Computational physics Final project

Fin analysis using finite element method

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Presentation context

- 1. Basic of FEM with fin analysis
- FEM with solid conduction heat transfer
- 3. FEM with given fin mesh
- 4. Result in 2D & 3D
- 5. Analysis

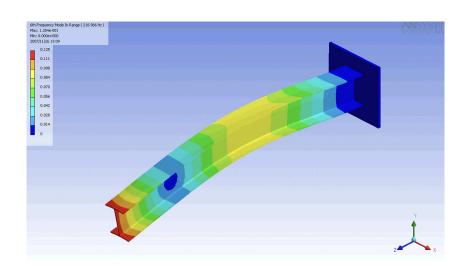
a. What is Finite Element Method?

a. What is fin?

a. How can we do this?

What is Finite Element Method?

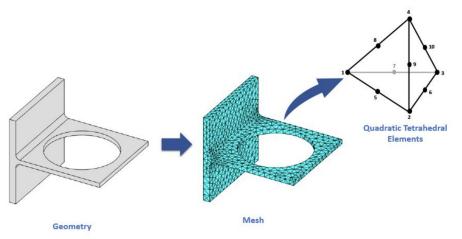
FEM is an analytic method to find solution by calculating mesh.



For example, it can be used analyzing critical stress or temperature of material, deflection of beam.

What is Finite Element Method?

- FEM is an analytic method to find solution by calculating mesh.



We slice given geometry to "element".

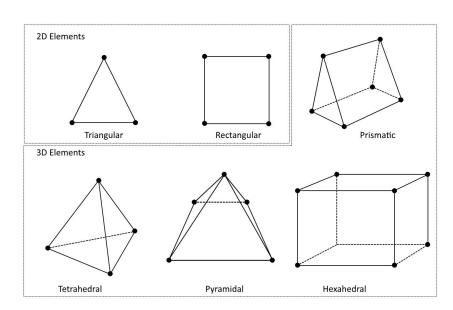
We call the set of every elements, "mesh".

What is Finite Element Method?

- FEM is an analytic method to find solution by calculating mesh.

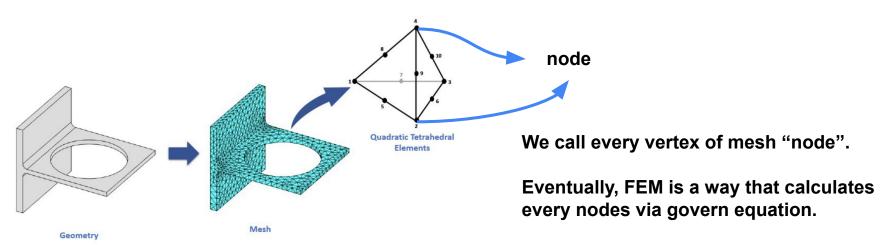
There could be multiple ways to generating mesh.

The geometry of mesh may affect the result.



What is Finite Element Method?

FEM is an analytic method to find solution by calculating mesh.



What is fin?



Fin is a surface that extend from an hot object to increase the heat transfer rate.

The amount of conduction, convection and radiation will affect the heat transfer.

In short, if the fin can transfer heat faster, the CPU can cooler.

How can we do this?

- There are several important coefficient about transient fin heat transfer.

1. Biot number (Bi)
$$Bi=rac{hL_c}{k}$$

1. Fourier number (Fo)
$$Fo = rac{lpha \Delta t}{dx*dy}$$

How can we do this?

- Biot number (Bi)

$$Bi = rac{hL_c}{k}$$

 L_c : characteristic length

 $h: {
m convection\ heat\ transfer\ coefficient}$

k: conduction heat transfer coefficient

- Biot number is a coefficient that shows contribution of convection versus conduction in transient heat transfer.
- If Biot number >> 1, convection will be the dominant factor that contributes heat transfer
- If Biot number << 1, conduction will be the dominant factor that contributes heat transfer

How can we do this?

- Biot number (Bi)
$$Bi=rac{hL_c}{k}$$
 h: convection heat transfer coefficient

 L_c : characteristic length

k: conduction heat transfer coefficient

characteristic length is approximated length that describes "outer region VS inner region"

$$L_c pprox rac{ ext{Surface}}{ ext{Volume}} ext{ or } rac{ ext{Circumference}}{ ext{Surface}}$$

How can we do this?

