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## BPL\_IEC\_validation script with PyFMI

The key library PyFMI is installed.

After the installation a small application BPL\_IEC\_validation is loaded and run. You can continue with this example if you like.

```
!lsb release -a # Actual VM Ubuntu version used by Google

→ No LSB modules are available.
     Distributor ID: Ubuntu
    Description:
                      Ubuntu 22.04.3 LTS
    Release:
                      22.04
     Codename:
                      iammv
%env PYTHONPATH=
→ env: PYTHONPATH=
!wget https://repo.anaconda.com/miniconda/Miniconda3-py310_23.1.0-1-Linux-x86_64.sh
!chmod +x Miniconda3-py310_23.1.0-1-Linux-x86_64.sh
!bash ./Miniconda3-py310_23.1.0-1-Linux-x86_64.sh -b -f -p /usr/local
import sys
sys.path.append('/usr/local/lib/python3.10/site-packages/')
    --2025-01-14 09:49:20-- <a href="https://repo.anaconda.com/miniconda/Miniconda3-py310_23.1.0-1-Linux-x86_64.sh">https://repo.anaconda.com/miniconda/Miniconda3-py310_23.1.0-1-Linux-x86_64.sh</a>
    Resolving repo.anaconda.com (repo.anaconda.com)... 104.16.32.241, 104.16.191.158, 2606:4700::6810:20f1,
     Connecting to repo.anaconda.com (repo.anaconda.com)|104.16.32.241|:443... connected.
    HTTP request sent, awaiting response... 200 OK Length: 74403966 (71M) [application/x-sh]
     Saving to: 'Miniconda3-py310_23.1.0-1-Linux-x86_64.sh'
    Miniconda3-py310_23 100%[===========] 70.96M 76.1MB/s
     2025-01-14 09:49:21 (76.1 MB/s) - 'Miniconda3-py310_23.1.0-1-Linux-x86_64.sh' saved [74403966/74403966]
     PREFIX=/usr/local
     Unpacking payload ...
     Installing base environment...
     Downloading and Extracting Packages
     Downloading and Extracting Packages
     Preparing transaction: done
     Executing transaction: done
     installation finished.
!conda update -n base -c defaults conda --yes
```

Preparing transaction: done Verifying transaction: done Executing transaction: done

!conda --version
!python --version

conda 23.1.0 Python 3.10.16

!conda install -c conda-forge pyfmi --yes # Install the key package

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```
Preparing transaction: done
Verifying transaction: done
Executing transaction: done
```

# Notes of BPL\_IEC\_validation

Now specific installation and the run simulations. Start with connecting to Github. Then upload the two files:

- FMU BPL\_IEC\_Column\_system\_linux\_om\_me
- Setup-file BPL\_IEC\_explore

```
%%bash
git clone https://github.com/janpeter19/BPL_IEC_validation

Cloning into 'BPL_IEC_validation'...

%cd BPL_IEC_validation

/content/BPL_IEC_validation
```

#### BPL IEC validation

```
Author: Jan Peter Axelsson

run -i BPL_IEC_explore.py

→ Linux - run FMU pre-compiled OpenModelica
```

```
Model for bioreactor has been setup. Key commands:
- par()

    change of parameters and initial values

              - change initial values only
- init()

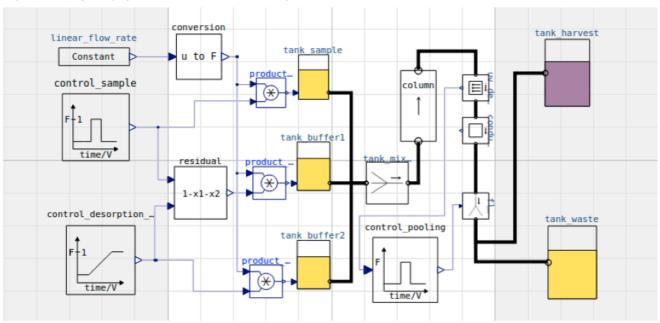
    simulate and plot

- simu()
- newplot() - make a new plot
              - show plot from previous simulation
               - display parameters and initial values from the last simulation
- disp()
- describe() - describe culture, broth, parameters, variables with values/units
Note that both disp() and describe() takes values from the last simulation
and the command process_diagram() brings up the main configuration
Brief information about a command by help(), eg help(simu)
Key system information is listed with the command system info()
```

