

Modelling and Numerical Methods

Lecture 4

Conservation Equations and Rheology

Outline

- Conservation equations
- Energy equation
- Constitutive equations: Rheology
- Elasticity and Wave Equation
- Newtonian Viscosity and Navier Stokes

Learning Objectives

- Learn main conservation equations used in continuum mechanics modelling and understand what different terms in these equations represent
- Be able to solve conservation equations for basic analytical solutions given boundary/initial conditions.
- Understand basic properties of elastic and viscous rheology and understand how the choice of rheology leads to different forms of the momentum conservation equation
- Using tensor analysis to obtain relations between the main isotropic elastic parameters

Continuum Mechanics Equations

General:

1. Kinematics – describing deformation and velocity without considering forces
2. Dynamics – equations that describe force balance, conservation of linear and angular momentum
3. Thermodynamics – relations temperature, heatflux, stress, entropy

Material-specific

4. Constitutive equations – relations describing how material properties vary as a function of T,P, stress,.... Such material properties govern dynamics (e.g., *density*), response to stress (*viscosity, elastic parameters*), heat transport (*thermal conductivity, heat capacity*)

Thermodynamics: Conservation of Energy

- First law of thermodynamics
- Preservation of energy, i.e any change in kinetic or internal energy is balanced by work done and heat used/produced

$$\frac{D(K + U)}{Dt} = W + Q$$

K - kinetic energy, U - internal energy,
 W – power input, Q – heat input

- Let's start with the form that describes preservation of thermal energy, in 2-D

2-D energy equation

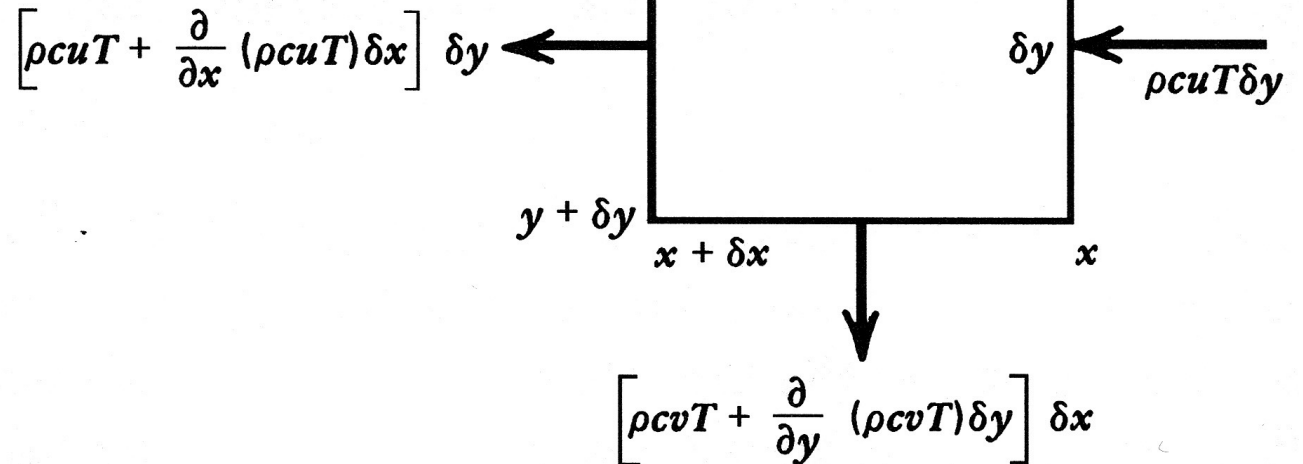
Spatial, constant ρ , C_P , k , incompressible

