

# Proposal 20180741

Title
Revealing the water redistribution dynamics in PEFC gas diffusion layers during load changes

Abstract
Automotive application requires highly dynamic and efficient operation of polymer electrolyte fuel cells (PEFCs). The short-term load changes lead to fast changes of the liquid saturation in the gas diffusion layers (GDL) which are so far not fully understood. Operando X-ray tomographic microscopy (XTM) with 0.4 ~ 0.8 s acquisition time is required to reveal and understand the water redistribution dynamics in the opaque GDL structures and associate them with efficiency losses.

Proposer / Spokesperson
<b>Mr. Hong Xu</b> Allgemeine Energie (ENE), Paul Scherrer Institut hong.xu@psi.ch

Principal investigator
<b>Dr. Jens Eller</b> Allgemeine Energie (ENE), Paul Scherrer Institut

Co-Proposer
<b>Dr. Felix N Buechi</b> Allgemeine Energie (ENE), Paul Scherrer Institut
<b>Mrs. Minna Bührer</b> Photon Science (PSD), Paul Scherrer Institut

Experiment Category	
Experiment Type	Normal
Research Area	Catalytic Materials/Surface Science

Experiment Requirements	
Eligible for EU Support	No
Number of Shifts Required	6
Schedule Preferences	Nov/Dec
Beamline/Station	TOMCAT

Links to related proposals of relevance to the current proposal		
Proposal	Title/Proposer/Infos given by the proposer about the relation	Report
20170876	<p>Title: Water feature detectability in subsecond XTM of gas diffusion layer of PEFC</p> <p>Proposer: Dr. Jens Eller</p> <p>Infos: During this campaign, water feature detectability under different imaging parameters will be quantified and guide the imaging conditions for operando experiments proposed in this proposal.</p>	<a href="#">Available</a>
20171538	<p>Title: Fundamental understanding of dominating water transport mode in PEFC gas diffusion layers</p> <p>Proposer: Dr. Jens Eller</p> <p>Infos: Operando X-ray tomographic microscopy with 1-2s acquisition time is required to capture the water distribution in the opaque GDL structures dynamically and to conclude on the dominating water transport mode.</p>	<a href="#">Available</a>

**A. Goal of the experiment**

The automotive application of polymer electrolyte fuel cells (PEFCs) requires a highly dynamic response of fuel cell power to fulfill the requirements of real world driving cycles. This includes load changes  $> 50\%$  of the maximum fuel cell power within a few seconds or even less than a second, while maintaining high system and fuel efficiency, especially during fuel cell startup and vehicle acceleration. Therefore the goal of the proposed experiment is to achieve fundamental insight into the dynamics of the water redistribution in the porous gas diffusion layer (GDL) in PEFCs under transient operating conditions due to fast load changes.

**B. Background**

Hydrogen fed polymer electrolyte fuel cells (PEFC) are expected to play a major role in a future decarbonized energy system [1], especially in the mobility sector where most of the major car manufactures have fuel cell electric vehicles under development. Today, water management is a major limiting factor in PEFC for further increasing power density [2]. Inside the PEFC, the water management is complex: on one hand, the membrane needs a certain hydration state in order to ensure sufficient proton conductivity; on the other hand, excessive water leads to blocked gas pathways in the porous structures with increased mass transport losses (see Fig. 1) [3]. These flooding effects can dramatically decrease the accessibility of oxygen, resulting in mass transport limitations that prevent high current density operation which is necessary for high power automotive applications. Moreover, the transient response of water distribution in PEFCs is an important criterion in their application to automotive systems during start-up, acceleration and deceleration.