- Fourier number (Fo) $Fo=rac{lpha\Delta t}{dx*dy}$ $\Delta t: ext{unit time step} \ dx ext{ and } dy: ext{unit length of mesh}$

 α : thermal diffusivity

- Fourier number is a coefficient that describes "how much heat will travel during the unit time step".

How can we do this?

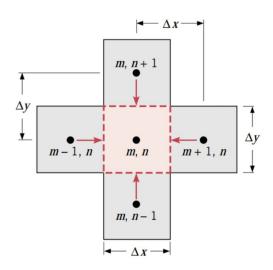
- α : thermal diffusivity - Fourier number $_{(Fo)}$ $Fo=rac{lpha\Delta t}{dx*du}$ Δt : unit time step dx and dy: unit length of mesh
- Larger the unit time step becomes, unit mesh length has to be larger too.

If we set smaller unit mesh, FEM will collapse, since heat will pass through current mesh element and affect the others.

How can we do this?

- FEM is based on energy equilibrium.





(Heat flows to (m,n)) + (Heat that generated by (m,n)) = (Heat that (m,n) emit)

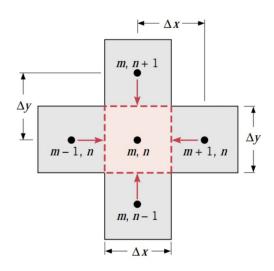
Assume there's no heat generated by material, (q = 0) and apply this condition to Heat diffusion equation

$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} + \frac{\dot{q}}{k} = \frac{1}{\alpha} \frac{\partial T}{\partial t}$$

We can use finite difference approximation to calculate second derivative.

How can we do this?

- Eventually, we can describe the node like below



$$egin{aligned} T_{m,n}^{p+1} &= Fo(T_{m+1,n}^p + T_{m-1,n}^p + T_{m,n+1}^p + T_{m,n-1}^p) \ &+ (1-4Fo)T_{m,n}^p \end{aligned}$$

 $ar{T}_{p}^{\uparrow} \ T_{m,n}^{p} : ext{temperature of node (m,n) in time (p)}$

Note that in only applies 2-dimensional, closed mesh (4 nodes are adjacent with node (m,n))

Other mesh case can be calculated like this

TABLE 5.3 Transient, two-dimensional finite-difference equations $(\Delta x = \Delta y)$

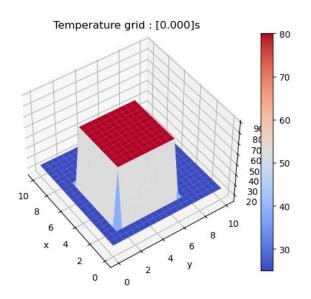
	(a) Explicit Method		
Configuration	Finite-Difference Equation	Stability Criterion	(b) Implicit Method
$\begin{array}{c c} & & & & & \\ & & & & \\ & & & \\ & & & \\ & & & \\ & & & \\ & & & \\ & & & \\ & \\ & & \\ & & \\ & & \\ & & \\ & & \\ & & \\ & & \\ & & \\ & & \\ & & \\ &$	$\begin{split} T_{m,n}^{p+1} &= Fo(T_{m+1,n}^p + T_{m-1,n}^p \\ &+ T_{m,n+1}^p + T_{m,n-1}^p) \\ &+ (1 - 4Fo)T_{m,n}^p \end{split} \tag{5.76}$ 1. Interior node	$Fo \le \frac{1}{4} \tag{5.80}$	$(1 + 4Fo) T_{m,n}^{p+1} - Fo(T_{m+1,n}^{p+1} + T_{m-1,n}^{p+1} + T_{m,n+1}^{p+1} + T_{m,n-1}^{p+1}) = T_{m,n}^{p} $ (5.92)
m-1, m , $n+1$ m , $n-1$ m , $n-1$	$T_{m,n}^{p+1} = \frac{2}{3}Fo(T_{m+1,n}^p + 2T_{m-1,n}^p + 2T_{m,n+1}^p + T_{m,n-1}^p + 2BiT_{\infty}) + (1 - 4Fo - \frac{4}{3}BiFo)T_{m,n}^p $ (5.85) 2. Node at interior corner with convection	$Fo(3 + Bt) \le \frac{3}{4}$ (5.86)	$(1 + 4Fo(1 + \frac{1}{3}Bh))T_{m-1,n}^{p+1} - \frac{2}{3}Fo \cdot (T_{m+1,n}^{p+1} + 2T_{m-1,n}^{p+1} + 2T_{m,n+1}^{p+1} + T_{m,n-1}^{p+1})$ $= T_{m,n}^{p} + \frac{4}{3}BiFoT_{\infty} $ (5.95)
$ \begin{array}{c c} & m & n+1 \\ & \Delta y \\ & m-1, & n \\ & m, & n-1 \end{array} $	$T_{m,n}^{p+1} = Fo(2T_{m-1,n}^p + T_{m,n+1}^p + T_{m,n-1}^p + 2Bi T_{\infty}) + (1 - 4Fo - 2Bi Fo) T_{m,n}^p$ (5.87) 3. Node at plane surface with convection ^a	$Fo(2 + Bi) \le \frac{1}{2}$ (5.88)	$(1 + 2Fo(2 + Bi)) T_{m,n}^{p+1} - Fo(2T_{m-1,n}^{p+1} + T_{m,n+1}^{p+1} + T_{m,n-1}^{p+1}) = T_{m,n}^{p} + 2Bi Fo T_{\infty} $ (5.96)
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	$T_{m,n}^{p+1} = 2Fo(T_{m-1,n}^p + T_{m,n-1}^p + 2Bi T_{\infty}) + (1 - 4Fo - 4Bi Fo) T_{m,n}^p$ (5.89)	$Fo(1 + B\hat{\imath}) \le \frac{1}{4}$ (5.90)	$(1 + 4Fo(1 + Bi)) T_{m,n}^{p+1} - 2Fo(T_{m-1,n}^{p+1} + T_{m,n-1}^{p+1}) = T_{m,n}^{p} + 4Bi Fo T_{\infty} $ (5.97)

