Chapter 6::Chemical equilibrium

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March 13, 2023

Gibbs energy

Abstract

We would like to determine the spontaneity of a reaction mixture to approach equilibrium, along with deriving the thermodynamic equilibrium constant K_p and equilibrium concentrations of reactants and products in a mixture of reactive ideal gases. We define Gibbs energy (ΔG) , which expresses spontaneity in terms of properties of the system alone.

Suppose we have an arbitrary system σ in thermal equilibrium with the surroundings. What determines the directions of a spontaneous change? Well, it would be the tendency of a system to minimize energy.

$$-dq_{\sigma} = dq_{surr} \implies dS_{\Omega} + dS_{surr} \ge 0 \implies dS_{\sigma} + \frac{dq_{surr}}{T} \ge 0$$

Definition

$$\Delta G_{\sigma} = \Delta H_{\sigma} - T\Delta S_{\sigma} \implies dG_{\sigma} = dH_{\sigma} - TdS_{\sigma}$$

If we graph this relation, we notice that ΔG is a function of T. ΔH would be ΔG_0 and the slope would be ΔS .

Gibbs energy holds the following properties::

- $\Delta G < 0 \implies \sigma \equiv spont \implies exergonic$
- $\Delta G > 0 \implies \sigma \equiv \neg spont \implies endergonic$
- Gibbs energy is an extensive property, and is a state function.

When a problem concerns Gibbs energy, we only care about **what happens in** the system, not the surroundings.

Differential forms of U, H, and G

For an infinitessimal process::

$$G = H + TS \implies dG = dH - TdS - SdT$$

According to the first law::

$$dH = dU + PdV + VdP \implies dU = dq + dw \implies dU = dq - PdV$$

For a reversible process::

$$dq_{rev} = TdS, dU = TdS - PdV$$

So,

$$dH = TdS + VdP, dG = VdP - SdT, dU = TdS - PdV$$

This only applies for **expansion** work.

Example

Calculate the maximum nonexpansion work that can be gained from the combustion of benzene (l) and of H_2 (g) on a per gram and a per mole basis under standard conditions. Is it apparent from this calculation why fuel cells based on hydrogen oxidation are under development for mobile applications? Thermodynamic values available in appendix.

$$R: C_6H_6(l) + O_2(g) \rightarrow 6CO_2(g) + 3H_2O(l)$$

To calculate maximum nonexpansion work, simply calculate ΔG

$$\Delta G = 3\Delta G(H_2O, l) + 6\Delta G(CO_2, g) - \Delta G(G_6H_6, l) \approx 3202.2kJ$$

The above value is per mole, so we need to multiply by molar mass $(\frac{1mol}{78.18g})$. In the end, we get $-40.99 \frac{kJ}{g}$ For formation of water, we have that

$$\Delta G = \Delta G(H_2O, l) = -237.1kJmol^{-1} \implies -237.1kJmol^{-1} \left(\frac{1mol}{2g}\right) = -117.6kJg^{-1}$$

Helmholtz energy and spontaneity

This property is derived for processes occurring at $V \equiv const \wedge T \equiv const$. We use A to represent the quantity.

$$A = U - TS$$

Gibbs free energy gives maximum nonexpansion work, whereas Helmholtz energy gives maximum overall work.

Exact differentials and Maxwell relations

Take a function z = f(x, y) where dz = M(x, y)dx + N(x, y)dyRecall that by Euler's theorem, a function is a state function if and only if::

$$\left(\frac{\partial M}{\partial y}\right)_{x} = \left(\frac{\partial N}{\partial x}\right)_{y}$$

The total differentials for U(S, V), H(S, P), G(T, P) can be modelled as follows::

$$dU = TdS - PdV = \frac{\partial U}{\partial S}dS + \frac{\partial U}{\partial V}dV | T = \frac{\partial U}{\partial S}, -P = \frac{\partial U}{\partial V}$$

$$dH = TdS + VdP = \frac{\partial H}{\partial S}dS + \frac{\partial H}{\partial P}dP|T = \frac{\partial H}{\partial S}, V = \frac{\partial H}{\partial P}$$

$$dG = -SdT + VdP = \frac{\partial G}{\partial T}dT + \frac{\partial G}{\partial P}dP - S = \frac{\partial G}{\partial T}, V = \frac{\partial G}{\partial P}$$

Because dU is an exact differential,

$$\frac{\partial}{\partial V} \left(\frac{\partial U(S, V)}{\partial S} \right) = \frac{\partial}{\partial S} \left(\frac{\partial U(S, V)}{\partial V} \right)$$

