



**OREGON STATE UNIVERSITY**  
**School of Chemical, Biological, and Environmental Engineering**

**CHE 331**  
**Transport Phenomena I**

**Dr. Goran Jovanovic**

**Flow Through Porous Media**  
**Darcy and Brinkman Equations**

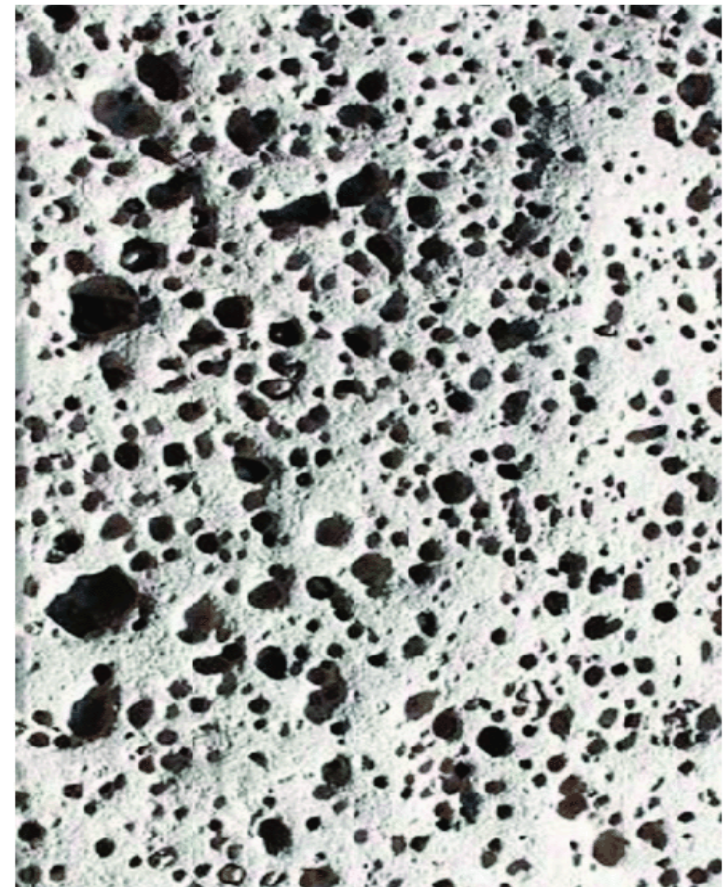
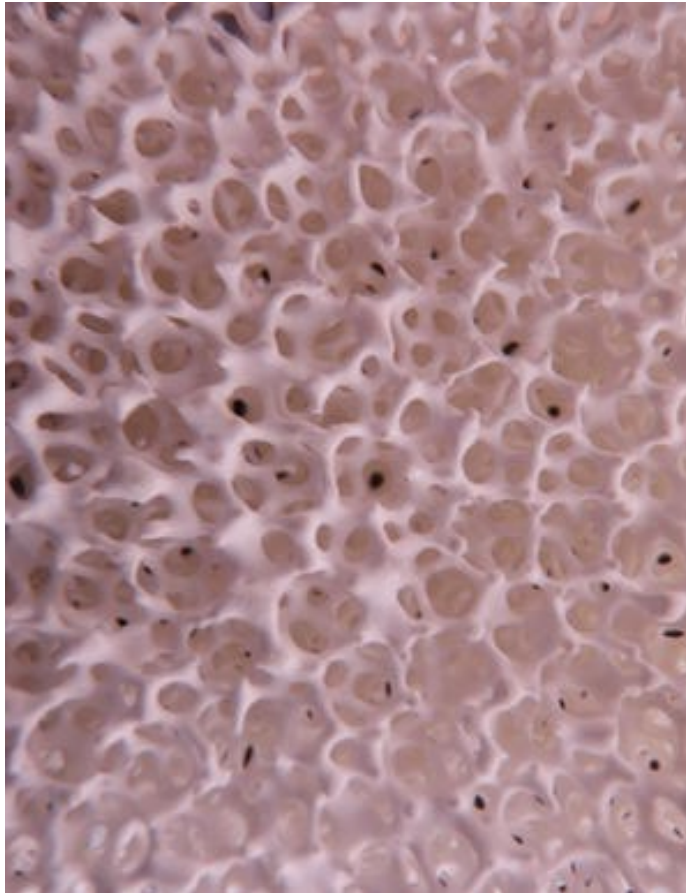
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## Flow Through Consolidated Media

