

BPL_TEST2_Perfusion script with FMPy

The key library FMPy is installed.

After the installation a small application BPL_TEST2_Perfusion is loaded and run. You can continue with this example if you like.

```
In [1]: !lsb_release -a # Actual VM Ubuntu version used by Google
```

```
No LSB modules are available.  
Distributor ID: Ubuntu  
Description:    Ubuntu 22.04.4 LTS  
Release:        22.04  
Codename:       jammy
```

```
In [2]: !python --version
```

```
Python 3.11.11
```

```
In [3]: !pip install fmpy
```

```
Collecting fmpy  
  Downloading FMPy-0.3.22-py3-none-any.whl.metadata (1.9 kB)  
Requirement already satisfied: attrs in /usr/local/lib/python3.11/dist-packages (from fmpy) (25.1.0)  
Requirement already satisfied: Jinja2 in /usr/local/lib/python3.11/dist-packages (from fmpy) (3.1.5)  
Collecting lark (from fmpy)  
  Downloading lark-1.2.2-py3-none-any.whl.metadata (1.8 kB)  
Requirement already satisfied: lxml in /usr/local/lib/python3.11/dist-packages (from fmpy) (5.3.1)  
Requirement already satisfied: msgpack in /usr/local/lib/python3.11/dist-packages (from fmpy) (1.1.0)  
Requirement already satisfied: numpy in /usr/local/lib/python3.11/dist-packages (from fmpy) (1.26.4)  
Requirement already satisfied: MarkupSafe>=2.0 in /usr/local/lib/python3.11/dist-packages (from Jinja2->fmpy) (3.0.2)  
Downloading FMPy-0.3.22-py3-none-any.whl (4.9 MB)  
_____ 4.9/4.9 MB 21.2 MB/s eta 0:00:00  
Downloading lark-1.2.2-py3-none-any.whl (111 kB)  
_____ 111.0/111.0 kB 4.9 MB/s eta 0:00:00  
Installing collected packages: lark, fmpy  
Successfully installed fmpy-0.3.22 lark-1.2.2
```

Notes of BPL_TEST2_Perfusion

This notebook explore perfusion cultivation in comparison with ordinary continuous cultivation (chemostat) and use comparable settings to earlier notebook. Further you see here examples of interaction with the simplified commands `par()`, `init()`, `simu()` etc as well as direct interaction with the FMU which is called "model" here. The last simulation is always

available in the workspace and called "sim_res". Note that describe() brings mainly up from descriptive information from the Modelica code from the FMU but is complemented by some information given in the Python setup file.

Now specific installation run a simulation and notebook for that Start with connecting to Github. Then upload the two files:

- FMU - BPL_TEST2_Perfusion_linux_om_me.fmu
- Setup-file - BPL_TEST2_Perfusion_fmpy_explore.py

```
In [4]: %%bash
git clone https://github.com/janpeter19/BPL_TEST2_Perfusion
```

Cloning into 'BPL_TEST2_Perfusion'...

```
In [5]: %cd BPL_TEST2_Perfusion
/content/BPL_TEST2_Perfusion
```

```
In [6]: run -i BPL_TEST2_Perfusion_fmpy_explore.py
```

Linux - run FMU pre-compiled OpenModelica

Model for the process has been setup. Key commands:

- par() - change of parameters and initial values
- init() - change initial values only
- simu() - simulate and plot
- newplot() - make a new plot
- show() - show plot from previous simulation
- disp() - display parameters and initial values from the last simulation
- describe() - describe culture, broth, parameters, variables with values/units

Note that both disp() and describe() takes values from the last simulation and the command process_diagram() brings up the main configuration

