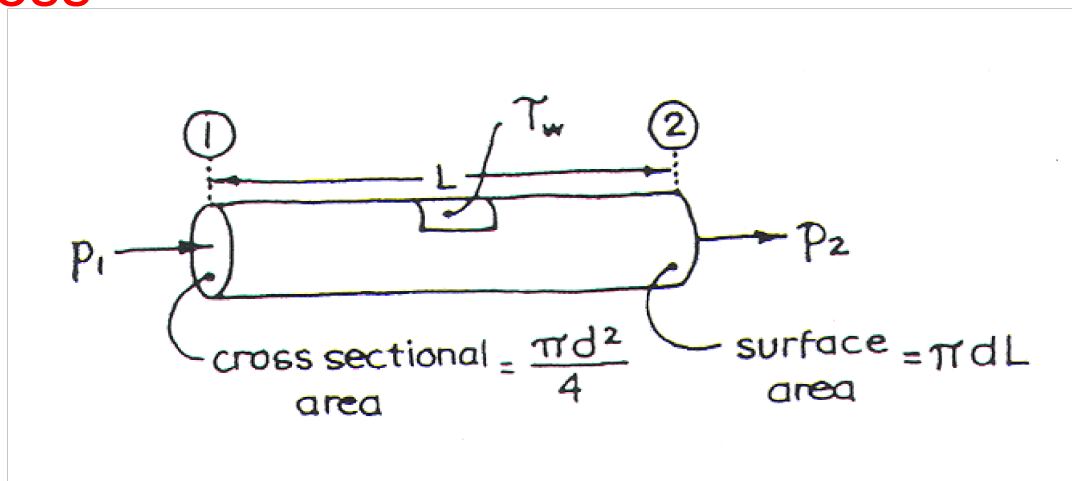
## MECHANICAL ENERGY BALANCE EQUATION

$$F_{Drag} = f_F A_{pipe} \frac{\rho \bar{u}^2}{2} \Rightarrow \frac{F_{Drag}}{A_{pipe}} = \tau_w = f_F \frac{\rho \bar{u}^2}{2}$$

$$\tau_w = f_F \frac{\rho \bar{u}^2}{2}$$

Average velocity

Shear Stress





$$\sum F = -\frac{P_2 - P_1}{\rho} \Rightarrow \rho \sum F = P_1 - P_2 = \Delta P_{friction}$$

*{Energy lost by the fluid} = {Energy transmitted to the walls}*

$$\left\{ L \left( \frac{\pi d^2}{4} \right) (P_1 - P_2) \right\} = \{ L * L \pi d * \tau_w \}$$

$$\left\{ L \left( \frac{\pi d^2}{4} \right) \rho \sum F \right\} = \left\{ L * L \pi d * f_F \frac{\rho u^2}{2} \right\}$$

$$\left\{ L \left( \frac{\pi d^2}{4} \right) \rho \sum F \right\} = \left\{ L * L \pi d * f_F \frac{\rho u^2}{2} \right\}$$