Bergman, T. L., and Frank P. Incropera. *Fundamentals of Heat and Mass Transfer*. Seventh edition. Wiley, 2011, 330-334

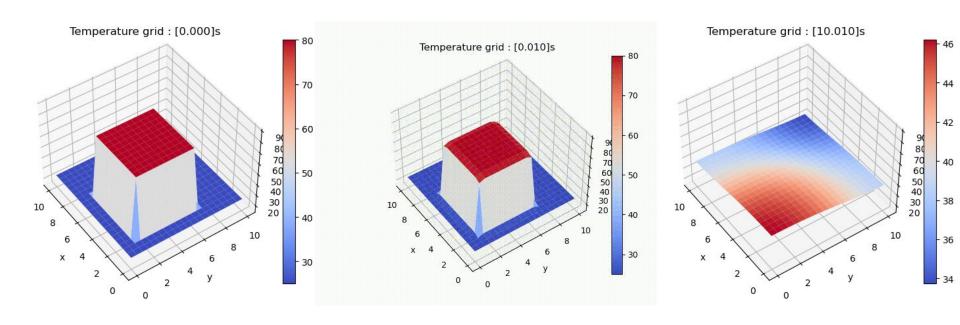
[&]quot;To obtain the finite-difference equation and/or stability criterion for an adiabatic surface (or surface of symmetry), simply set Bi equal to zero.

We made first model using numpy, matplotlib, and OpenCV to export animation

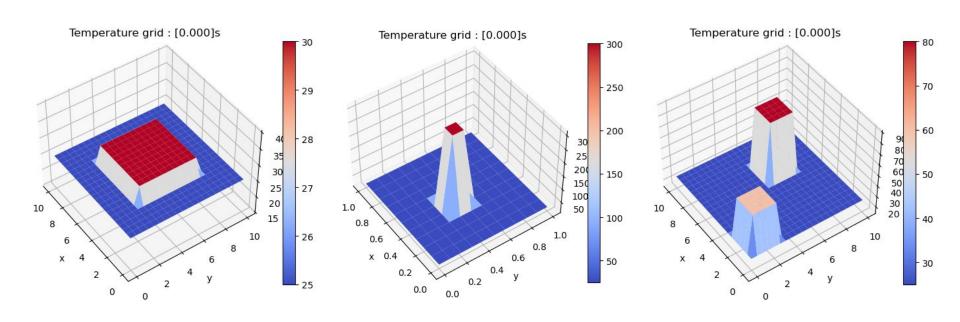
```
1 import numpy as np
   import matplotlib.pyplot as plt
   from matplotlib.cm import coolwarm
   from matplotlib.backends.backend_agg import FigureCanvasAgg
7 class FEM_2d:
       def __init__(self, alpha, X, Y, T, dx, dy) : --
       def return_index(self, x, y) : --
       def set_ic_rect(self, T, pt1 : list, pt2 : list) :
       def set_bc(self, T, X_axis : list=None, Y_axis : list=None) : "
       def return_plot(self, elev=45, azim=145) : ...
       def plot_status(self, elev=45, azim=145) : "
       def print_status(self) : --
       def build(self, dt) : ...
       def compute(self, t_end, verbose=False, save_gif=False, elev=45, azim=145) : ...
       def save_animation(self, t_end) : --
```