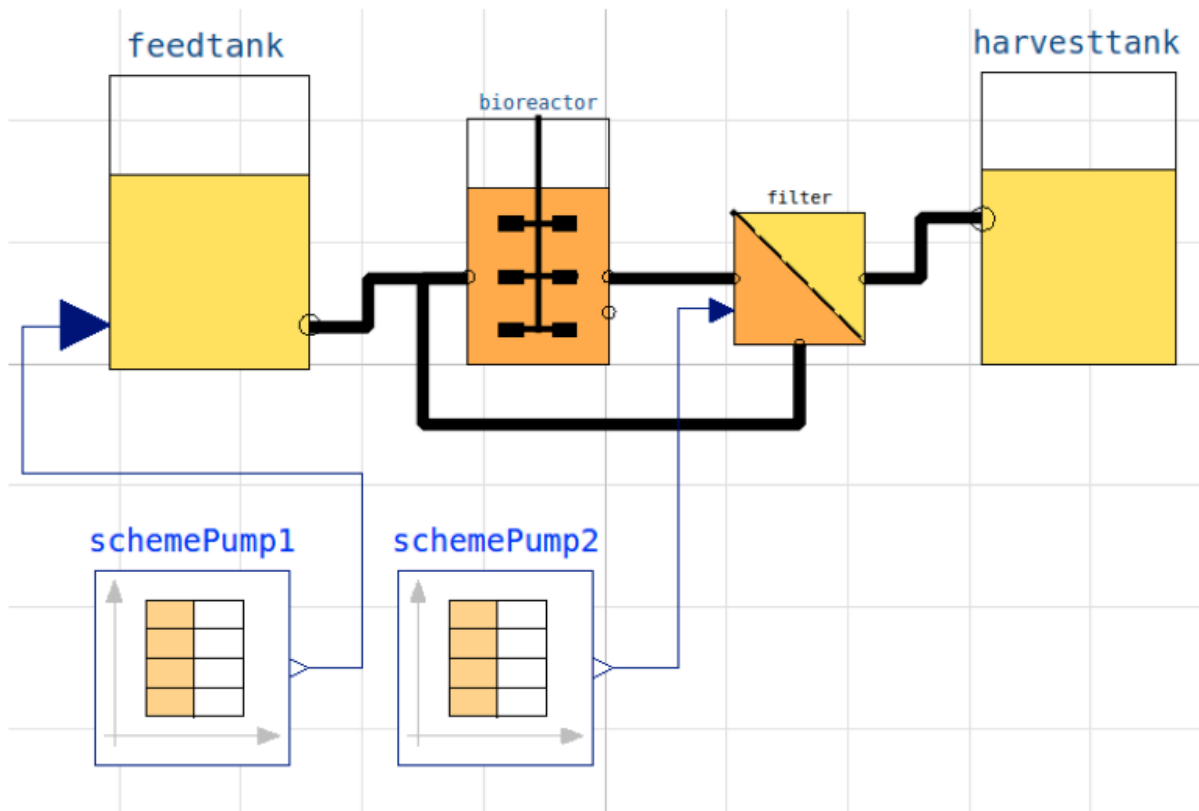
Brief information about a command by help(), eg help(simu)

Key system information is listed with the command system_info()

```
In [7]: %matplotlib inline
plt.rcParams['figure.figsize'] = [25/2.54, 20/2.54]
```

```
In [8]: process_diagram()
```

No processDiagram.png file in the FMU, but try the file on disk.



```

In [9]: # Process parameters used throughout
par(Y=0.5, qSmax=0.75, Ks=0.1) # Culture
par(filter_eps=0.10, filter_alpha_X=0.02, filter_alpha_S=0.10) # Filter
par(S_in=30.0) # Inlet substrate
init(V_start=1.0, VX_start=1.0) # Process initial
eps = parDict['filter_eps'] # Pump schedule

