

# EGR3030 – Energy Systems and Conversion 2024/25 session

# Week 4 – Introduction to exergy analysis for closed and open systems

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#### Learning outcomes

- What is exergy
- Types
- Definitions
- Exergy balance
  - Closed systems
  - Steady flow systems
- Relationship with heat (or energy) and entropy



#### Exergy

Exergy is the measure of the maximum theoretical useful work that can be obtained from a process as it is brought from its current state into equilibrium with the environment

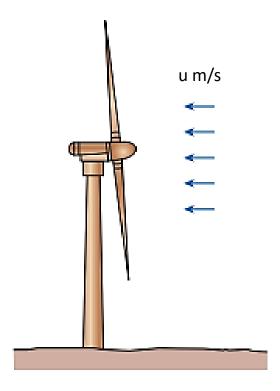
Or

It is a property that determines the useful work potential of a given amount of energy at some specified state.

- Also known as work potential, or available energy.
- Very useful in determining the viability of new energy sources, such as wind, oil and gas reserves, or geothermal wells.

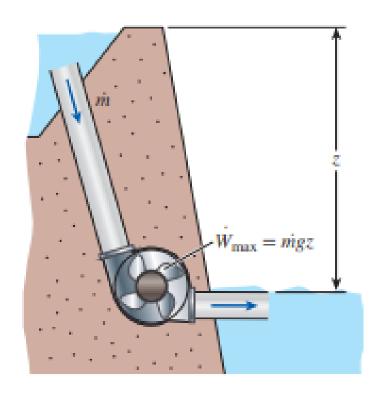


#### Energy potential

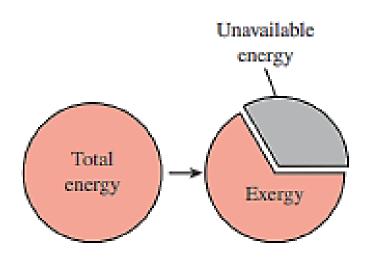


Horizontal axis wind turbine

$$P = \frac{1}{2}\rho A u^3$$



Hydro turbine

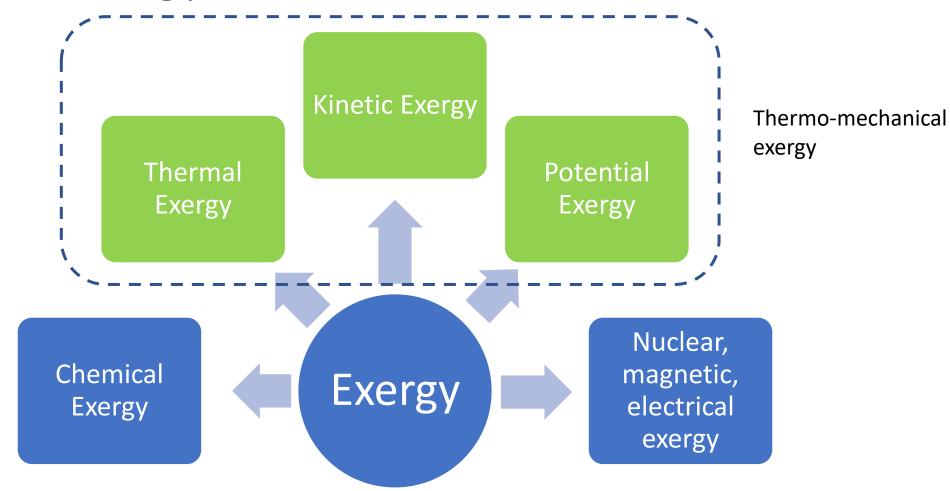


Unavailable energy is the part or portion of energy that cannot be converted to useful work even by a reversible system.

EXERGY is the <u>available</u> energy



## Kinds of exergy





#### Exergy destruction and entropy

- Irreversibilities generate entropy e.g. friction, mixing, chemical reactions, heat transfer through a finite temperature difference, non-quasi-equilibrium compression/expansion
- When entropy is generated, exergy is destroyed

Hence:

$$X_{destroyed} = T_o S_{gen} \ge 0$$

In general

$$X_{destroyed} \begin{cases} > 0 & irreversible \ process \\ = 0 & reversible \ process \\ < 0 & impossible \ process \end{cases}$$



# Definition of terms required for exergy analysis

#### Dead state

• A system is said to be in a dead state when it is in equilibrium with the environment

