# Imperial College London

# Direct Numerical Simulation of a 2D heat exchanger based on circular cylinders



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 AERO70008

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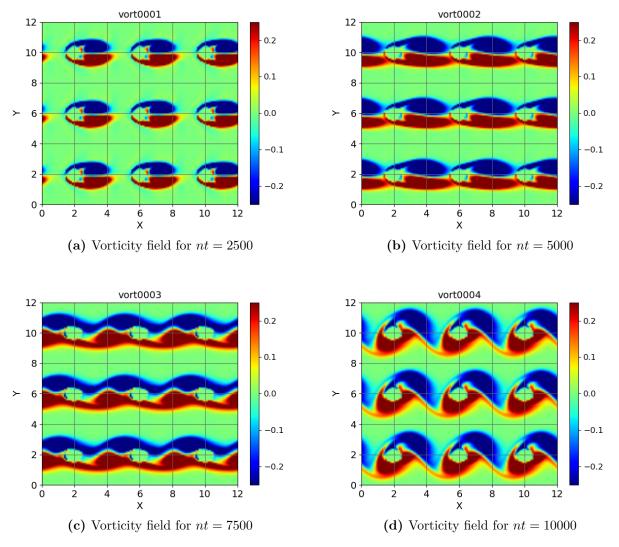
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# 1 Baseline Simulation with Second-Order Adams-Bashforth

The results demonstrate numerical stability under given perturbation, and shows typical pattern under given Reynolds number. The vortices formed behind the cylinder with maximum range around 0.22. The upper vortices are clockwise and lowers are anticlockwise.

From nt = 7500 onward, alternative periodic vortex sheddings develop downstream the cylinders, and they influence each other and formed typical Karman vortex street [1]. Hence, the simulation demonstrates expected flow features for a subcritical Reynolds number regime.

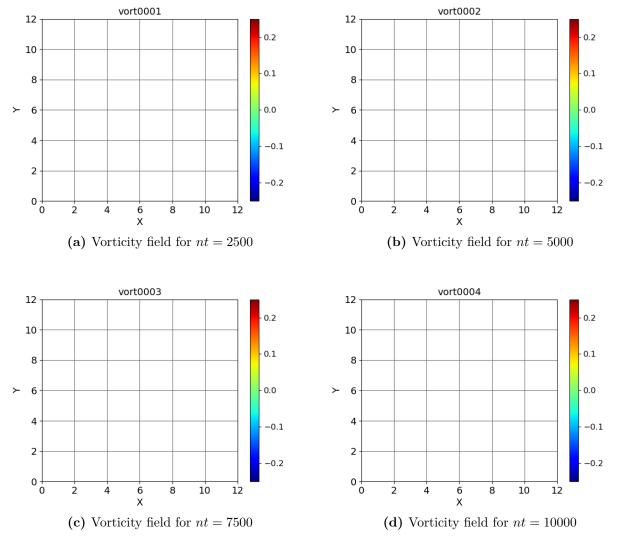


**Figure 1.** Time evolution of the vorticity field for different time steps (nt = 2500, 5000, 7500, 10000) using the second-order Adams-Bashforth scheme with Re = 200 and CFL = 0.25.

# 2 Stability Analysis with Increased CFL

There is no meaningful result generated. The numerical values grew unbounded and the scheme becomes numerically unstable. Adams-Bashforth is an explicit scheme, thus sensitive to time step, which is determined by CFL condition (1). Large time step causing oscillation and eventually grow unbounded. CFL = 0.75 is above the threshold value and caused unstable

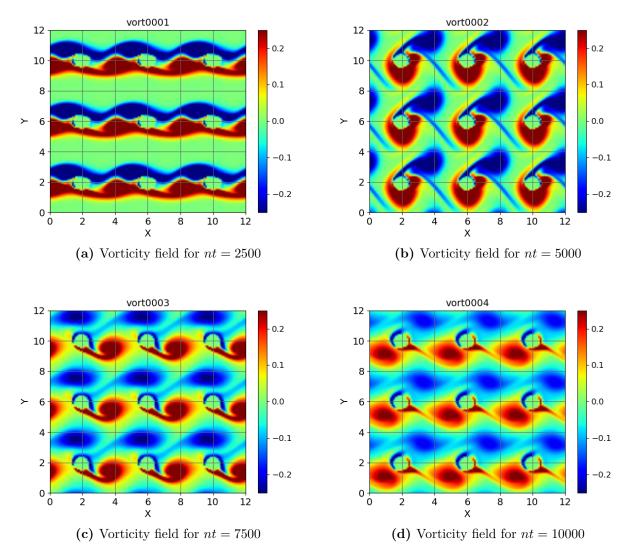
$$CFL = \frac{u \Delta t}{\Delta x} \le \text{ (Threshold Value)}. \tag{1}$$