It would follow that::

$$\frac{\partial T}{\partial V} = -\frac{\partial V}{\partial S}$$

Example

Derive the maxwell relation $\left(\frac{\partial T}{\partial V}\right)_S = -\left(\frac{\partial P}{\partial S}\right)_V$ Because S and V are constant, we can use the exact differential::

$$dU = TdS - PdV$$

Now we can form the mixed derivative::

$$\left(\frac{\partial}{\partial V} \left(\frac{\partial U(S,V)}{\partial S}\right)_{V}\right)_{S} = \left(\frac{\partial}{\partial S} \left(\frac{\partial U(S,V)}{\partial V}\right)_{S}\right)_{V}$$

Substituting dU = TdS - PdV, we have that

$$\left(\frac{\partial}{\partial V} \left(\frac{\partial \left[TdS - PdV\right]}{\partial S}\right)_{V}\right)_{S} = \left(\frac{\partial}{\partial S} \left(\frac{\partial \left[TdS - PdV\right]}{\partial V}\right)_{S}\right)_{V}$$

After simplifying, we can conclude that

$$\left(\frac{\partial T}{\partial V}\right)_S = -\left(\frac{\partial P}{\partial S}\right)_V \blacksquare$$

Dependence of ΔG on T

Recall that dG = VdP - SdT. At $P \equiv const, dG = -SdT$. When $P \equiv const$, it also follows that

$$\frac{\partial G}{\partial T} = -S, S \ge 0$$

So it would follow that Gibbs energy decreases as energy increases.

The Gibbs-Helmholtz equation states that for a finite process,

$$\frac{\partial \left(\frac{\Delta G}{T}\right)}{T} = -\frac{\Delta H}{T^2}$$

Assume that $\Delta H \wedge \Delta S$ are independent of T and that P = 1atm. We can integrate both sides of the equation to give us that

$$\int d\left(\frac{\Delta G}{T}\right) = \int \Delta H d\frac{1}{T}$$

$$\frac{\Delta G(T)}{T} - \frac{\Delta G(298)}{298} \approxeq \left(\frac{1}{T} - \frac{1}{298}\right) \Delta H(298)$$

So in the end, we have that the Gibbs-Helmholtz equation can be approximated as::

$$\frac{\Delta G(T_2)}{T_2} - \frac{\Delta G(T_1)}{T_1} \approxeq \left(\frac{1}{T_2} - \frac{1}{T_1}\right) \Delta H(T_1)$$

Dependence of ΔG on P

Recall that dG = VdP - SdT, then at $T \equiv const$, we have that $dG = VdP \implies \frac{\partial G}{\partial P} = V$.

We model dependence of ΔG on P as follows::

$$\Delta G = \int_{1}^{2} dG = G_{2} - G - 1 = \int_{P_{1}}^{P_{2}} V dP$$

If $V \equiv const$ and the process concerns liquids and solids, we have that::

$$\Delta G = G(P_2) - G(P_1) = V(P_2 - P_2)$$

For $g \in \mathbb{C}$, we have that::

$$\Delta G = G_2 - G_1 = \int_{P_1}^{P_2} \frac{nRT}{P} dP = nRT \ln \left(\frac{P_2}{P_1}\right)$$

Now set $P_1 = 1bar$ and set $P_2 = P$, therefore,

$$G = G^{\circ} + nRTln(P) \implies \bar{G} = \bar{G}^{\circ} + RT\ln(P)$$

If $\forall products, reactants \in \sigma((products \equiv ((s) \lor (l))) \lor (reactants \equiv ((s) \lor (l))))$, then

$$\Delta G = G(P_2) - G(P_1) = V(P_2 - P_1) = V\Delta P$$

This is not very important, since we can just ignore the quantity altogether.

However, if $\exists product \lor reactant \in \sigma(product \lor reactant \equiv (g))$, then the volume of solids and liquids is ignored, and::

$$\Delta G = G(P_2) - G(P_1) = \Delta nRT \ln \left(\frac{P_2}{P_1}\right)$$

Hess's law for Gibbs energy

It's the same thing as enthalpy.

Example

For the synthesis of urea::

$$R: CO_2(g) + 2NH_3(g) \to (NH_2)_2CO(s) + H_2O(l)$$

- a) Calculate $\Delta_r G$ for the reaction at 298K and 1bar (Ans: -6.8kJ)
- b) Assume $q \in \mathbb{C}$, calculate $\Delta_r G$ at P = 10bar.

To calculate $\Delta G(10bar)$, we can plug in the values into the equation we derived.

$$\Delta G(10bar) = \Delta G(1bar) + \Delta nRT \ln \left(\frac{P_2}{P_1}\right)$$

$$= (6800 J mol^{-1}) + (-3)(8.314 J K^{-1} mol^{-1})(298 K) (\ln \left(\frac{10}{1}\right) = -23.9 k J mol^{-1})$$

So it would suffice to say that a reaction at higher pressure is **more spontaneous** than at lower pressure.

Haber process