#### Surroundings

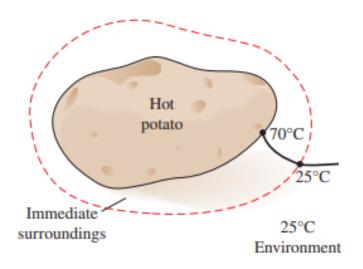
Outside the system boundaries

# Immediate surroundings

 Portion of the surroundings affected by the process

#### **Environment**

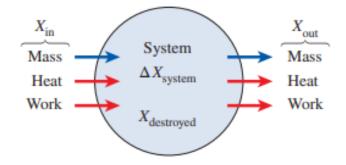
 Region beyond the immediate surroundings whose properties are not affected by the process at any point





### Exergy balance

- Unlike energy, exergy is <u>not</u> conserved it can be destroyed (but not created)
- Consider a hypothetical system undergoing a process:



- The exergy change of the system:
  - Is the difference between the net exergy transfer through the system's boundary and the exergy destroyed within boundary due to irreversibilities



## Exergy balance

In mathematical form:

$$\begin{pmatrix} Change\ in \\ total\ exergy \\ of\ system \end{pmatrix} = \begin{pmatrix} total \\ exergy \\ entering \end{pmatrix} - \begin{pmatrix} total \\ exergy \\ leaving \end{pmatrix} - \begin{pmatrix} total \\ exergy \\ destroyed \end{pmatrix}$$

$$\Delta X_{system} = X_{in} - X_{out} - X_{destroyed}$$

$$X_{in} - X_{out} - X_{out} - X_{destroyed}$$

$$X_{in} - X_{out} - X_{out} - X_{out}$$

$$X_{in} - X_{out} - X_{out} - X_{out} - X_{out}$$

$$X_{in} - X_{out} - X_$$

In rate form: 
$$\frac{dX_{system}}{dt} = \dot{X}_n - \dot{X}_{out} - \dot{X}_{destroyed}$$
 (kW)

In unit mass form:  $\Delta x_{system} = x_{in} - x_{out} - x_{destroyed}$  (kJ/kg)

### Exergy balance

Rate of exergy transfer by heat:

$$\dot{X}_{heat} = \left(1 - \frac{T_o}{T}\right)\dot{Q}$$

$$\dot{X}_{heat} = \eta_c \dot{Q}_{in}$$

Rate of exergy transfer by work

$$\dot{X}_{work} = W_{useful}$$

Rate of exergy transfer by mass:

$$\dot{X}_{mass} = \dot{m}\psi$$

Where  $\psi$  is the flow (or stream) exergy given by:

$$\psi = (h - h_o) - T_o(s - s_o) + \frac{V^2}{2} + gz$$



#### Exergy balance for a closed system

Starting from our first law energy balance:

$$\Delta E_{system} = E_{in} - E_{out} \Rightarrow E_2 - E_1 = Q - W \tag{1}$$

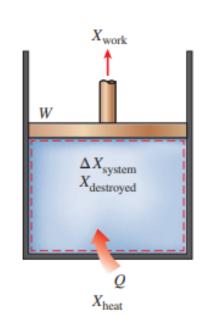
Entropy balance:

$$\Delta S_{system} = S_{in} - S_{out} + S_{gen} \Rightarrow S_2 - S_1 = \int_1^2 \left(\frac{\delta Q}{T}\right)_{boundary} + S_{gen}$$
 (2)

Multiplying (2) by  $T_o$  and subtracting from (1),

$$E_2 - E_1 - T_o(s_2 - s_1) = Q - T_o \int_1^2 \left(\frac{\delta Q}{T}\right)_{boundary} - W - T_o S_{gen}$$
 (3)

For heat transfer between the two states 1 and 2,  $Q=\int_1^2 \delta Q$  and the LHS of (3) can be shown to be  $X_2-X_1-P_o(V_2-V_1)$  (See eq. 8-17 in Cengel & Boles 4<sup>th</sup> Ed.)