```

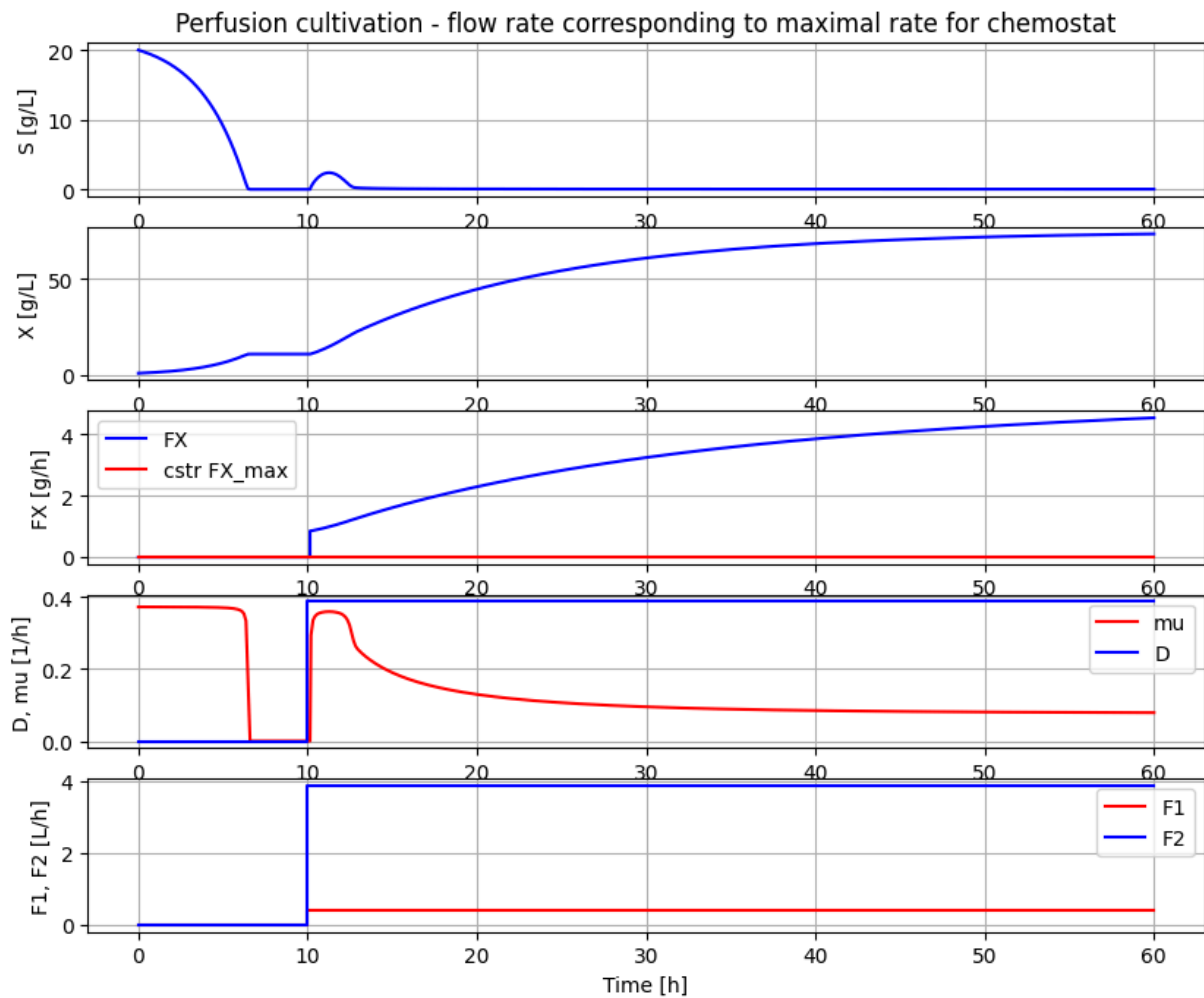
```

In [10]: # Simulation of process with flow rate plot to wash-out for chemostat

init(VS_start=20) # Process initial
par(pump1_t1=10, pump2_t1=10) # Pump schedule - recycle
par(pump1_F1=2.5*0.155, pump2_F1=2.5*0.155/eps)
par(pump1_t2=940, pump2_t2=940, pump1_t3=950, pump2_t3=950, pump1_t4=960, pump2_t4=960)

newplot(title='Perfusion cultivation - flow rate corresponding to maximal rate for
simu(60)

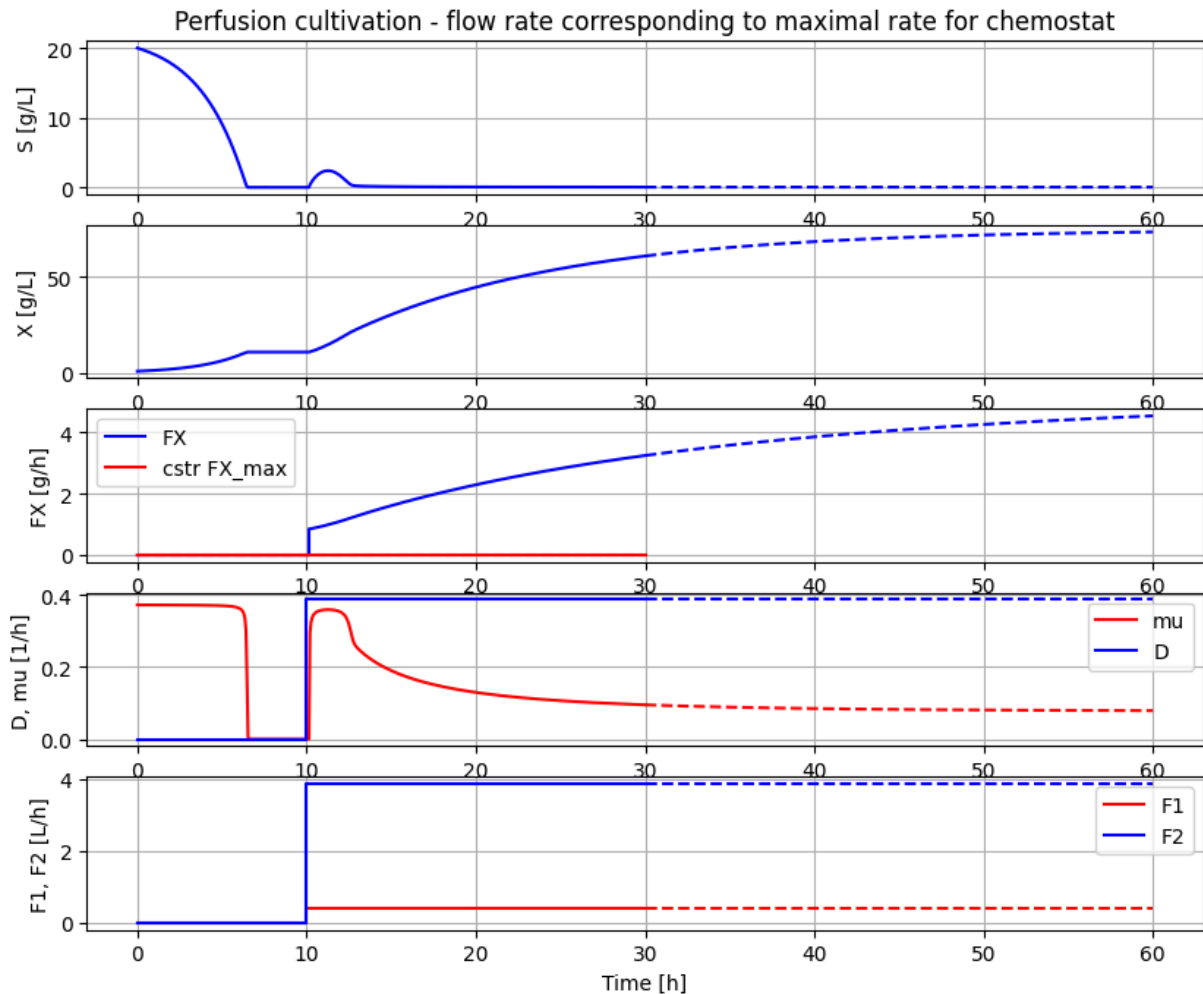
```



```
In [11]: # Simulation of process with flow rate close to wash-out for chemostat

init(VS_start=20)                                # Process initial
par(pump1_t1=10, pump2_t1=10)                    # Pump schedule - recycle
par(pump1_F1=2.5*0.155, pump2_F1=2.5*0.155/eps)
par(pump1_t2=940, pump2_t2=940, pump1_t3=950, pump2_t3=950, pump1_t4=960, pump2_t4=960)

newplot(title='Perfusion cultivation - flow rate corresponding to maximal rate for
simu(30)
simu(30,'cont')
```



```
In [12]: # Concentration factor of the filter
c=model_get('filter.retentate.c[1]')/model_get('filter.inlet.c[1]')
print('Conc factor of perfusion filter =', np.round(c,3))
```