It's a model for rectangular fin, only affected by conduction and boundary condition.



You can adjust mesh size, initial conditions and boundary conditions



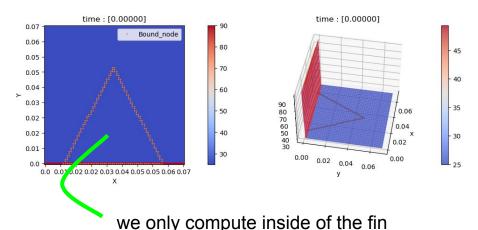
There are disadvantage with this model

- 1. There's too many meshes to calculate.
- 2. Using OpenCV to animate process wasn't good idea.
- 3. There's no utils for computing mesh until steady-state is reached.

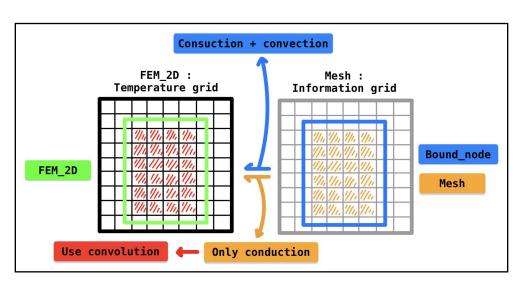
We've made a second model that decrease computation, and uses FuncAnimation of matplotlib to animate process.

```
import numpy as np
     import matplotlib.pyplot as plt
     import time, sys
     from numpy import pi, sin, cos
     from math import sqrt
     from functools import partial
     from matplotlib.cm import coolwarm
     from matplotlib.animation import FuncAnimation
 11 > class Bound_node : -
 14 > class Mesh : ...
247 > class FEM 2D() : --
```

To decrease computation, we only compute the mesh inside the fin.



We've made a second model that decrease computation, and uses FuncAnimation of matplotlib to animate process.



To decrease computation, we use convolution to compute inner temperature of fin.

Because inside the fin, every nodes have 4 adjacent nodes, which means only conduction occurs, makes computation easier.

Details at final report - [2. model idea]

$$T_{m,n}^{p+1} = Fo(T_{m+1,n}^p + T_{m-1,n}^p + T_{m,n+1}^p + T_{m,n-1}^p) + (1-4Fo)T_{m,n}^p$$

TABLE 5.3 Transient, two-dimensional finite-difference

	(a) Explicit Metho				
Configuration	Finite-Difference Equation		(b) Implicit Method		
m, n+1 $m, n+1$ $m, n+1$ $m+1, n$	$T_{m,n}^{p+1} = Fo(T_{m+1,n}^p + T_{m-1,n}^p + T_{m,n+1}^p + T_{m,n-1}^p) + (1 - 4Fo) T_{m,n}^p$ (5)	(1 - 5.76)	$+4Fo)T_{m,n}^{p+1} - Fo(T_{m+1,n}^{p+1} + T_{m-1,n}^{p+1} + T_{m,n+1}^{p+1} + T_{m,n-1}^{p+1}) = T_{m,n}^{p}$	(5.92)	
m-1, n $m, n+1$ m, n $m, n-1$	$T_{m,n}^{p+1} = \frac{2}{3}Fo(T_{m+1,n}^p + 2T_{m-1,n}^p + 2T_{m,n+1}^p + T_{m,n-1}^p + 2BiT_{\infty}) + (1 - 4Fo - \frac{4}{3}BiFo)T_{m,n}^p $ (5) 2. Node at interior corner with convection	5.85)	$+4Fo(1+\frac{1}{3}Bi))T_{m,n}^{p+1}-\frac{2}{3}Fo\cdot (T_{m+1,n}^{p+1}+2T_{m-1,n}^{p+1}+2T_{m,n+1}^{p+1}+T_{m,n-1}^{p+1})$ $=T_{m,n}^{p}+\frac{4}{3}BiFoT_{\infty}$) (5.95)	
$ \begin{array}{c c} & m, n+1 \\ & \lambda y \\ & m-1, n \end{array} $ $ \begin{array}{c c} & m, n+1 \\ & m, n+1 \\ & m, n-1 \end{array} $	$\begin{split} T_{m,n}^{p+1} &= Fo(2T_{m-1,n}^p + T_{m,n+1}^p \\ &+ T_{m,n-1}^p + 2BiT_{\infty}) \\ &+ (1 - 4Fo - 2BiFo)T_{m,n}^p \end{split} \tag{5}$ 3. Node at plane surface with convection	5.87)	$+ 2Fo(2 + Bi) T_{m,n}^{p+1}$ $- Fo(2T_{m-1,n}^{p+1} + T_{m,n+1}^{p+1} + T_{m,n-1}^{p+1})$ $= T_{m,n}^{p} + 2Bi Fo T_{\infty}$	(5.96)	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	$T_{m,n}^{p+1} = 2Fo(T_{m-1,n}^p + T_{m,n-1}^p + 2Bi T_{\infty}) + (1 - 4Fo - 4Bi Fo) T_{m,n}^p$ (5	5.89)	(-111-1,11 - 111,11-1)	(5.97)	

computation, and uses FuncAnimation

To decrease computation, we use convolution to compute inner temperature of fin.

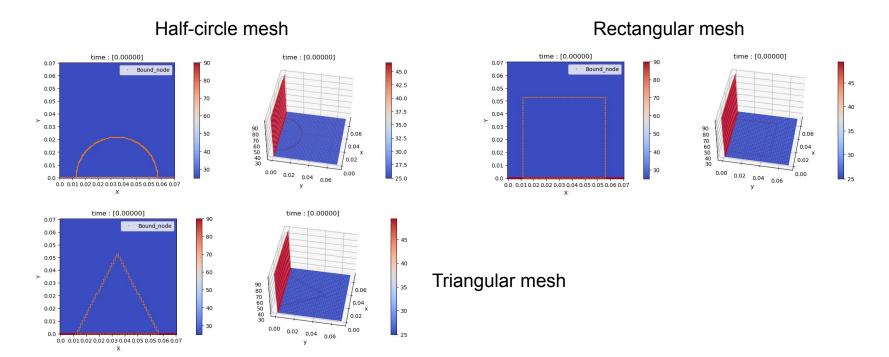
Because inside the fin, every nodes have 4 adjacent nodes, which means only conduction occurs, makes computation easier.

Details at final report - [2. model idea]

$$T_{m,n}^{p+1} = Fo(T_{m+1,n}^p + T_{m-1,n}^p + T_{m,n+1}^p + T_{m,n-1}^p) + (1-4Fo)T_{m,n}^p$$

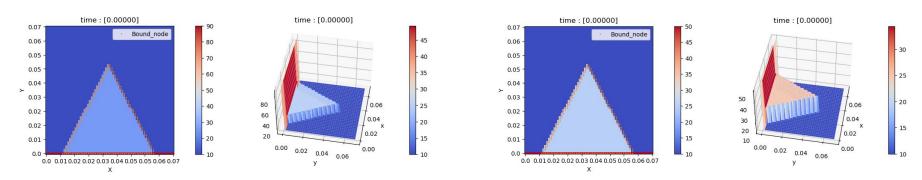
 $[^]a$ To obtain the finite-difference equation and/or stability criterion for an adiabatic simply set $\it Bi$ equal to zero.

There are three geometry of second model



Model can adjust boundary condition, initial condition, and mesh size.

This model includes the convection heat transfer via surrounding air with given coefficient and temperature



You can see both the air and boundary temperature are different

We made a utils that compute mesh until steady-state.