#### Exergy balance for a closed system

Hence,

$$X_2 - X_1 - P_o(V_2 - V_1) = \int_1^2 \delta Q - T_o \int_1^2 \left(\frac{\delta Q}{T}\right)_{boundary} - W - T_o S_{gen}$$

Rearranging

$$X_2 - X_1 = \int_1^2 \left( 1 - \frac{T_o}{T_b} \right) \delta Q - \left[ W + P_o(V_2 - V_1) \right] - T_o S_{gen}$$



#### Exergy balance of steady flow systems

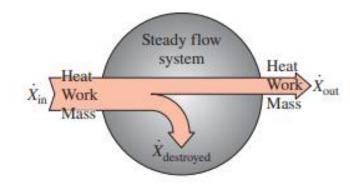
For a steady flow system, 
$$\frac{dX_{CV}}{dt} = ?$$
 
$$\frac{dX_{CV}}{dt} = 0$$

For steady flow, we simply substitute this into the closed system equation and replace the PdV part with the "stream" exergy  $\psi$ . Hence:

$$0 = \int_{1}^{2} \left( 1 - \frac{T_o}{T_b} \right) \delta \dot{q}_b - \dot{W} + \dot{m} \left( \psi_1 - \psi_2 \right) - \dot{X}_{destroyed}$$

If the process involves >1 streams (not a one-inlet, one-outlet system),

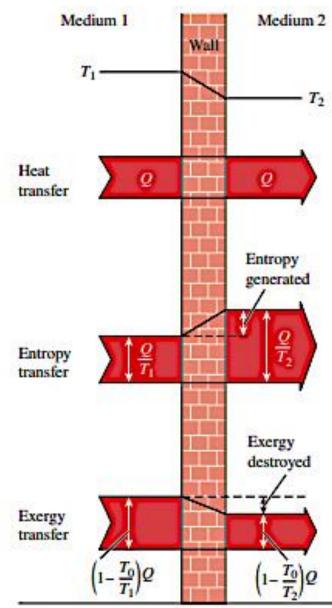
$$0 = \int_{1}^{2} \left( 1 - \frac{T_o}{T_b} \right) \delta \dot{q}_b - \dot{W} + \sum_{in} \dot{m}\psi - \sum_{out} \dot{m}\psi - \dot{X}_{destroyed}$$



Relationship between heat, entropy, and

exergy transfer in general...

Heat transfer Q at a location at temperature T is always accompanied by entropy transfer in the amount of  $\frac{Q}{T}$  and exergy transfer in the amount of  $\left(1 - \frac{T_0}{T}\right)Q$ .





#### Summary

- We defined exergy
- Types
- Definitions necessary for understanding exergy
- Exergy balance
  - Closed systems
  - Steady flow systems
- Relationship with heat (or energy) and entropy

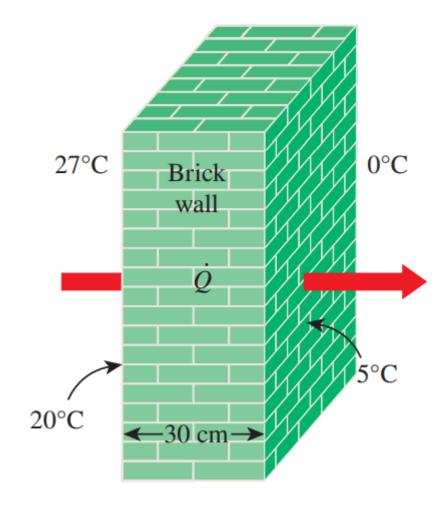


### Tutorial Q1 - exergy without work

Exergy destruction during heat conduction

Heat is transferred through a brick wall as shown in the figure. On a certain day, the temperature of the outdoors is 0°C and the internal of the house is maintained at 27°C. The temperatures of the inner and outer surfaces of the brick wall are measured to be 20°C and 5°C, respectively, and the rate of heat transfer through the wall is 1100 W. Determine

- (a) the rate of exergy destruction in the wall and
- (b) the rate of total exergy destruction associated with this heat transfer process.





#### Tutorial Q2 – exergy with work

Exergy destruction of steam expansion

A piston—cylinder device contains 0.05 kg of steam at 1 MPa and 300°C. Steam now expands to a final state of 200 kPa and 150°C, doing work. Heat losses from the system to the surroundings are estimated to be 2 kJ during this process. Assuming the surroundings to be at  $T_0 = 25$ °C and  $P_0 = 100$  kPa, determine the

- (a) exergy of the steam at the initial and the final states,
- (b) exergy change of the steam,
- (c) exergy destroyed, and
- (d) second-law efficiency for the process.



#### Homework

exergy analysis of a steam turbine

Steam enters a turbine steadily at 3 MPa and 450°C at a rate of 8 kg/s and exits at 0.2 MPa and 150°C. The steam is losing heat to the surrounding air at 100 kPa and 25°C at a rate of 300 kW, and the kinetic and potential energy changes are negligible. Calculate the

- (a) actual power output,
- (b) maximum possible power output
- (c) second-law efficiency
- (d) exergy destroyed, and
- (e) exergy of the steam at the inlet conditions.