no heat sources

- **Change in heat content**

$$\frac{\partial(\rho C_P T)}{\partial t} \delta x \delta y$$

- **Advection**



- **Conduction**

C_P – heat capacity (J/kg/K)
 u, v - velocity

2-D energy equation

Spatial, constant ρ , C_P , k , incompressible

no heat sources

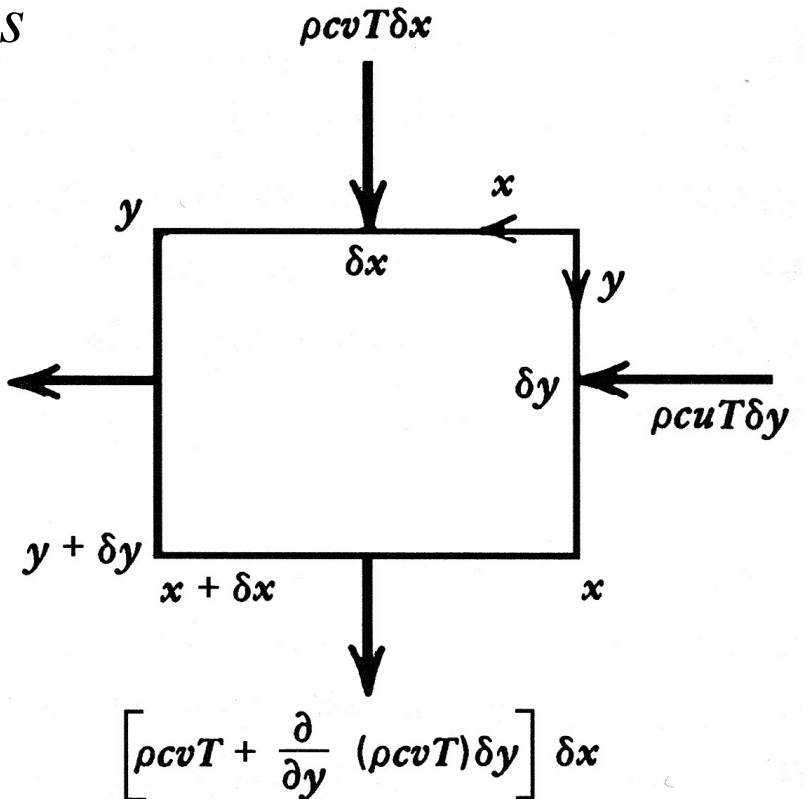
- **Change in heat content**

$$\frac{\partial(\rho C_P T)}{\partial t} \delta x \delta y$$

- **Advection**

$$\left[\frac{\partial(\rho C_P u T)}{\partial x} + \frac{\partial(\rho C_P v T)}{\partial y} \right] \delta x \delta y$$

- **Conduction**



C_P – heat capacity (J/kg/K)
 u, v - velocity

2-D energy equation

Spatial, constant ρ , C_P , k , incompressible

no heat sources

- **Change in heat content**

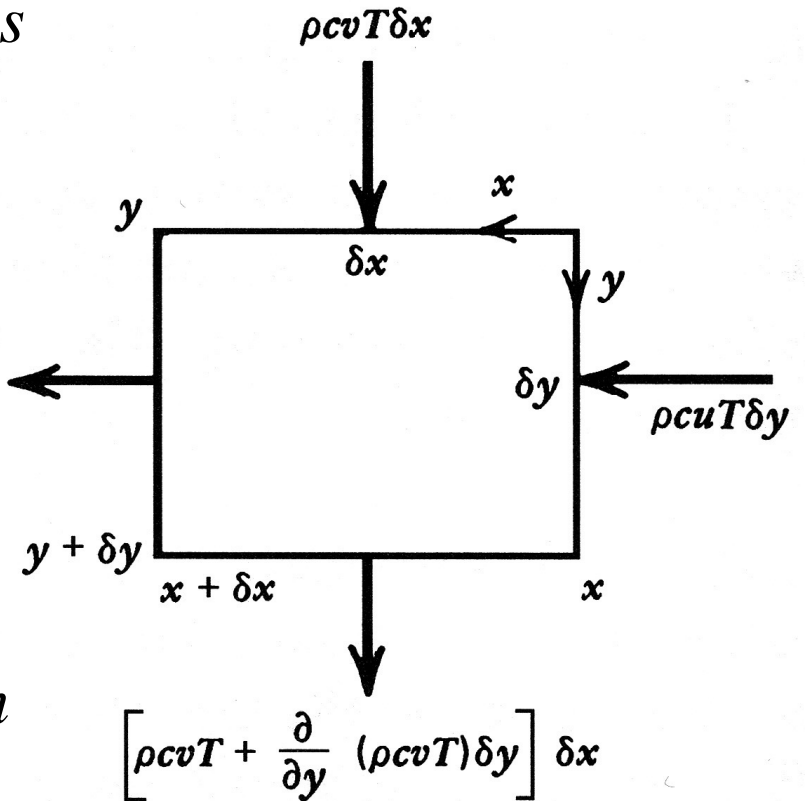
$$\frac{\partial(\rho C_P T)}{\partial t} \delta x \delta y$$

- **Advection**

$$\left[\frac{\partial(\rho C_P u T)}{\partial x} + \frac{\partial(\rho C_P v T)}{\partial y} \right] \delta x \delta y$$

*conservation
of mass*

How does this simplify?