**Figure 2.** Time evolution of the vorticity field for different time steps (nt = 2500, 5000, 7500, 10000) using the second-order Adams-Bashforth scheme with Re = 200 and CFL = 0.75. No meaningful results generated.

# 3 Implementing a Third-Order Runge-Kutta Scheme

The third order Runge-Kutta scheme remains stable and confirming robust robustness at CFL = 0.75. Compared with second-order Adams-Bashforth, the higher-order Runge-Kutta scheme captures finer details, and has a larger stability region Compared to Second-Order Adams-Bashforth scheme, Runge-Kutta has more accuracy at high frequency and phase error, allowing it remains stable at a larger time step. Meanwhile, larger time step reduces the computational cost. Figure 3a and Figure 1c are the same time second simulation and shows the same pattern vortex sheddings.



**Figure 3.** Time evolution of the vorticity field for different time steps (nt = 2500, 5000, 7500, 10000) using the third-order Runge-kutta scheme with Re = 200 and CFL = 0.75.

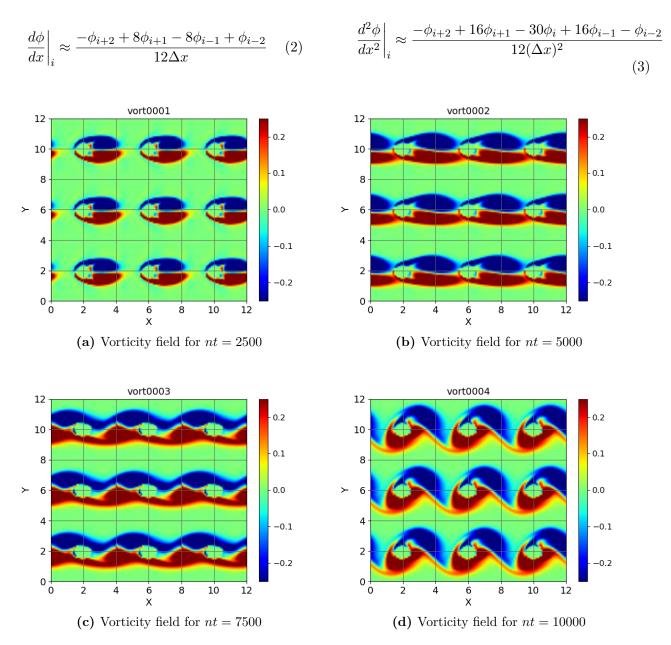
### • Subroutine rkutta():

```
subroutine rkutta(rho,rou,rov,roe,fro,gro,fru,gru,frv,grv,&
1
2
       fre, gre, nx, ny, ns, dlt, coef, k)
3
  4
5
    implicit none
6
7
    real(8),dimension(nx,ny) :: rho,rou,rov,roe,fro,gro,fru,gru,frv
8
    real(8),dimension(nx,ny) :: grv,fre,gre
10
    real(8),dimension(2,ns) :: coef
```

```
real(8) :: dlt
11
        integer :: i,j,nx,ny,ns,k
12
13
     !coefficient for RK sub-time steps
14
15
       coef(1,1)=8./15.
16
       coef(1,2)=5./12.
^{17}
       coef(1,3)=3./4.
       coef(2,1)=0.
18
       coef(2,2) = -17./60.
19
       coef(2,3) = -5./12.
20
21
       do j=1,ny
22
           do i=1,nx
23
     1.1
24
25
                  rho(i,j)=rho(i,j)+dlt*(coef(1,k)*fro(i,j)+coef(2,k)*gro(i,j))
26
                  gro(i,j)=fro(i,j)!g is k-1
                  rou(i,j)=rou(i,j)+dlt*(coef(1,k)*fru(i,j)+coef(2,k)*gru(i,j))
^{27}
                  gru(i,j)=fru(i,j)
^{28}
29
                  \texttt{rov(i,j)=rov(i,j)+dlt*(coef(1,k)*frv(i,j)+coef(2,k)*grv(i,j))}
30
                  grv(i,j)=frv(i,j)
                  \texttt{roe}(\texttt{i},\texttt{j}) \texttt{=} \texttt{roe}(\texttt{i},\texttt{j}) \texttt{+} \texttt{dlt} * (\texttt{coef}(\texttt{1},\texttt{k}) * \texttt{fre}(\texttt{i},\texttt{j}) \texttt{+} \texttt{coef}(\texttt{2},\texttt{k}) * \texttt{gre}(\texttt{i},\texttt{j}))
31
                  gre(i,j)=fre(i,j)
32
33
            enddo
34
        enddo
35
36
37
       return
     end subroutine rkutta
```

# 4 Implementing Fourth-Order Centered Differences

The centered fourth-order schemes are computed from Taylor's expansion as equations (2) and (3). Compared to task 1, a longer computational time is seen as more points involved in computations. It is expected that centered fourth-order schemes should have less dissipation and dispersion error, capturing finer details such as turbulence, small vortices, and shear layer [2]. However, no significant difference is seen. This might due to the large grid size which also causes the error, or due to time step  $\Delta t$  too small, making the advantage of higher order scheme difficult to be seen.



**Figure 4.** Time evolution of the vorticity field for different time steps (nt = 2500, 5000, 7500, 10000) using the second-order Adams-Bashforth scheme with Re = 200 and CFL = 0.25.

• Subroutine derix4(), deriy4(), derxx4(), and deryy4():

```
subroutine derix4(phi,nx,ny,dfi,xlx)
!
subroutine derix4(phi,nx,ny,dfi,xlx)
!
Fourth-order first derivative in the x direction
```

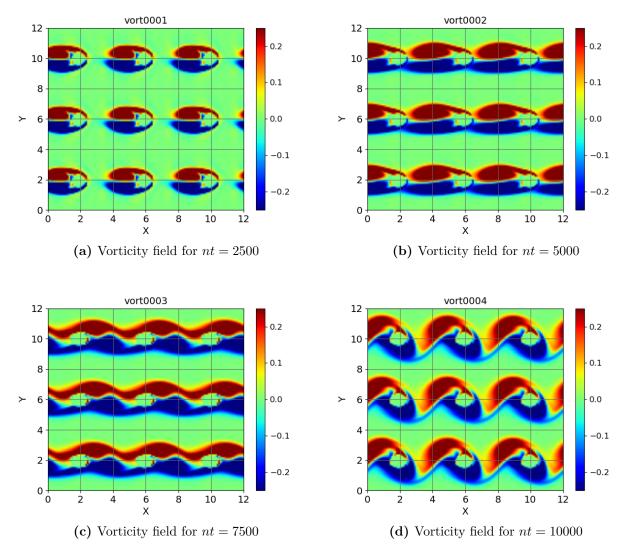
```
4
5
    implicit none
6
7
    real(8),dimension(nx,ny) :: phi,dfi
8
    real(8) :: dlx,xlx,udx
9
10
    integer :: i,j,nx,ny
11
12
    dlx=xlx/nx
13
    udx=1./(12.*dlx)
                     !updated multiplier
14
    do j=1,ny
15
        dfi(1,j)=udx*(-phi(3,j)+8.*phi(2,j)-8.*phi(nx,j)+phi(nx-1,j)) !Boundary
16
           Condition: i=1
        dfi(2,j)=udx*(-phi(4,j)+8.*phi(3,j)-8.*phi(1,j)+phi(nx,j)) !Boundary Condition:
17
           i=2
       do i=3, nx-2
         dfi(i,j)=udx*(-phi(i+2,j)+8.*phi(i+1,j)-8.*phi(i-1,j)+phi(i-2,j)) !i=3 to nx-2
19
20
       enddo
       dfi(nx-1,j)=udx*(-phi(1,j)+8.*phi(nx,j)-8.*phi(nx-2,j)+phi(nx-3,j))! Boundary
21
          Condition: i=nx-1
       dfi(nx,j)=udx*(-phi(2,j)+8.*phi(1,j)-8.*phi(nx-1,j)+phi(nx-2,j)) !Boundary
22
          Condition: i=nx
    enddo
23
24
25
    return
26
   end subroutine derix4
27
   28
   29
30
   subroutine deriy4(phi,nx,ny,dfi,yly)
31
32
33
   !Fourth-order first derivative in the y direction
34
   35
36
    implicit none
37
38
    real(8),dimension(nx,ny) :: phi,dfi
39
    real(8) :: dly,yly,udy
40
    integer :: i,j,nx,ny
41
42
    dly=yly/ny !dly:grid size; yly: total length
43
    udy=1./(12.*dly) !updated multiplier
44
45
    do j=3, ny-2
       do i=1,nx
46
         47
       enddo
49
    enddo
    do i=1,nx !Boundary Condition
50
       dfi(i,1)=udy*(-phi(i,3)+8.*phi(i,2)-8.*phi(i,ny)+phi(i,ny-1))
                                                               !Boundary
51
          Condition: j=1
       dfi(i,2)=udy*(-phi(i,4)+8.*phi(i,3)-8.*phi(i,1)+phi(i,ny))
                                                           !Boundary Condition:
52
          j=2
       dfi(i,ny-1)=udy*(-phi(i,1)+8.*phi(i,ny)-8.*phi(i,ny-2)+phi(i,ny-3)) !Boundary
53
          Condition: j=ny-1
54
       dfi(i,ny)=udy*(-phi(i,2)+8.*phi(i,1)-8.*phi(i,ny-1)+phi(i,ny-2)) !Boundary
          Condition: j=ny
55
    enddo
56
57
58
    return
  end subroutine deriy4
59
  60
```

```
61
   62
63
64
   subroutine derxx4(phi,nx,ny,dfi,xlx)
65
   !Fourth-order second derivative in y direction
66
67
   68
69
     implicit none
70
     real(8),dimension(nx,ny) :: phi,dfi
71
     real(8) :: dlx,xlx,udx
72
     integer :: i,j,nx,ny
73
74
     dlx=xlx/nx
75
76
     udx=1./(12.*dlx*dlx)
                           !updated multiplier
77
     do j=1,ny
        dfi(1,j)=udx*(-phi(3,j)+16.*phi(2,j)-30.*phi(1,j)+16.*phi(nx,j)-phi(nx-1,j))
78
            !Boundary Condition: i=1
79
        dfi(2,j)=udx*(-phi(4,j)+16.*phi(2,j)-30.*phi(2,j)+16.*phi(1,j)-phi(nx,j))
            !Boundary Condition: i=2
        do i=3, nx-2
80
           dfi(i,j)=udx*(-phi(i+2,j)+16.*phi(i+1,j)-30.*phi(i,j)+16.*phi(i-1,j)-phi(i-2,j))
81
               !i=3 to nx-2
82
        enddo
        dfi(nx-1,j)=udx*(-phi(1,j)+16.*phi(nx,j)-30.*phi(nx-1,j)+16.*phi(nx-2,j)-phi(nx-3,j))
83
              !Boundary Condition: i=nx-1
        dfi(nx,j)=udx*(-phi(2,j)+16.*phi(1,j)-30.*phi(nx,j)+16.*phi(nx-1,j)-phi(nx-2,j))
            !Boundary Condition: i=nx
85
      enddo
86
     return
87
   end subroutine derxx4
88
   89
90
   91
92
   subroutine deryy4(phi,nx,ny,dfi,yly)
93
94
95
   !Fourth-order second derivative in the y direction
   96
97
     implicit none
98
99
     real(8),dimension(nx,ny) :: phi,dfi
100
     real(8) :: dly,yly,udy
101
     integer :: i,j,nx,ny
102
103
104
     dly=yly/ny
105
     udy=1./(12.*dly*dly)
                           !updated multiplier
106
     do j=3,ny-2
107
        do i=1.nx
108
           dfi(i,j) = udy * (-phi(i,j+2) + 16.*phi(i,j+1) - 30.*phi(i,j) + 16.*phi(i,j-1) - phi(i,j-2))
109
               !j=3 to ny-2
        enddo
110
     enddo
111
112
     do i=1,nx
113
      dfi(i,1) = udy*(-phi(i,3)+16.*phi(i,2)-30.*phi(i,1)+16.*phi(i,ny)-phi(i,ny-1))
          !Boundary Condition: j=1
      dfi(i,2)=udy*(-phi(i,4)+16.*phi(i,3)-30.*phi(i,2)+16.*phi(i,1)-phi(i,ny)) !Boundary
114
          Condition: j=2
      dfi(i,ny-1)=udy*(-phi(i,1)+16.*phi(i,ny)-30.*phi(i,ny-1)+16.*phi(i,ny-2)-phi(i,ny-3))
115
           !Boundary Condition: j=ny-1
      dfi(i,ny)=udy*(-phi(i,2)+16.*phi(i,1)-30.*phi(i,ny)+16.*phi(i,ny-1)-phi(i,ny-2))
116
```