```
plt.rcParams['figure.figsize'] = [30/2.54, 24/2.54]
```

# The process diagram is made outside Modelica to illustrate the configuration
process\_diagram()

No processDiagram.png file in the FMU, but try the file on disk.



describe('chromatography'); # print(); describe('liquidphase')

For Ion exchange chromatorgraphy controlled with varying salt-concentration. The pH is kept constant.

### Loading or adsorption

The parameter notation and values are the same as in the referred report. However the flow rate is here denoted F while q in the report. The column is diveded in n=8 sections and set at compilation time. The values are arbitrarily chosen in the report and the focus is on qualitative aspects of the model.

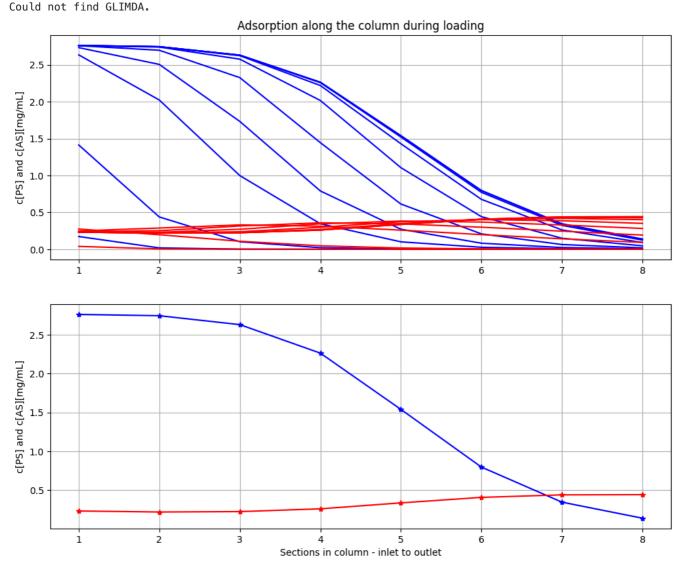
The simplified model describe only the column in terms of volume and does not distinguish a high column with a small diameter from a lower with larger diameter.

The parameters k1, k2, k3, k4 and Q\_av are given relative volume and with increased column volume a larger capacity is thus obtained.

```
# Loading of the column - try to reproduce Jonas figure 13.
newplot(title='Adsorption along the column during loading', plotType='Loading')
# Sample
par(P_in=1.0, A_in=1.0, E_in=0)
# Column properties
par(k1=0.3, k2=0.05, k3=0.05, k4=0.3, Q_av=3.0)
par(height=20, diameter=0.714)
par(x_m=0.3)
# Operation
par(E_in_desorption_buffer=8)
par(LFR=12)
#par(scale_volume=False)
par(start_adsorption=0, stop_adsorption=50)
par(start_desorption=150, stationary_desorption=450)
par(start_pooling=220, stop_pooling=450)
# Simulation
simu(100)
```

Could not find cannot import name 'dopri5' from 'assimulo.lib' (/usr/local/lib/python3.10/site-packages/Could not find cannot import name 'rodas' from 'assimulo.lib' (/usr/local/lib/python3.10/site-packages/Could not find cannot import name 'odassl' from 'assimulo.lib' (/usr/local/lib/python3.10/site-packages/Could not find ODEPACK functions.

Could not find RADAR5



The results are the same af Figure 13 in [1].

```
#describe('column.n')
```

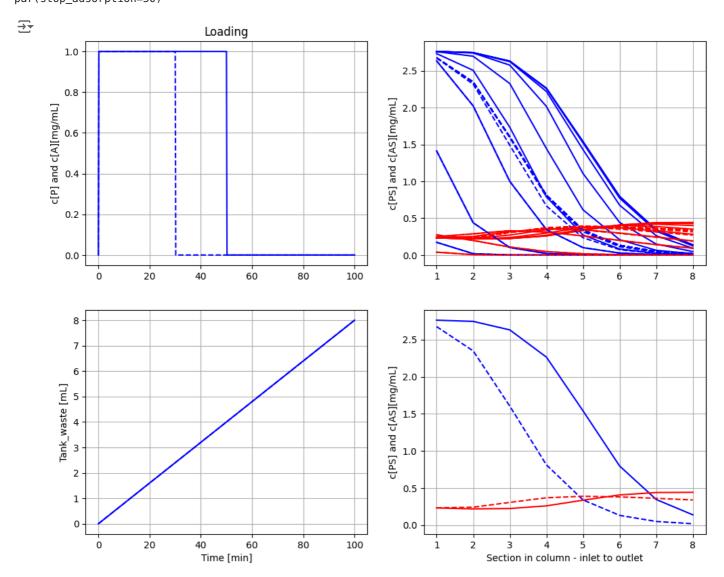
model.get('column.column\_section[1].V\_m')

