BPL CHO Perfusion cspr openloop - demo

This notebook is about CHO perfusion cultivation and focus on the concept of Cell Specific Perfusion Rate (CSPR). Recombinant protein production is included in the model but not shown in the diagrams here.

The model used here was orignally developed and validated for fed-batch cultivation of CHO cultures [1], but also got some influence from perfusion cultivation [2]. The model emphasize the bottlenecks of metabolism and growth and inspired from similar models of microbial cultures. One interesting aspect is that the model brings a theoretical base for the usefulness of the CSPR concept often used experimentally [4] and [5]. The results of simulation shown here are in accordance with experiments in a qualititative way, howerver not tested more quantitatively, to the authors knowledge.

The main result is that when the perfusion rate should be increased from one set-point to another, it should be changed slowly. An abrupt step-wise increase should be avoided. A slow increase in the pefusion rate minimize the risk of unnecessary by-product formation of lactate and amonia and make the culture increase in cell concentration quicker to a new steady-state compared to a step-wise perfusion rate change. The rate of change of perfusion rate should not exceed the maximal culture growth rate.

The strategy to limit rate of change of perfusion rate is much more important for mammalian cultures than for microbial cultures. The reason is that mammalian cell cutures increase in cell density after an inrease in perfusion rate, while mibrobial cultures remains constant in cell density. This difference is most likely due to the fact that maintenance metabolism is a larger part in mammalian cultures and at higher growth rates the percentage of maintenance becomes smaller and the overall yield increase, while microbial cultures has a much more contsant yield over a broad range of growth rates. These ideas are discussed in section 2.2 in [3], together with other insights into perfusion cultivation obtained from simulation studies of the current model.

Once again, it would be good to compare simulations with relevant experimental data from perfusion cultivation. Hopefully, the material presented here can stimulate work in this direction.

Setup of the simulation model

```
In [1]:  run -i BPL_CHO_perfusion_cspr_openloop_explore.py
```

```
Windows - run FMU pre-compiled JModelica 2.14

Model for the process has been setup. Key commands:
 - par()        - change of parameters and initial values
 - init()       - change initial values only
 - simu()       - simulate and plot
 - newplot()    - make a new plot
 - show()       - show plot from previous simulation
 - disp()       - display parameters and initial values from the last simulation
 - describe()   - describe culture, broth, parameters, variables with values/units

Note that both disp() and describe() takes values from the last simulation
and the command process_diagram() brings up the main configuration

Brief information about a command by help(), eg help(simu)
Key system information is listed with the command system_info()
```
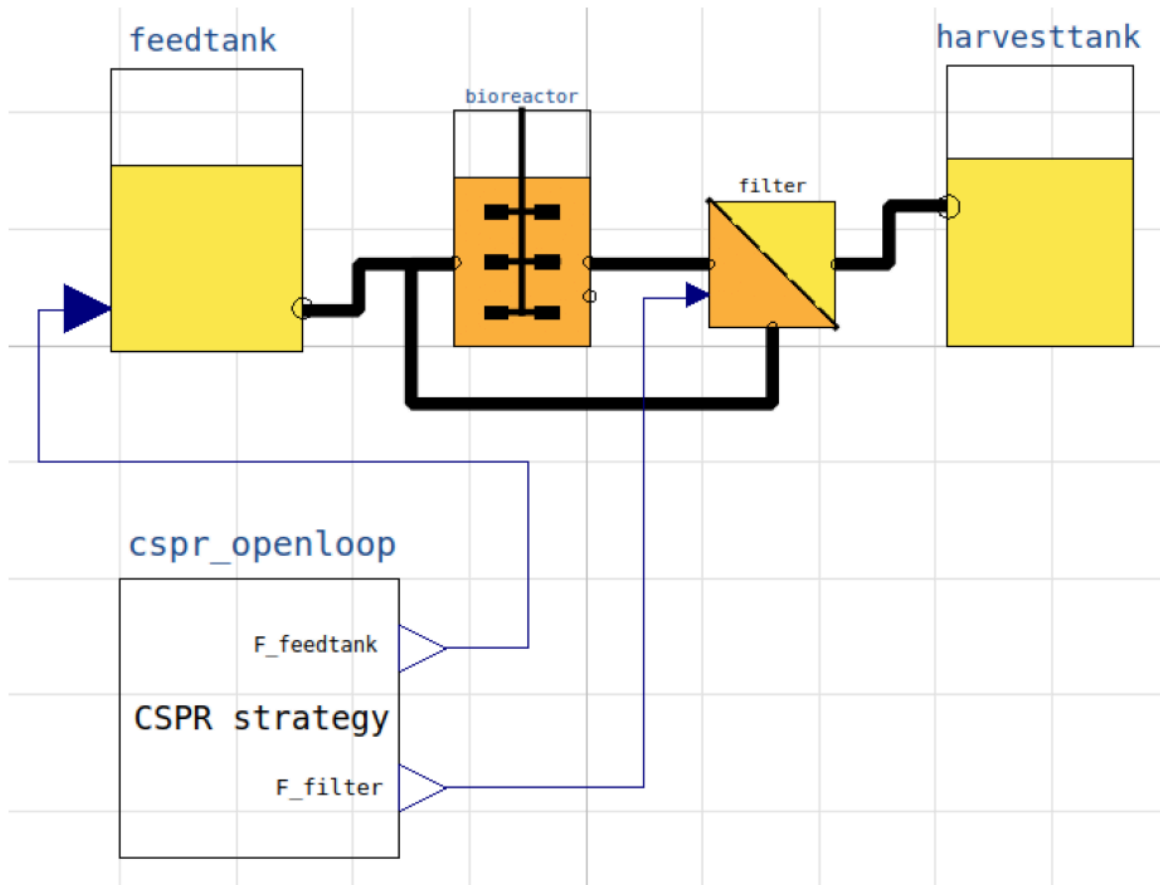
In [2]:
```python
# Set the size of diagrams
plt.rcParams['figure.figsize'] = [30/2.54, 24/2.54]
```