2-D energy equation

Spatial, constant ρ , C_P , k , incompressible

no heat sources

- **Change in heat content**

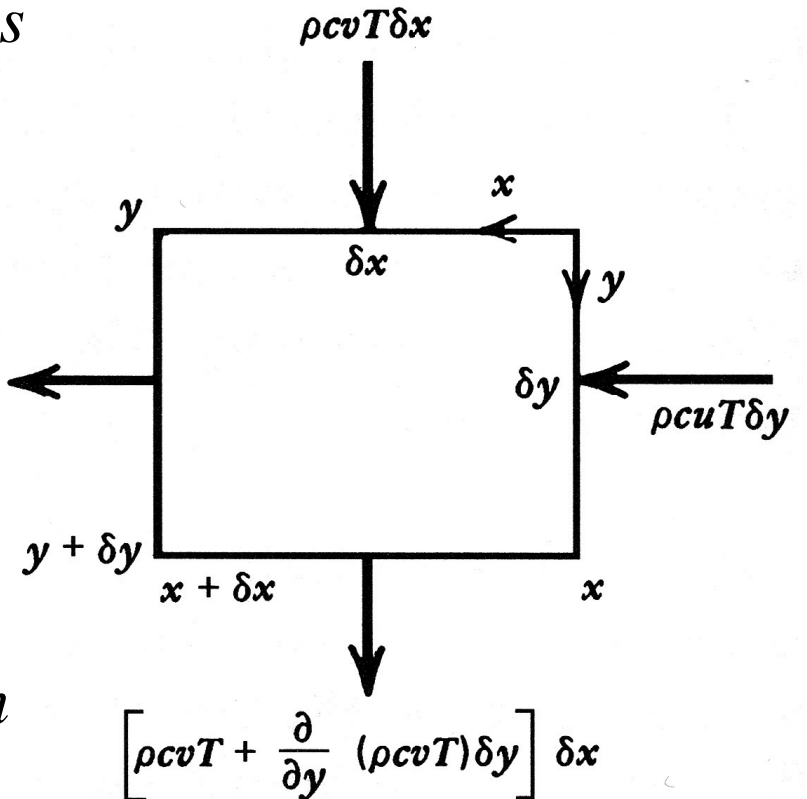
$$\frac{\partial(\rho C_P T)}{\partial t} \delta x \delta y$$

- **Advection**

$$\left[\frac{\partial(\rho C_P u T)}{\partial x} + \frac{\partial(\rho C_P v T)}{\partial y} \right] \delta x \delta y$$

$$\rho C_P \left[u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right] \delta x \delta y$$