```
→ array([0.30029463])
```

# Impact of shorter time for loading and then less material newplot(title='Loading', plotType='Loading-combined') show()

# Simulation with changed parameter t2
par(stop\_adsorption=30); simu(100)

# Reset changed parameter
par(stop\_adsorption=50)



To the left the inlet loading over time. To the right upper concentration along the column at different times and in steady states finally To the right lower concentrations along the column in steady state.

We see that a shorter time and then less material makes less of the column capacity used.

Note that the flow through the column is constant despite change from sample to just buffer 1, and shown in how the volume of the waste tank increase with time.

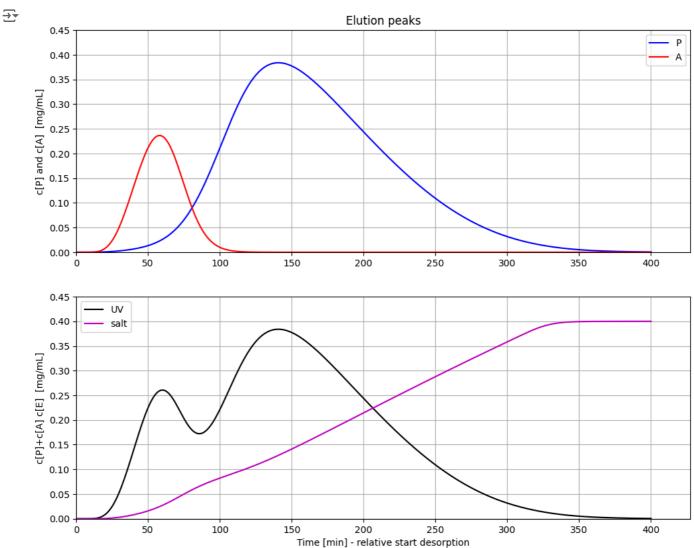
#### Elution or desorption

```
# Elution of the column
newplot(title='Elution peaks', plotType='Elution')

# Sample
par(P_in=1, A_in=1.0, E_in=0)

# Operation
par(E_in_desorption_buffer=8)
par(LFR=12.0, start_adsorption=0, stop_adsorption=50, start_desorption=150, stationary_desorption=450)