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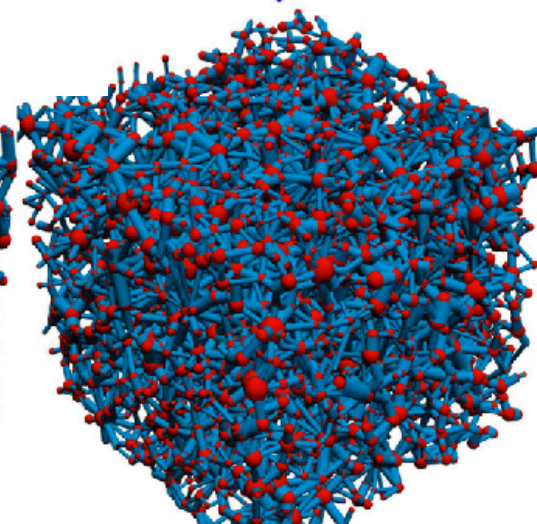
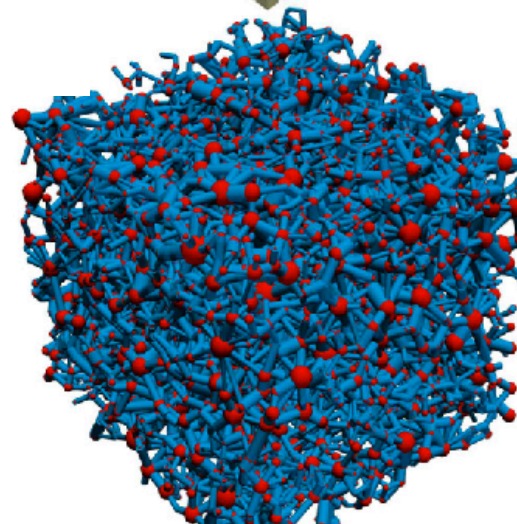
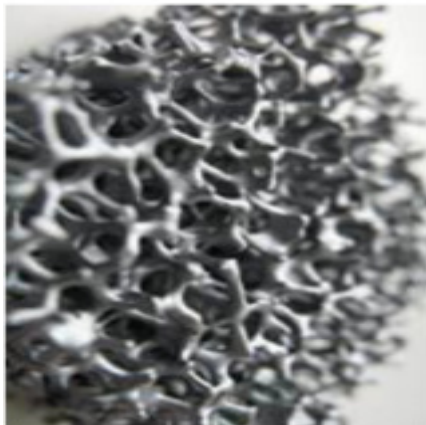
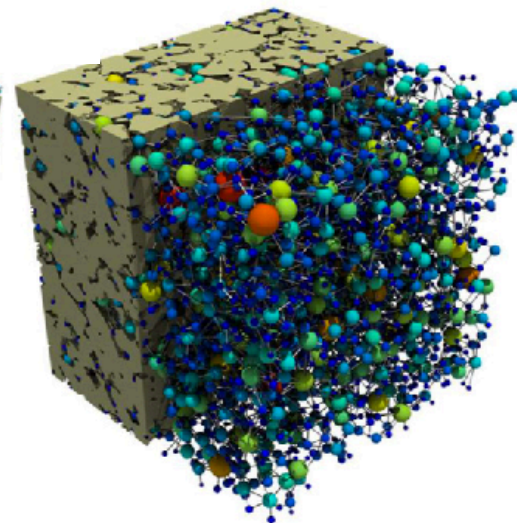
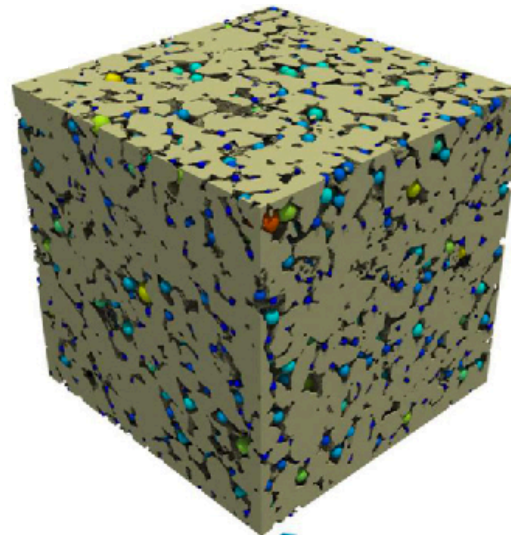
Not all porous media are made of particles; such as flow of groundwater in aquifers, flow of gas in petroleum reservoirs, etc. We refer to these cemented solids as consolidated media. We use basic principals to model flow through consolidated materials.