conservation
of mass

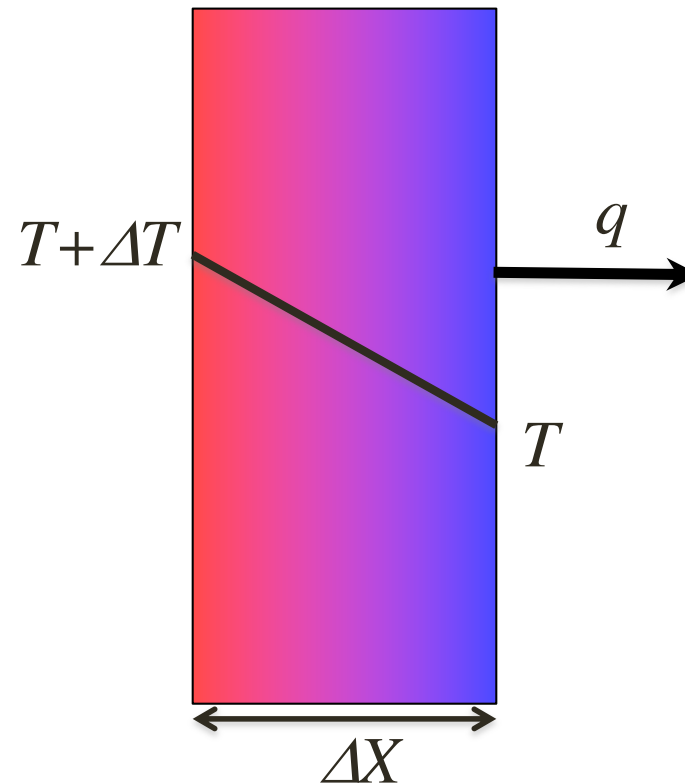


- **Conduction**

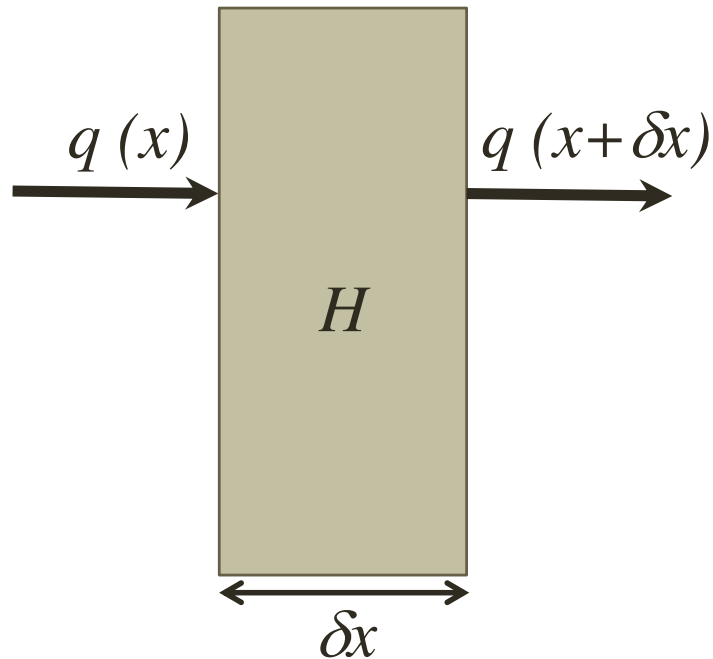
Fourier's Law for conduction

$$q = -k \frac{dT}{dx}$$

- **Heat flux**, q , = heat/area = energy/time/area,
unit: J/s/m² = W/m²
- Heat flux proportional to **temperature gradient**
- Minus sign because heat flows from hot to cold
- Constant of proportionality: **thermal conductivity**, k ,
unit: W/m/K



1-D Steady State Conduction



$$-k \frac{d^2 T}{dx^2} = \rho H = A$$

- **net heat flow/unit area/unit time =**

$$q(x + \delta x) - q(x)$$

$$q(x + \delta x) = q(x) + \delta x \frac{dq}{dx} + \dots$$

$$q(x + \delta x) - q(x) \approx \delta x \frac{dq}{dx}$$

$$\delta x \frac{dq}{dx} = \delta x \left[\frac{d}{dx} \left(-k \frac{dT}{dx} \right) \right]$$

$$\delta x \frac{dq}{dx} = \delta x \left[-k \frac{d^2 T}{dx^2} \right] \quad \text{for constant } k$$

- **heat produced = $\rho H \delta x = A \delta x$**

H - heat production rate/unit mass (W/kg)

A - heat production/unit volume (W/m³)

2-D energy equation

Spatial, constant ρ , C_P , k , , incompressible, no heat production

- **Change in heat content**

$$\frac{\partial(\rho C_P T)}{\partial t} \delta x \delta y$$

- **Advection**

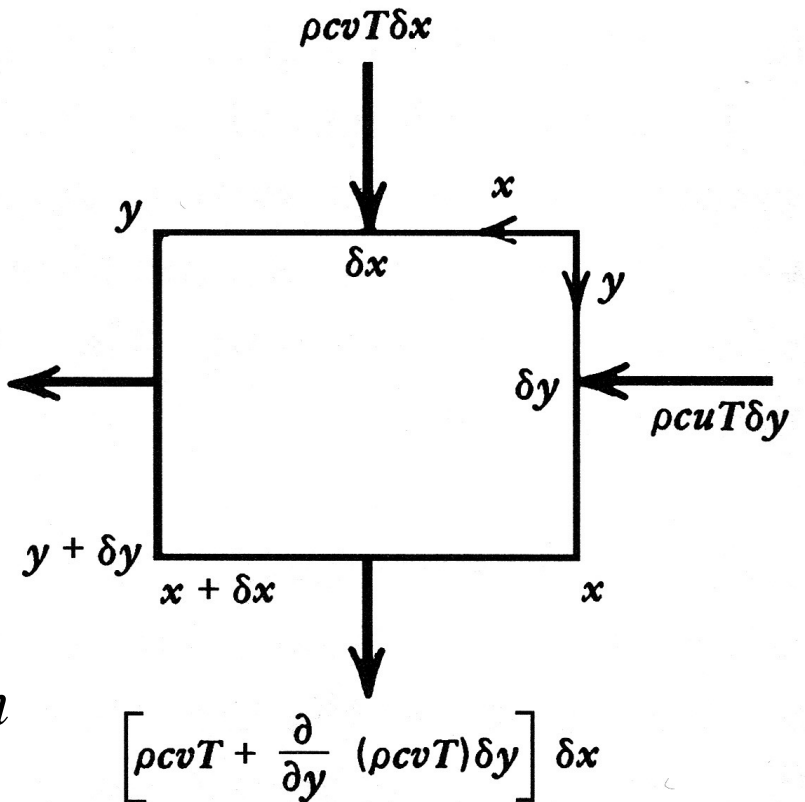
$$\left[\frac{\partial(\rho C_P u T)}{\partial x} + \frac{\partial(\rho C_P v T)}{\partial y} \right] \delta x \delta y$$

$$\rho C_P \left[u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right] \delta x \delta y$$

conservation
of mass

- **Conduction**

$$-k \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right) \delta x \delta y$$



