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Industrial PID Controller Tuning

with a multi-objective framework using MATLAB®

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Contents

I	Intr	oductio	on	1
2	Ind	ustrial]	PID Control	3
	2.1		ol System Design Scenario	3
	2.2		rial Process Characteristics	3
		2.2.1	Controlled Process Model	3
	2.3	The P	ID Controller	3
		2.3.1	PID Controller formulations	3
		2.3.2	Reference Processing and 2-DoF PID	4
	2.4	Norma	alised Representations	4
		2.4.1	Process Model Normalisation	4
		2.4.2	Controller Normalisation	4
3	PID	Contr	oller Considerations	5
	3.1		ol System Evaluation Metrics	5
	0.1	3.1.1	Performance	5
		3.1.2	Robustness	5
		3.1.3	Input Usage	5
	3.2	Contro	ol System Tradeoffs	5
		3.2.1	Servo vs. Regulation	6
		3.2.2	Performance vs. Robustness	6
		3.2.3	Input vs. Output Disturbances	6
4	PID	Contr	oller Design	7
•	4.1		Controller Tuning	7
		4.1.1	Analytical Tuning Methods	7
		4.1.2	Tuning based on Minimisation of a Performance Criterions .	7
		4.1.3		7
	4.2		alization of PID tuning as a multiobjective optimization	,
	1.2		em	7
			Cost functions and constraints selection	

vi Contents

		4.2.2	PID tuning problem formulation for integral cost functions.	8
5	Mul	lti-obje	ctive optimization	9
	5.1		alization of the multi-objective optimization problem	9
		5.1.1	Definition of the Pareto front	9
		5.1.2	Different approaches to obtain the Pareto front	9
	5.2	Scalar	rization algorithms to find the Pareto front	9
		5.2.1	Weighted Sum	9
		5.2.2	Normal Boundary Intersection	10
		5.2.3	Normalized Normal Constraint	10
		5.2.4	Enhanced Normalized Normal Constraint	10
	5.3	Soluti	on selection from the Pareto front	10
6	PID	tuning	as a multi-objective optimization method	11
	6.1	Soluti	on of the multi-objective optimization tuning	11
	6.2	Viabil	ity for tuning rules	11
	6.3	Datab	ase approach for the final tuning	11
7	App	lication	n examples	13
	7.1	Comp	arison of different tuning methods from a multi-objective	
		frame		13
	7.2	High o	order benchmark plant	13
	7.3		O ₃ Thin Film Deposition Process	13
	7.4	Contin	nuous stirred tank reactor	13
	Refe	erences		15

Abbreviations

ENNC enhanced normalized normal constraint.

MOO multiobjective optimization.

MOOP multiobjective optimization problem.

NBI normal boundary intersection.NNC normalized normal constraint.PID proportional integral derivative.

WS weighted sum.

Chapter 1 Introduction

The design of control systems always has to consider multiple and possibly conflicting design objectives. Under this perspective, the task of the engineer in charge of the control system, becomes to find the optimal point of compromise within this set of distinct objectives [8].

The most used control algorithm in industry is the proportional integral derivative (PID). This type of algorithm is used in a wide variety of applications, due to its limited number of parameters, its ease of implementation and its robustness [2] and represents an area of active study since the first tuning methodology was proposed in the 1940s [20]. In the case of this particular project, in order to have a direct impact on the industry and the research community in process control systems, it will focus on the problem of the tuning of the parameters of controllers PID.

It is common that the problem of tuning the parameters of industrial controllers is posed as an optimization problem. When all the objectives need to be taken into account at the same time, this problem becomes a multivariate multiobjective optimization problem. In the particular case of industrial PID controllers, this problem is also non-lineal and (possibly) non convex, therefore, the problem at hand is not trivial.

Regardless of the methodology to be used, it is generally computationally expensive to solve a multiobjective optimization problem, which can lead to a scenario of multiple solutions equally optimal, so that in addition to solving the optimization problem, the control engineer, ends up with the extra responsibility of entering into a decision phase a posteriori to finally choose the best set of parameters for its specific application.

In this sense, multiobjective optimization (MOO) tuning of PID controllers remains as an open research subject, even though it has bee studied for several decades. For example, in [16] a type of MOO is used to tune PID controllers in a plastic injection molding process. In [1], an algorithm based on several optimizations is proposed to find the optimal parameters of a PID controller; this algorithm took into account several variables such as stationary error, rise time, overrun, settling time and maximum controller output within the feedback loop. More recently, bio-inspired techniques such as neural networks, fuzzy logic or genetic algorithms

2 1 Introduction

have been used to solve the optimization problem [14]. In [3], A Tabu search algorithm is used to tune PID controllers in real time, based in a set of closed loop specifications and a cost function. In [4] the multiobjective optimization problem (MOOP) for PID controllers is solved using the ant colony approach, this methodology tries to simulate the behavior of real ants when they are looking of the shortest path to a given objective.

Beside bio-inspired methods for MOOP, there are several methologies that transform the MOOP into a single function optimization problem, by rewriting the problem with extra constrains. The simplest method is the weighted sum (WS) [10]. With the WS method, the multiobjective cost function is transform in a one dimensional function using a weighted sum that give a greater relative weight to a function in comparison to the others. For each set of weight values a different optimal solution is found for the same problem. The set of all solutions is part of the Pareto front [10]. The Pareto front corresponds to all equally optimal solutions for a MOOP. The problem with the WS method is that, although the results obtained are from the Pareto front, it is not possible to satisfactorily construct the entire front [5, 11, 13].