# Consolidated Media



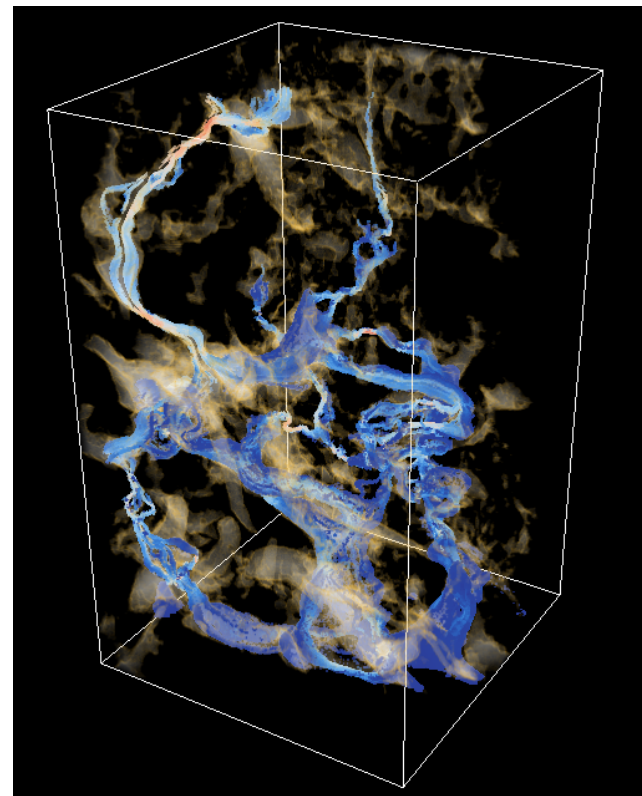
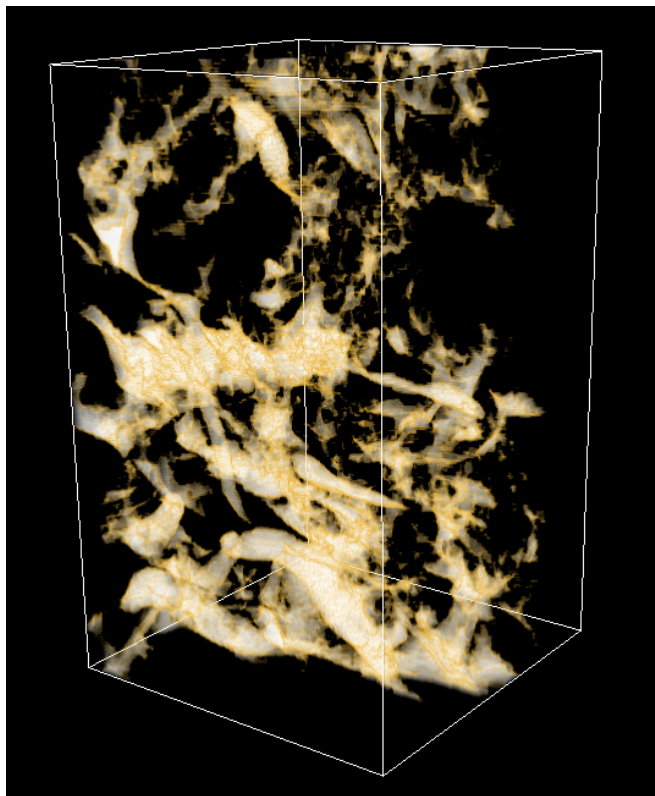