# 5 Long-Term Flow Behavior Analysis

When the simulation continues, the vortex shedding begin to vanish, and the flow becomes uniformed. The numerical value of the simulation gradually dissipates, and the outline of the vortices becomes blurry. This is due to the dissipation of the second-order Adams-Bashforth scheme and finite difference, and the boundary condition which smooth out the small-scale vortices.

# 6 Reverse Flow Direction Simulation



**Figure 5.** Time evolution of the vorticity field for different time steps (nt = 2500, 5000, 7500, 10000) using the second-order Adams-Bashforth scheme with Re = 200 and CFL = 0.25, with flow coming from right to left.

• In the subroutine **initl**, change *uuu* to the negative direction.

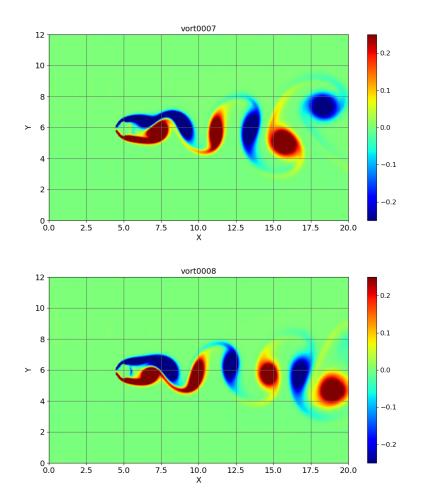
```
uuu(i,j)=-uu0 !negtive
```

• Additional: change the index of y-direction turbulence to nx + 1 - i to get a more accurate mirrored pattern the original case.

```
vvv(i,j)=0.01*(sin(4.*pi*(nx+1-i)*dlx/xlx)&

+sin(7.*pi*(nx+1-i)*dlx/xlx))*&
exp(-(j*dly-yly/2.)**2)
```

# 7 Simulation of a Single Cylinder with Inflow/Outflow Boundary Conditions



**Figure 6.** Instantaneous visualisations of the flow around a single cylinder with inflow/outflow boundary conditions in the streamwise direction.

## 1. New subroutine boundary():

```
subroutine boundary(uuu, vvv, rho, eee, tmp, rou, rov, roe, nx, ny, &
   xlx,yly,xmu,xba,gma,dlx,dlt,uu0)
2
3
     implicit none
4
5
     real(8),dimension(nx,ny) :: uuu,vvv,rho,eee,tmp,rou,rov,roe
6
     real(8) :: xlx,yly,xmu,xba,gma,roi,cci,d,tpi,chv,uu0
     real(8) :: pi,dlx,dly,dlt,ct6
8
     integer :: nx,ny,j
10
      call param(xlx,yly,xmu,xba,gma,roi,cci,d,tpi,chv,uu0)
11
12
     ct6=(gma-1.)/gma
13
     pi=acos(-1.)
14
15
      16
     do j=1,ny
17
        uuu(1,j)=uu0
18
19
        vvv(1,j)=0.01*(sin(4.*pi*(1)*dlx/xlx)&
```

```
+sin(7.*pi*(1)*dlx/xlx))*&
20
           exp(-(j*dly-yly/2.)**2)
21
         tmp(1,j)=tpi
22
         eee(1,j)=chv*tmp(1,j)+0.5*(uuu(1,j)*uuu(1,j)+vvv(1,j)*vvv(1,j))
23
         rho(1,j)=roi
24
25
         rou(1,j)=rho(1,j)*uuu(1,j)
26
         rov(1,j)=rho(1,j)*vvv(1,j)
27
         roe(1,j)=rho(1,j)*eee(1,j)
      enddo
28
29
      30
      do j=1,ny
31
        rho(nx,j)=rho(nx,j)-uu0*dlt/dlx*(rho(nx,j)-rho(nx-1,j))
32
         rou(nx,j)=rou(nx,j)-uu0*dlt/dlx*(rou(nx,j)-rou(nx-1,j))
33
         rov(nx,j)=rov(nx,j)-uu0*dlt/dlx*(rov(nx,j)-rov(nx-1,j))
34
35
         roe(nx,j)=roe(nx,j)-uu0*dlt/dlx*(roe(nx,j)-roe(nx-1,j))
36
      enddo
37
38
39
      return
   end subroutine boundary
40
```