About the process model

Here a process diagram is shown of the process. Further information about the culutre stored in the model code is extracted.

In [3]:
```python
process_diagram()
```

```
No processDiagram.png file in the FMU, but try the file on disk.
```


In [4]:
```python
#describe('culture'); print(); describe('broth')
```

Simulaton study

The simulations are run with default parameters from [1]. The parameters for the change of perfusion rate is done here. The parameter mu_ref gives the rate of increase in [1/h]. With the value mu_ref=1 you get an abrupt step directly to the set-point. The parameters F1 and F2 give the flow rate [L/h] before and after the change. The corresponding time parameters t1 and t2 are given by default.

```
In [5]: newplot('Perfusion cultivation', plotType='Extended')

par(samplePeriod=1); par(F1=0.0020, F2=0.030)      # General parameters
par(mu_ref=0.04); simu()                           # First simulation (solid)
par(mu_ref=1); simu()                              # Second simulation (dashed)
```


Perfusion cultivation
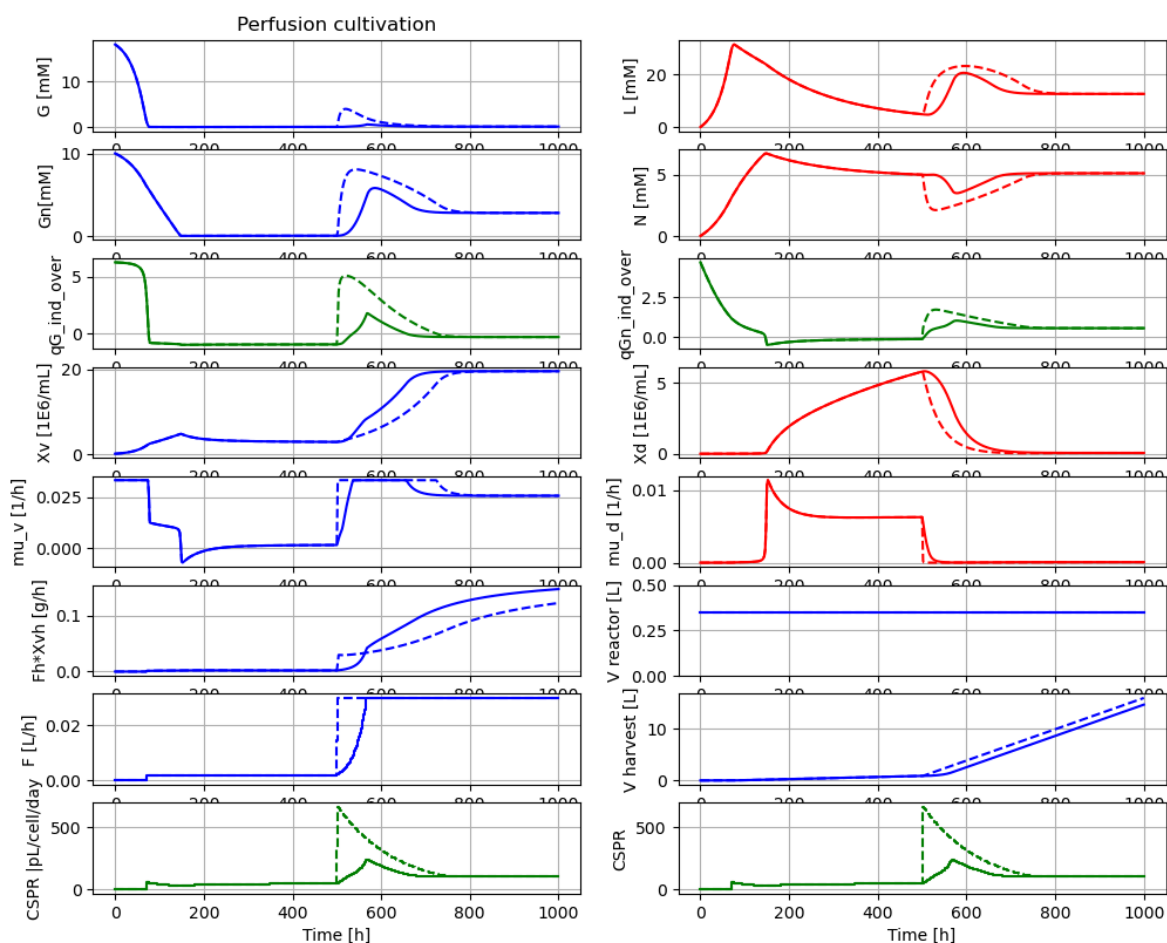
We see here the shorter settling time for cell conc Xv when the slower exponential increase of perfusion rate is used, compared to an abrupt change.

The different sets of parameters that can be changed are shown below

```
