BPL_IEC_validation script with PyFMI

The key library PyFMI is installed.

After the installation a small application BPL_IEC_validation is loaded and run. You can continue with this example if you like.

```
!lsb_release -a # Actual VM Ubuntu version used by Google
    No LSB modules are available.
    Distributor ID: Ubuntu
    Description:
                   Ubuntu 22.04.3 LTS
    Release:
                   22.04
    Codename:
                   jammy
%env PYTH0NPATH=
    env: PYTHONPATH=
!wget https://repo.anaconda.com/miniconda/Miniconda3-py310_23.1.0-1-Linux-x86_64.
!chmod +x Miniconda3-py310_23.1.0-1-Linux-x86_64.sh
!bash ./Miniconda3-py310 23.1.0-1-Linux-x86 64.sh -b -f -p /usr/local
import sys
sys.path.append('/usr/local/lib/python3.10/site-packages/')
    --2024-01-18 11:11:45-- https://repo.anaconda.com/miniconda/Miniconda3-py310
    Resolving repo.anaconda.com (repo.anaconda.com)... 104.16.131.3, 104.16.130.3
    Connecting to repo.anaconda.com (repo.anaconda.com)|104.16.131.3|:443... connecting
    HTTP request sent, awaiting response... 200 OK
    Length: 74403966 (71M) [application/x-sh]
    Saving to: 'Miniconda3-py310_23.1.0-1-Linux-x86_64.sh'
    in 0.8s
    2024-01-18 11:11:46 (92.0 MB/s) - 'Miniconda3-py310_23.1.0-1-Linux-x86_64.sh'
    PREFIX=/usr/local
    Unpacking payload ...
    Installing base environment...
    Downloading and Extracting Packages
    Downloading and Extracting Packages
    Preparing transaction: done
    Executing transaction: done
    installation finished.
```

!conda update -n base -c defaults conda --yes

Preparing transaction: done Verifying transaction: done Executing transaction: done

```
!conda --version
!python --version
```

conda 23.11.0 Python 3.10.13

!conda install -c conda-forge pyfmi --yes # Install the key package

```
Preparing transaction: done Verifying transaction: done Fxecuting transaction: done
```

```
# Notes of BPL_IEC_validation
```

Now specific installation and the run simulations. Start with connecting to Github. Then upload the two files:

- FMU BPL_IEC_Column_system_linux_om_me
- Setup-file BPL_IEC_explore

```
%%bash
git clone https://github.com/janpeter19/BPL_IEC_validation
    Cloning into 'BPL_IEC_validation'...
%cd BPL_IEC_validation
    /content/BPL_IEC_validation
```

BPL IEC validation

Author: Jan Peter Axelsson

```
run -i BPL_IEC_explore.py
    Linux - run FMU pre-comiled OpenModelica 1.21.0
    Model for bioreactor has been setup. Key commands:
     - par()

    change of parameters and initial values

     - init()

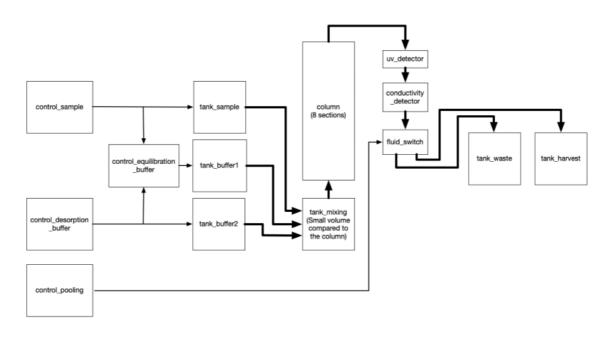
    change initial values only

     - simu()

    simulate and plot

     - newplot() - make a new plot
     - show()
                   - show plot from previous simulation
                   - display parameters and initial values from the last simulation
     - disp()
     describe() - describe culture, broth, parameters, variables with values/ur
    Note that both disp() and describe() takes values from the last simulation
    and the command process_diagram() brings up the main configuration
    Brief information about a command by help(), eg help(simu)
    Key system information is listed with the command system_info()
```

The process diagram is made outside Modelica to illustrate the configuration process diagram()



describe('chromatography'); # print(); describe('liquidphase')

Ion exchange chromatorgraphy controlled with varying salt-concentration. The process of the concentration of the concentration of the process of the concentration of the concentrat