2-D energy equation

Spatial, constant ρ , C_P , k , , incompressible, no heat production

- Change in heat content**

$$\frac{\partial(\rho C_P T)}{\partial t} \delta x \delta y = \rho C_P \frac{\partial T}{\partial t} \delta x \delta y$$

- Advection**

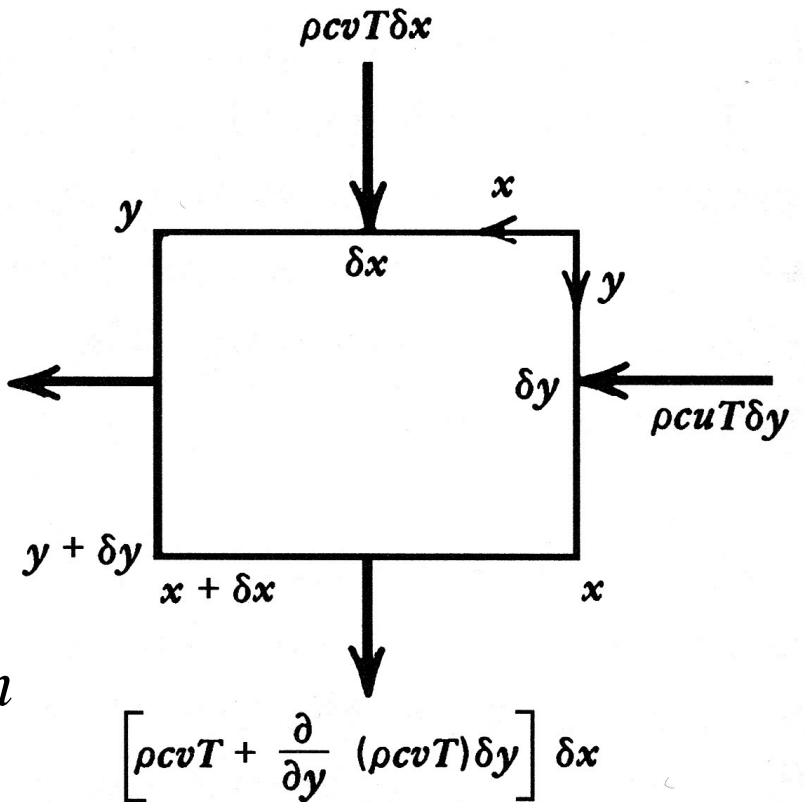
$$\left[\frac{\partial(\rho C_P u T)}{\partial x} + \frac{\partial(\rho C_P v T)}{\partial y} \right] \delta x \delta y$$

conservation of mass

$$\rho C_P \left[u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right] \delta x \delta y$$

- Conduction**

$$-k \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right) \delta x \delta y$$



$$\rho C_P \left[\frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right] = k \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right)$$

$$\rho C_P \left[\frac{\partial T}{\partial t} + \mathbf{u} \cdot \nabla T \right] = k \nabla^2 T$$

Energy equation

$$\frac{D(K + U)}{Dt} = W + Q$$

- **Material derivative internal heat**

$$\rho C_p \left[\frac{\partial T}{\partial t} + u \cdot \nabla T \right] = \rho C_p \frac{DT}{Dt} \Rightarrow \frac{D(\rho C_p T)}{Dt}$$

Allowing for
spatial
variations of
material
parameters

- **Heat input**

$$k \nabla^2 T \Rightarrow \nabla \cdot k \nabla T$$

Conduction

$$+A$$

Internal heat production

- **Work done**

\Rightarrow Changes in *motion* (kinetic energy) and *internal deformation*

Net effect of $W - \frac{DK}{Dt}$ becomes

$$\sigma : \mathbf{D}$$

\mathbf{D} – strain rate

Energy equation

conservation of heat

I	II	III	IV	V	VI
$D(\rho C_p T)/Dt =$	$\nabla \cdot \mathbf{k} \nabla T$	$+ A$	$+ \boldsymbol{\sigma} : \mathbf{D}$	$(+ \alpha T \mathbf{v} \cdot \nabla P$	$\dots)$

I - change in temperature with time

II - heat transfer by conduction (and radiation)

III - heat production (including latent heat)

IV - heat generated by internal deformation

V - heat generated by adiabatic compression

VI - other heat sources, e.g. latent heat

Conservation equations

- Conservation of mass

- Kinematics

$$\frac{D\rho}{Dt} + \rho \nabla \cdot \mathbf{v} = 0$$

- Conservation of momentum

- Dynamics

- Newton's second law

- Angular momentum

$$\rho \frac{D\mathbf{v}}{Dt} = \nabla \cdot \underline{\underline{\boldsymbol{\sigma}}} + \mathbf{f}$$

$$\boldsymbol{\sigma} = \boldsymbol{\sigma}^T$$

- Conservation of energy

- First law of thermodynamics

$$\frac{D(\rho C_p T)}{Dt} = \nabla \cdot k \nabla T + A + \boldsymbol{\sigma} : \mathbf{D}$$

- Entropy inequality

Which law is this?