# Simulation
simu(550)
```



The results are the same af Figure 14 in [1].

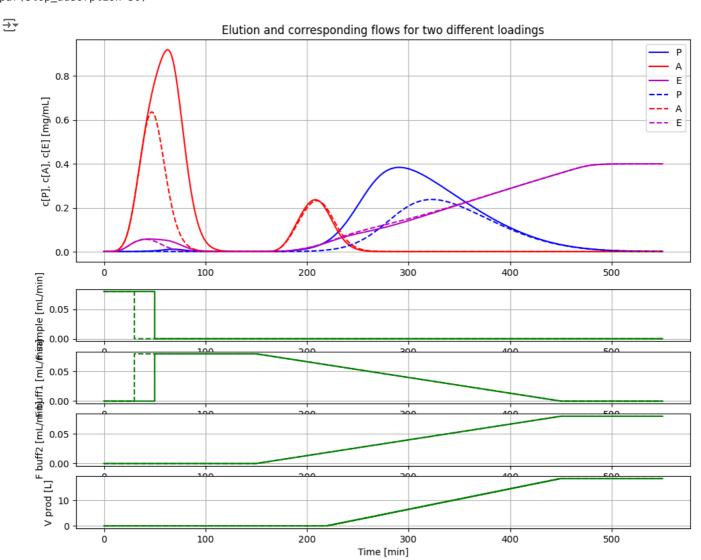
The upper diagrams shows the column outlet concentrations of P and A over time.

The lower diagram shows the sum (or possibly the UV signal) at column outlet as well as the salt concentration. We have some separation between the two peaks.

Note that the salt concentration deviates slightly from the linear increse between time 50 to 100. This is due to ion interaction with P and A in the column. This is phenomenon can also be seen in real data. The ion-salt concentration is scaled with factor 0.05 to get comparable concentrations to P and A.

I have here simulated time 150 of adsorbtion and then started elution. Here is time counted as zero at time of start of elutions. Not sure how long Jonas simulated to get steady state before he did elution. # More complete visualization of the elution phase and the different flows
newplot(title='Elution and corresponding flows for two different loadings', plotType='Elution-combined')
par(stop\_adsorption=50); simu(550)

- # Simulation with changed parameter t2
  par(stop\_adsorption=30); simu(550)
- # Reset changed parameter
  par(stop\_adsorption=50)



Here a diagram that shows the peaks at the outlet as shown in the previous diagram. Below the flow rates of the three differnet sorces. Here time is 0 at start of adsorbtion and elution starts at time 150.

 $\label{problem} \mbox{Automatic pooling based on UV-mmeasurement is tested in another notebook.}$ 

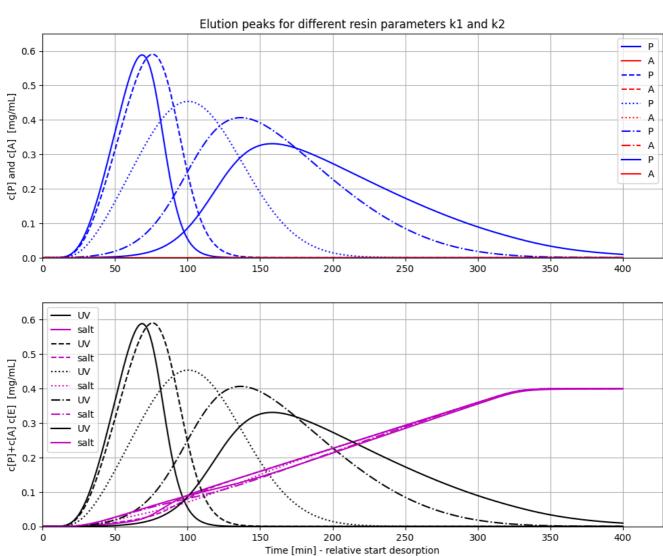
## Change of resin properties

```
# Elution of the column
newplot(title='Elution peaks for different resin parameters k1 and k2', plotType='Elution')
# Sample
par(P_in=1, A_in=0.0, E_in=0)
# Operation
par(E_in_desorption_buffer=8)
par(LFR=12.0, start_adsorption=0, stop_adsorption=50, start_desorption=150, stationary_desorption=450)
```

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```
# Simulations
par(k1=0.05, k2=0.50); simu(550)
par(k1=0.05, k2=0.25); simu(550)
par(k1=0.05, k2=0.05); simu(550)
par(k1=0.25, k2=0.05); simu(550)
par(k1=0.50, k2=0.05); simu(550)

# Adjust diagrams
ax1.set_ylim([0, 0.65])
ax2.set_ylim([0, 0.65])
plt.show()
```



The results are the same af Figure 17 in [1].

## Summary

Three important diagrams Figure 13, 14 and 17 in the original report [1] were reproduced and the implementation in Modelica used here is considered validated.

The model is now extended with an improved parametrization of the column that match the industrial practice.

# Acknowledgement

The author thank Karl Johan Brink for sharing his know-how of chromatography operation. He has especially given input to how to parametrize the model in terms often used in the industrial practice.

#### References

- 1) Månsson, Jonas, "Control of chromatography comlumn in production scale", Master thesis TFRT-5599, Department of Automatic Control, LTH, Lund Sweden, 1998.
- 2) Pharmacia LKB Biotechnology. "Ion Exchange chromatography. Principles and Mathods.", 3rd edition, 1991.

### Appendix

```
describe('MSL')

→ MSL: 3.2.3 – used components: RealInput, RealOutput, CombiTimeTable, Types

system_info()
\overline{2}
    System information
     -OS: Linux
     -Python: 3.10.12
     -Scipy: not installed in the notebook
     -PyFMI: 2.16.1
     -FMU by: OpenModelica Compiler OpenModelica 1.25.0∼dev-133-ga5470be
     -FMI: 2.0
     -Type: FMUModelME2
-Name: Column_system
     -Generated: 2024-11-07T11:26:29Z
     -MSL: 3.2.3
     -Description: Bioprocess Library version 2.3.0
     -Interaction: FMU-explore version 1.0.0
Start coding or generate with AI.
```