In [6]: disp(mode='long')
```

```
bioreactor.V_start : V_start : 0.35
bioreactor.m_start[1] : VXv_start : 0.07
bioreactor.m_start[2] : VXd_start : 0.0
bioreactor.m_start[3] : VXl_start : 0.0
bioreactor.m_start[4] : VG_start : 6.3
bioreactor.m_start[5] : VGn_start : 3.5
bioreactor.m_start[6] : VL_start : 0.0
bioreactor.m_start[7] : VN_start : 0.0
bioreactor.culture.qG_max1 : qG_max1 : 0.297
bioreactor.culture.qG_max2 : qG_max2 : 0.038
bioreactor.culture.qGn_max1 : qGn_max1 : 0.124
bioreactor.culture.qGn_max2 : qGn_max2 : 0.022
bioreactor.culture.mu_d_max : mu_d_max : 0.13
bioreactor.culture.k_toxic : k_toxic : 0.0
bioreactor.culture.alpha : alpha : 0.0
bioreactor.culture.beta : beta : 0.417
bioreactor.broth_decay.k_lysis_v : k_lysis_v : 0.0
bioreactor.broth_decay.k_lysis_d : k_lysis_d : 0.0
filter.eps : eps : 0.1
filter.alpha[1] : alpha_Xv : 0.03
filter.alpha[2] : alpha_Xd : 0.03
filter.alpha[3] : alpha_Xl : 0.1
filter.alpha[4] : alpha_G : 0.1
filter.alpha[5] : alpha_Gn : 0.1
filter.alpha[6] : alpha_L : 0.1
filter.alpha[7] : alpha_N : 0.1
filter.alpha[8] : alpha_Pr : 0.1
feedtank.c_in[4] : G_in : 15.0
feedtank.c_in[5] : Gn_in : 11.0
cspr_openloop.samplePeriod : samplePeriod : 1.0
cspr_openloop.mu_ref : mu_ref : 1.0
cspr_openloop.t1 : t1 : 70.0
cspr_openloop.F1 : F1 : 0.002
cspr_openloop.t2 : t2 : 500.0
cspr_openloop.F2 : F2 : 0.03
```