Conc factor of perfusion filter = 1.179

```
In [13]: c_data=sim_res['filter.retentate.c[1]']/sim_res['filter.inlet.c[1]']
print('Conc factor variation', np.round(min(c_data[151:]), 3), np.round(max(c_data[
```

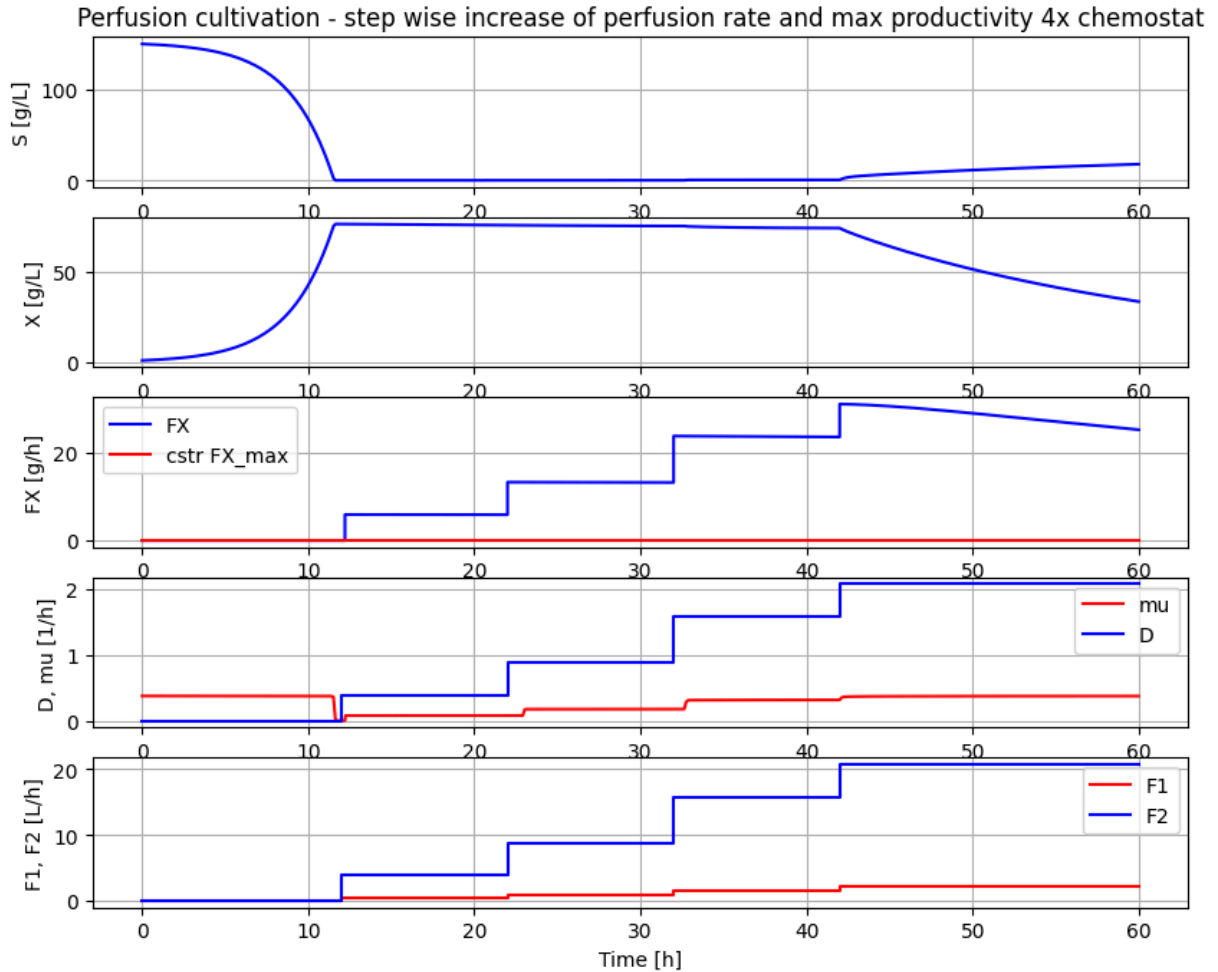
Conc factor variation 1.179 1.179

```
In [14]: # Simulation of process with step-wise increase of pefusion rate until wash-out.
# This means that re-circulation rate change at the same time as the perfusion rate

init(VS_start=150) # Process initial varied

par(pump1_t1=12, pump2_t1=12) # Pump schedule - recycle
par(pump1_F1=2.5*0.155, pump2_F1=2.5*0.155/eps)
par(pump1_t2=22, pump2_t2=22)
par(pump1_F2=2.5*0.35, pump2_F2=2.5*0.35/eps)
par(pump1_t3=32, pump2_t3=32)
par(pump1_F3=2.5*0.63, pump2_F3=2.5*0.63/eps)
par(pump1_t4=42, pump2_t4=42)
par(pump1_F4=2.5*0.83, pump2_F4=2.5*0.83/eps)
```

```
newplot(title='Perfusion cultivation - step wise increase of perfusion rate and max  
simu(60)
```



```
In [15]: # Simulation without a plot and just to check typical values at high production rat
#simu(40)
#c_data=sim_res['filter.retentate.c[1]']/sim_res['filter.inlet.c[1]']
#print('Conc factor variation', np.round(min(c_data[190:]), 3), 'to', np.round(max(
```

```
In [16]: #describe('cstrProdMax')
```

```
In [17]: # The maximal biomass productivity before washout is obtained aroudn 40 hours
np.round(model_get('harvesttank.inlet.F')*model_get('harvesttank.inlet.c[1]'),1)
```

```
Out[17]: 25.2
```

```
In [18]: # Thus perfusion (with this filter) brings a productivity improvement of about
np.round(23.5/5.6,1)
```

```
Out[18]: 4.2
```

```
In [19]: # Finally we check the filter flow rates at time 40 hour - note the negative sign f
model_get('filter.inlet.F')
```

```
Out[19]: 20.749999999999996
```

```
In [20]: model_get('filter.filtrate.F')
```

```
Out[20]: -2.0749999999999997
```

```
In [21]: model_get('filter.retentate.F')
```

```
Out[21]: -18.674999999999997
```

