

PGE 392K: Numerical Simulation of Reservoirs

Assignment #11

Due Monday, December 5 (No Penalty through Fri, Dec 9)

- (25 points). Adapt your “2-phase” IMPES simulator to be applicable for three-phase flow. In particular you will need to allow for:
 - Pressure-dependent PVT variables, R_s , B_o , and B_g
 - Three-phase relative permeability (see assignment #1)
 - Calculation of S_w , S_o , and S_g .

You might choose to make your simulator more flexible, but here we will only apply the code for 1D, no gravity, no capillary pressure, and no horizontal wells.

- (75 points). Run your simulator for a 1D reservoir that is $L = 1000$ ft, $w = 100$ feet, and $h = 100$ ft with permeability that is 10 mD and porosity is 0.20. There is a vertical, constant BHP producer at $x = 500$ ft of 100 STB/day liquid (oil + water). After 2 years, vertical injectors at $x = 0$ and $x = L$ inject 50 STB/day water each. If the producer BHP reaches 14.7 psia, convert to a BHP well of 14.7 psia and leave it at that BHP for the remainder of the simulation.

The reservoir temperature is 175 F and initial pressure is 1000 psia which is also the bubble point; $S_{wi} = S_{wr} = 0.10$. The water, *undersaturated* oil, and formation compressibility are $3E-6 \text{ psi}^{-1}$, $2.87E-6 \text{ psi}^{-1}$, and $1.0E-6 \text{ psi}^{-1}$, respectively. The water viscosity and formation volume factor can be assumed constant, 0.383 cp and 1.023, respectively. Other PVT properties are pressure dependent and summarized in equations below the bubble point. 3-phase relative permeability is given by the Stone I model (see assignment #1); $S_{wr} = 0.1$, $S_{orw} = 0.4$, $S_{org} = 0.2$, $S_{gr} = 0.05$, $k_{rw}^0 = 0.3$, $k_{row}^0 = 0.8$, $k_{rog}^0 = 0.8$, $k_{rg}^0 = 0.3$, $N_w = 2.0$, $N_g = 2.0$, $N_{ow} = 2.0$, $N_{og} = 2.0$.

$$R_s \left(\frac{\text{scf}}{\text{STB}} \right) = (3.43E-05) p^2 + 9.21E-02 p$$

$$B_o \left(\frac{\text{RB}}{\text{STB}} \right) = 6.119E-05 p + 1.083$$

$$z = 1.336E-08 p^2 - 8.804E-05 p + 0.9952$$

$$\mu_o [\text{cp}] = 4.846E-07 p^2 - 1.533E-03 p + 2.375$$

$$\mu_g [\text{cp}] = 5.929E-10 p^2 - 6.764E-07 p + 0.01309$$

Recall that below the bubble point,

$$c_o^* = -\frac{1}{B_o} \frac{\partial B_o}{\partial p}; \quad c_o = -\frac{1}{B_o} \left(\frac{\partial B_o}{\partial p} - B_g \frac{\partial R_s}{\partial p} \right)$$
$$B_g = 0.0282 \frac{zT}{p} \left[\frac{\text{ft}^3}{\text{scf}} \right]$$

Where P is in psia and T is in Rankine ($=^{\circ}\text{F} + 460$).

Note: In the calculation of interblock phase transmissibilities (e.g. Tg matrix) an **upwinded** formation volume factor must be used. However, when creating T, etc. the phase transmissibilities must be multiplied by a diagonal matrix of **block** formation volume factors.

Run your simulation for 6 years using a time step of 1 day for the following cases:

- a. 3 uniform grid blocks
- b. 100 grid blocks and make plots of the bottomhole pressure (all wells), oil rate (producer), and surface Gas-Oil Ratio (producer) versus time.