Rate of entropy increase of a particle always \geq entropy supply

Continuum Mechanics Equations

General:

1. Kinematics – describing deformation and velocity without considering forces
2. Dynamics – equations that describe force balance, conservation of linear and angular momentum
3. Thermodynamics – relations temperature, heatflux, stress, entropy

Material-specific

4. Constitutive equations – relations describing how material properties vary as a function of T,P, stress,.... Such material properties govern dynamics (e.g., *density*), response to stress (*viscosity, elastic parameters*), heat transport (*thermal conductivity, heat capacity*)

1-D advection-diffusion solution

$$-v_z \frac{\partial T}{\partial z} = \kappa \frac{\partial^2 T}{\partial z^2}$$

$$\kappa = \frac{k}{\rho C_p}$$

Take $f(z) = \frac{\partial T}{\partial z}$ and $c = \frac{v_z}{\kappa}$

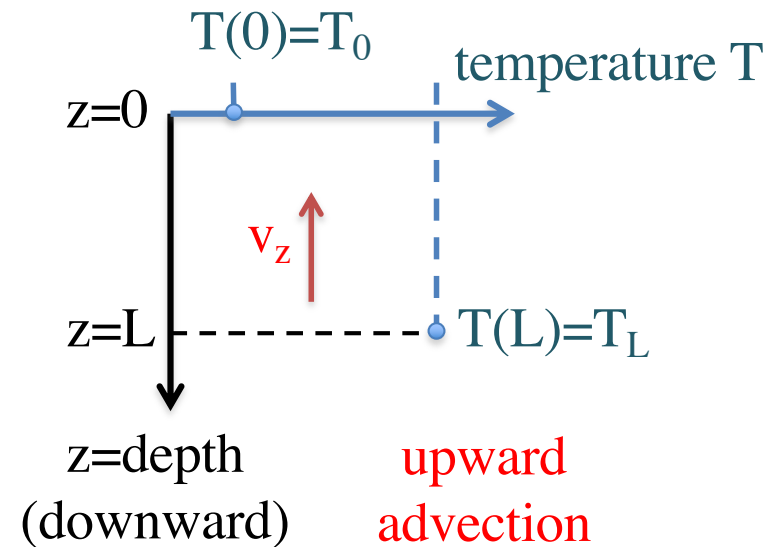
Then $\frac{\partial f}{\partial z} = -cf(z)$

\Rightarrow This yields $f(z) = f(0)e^{-cz}$, i.e. $\frac{\partial T}{\partial z}(z) = A e^{-v_z z / \kappa}$ where A, B are integration constants

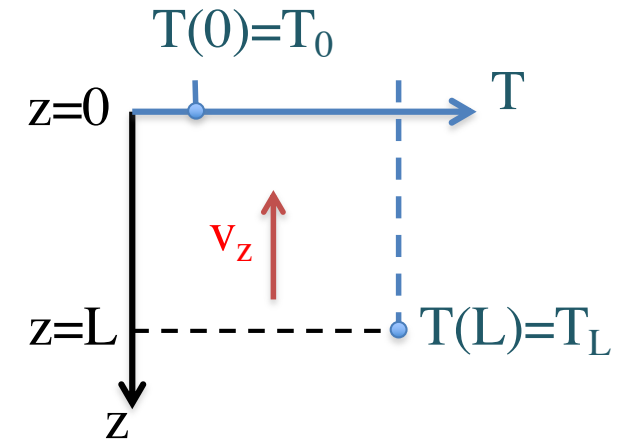
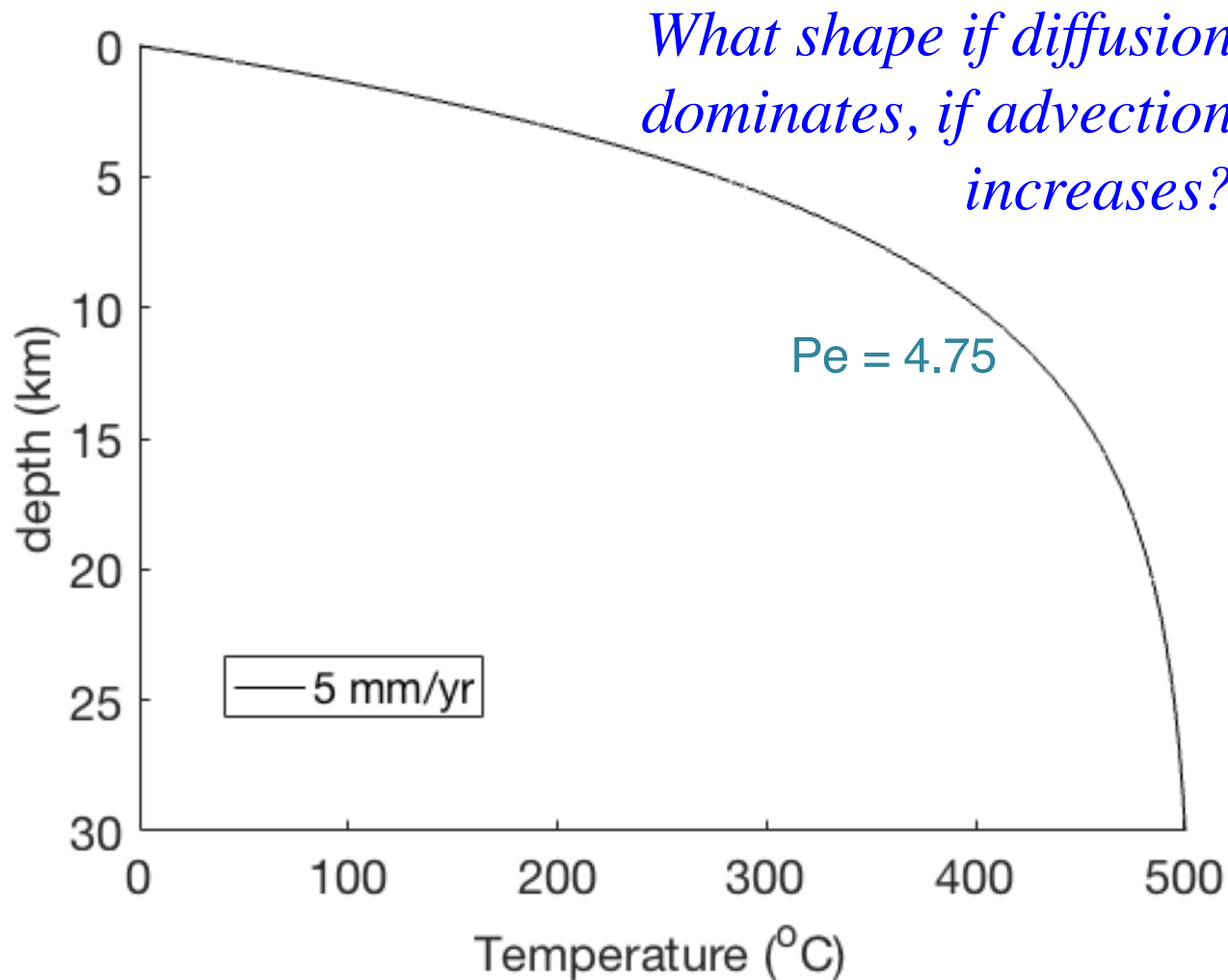
$$T(z) = B - \frac{A}{v_z / \kappa} e^{-v_z z / \kappa}$$

For constant temperature boundary conditions $T(z=0)=0$ and $T(z=L)=T_L$

\Rightarrow Integration gives: $T(z) = T_L \left[\frac{1 - e^{-v_z z / \kappa}}{1 - e^{-v_z L / \kappa}} \right]$



1-D advection-diffusion solution



$$T(z) = T_L \left[\frac{1 - e^{-v_z z / \kappa}}{1 - e^{-v_z L / \kappa}} \right]$$