Summary

- The perfusion filter had a concentration factor of cells around 1.08 and re-cycling flow was set to a factor 10 higher than the perfusion rate and changed when perfusion rate was change to keep the ratio factor 10.
- The first simulation showed that by cell retention using perfusion filter the process could be run at a perfusion flow rate at the maximal flow rate possible for corresponding chemostat culture and cell concentration increased steadily.
- The second simulation showed that with a proper startup cell concentration, the cell concentration remained constant when perfusion rate increased in a similar way as what we see in a chemostat.
- The second simulation also showed that biomass productivity in this case was increased by a factor 4.2 compared to chemostat.
- If the perfusion rate increased to higher levels washout started but the decrease of cell concentration was slow.

Some of you who read this may have your perfusion experience with CHO-cultures. For such cultures the cell concentration do increase with increase of perfusion rate and there are understood reasons for that. But for this simplified process as well as microbial processes they typically keep cell concentration constant when flow rate is chaged, and that under quite wide conditions. I will try come back to this phenomena in a later notebook.

```
In [22]: # List of components in the process setup and also a couple of other things like Li  
describe('parts')
```

```
['bioreactor', 'bioreactor.culture', 'D', 'feedtank', 'filter', 'harvesttank', 'schemePump1', 'schemePump2']
```

```
In [23]: describe('MSL')
```

```
MSL: 3.2.3 - used components: RealInput, RealOutput, CombiTimeTable, Types
```

```
In [24]: system_info()
```

System information

- OS: Linux
- Python: 3.11.11
- Scipy: not installed in the notebook
- FMPy: 0.3.22
- FMU by: OpenModelica Compiler OpenModelica 1.25.0~dev-133-ga5470be
- FMI: 2.0
- Type: ME
- Name: BPL.Examples_TEST2.Perfusion
- Generated: 2024-11-06T21:37:58Z
- MSL: 3.2.3
- Description: Bioprocess Library version 2.3.0
- Interaction: FMU-explore for FMPy version 1.0.1

In [24]: