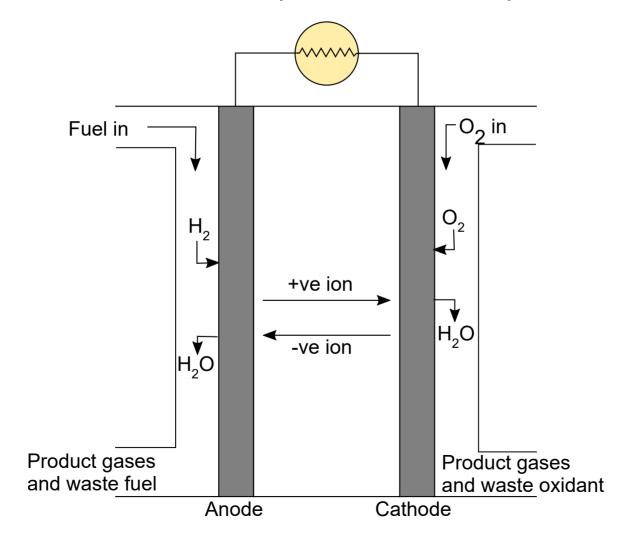
### **Fuel Cells**

### **Fuel Cells**

Fuel cells are similar to batteries; they have a cathode, electrolyte and anode.



# Fuel cell history

### Fuel cell fundamentals

$$\mathrm{Fuel} + \mathrm{O_2} \longrightarrow \mathrm{H_2O} + \mathrm{nCO_2}$$

- Fuel cells a divided into *low-temperature (LT)* (< 200 °C) and *high-temperature (HT)* (> 450 °C).
- H<sub>2</sub> is the preferred fuel
  - Particularly for LT devices.
  - Doesn't produce CO<sub>2</sub>
- Other fuels (e.g. CH<sub>3</sub>OH, CH<sub>4</sub>, NH<sub>3</sub>) can also be used, particularly for HT devices
  - $\circ$  *e.g.* for CH<sub>4</sub>, steam reforming  $(CH_4 + H_2O \xrightarrow{>700^{\circ}C} CO + 3\,H_2)$  can be achieved in HT cells, but must be performed separately for LT cells.

# Fuel cell efficiency

Fuel cells are very efficient

Convert fuel → electricity directly, rather than fuel → heat → electricity (as in combustion)

Thermodynamic efficiency 
$$=rac{\Delta G}{\Delta H}$$

e.g. for 
$$2\,\mathrm{H_2} + \mathrm{O_2} \longrightarrow 2\,\mathrm{H_2O}~(\Delta H = -571.6~\mathrm{kJ~mol}^{-1})$$
:

Cathode: 
$$4\,\mathrm{H^+} + \mathrm{O_2} + 4\,\mathrm{e^-} \longrightarrow 2\,\mathrm{H_2O}$$
  $\mathrm{E} = +1.229\,\mathrm{V}$  Anode:  $4\,\mathrm{H^+} + 4\,\mathrm{e^-} \longleftarrow 2\,\mathrm{H_2}$   $E = 0.00\,\mathrm{V}$ 

$$egin{aligned} \Delta G &= -nFE \ &= -4 imes F imes 1.229 \ &= -474.3 ext{ kJ mol}^{-1} \end{aligned} \qquad ext{(per mole O}_2) \end{aligned}$$

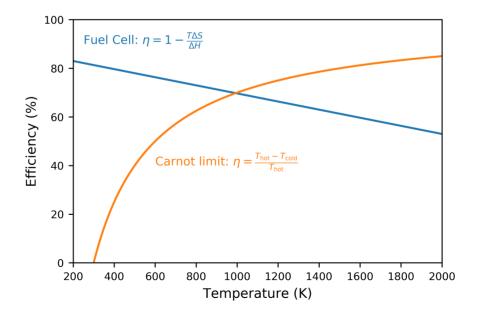
Efficiency =  $\eta$  = -474.3 / 571.6 = **83%** 

### Efficiency with temperature

$$\Delta G = \Delta H - T \Delta S, \quad \therefore \quad rac{\Delta G}{\Delta H} = \eta = 1 - rac{T \Delta S}{\Delta H}$$

For an 'ideal' heat engine (a perfectly efficient combustion engine) the maximum efficiency is determined by the Carnot limit:

$$\eta = rac{T_{
m hot} - T_{
m cold}}{T_{
m hot}}$$



# Types of fuel cell

Туре	Mobile ion	Operating temperature (°C)	Applications
Alkaline	OH-	50-100	Stationary power, space missions
Polymer	H <sup>+</sup> or OH <sup>-</sup>	50-100	Portable devices, transport
Phosphoric acid (PAFC)	H <sup>+</sup>	220	Medium to large scale combined heat and power (CHP) systems
Molten Carbonate (MCFC)	CO <sub>3</sub> <sup>2-</sup>	650	
Solid Oxide (SOFC)	O <sup>2-</sup>	500 - 1000	:

# Alkaline Fuel cell (AFC)

Anode: 
$$2 \, \mathrm{H_2O} + 2 \, \mathrm{e^-} \longleftarrow \mathrm{H_2} + 2 \, \mathrm{OH^-}$$
  $E = -0.829 \, \mathrm{V}$ 

Cathode: 
$$\frac{1}{2}$$
O $_2 + 2$ H $_2$ O + 2 e $^- \longrightarrow 2$  OH $^ E = +0.401$  V

Overall: 
$${\rm H_2} + \frac{1}{2}{\rm O_2} \longrightarrow {\rm H_2O} \qquad \qquad E = +1.23 \; {\rm V}$$

- First developed for the Apollo missions
  - Updated version still used in current space shuttle
- Based around concentrated KOH electrolyte with Ni anode and catalytic cathode (such as Pt, Pd or Ag)
- Cheap fuel cell to produce √
- Susceptible to CO<sub>2</sub> poisoning: X

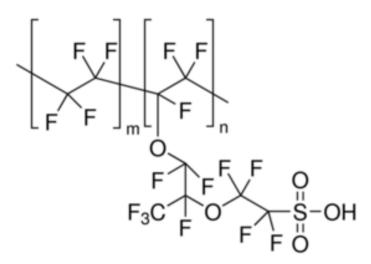
$$\circ \ 2\operatorname{KOH} + \operatorname{CO}_2 \longrightarrow \operatorname{K}_2\operatorname{CO}_3 + \operatorname{H}_2\operatorname{O}$$

- ∘ K<sub>2</sub>CO<sub>3</sub> goes on to block electrode
- Requires pure H<sub>2</sub> and O<sub>2</sub> X



# Proton exchange membrane fuel cell (PEMFC)

- First developed for the Gemini space vehicle
- Based around an acidic proton-conducting polymer
  - ∘ *e.g.* Nafion





• Use H<sub>2</sub> as fuel, but can work with MeOH (less efficiently)

### PEMFC + H<sub>2</sub>

$$\begin{array}{lll} \text{Anode:} & 2\,\mathrm{H}^+ + 2\,\mathrm{e}^- \longleftarrow \mathrm{H}_2 & E = 0\,\mathrm{V} \\ \text{Cathode:} & \mathrm{O}_2 + 2\,\mathrm{H}^+ + 2\,\mathrm{e}^- \longrightarrow \mathrm{H}_2\mathrm{O}_2 & E = 0.695\,\mathrm{V} \\ & \mathrm{H}_2\mathrm{O}_2 + 2\,\mathrm{H}^+ + 2\,\mathrm{e}^- \longrightarrow 2\,\mathrm{H}_2\mathrm{O} & E = 1.776\,\mathrm{V} \\ \text{Cathode (Overall):} & \mathrm{O}_2 + 4\,\mathrm{H}^+ + 4\,\mathrm{e}^- \longrightarrow 2\,\mathrm{H}_2\mathrm{O} & E = 1.229\,\mathrm{V} \end{array}$$

- PEMFCs give good Low-temperature (< 100 °C) operation √</li>
  - Quick to start/stop
  - Suitable for portable applications
- In acidic conditions, H<sub>2</sub>O<sub>2</sub> forms
  - Corrodes carbon-containing electrodes
  - Lowers cell voltage
  - Requires Pt or Pd catalysts to promote H<sub>2</sub>O<sub>2</sub> decomposition
    - $\sim 0.5 \text{ mg cm}^{-3}$
    - Expensive
    - Poor tolerance to CO or NH<sub>3</sub>
- Require careful hydration to ensure H<sup>+</sup> conduction X

### PEMFC + Methanol

Methanol is easier to store/transport than H<sub>2</sub> and almost as efficient

Readily oxidised, does not require C-C bond breaking

Anode: 
$$CO_2 + 6H^+ + 6e^- \leftarrow CH_3OH + H_2O$$
  $E = 0.046 V$ 

Cathode: 
$$\frac{3}{2}$$
O<sub>2</sub> + 6 H<sup>+</sup> + 6 e<sup>-</sup>  $\longrightarrow$  3 H<sub>2</sub>O  $E = 1.229$  V

Overall: 
$${
m CH_3OH} + {3\over 2}{
m O}_2 \longrightarrow {
m CO}_2 + 2{
m H}_2{
m O}$$
  $E=1.183{
m ~V}$ 

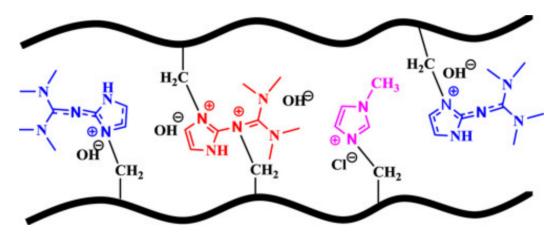
#### Problems:

- MeOH is fairly soluble in membrane, crossing from anode to cathode X
  - Reduces cell voltage to ~0.5 V
- CO is formed in a side-reaction, blocking reaction sites X
  - Improved by adding more Pt catalyst (~3 mg cm<sup>-2</sup>)



### Towards alkaline polymers?

- OH<sup>-</sup> conduction removes the problems associated with H<sub>2</sub>O<sub>2</sub> formation
- Attaching the counter-cation to the polymer reduces the risk of electrode poisoning
- pH change also modifies redox energies, allowing Ni catalysts to replace Pt



Unfortunately, current OH<sup>-</sup> conducting polymers currently have low ionic conductivity at practical temperatures!

# Phosphoric Acid (PAFC)

#### Operates at 200 °C

- High temperature acid prevents build up of H<sub>2</sub>O<sub>2</sub> ✓
- Temperature makes cell more tolerant to CO<sub>2</sub> impurities ✓
- Below 150 °C conductivity is low X
- Above 200 °C H<sub>3</sub>PO<sub>4</sub> decomposes into a range of acids X
- Hot H<sub>3</sub>PO<sub>4</sub> is highly corrosive! X
  - Materials stability challenge



### Molten Carbonate (MCFC)

- Optimum temperature 560 °C
- Range of fuel choices
  - High temperature allows steam reforming (water-gas shift reaction) to generate H<sub>2</sub>:

$$\begin{array}{cccc} \mathrm{CH}_4 + 2\,\mathrm{H}_2\mathrm{O} &\longrightarrow & \mathrm{CO}_2 + 4\,\mathrm{H}_2 & \mathrm{or} & \mathrm{CH}_4 + \mathrm{H}_2\mathrm{O} &\longrightarrow \mathrm{CO} + 3\,\mathrm{H}_2 \\ \mathrm{followed} \ \mathrm{by:} & \mathrm{CO} + \mathrm{H}_2\mathrm{O} & \rightleftharpoons & \mathrm{CO}_2 + \mathrm{H}_2 \\ & \mathrm{Anode:} & \mathrm{CO}_2 + \mathrm{H}_2\mathrm{O} + 2\,\mathrm{e}^- &\longleftarrow \mathrm{H}_2 + \mathrm{CO}_3^{2\,-} \\ & \mathrm{Cathode:} & \frac{1}{2}\,\mathrm{O}_2 + \mathrm{CO}_2 + 2\,\mathrm{e}^- &\longrightarrow \mathrm{CO}_3^{2\,-} \end{array}$$

- Cathode porous NiO
- Anode porous Ni
- No need for expensive catalyst materials
- Molten alkali-metal carbonates are highly corrosive
  - Conductivity is also limited
- Ni electrodes are sensitive to sulfur contaminants



### Solid Oxide (SOFC)

- All solid state system (i.e. solid electrolyte)
- Two sub-groups
  - High-temperature (HT) SOFC: 800 1000 °C
  - Intermediate temperature (IT) SOFC: 500 700 °C
- Based around redox and conduction of O<sup>2</sup>-:

#### Cathode:

- The high temperature operation means that internal steam reforming occurs readily
  - a wide range of fuels can be used
- No precious metal catalysts are required
- Excess heat from exhaust gas can be used to increase efficiency (can reach ~90%)
  - e.g. drive a turbine to generate extra electricity
  - Combined heat and power (CHP)

### **SOFC Limitations**

#### High temperatures:

- Prevent rapid start/stop. SOFCs are limited to stationary power applications
- Cause problems in terms of reactivity between electrolyte and electrodes
- · Make sealing the cell difficult

There is a delicate balance between optimum temperature for redox and/or ionic conductivity, and issues with thermal expansion, reactivity and device construction

• Intermediate-temperature (IT) SOFCs are the current optimum.