# Consolidated Media

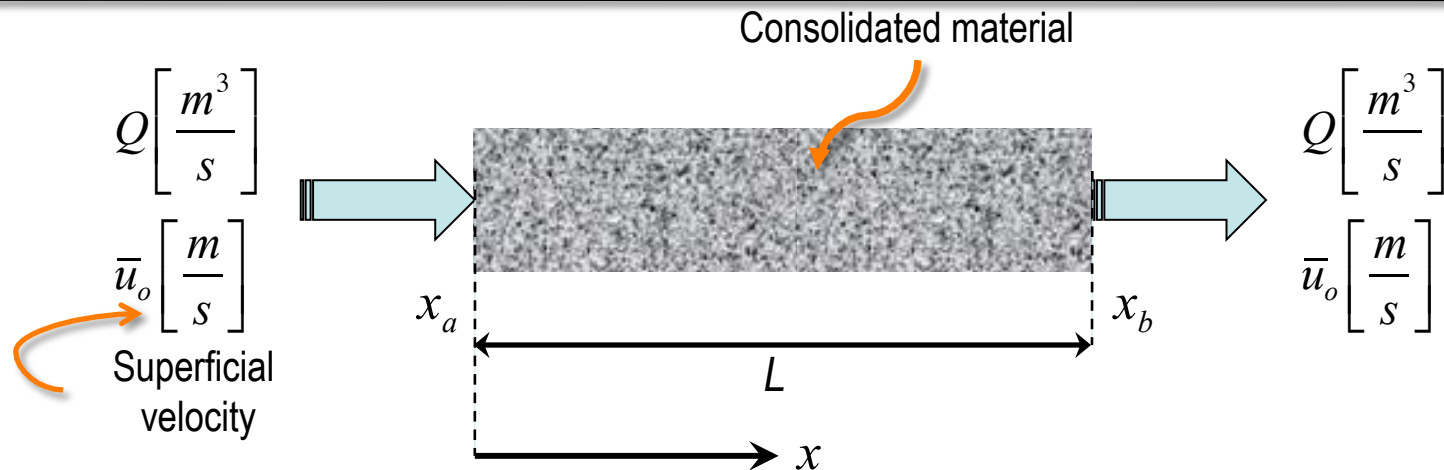




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# Darcy's Law for Laminar Flow through Porous Media



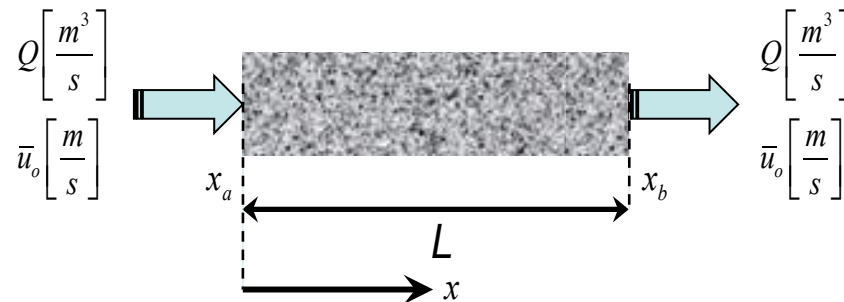
**Darcy's Law** is (actually not a Law) but an equation that describes the flow of a fluid through a porous medium. Henry Darcy derived the equation from the experimental results ( $Q$  vs.  $\Delta P$ ) of water flow through sand beds. This equation is used in hydrogeology, civil engineering, and other applications.