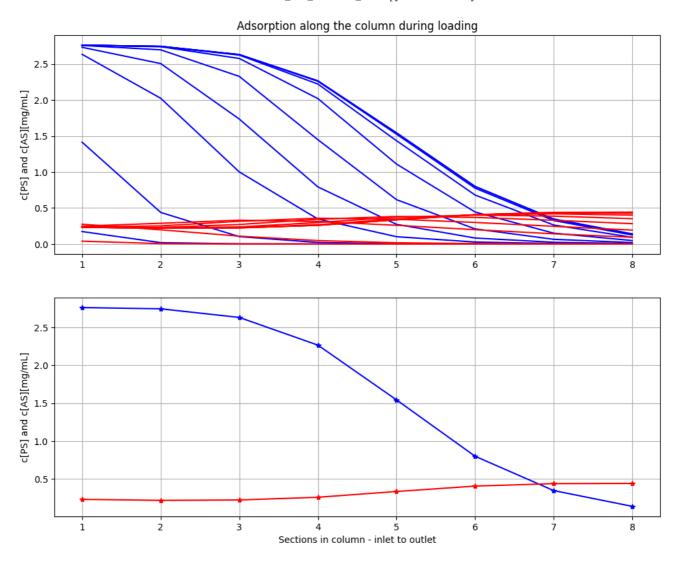
Loading or adsorption

The parameter notation and values are the same as in the referred report. However the flow rate is here denoted F while q in the report. The column is diveded in n=8 sections and set at compilation time. The values are arbitrarly chosen in the report and the focus is on qualitative aspects of the model.

The simplified model describe only the column in terms of volume and does not distinguish a high column with a small diameter from a lower with larger diameter.

The parameters k1, k2, k3, k4 and Q_av are given relative volume and with increased column volume a larger capacity is thus obtained.

```
# Loading of the column - try to reproduce Jonas figure 13.
newplot(title='Adsorption along the column during loading', plotType='Loading')
# Sample
par(P_in=1.0, A_in=1.0, E_in=0)
# Column properties
par(k1=0.3, k2=0.05, k3=0.05, k4=0.3, Q_av=3.0)
par(height=20, diameter=0.714)
par(x_m=0.3)
# Operation
par(E_in_desorption_buffer=8)
par(LFR=12)
par(scale_volume=False)
par(start_adsorption=0, stop_adsorption=50)
par(start_desorption=150, stationary_desorption=450)
par(start_pooling=220, stop_pooling=450)
# Simulation
simu(100)
```



The results are the same af Figure 13 in [1].

We just check that we had the same volume flow rate as Jonas describe('F')

Column volumetric flow rate : 0.08 [mL/min]

describe('V')

```
Column volume total - derived : 8.008 [ mL ]

model.get('column.x_m')
    array([0.3])

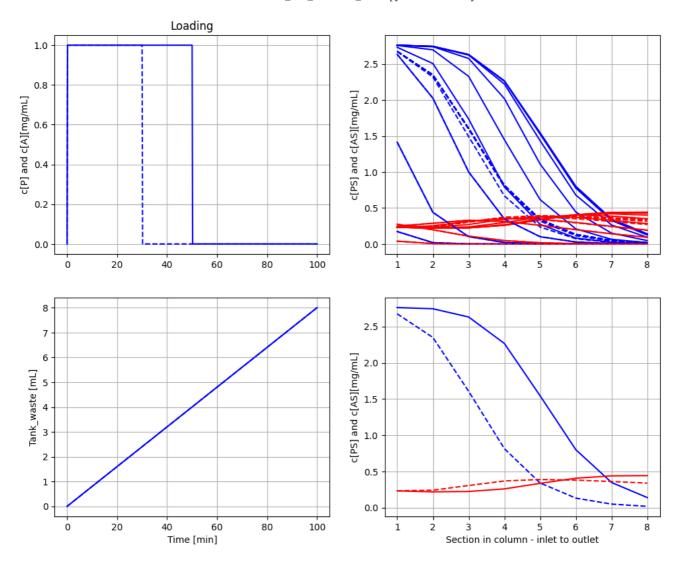
model.get('column.V_m')
    array([2.40235705])

#describe('column.column_section[1].V_m')
    array([0.30029463])

# Impact of shorter time for loading and then less material newplot(title='Loading', plotType='Loading-combined') show()

# Simulation with changed parameter t2
par(stop_adsorption=30); simu(100)

# Reset changed parameter
par(stop_adsorption=50)
```



To the left the inlet loading over time. To the right upper concentration along the column at different times and in steady states finally To the right lower concentrations along the column in steady state.