Some other important parameters for information, but cannot be changed

In [7]:
```python
describe('bioreactor.broth_decay.k_decay')
```

Rate of decay of viable cells : 0.0 [1E9 cells/(L*h)]

In [8]:
```python
describe('k_lysis_d')
```

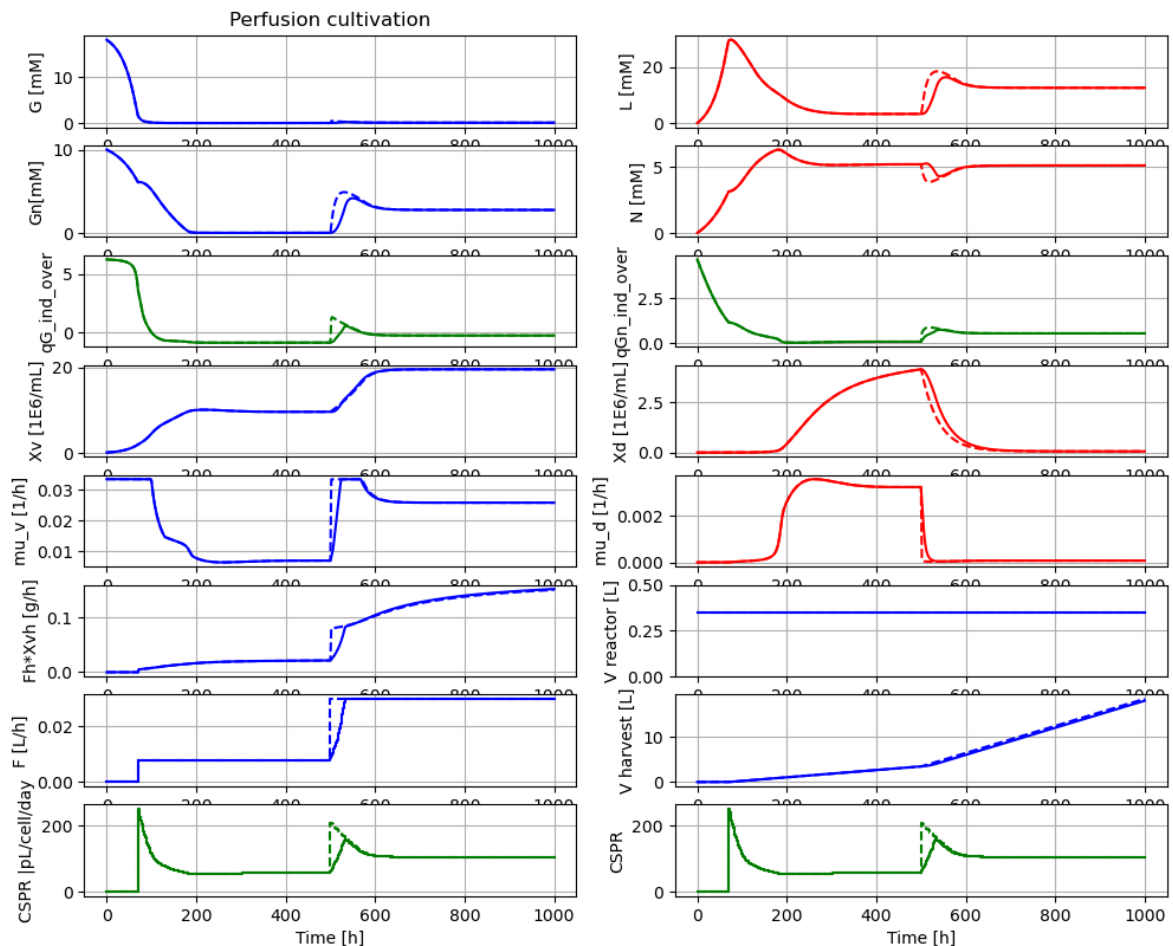Specific rate of lysis of dead cells : 0.0 [1/h]