$$\vec{u}_o = -\frac{k}{\mu} \nabla P \quad \Rightarrow \quad \vec{u}_{ox} = -\frac{k}{\mu} \frac{dP}{dx} \quad (\text{one dimensional case})$$

$$\left( \frac{m}{s} \right) \sim \frac{(m^2)}{(Pa \cdot s)} \frac{(Pa)}{(m)}$$

# Darcy's Law for Laminar Flow through Porous Media

$$\vec{u}_{ox} = -\frac{\kappa}{\mu} \frac{dP}{dx} \Rightarrow \vec{u}_{ox} \int_{x=0}^{x=L} dx = -\frac{\kappa}{\mu} \int_{P_o}^{P_L} dP \Rightarrow \vec{u}_{ox} = -\frac{\kappa}{\mu} \frac{\Delta P}{L}$$



$\kappa$  = permeability of porous media  $[m^2]$

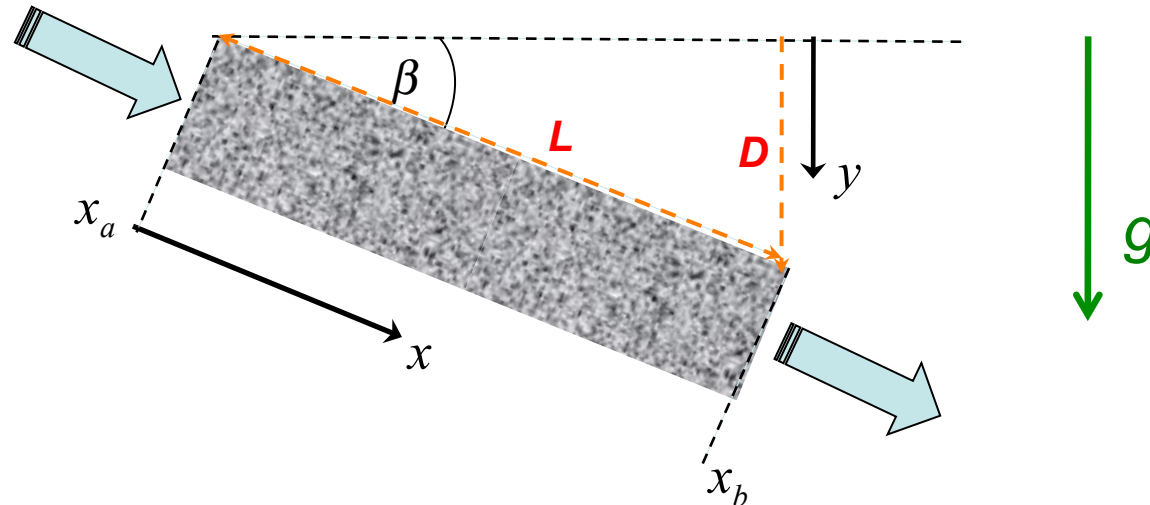
Permeability of porous media is function of porous structure, voidage, size distributions of pores, tortuosity, nature of porous media (particles, consolidated media, fibers, . . . )

$$\kappa = C \cdot \bar{d}_p^2 \quad \kappa = \bar{d}_f^2 \cdot C_1 \left( \sqrt{\frac{1 - \epsilon_c}{1 - \epsilon}} - 1 \right)^{C_2}$$

where  $d_p$  is the average pore diameter, and  $d_f$  is the average fiber diameter.

## Darcy's Law for Laminar Flow through Porous Media

For flow in inclined media where hydrostatic pressure may be important, the Darcy equation becomes:

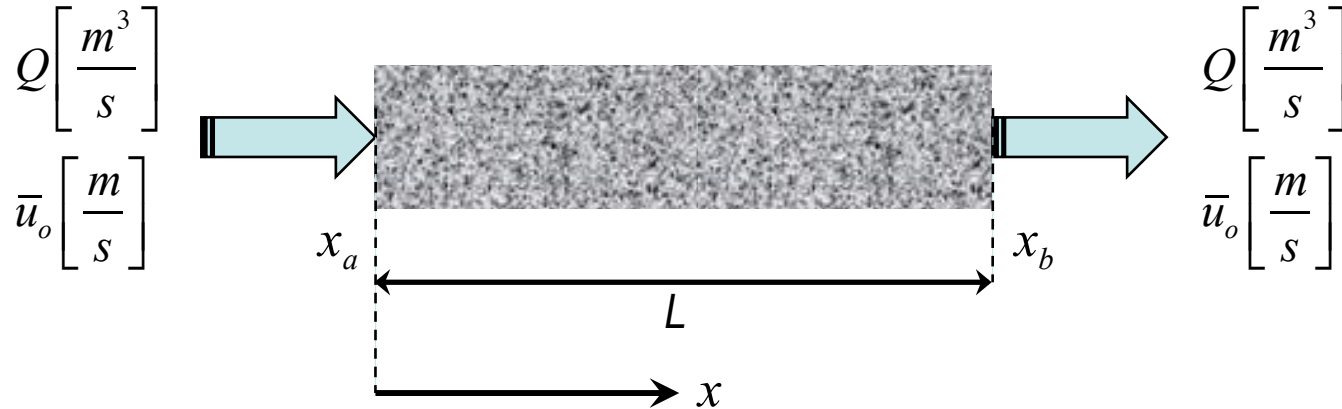


$$\vec{u}_{ox} = -\frac{\kappa}{\mu} \left( \frac{dP}{dx} - \rho g \frac{dy}{dx} \right) \Rightarrow \vec{u}_{ox} \int_{x_a}^{x_b} dx = \frac{\kappa}{\mu} \left( \int_{P_{x_b}}^{P_{x_a}} dP + \rho g \int_{y=0}^D dy \right)$$

$$\vec{u}_{ox} = \frac{\kappa}{\mu} \left( \frac{\Delta P}{L} + \rho g \frac{D}{L} \right) \Leftrightarrow \vec{u}_{ox} = \frac{\kappa}{\mu} \left( \frac{\Delta P}{L} + \rho g \sin(\beta) \right)$$



# Darcy's Law for Laminar Flow through Porous Media



Now, if we write the energy balance equation for this system:

$$g\Delta Z + \cancel{\frac{\Delta u_o^2}{2}} + \frac{\Delta P}{\rho} + \sum F + \cancel{W_{Sout}} = 0$$

$$-\rho g\Delta Z - \Delta P = \rho \sum F$$

$\Rightarrow$

$$\vec{u}_{ox} = \frac{\kappa}{\mu} \left( \frac{\Delta P + \rho g D}{L} \right)$$

$\Downarrow$

$$\Rightarrow \vec{u}_{ox} \frac{\mu \cdot L}{\kappa} = \rho \sum F$$

$$(\Delta P + \rho g D) = \vec{u}_{ox} \frac{\mu \cdot L}{\kappa}$$

# Brinkman Equation

One could use Ergun's equation to define permeability of flow in packed beds:

$$\vec{u}_{ox} \frac{\mu \cdot L}{\kappa} = \rho \sum F \Rightarrow \kappa = \vec{u}_{ox} \frac{\mu \cdot L}{\rho \sum F}$$

Use Ergun Equation

The *Brinkman* Equation for laminar flow through porous and non-porous media is:

$$-\left(\frac{dP}{dx} - \rho g \sin(\beta)\right) = \vec{u}_{ox} \frac{\mu}{\kappa} - \mu \frac{d^2 \vec{u}_{ox}^2}{dx^2}$$

Pressure drop in laminar  
flow through pipes/channels



Pressure drop in  
porous media



# Darcy Equation in Multidimensional Flow

In operator form, *Darcy* equation can be written:

$$\vec{u}_o = -\frac{\kappa}{\mu}(\nabla P - \rho g \nabla D)$$

*Darcy* equation in Cartesian coordinate system:

$$\vec{u}_{ox} = -\frac{\kappa_x}{\mu} \left( \frac{dP}{dx} - \rho g \frac{dD}{dx} \right)$$

$$\vec{u}_{oy} = -\frac{\kappa_y}{\mu} \left( \frac{dP}{dy} - \rho g \frac{dD}{dy} \right)$$

$$\vec{u}_{oz} = -\frac{\kappa_z}{\mu} \left( \frac{dP}{dz} - \rho g \frac{dD}{dz} \right)$$