### Requirements for SOFC materials

#### **Anode**

- High electronic conductivity
- High catalytic activity for fuel oxidation
- High ionic conductivity
- High stability under HT reducing conditions

Typically a cermet (*i.e.* mixture) of Ni and electrolyte

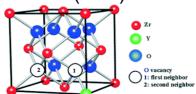
- Ni has high electronic conductivity and catalytic activity
- High ionic conductivity from electrolyte

#### **Electrolyte**

- High ionic conductivity
- Negligible electronic conductivity
- High stability in oxidising and reducing environments

#### e.g.

- $\begin{array}{cc} \bullet & \mathrm{Gd_{0.1}Ce_{0.9}O_{1.95}} \\ & \mathrm{(CGO)} \end{array}$
- $\begin{array}{cc} \bullet & Y_{0.15}Zr_{0.85}O_{1.925} \\ \text{(YSZ)} \end{array}$



#### Cathode

- High electronic conductivity
- High catalytic activity for O<sub>2</sub> reduction
- High ionic conductivity
- Stable in HT oxidising conditions
- $La_{1-x}Sr_xCoO_{3-y}$ : a good mixed conductor, but with high thermal expansion
- ullet La $_2{
  m NiO}_{4\,+{
  m x}}$ : an intersitial oxide ion conductor

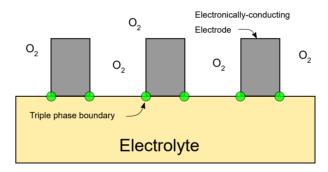
As well as: Chemical stability, similar thermal expansion, cost, ...

### Improving electrodes

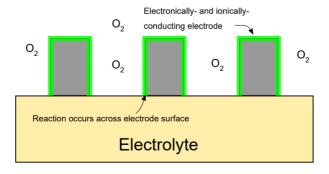
Ideally want a perfect mixed electronic/ionic conductor, with high chemical stability, high catalytic activity etc...

In reality, we can use a mixture of good (and chemically-stable) ionic and electronic conductors. Reactions will then occur at the **triple phase boundary** 

#### **Electronic Conductor**



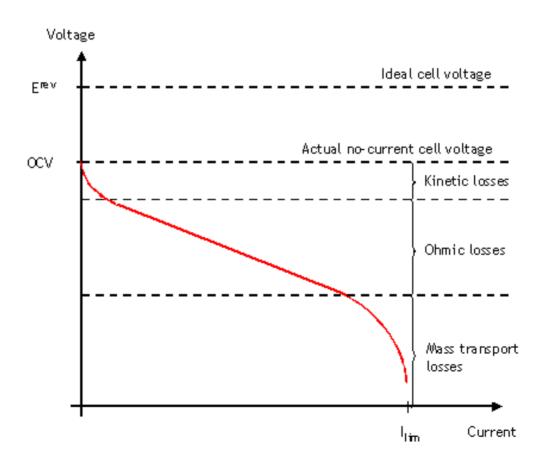
#### **Mixed conductor**



# Practical efficiency

We can calculate maximum thermodynamic efficiencies, but how do realistic efficiencies compare?

Like batteries, the obtainable voltage (and efficiency) depends on the current rate:

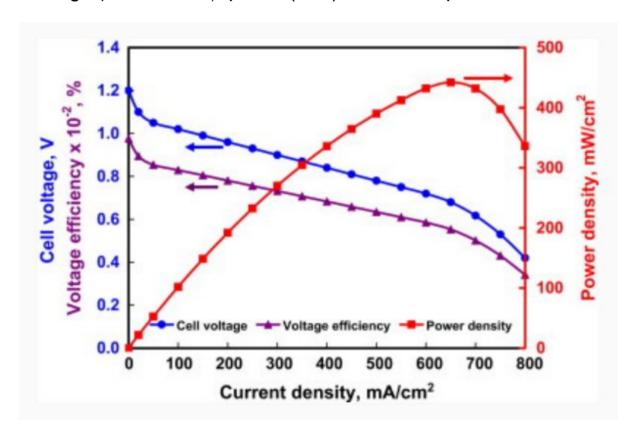


### Practical efficiency

- The difference between theoretical and **zero-current** voltage is due to issues such as small electronic conductivity of electrolyte and crossover of fuel
  - More pronounced for LT than HT cells
- At low currents, kinetic (or activation) losses cause a rapid drop in voltage
  - O<sub>2</sub> reduction is kinetically slow
  - Improved by higher temperatures or presence of catalysts
- At intermediate currents, **Ohmic losses** dominate
  - Caused by the resistance of ionic motion in the electrolyte
  - R constant with T, so voltage varies linearly with current (V = IR)
  - Major loss in both HT and LT cells
  - Can be decreased by thinner electrolyte layers
- At high currents, Mass transport causes rapid voltage drop
  - At high rates, the concentration of fuel and/or O<sub>2</sub> at the electrode surface gets depleted
  - Occurs for both HT and LT cells
  - Higher rates can be achieved by better controlling gas flow

### **Power limits**

Because voltage ↓ as current ↑, power (= IV) will show a peak:



Typically, these peak powers are lower than batteries