In order to obtain the Pareto front correctly, other methodologies have emerged that surpass the WS. The normal boundary intersection (NBI) method [6] consist in rewriting the optimization problem so that the feasible area is shortened by an equality constraint that depends on an extra parameter. The solution of this new problem will terminate at the Pareto border and by varying this extra parameter, it is possible to find the Pareto front so that each found point is equally spaced at the front. This feature is very useful since it gives an overall idea of the shape of the front. NBI has been applied to the tuning of controllers in [7] where the controller is selected taking into account different performance indexes like the integral of the squared error (ISE), the integral time-weighted squared error (ITSE) and the integral of the squared time-weighted squared error (ISTSE). Other methodology similar to NBI is the normalized normal constraint (NNC) [12], which converts the MOOP in a single function optimization with an extra inequality constraint.

It should be noted that these methodologies have also been used in other areas apart from the control of industrial processes. A few examples of the areas in which it has been applied are: calculation of optimal power flow in power systems [15] and distributed generation planning [19], for the control of biochemical processes [9], circuit analysis [17], development of optimal supply strategies for the participants of oligopolistic energy markets [18].

Although in the area of process control, there are examples of the use of these algorithms [7], they do not take into account the different sources of disturbance to the system, but are different measures of performance to the same source of disturbance (the change in reference), and using a simple PID controller of a single degree of freedom.

Chapter 2 Industrial PID Control

2.1 Control Sy	zstem Design	Scenario
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To do

2.2 Industrial Process Characteristics

To do

2.2.1 Controlled Process Model

To do

2.3 The PID Controller

To do

2.3.1 PID Controller formulations

2.3.2 Reference Processing and 2-DoF PID

To do

2.4 Normalised Representations

To do

2.4.1 Process Model Normalisation

To do

2.4.2 Controller Normalisation

Chapter 3 PID Controller Considerations

3.1 Control System Evaluation Metrics
To do
3.1.1 Performance To do
3.1.2 Robustness
To do
3.1.3 Input Usage
To do
3.2 Control System Tradeoffs

3.2.1 Servo vs. Regulation

To do

3.2.2 Performance vs. Robustness

To do

3.2.3 Input vs. Output Disturbances

Chapter 4 PID Controller Design

4.1 PID Controller Tuning
To do
4.1.1 Analytical Tuning Methods
To do
4.1.2 Tuning based on Minimisation of a Performance Criterions
To do
4.1.3 Tuning Rules for Robustness
To do
4.2 Formalization of PID tuning as a multiobjective optimization

4.2.1 Cost functions and constraints selection

To do

4.2.2 PID tuning problem formulation for integral cost functions

Chapter 5

Multi-objective optimization

5.1 Formalization of the multi-objective optimization problem

To do

5.1.1 Definition of the Pareto front

To do

5.1.2 Different approaches to obtain the Pareto front

To do

5.2 Scalarization algorithms to find the Pareto front

5.2.1 Weighted Sum

To do WS methodology is a popular procedure to transform a MOOP into a single objective problem by creating a new objective function that is the result of the aggregation of all the functions involved with certain weight for each one [10]. For example, if the two objectives to optimize are $f_1(\mathbf{x})$ and $f_1(\mathbf{x})$, the new function is given by:

$$F_{WS}(\mathbf{x}) = \alpha_{1WS}\hat{f}_1(\mathbf{x}) + \alpha_{2WS}\hat{f}_2(\mathbf{x}), \tag{5.1}$$

with $\alpha_{1WS} + \alpha_{2WS} = 1$, and $\hat{f}_1(\mathbf{x})$ and $\hat{f}_2(\mathbf{x})$ the normalized versions of $f_1(\mathbf{x})$ and $f_2(\mathbf{x})$, respectively. One possible normalization (see [10]) is given by:

$$\hat{f}_1(\mathbf{x}) = \frac{f_1(\mathbf{x}) - \min(f_1(\mathbf{x}))}{\max(f_1(\mathbf{x})) - \min(f_1(\mathbf{x}))}.$$
(5.2)

With this normalization, the utopia point is moved to the origin and the maximum value of the new normalized function is 1.

The optimization problem then is written as:

$$\min_{\mathbf{x}} F_{WS}(\mathbf{x}),$$
s.t. $h(\mathbf{x}) = 0$,
$$g(\mathbf{x}) \le 0,$$
(5.3)

where $h(\mathbf{x})$ and $g(\mathbf{x})$ are the equality and inequality constraints of the original problem.

There are certain drawbacks with this approach. In first place, when (5.1) is minimized for different values of α_{1WS} and α_{2WS} in order to obtain the Pareto front, an even distribution of the weights does not assure an even distribution of the points in the front. Also, with WS it is not possible to obtain Pareto points in the non-convex region of the front, and therefore, not all the possible solutions can be found [5].

5.2.2 Normal Boundary Intersection

To do

5.2.3 Normalized Normal Constraint

To do

5.2.4 Enhanced Normalized Normal Constraint

To do

5.3 Solution selection from the Pareto front

Chapter 6 PID tuning as a multi-objective optimization method

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U. I	Dolumon	OI.	uit	IIIUIUI-	VV.		Opun	IILU	HUH	tuillie

To do

6.2 Viability for tuning rules

To do

6.3 Database approach for the final tuning

Chapter 7 Application examples

7.1 Comparison of different tuning methods from a multi-objective frame

La idea acá es comparar algunos métodos y ver cómo terminan puestos en el Pareto

7.2 High order benchmark plant

To do

7.3 LiTaO₃ Thin Film Deposition Process

To do

7.4 Continuous stirred tank reactor

References 15

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