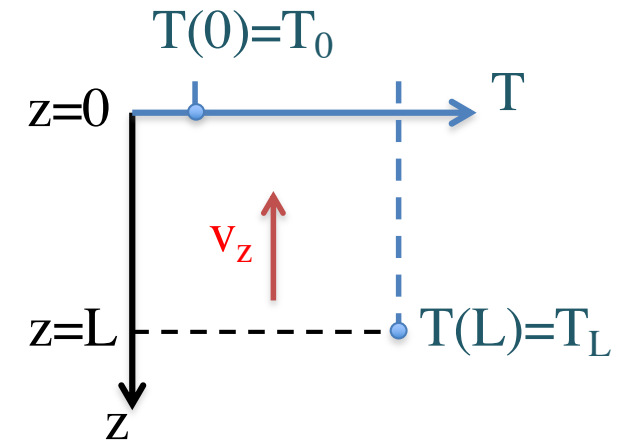
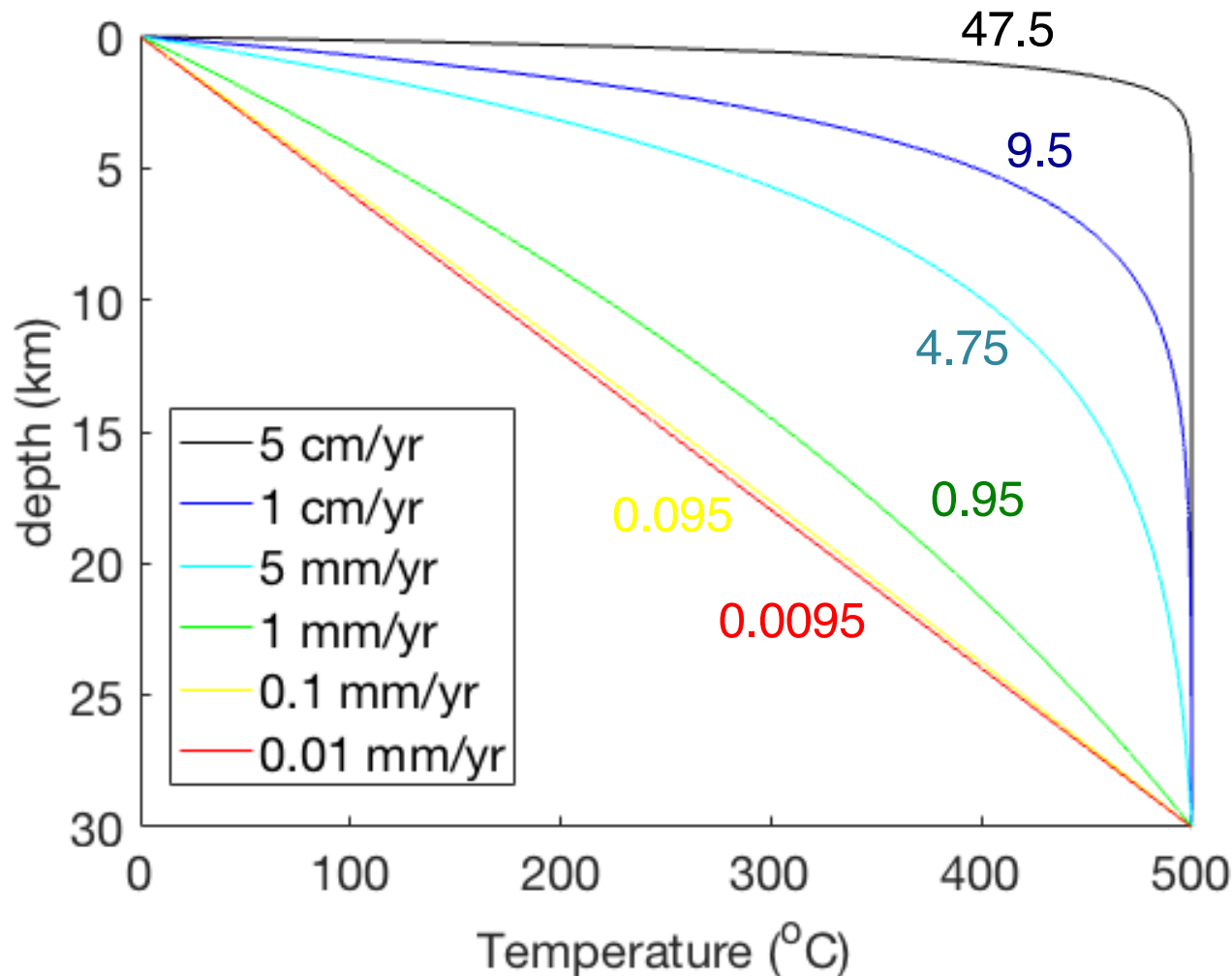
Peclet number, measure of relative importance advection/diffusion

$$Pe = \frac{v_z L}{\kappa} = \frac{[(m/s)m]}{[m^2/s]}$$

Take a break

- Use **Exercise 3** in chapter4.ipynb to look at the shape of the solutions
- **Exercise 4** for afternoon workshop

1-D advection-diffusion solution



$$T(z) = T_L \left[\frac{1 - e^{-v_z z / \kappa}}{1 - e^{-v_z L / \kappa}} \right]$$

Peclet number, measure of relative importance advection/diffusion

$$Pe = \frac{v_z L}{\kappa} = \frac{[(m/s)m]}{[m^2/s]}$$