#### 2. Modified subroutine derix():

```
subroutine derix(phi,nx,ny,dfi,xlx)
2
   !First derivative in the x direction
3
   4
5
     implicit none
6
     real(8),dimension(nx,ny) :: phi,dfi
8
     real(8) :: dlx,xlx,udx
     integer :: i,j,nx,ny
10
11
     dlx=xlx/nx
12
13
     udx=1./(dlx+dlx)
14
     do j=1,ny
       !Inlet Condition, First order forward difference scheme
15
        dfi(1,j)=(1./dlx)*(phi(2,j)-phi(1,j))
16
        do i=2, nx-1
17
           dfi(i,j)=udx*(phi(i+1,j)-phi(i-1,j))
18
19
       !Outlet Condition, First order backward difference scheme
20
21
        dfi(nx,j)=(1./dlx)*(phi(nx,j)-phi(nx-1,j))
22
     enddo
23
24
     return
   end subroutine derix
25
```

#### 3. Modified subroutine derxx():

```
subroutine derxx(phi,nx,ny,dfi,xlx)
2
3
  !Second derivative in x direction
  4
5
    implicit none
6
7
    real(8),dimension(nx,ny) :: phi,dfi
8
    real(8) :: dlx,xlx,udx
9
    integer :: i,j,nx,ny
10
11
```

```
dlx=xlx/nx
12
     udx=1./(dlx*dlx)
13
     do j=1,ny
14
         ! Inlet Boundary Condition, Second-order one-sided difference scheme
15
         dfi(1,j)=udx*((phi(1,j)+phi(1,j))-5.*phi(2,j)+4.*phi(3,j)-phi(4,j))
16
         do i=2, nx-1
18
            dfi(i,j)=udx*(phi(i+1,j)-(phi(i,j)+phi(i,j))&
19
                 +phi(i-1,j))
         enddo
20
         !Outlet Boundary Condition, Second-order one-sided difference scheme
21
          dfi(nx,j) = udx*((phi(nx,j)+phi(nx,j)) - 5.*phi(nx-1,j) + 4.*phi(nx-2,j)-phi(nx-3,j)) 
22
     enddo
23
24
25
     return
   end subroutine derxx
26
```

4. Additional. Implementing subroutine boundary in the time loop:

5. Additional. Layout amendments in the 2D\_compressible.f90 file:

```
!nx->513, ny->257, nf->1
integer,parameter :: nx=513,ny=257,nt=15000,ns=3,nf=1,mx=nf*nx,my=nf*ny
```

```
1
    do j=1,ny
2
      do i=1,nx
3
4
         !Centre of cylinder located at (5d,6d)
        if (((i*dlx-5.d0)**2+(j*dly-6.d0)**2).lt.radius**2) then
5
6
           eps(i,j)=1.
7
        else
           eps(i,j)=0.
8
        end if
9
      enddo
10
    enddo
11
```

```
1 xlx=20.*d !DOMAIN SIZE X DIRECTION
2 yly=12.*d !DOMAIN SIZE Y DIRECTION
```

**6.** Additional. Layout amendments in the **plot\_py** file:

```
#nx->513, ny->257, lx->20.0, ly->12.0
nx=513
ny=257
lx=20.0
ly=12.0

#12->lx
X=np.linspace(0,lx,num=nx)
```

```
#plot
fig,ax = plt.subplots(figsize=(12,6))
plt.figure((i+1),figsize=(20,12), edgecolor='none')
```

# References

- [1] Cooper JE. AEROELASTIC RESPONSE. In: Braun S, editor. Encyclopedia of Vibration. Oxford: Elsevier; 2001. p. 87-97. Available from: https://www.sciencedirect.com/science/article/pii/B0122270851001259.
- [2] Wang ZJ, Fidkowski K, Abgrall R, Bassi F, Caraeni D, Cary A, et al. High-Order CFD Methods: Current Status and Perspective. International Journal for Numerical Methods in Fluids. 2013;72(8):811-45. Available from: https://www.researchgate.net/publication/236950745\_High-Order\_CFD\_Methods\_Current\_Status\_and\_Perspective.