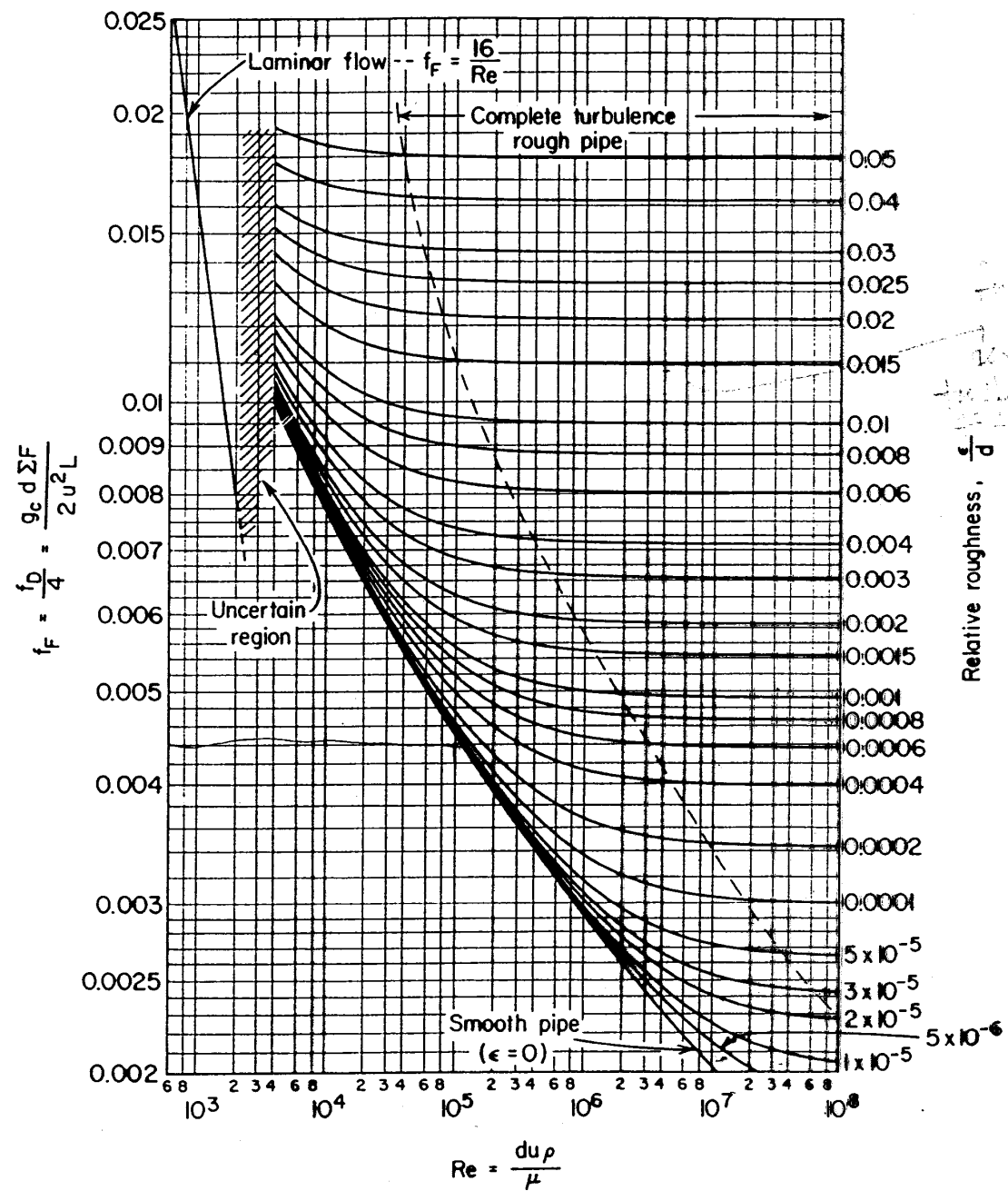
$$\sum F = \frac{2 f_F L u^2}{d}$$

At this point, we still do not know anything about frictional losses because we do not know how to evaluate  $f_F$ . Researchers have found that:

$$f_F = \varphi \{ \text{Reynolds number (Re); Pipe roughness } (\varepsilon) \}$$



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## MECHANICAL ENERGY BALANCE EQUATION

Finally:

$$g\Delta Z + \frac{\Delta \bar{u}^2}{2} + \frac{\Delta P}{\rho} + \sum F + \dot{W}_{Sout} = 0$$

$$\sum F = \frac{2f_F L \bar{u}^2}{d}$$

$$f_F = \frac{16}{\text{Re}} \quad \text{for laminar flow (Re} < 2100 \text{ for pipe)}$$

$$\text{Re} = \frac{\rho \bar{u} d}{\mu}$$



## MECHANICAL ENERGY BALANCE EQUATION

Friction Factor for Turbulent flow:

$$\frac{1}{\sqrt{f_F}} = -4 \log \left[ \frac{\varepsilon}{3.7 * d} + \frac{1.255}{\text{Re} \sqrt{f_F}} \right]$$

$$\frac{1}{\sqrt{f_F}} = -4 * \log \left[ \frac{\varepsilon}{3.7 d} + \frac{5.76}{\text{Re}^{0.9}} \right]$$

$$\frac{1}{\sqrt{f_F}} = +4 \log \left[ \frac{3.7 * d}{\varepsilon} \right] \quad \text{For friction factor independent of Re}$$

$$\frac{1}{\text{Re}} = \frac{\sqrt{f_F}}{1.255} \left[ 10^{-\frac{0.25}{\sqrt{f_F}}} - \frac{\varepsilon}{3.7 * d} \right]$$



## MECHANICAL ENERGY BALANCE EQUATION

For Laminar flow we can develop final expression for the frictional energy loss term:

$$\sum F = \frac{2 f_F L \bar{u}^2}{d} \quad \text{Re} = \frac{\rho \bar{u} d}{\mu}$$

$$f_F = \frac{16}{\text{Re}} \quad \text{for laminar flow (Re} < 2100 \text{ for pipe)}$$

$$\boxed{\sum F = \frac{32 \mu L \bar{u}}{d^2 \rho}}$$

## MECHANICAL ENERGY BALANCE EQUATION

Friction Losses  
in laminar flow  
(J/kg)

$$g\Delta Z + \frac{\Delta \bar{u}^2}{2} + \frac{\Delta P}{\rho} + \frac{32\mu L \bar{u}}{d^2 \rho} + \dot{W}_{Sout} = 0$$

Potential Energy    Kinetic Energy    Flow Work With  $\rho = \text{const}$     Shaft Work (out)    Steady State





*People. Ideas. Innovation.*

*Thank you for your attention!*