If the model reaches steady-state in max iteration, it will shows the precision of convergence and average temperature. Otherwise, it will stop

```
Estimate computing time

1  dt = 0.0025
2  t_end = dt * 500
3  Triangle_fin.is_good(dt, t_end)

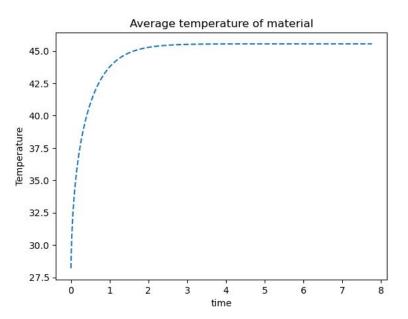
1  Triangle_fin.compute_steady_state(dt=0.0025, max_iter=1.0e+4)

[]
```



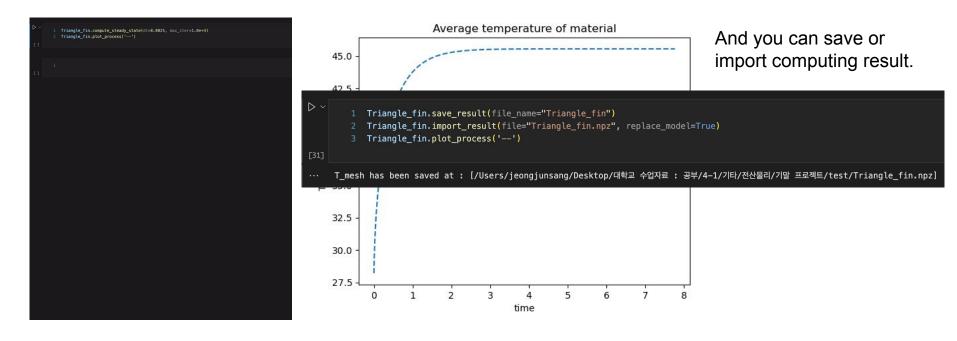
You can watch the average temperature difference via time.



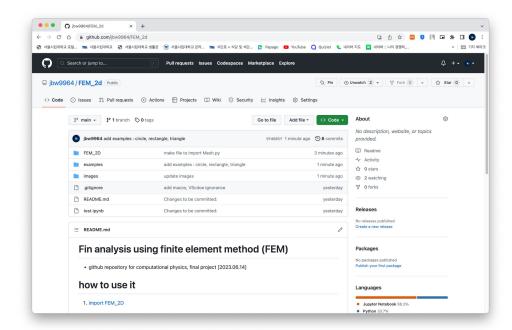


And you can save or import computing result.

You can watch the average temperature difference via time.



More details at github repository.



https://github.com/jbw9964/FEM_2d.git

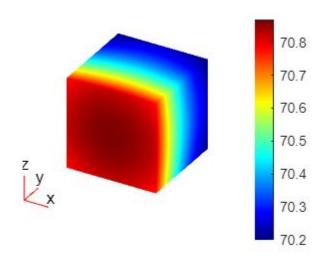
4. Result 2D & 3D

Shapes?

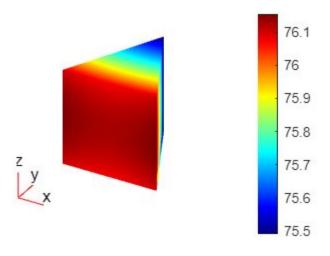
4-1. 2D results

4-2. 3D results

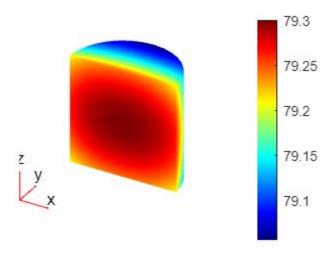
steady state transient video



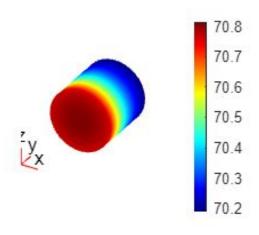
Average Temperature: 70.4851



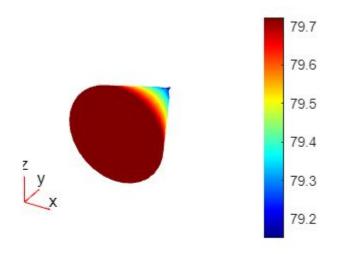
Average Temperature: 75.8988



Average Temperature: 79.1791



Average Temperature: 70.437



Average Temperature: 79.5971

transient video

5. Analysis

heat sink재료: 알루미늄 합금.. 접촉부분 Cu, 나머지(fin부분 등) AI사용 경우 多