We see that a shorter time and then less material makes less of the column capacity used.

Note that the flow through the column is constant despite change from sample to just buffer 1, and shown in how the volume of the waste tank increase with time.

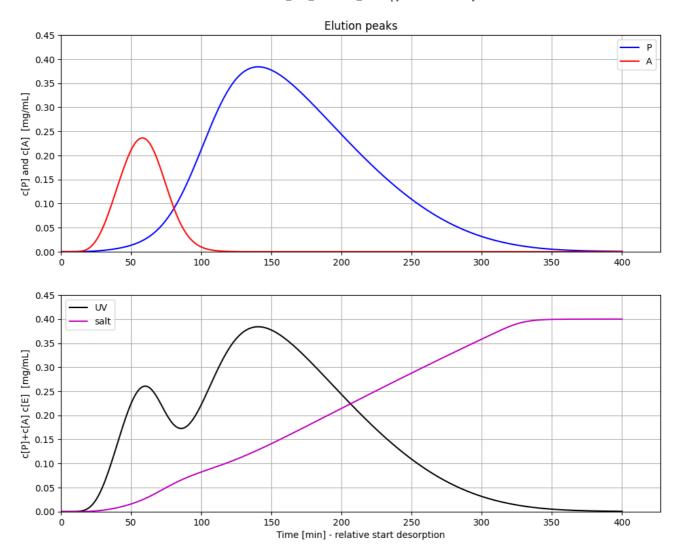
Elution or desorption

```
# Elution of the column
newplot(title='Elution peaks', plotType='Elution')

# Sample
par(P_in=1, A_in=1.0, E_in=0)

# Operation
par(E_in_desorption_buffer=8)
par(LFR=12.0, start_adsorption=0, stop_adsorption=50, start_desorption=150, stati

# Simulation
simu(550)
```



The results are the same af Figure 14 in [1].

The upper diagrams shows the column outlet concentrations of P and A over time.

The lower diagram shows the sum (or possibly the UV signal) at column outlet as well as the salt concentration. We have some separation between the two peaks.

Note that the salt concentration deviates slightly from the linear increse between time 50 to 100. This is due to ion interaction with P and A in the column. This is phenomenon can also be seen

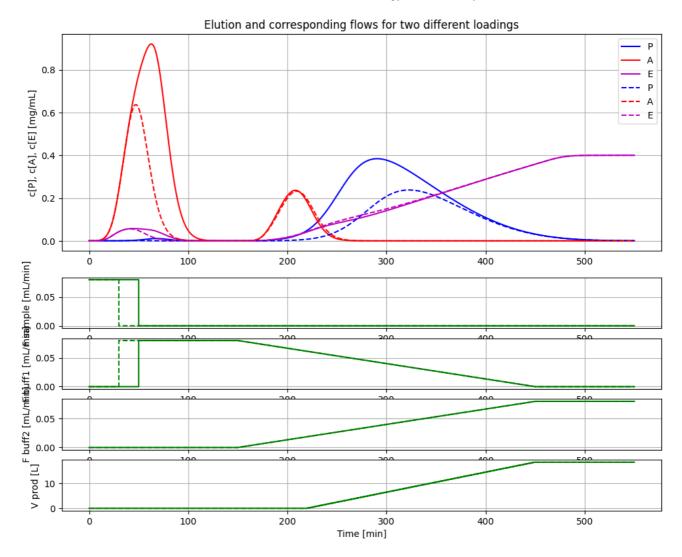
in real data. The ion-salt concentration is scaled with factor 0.05 to get comparable concentrations to P and A.

I have here simulated time 150 of adsorbtion and then started elution. Here is time counted as zero at time of start of elutions. Not sure how long Jonas simulated to get steady state before he did elution.

More complete visualization of the elution phase and the different flows newplot(title='Elution and corresponding flows for two different loadings', plotT par(stop_adsorption=50); simu(550)

Simulation with changed parameter t2
par(stop_adsorption=30); simu(550)

Reset changed parameter
par(stop_adsorption=50)



Here a diagram that shows the peaks at the outlet as shown in the previous diagram. Below the flow rates of the three different sorces. Here time is 0 at start of adsorbtion and elution starts at time 150.

Automatic pooling based on UV-mmeasurement is tested in another notebook.

Change of resin properties

```
# Elution of the column
newplot(title='Elution peaks for different resin parameters k1 and k2', plotType=
# Sample
par(P_in=1, A_in=0.0, E_in=0)
```