Now a new simulation where the flow rate F1 is higher before change to the new set-point F2.

In [9]:
```python
newplot('Perfusion cultivation', plotType='Extended')

par(samplePeriod=1); par(F1=0.0080, F2=0.03)      # General parameters
par(mu_ref=0.04); simu()                          # First simulation (solid)
par(mu_ref=1); simu()                             # Second simulation (dashed)
```

We see that a somewhat smaller change in perfusion rate make the differnce in settling time of Xv for the two strategies to almost disappear.

Summary

The simulation study shows that a slow increase in the perfusion rate that match the maximal culture growth rate gives a quicker increase in cell density than an abrupst step-wise change of perfusion rate.

The effect is more pronounced for a larger change of perfusion rate than for a smaller.

Here the change of perfusion rate was done usering a pre-calculated exponential scheme, i.e. open-loop control. A more robust method would be to measure the cell concentration on-line and adjust the perfusion rate change to more exactly maintan constant CSPR.

It is of interest to confirm the results with experimental data.

References

[1] Amribt, Z., Niu, H. and Bogaerts P.: "Macroscopic modelling of overflow metabolism and model based optimization of hybridoma cell fed-batch cultures.", Biochem. Eng. Journal, 2013.

[2] Niu,H., Amribt, Z., Fickers, P., Tan, W. and Bogaerts P.: "Metabolic pathway analysis and reduction for mammalian cell cultures - towards macroscopic modelling", Chem. Eng. Science, 2013.

[3] Axelsson, J. P.: "Simplified model of CHO-cultivation in Bioproces Library for Modelica - some experience", conference paper 22nd NPCW Lyngby, Denmark, August 22-23, 2019.

[4] Hu, W-S: "Cell culture bioprocess engineering", 2nd edition, CRC Press, 2020.

[5] Konstantinov, K. et al: "The push-to-low" approach for optimization of high density perfusion cultures of animal cells", Adv Biochem Engin/Biotechnol, 2006.

Appendix

```
In [10]: describe('parts')
```

```
['bioreactor', 'bioreactor.broth_decay', 'bioreactor.culture', 'CSPR', 'cspr_open
loop', 'D', 'feedtank', 'filter', 'harvesttank', 'liquidphase', 'MSL']
```

```
In [11]: describe('MSL')
```

```
MSL: RealInput, RealOutput
```

```
In [12]: system_info()
```

```
System information
 -OS: Windows
 -Python: 3.12.11
 -Scipy: not installed in the notebook
 -PyFMI: 2.18.3
 -FMU by: JModelica.org
 -FMI: 2.0
 -Type: FMUModelCS2
 -Name: BPL_CHO.Perfusion_cspr_openloop
 -Generated: 2025-07-22T18:04:14
 -MSL: 3.2.2 build 3
 -Description: Bioprocess Library version 2.3.1
 -Interaction: FMU-explore version 1.0.0
```

```
In [13]: !lsb_release -a
```

```
'lsb_release' is not recognized as an internal or external command,
operable program or batch file.
```