So far the dynamics of water removal from the GDL into the gas flow channel have been studied mainly by X-ray and neutron radiography, with limited insight into the detailed two phase transport processes in the porous layers. Operando X-ray tomographic imaging has become a very important tool to quantify the pore-scale water distribution in the GDL under realistic, but static operation conditions [4] (to due scan times around 10 s, see Fig. 2) and to link the micro-structural features to gas transport limitations [5]. Recent developments to decrease scan times towards 1 s and below (see Fig. 3) [6] have paved the way to study the dynamics of water redistribution in PEFCs with a verified and well characterized imaging pipeline [7] (see Fig. 4), and attracted a major car manufacturer for successful industry beamtime campaign with the proposer's setup in 2017.

**C. Experimental method; specific requirements**

Synchrotron radiation based X-ray tomographic microscopy is required to resolve the fine and opaque fiber structure of the GDL ( $\sim 7\text{ }\mu\text{m}$  fiber diameter) and track the transient water redistribution processes in PEFCs. The fuel cell set-up for operando XTM (see Fig. 5) was developed and exploited during previous campaigns (20090986, 20100287, 20100818, 20110297, 20120161, 20170719, 20170918) will be used. It allows precise control of fuel cell operation conditions, eg. in-let gas humidity and cell temperature. It will be upgraded with heated fluid slip rings to allow for continuous cell rotation and consecutive scans with no delay.

XTM scans with 13.5 keV monochromatic beam energy with voxel size of  $\leq 3\text{ }\mu\text{m}$  and scan times around 0.4 - 0.8 s are needed to capture the dynamics of liquid water during operando XTM experiments. With the ongoing upgrade of a high numerical

aperture 4x - microscope at TOMCAT, detectability of water structures  $\geq 80\%$  can be expected at such scan times (see Fig. 4, explained in exp. report 20170876). With shorter scan time also the dose to the cell per scan will reduce, allowing in total 40 - 80 scans per cell, distributed over a period of 1 - 2 minutes during and after the load change.

Cells will be scanned and operated at  $60^{\circ}\text{C}$  during load changes from moderate ( $0.2 \text{ A/cm}^2$ ) to high load ( $1.5 \text{ A/cm}^2$ ) with different feed gas saturations (50, 110 % rH) to mimic different local conditions in large cells. Two GDL samples with different pore structures from different manufacturers (SGL, Toray) will be examined.

#### **D. Results expected**

The 4D operando XTM data collected during current density variations with scan times around 0.4 - 0.8 s will improve the constitutive understanding of water dynamics in porous GDL materials. It will enable insights into dynamic pore filling processes, the stability of liquid water transport paths including Haines-jumps and ganglion dynamics between different water clusters, as well as droplet detachment dynamics on the GDL surface and their influence on bulk GDL saturation. The insights are of vital importance to reduce educt gas mass transport limitations due to overwhelming accumulation of liquid water in the porous GDL, to provide verified structure-transport property relationships to the PEFC community, to verify transient two-phase PEFC microstructure resolving models based on Lattice-Boltzmann and Volume-of-Fluid codes, and ultimately to guide future material developments.

#### **E. Estimate and justification of the beamtime**

XTM scans of cells with two different GDL samples (SGL, Toray) at two in-let gas relative humidity levels with two repetitions of each condition for statistical evidence will be acquired for 8 cells (= 2 mat. \* 2 rH \* 2 rep.). The estimated average test-time for one cell is 5 h in total (incl. mounting, preconditioning, XTM imaging at load change, and acquisition of dry cell reference scan). Together with fuel cell test bench set-up (4 h per campaign) and beamline setup (2 h) for 8 cells tested, a total time of 46 h (4 h + 2 h + 8 \* 5 h) is required. Therefore, we apply for a total of 6 shifts (48 h).

#### **F. References relevant to the experiment description**

- [1] IEA; Advanced Fuel Cells Implementing Agreement Annual Report (2009).
- [2] D. Hayashi, A. Ida, S. Magome, T. Suzuki, S. Yamaguchi, R. Hori, SAE Technical Paper 01-1188 (2017).
- [3] J. Owejan, J. Gagliardo, J. Sergi, S. Kandlikar, T. Trabold, Int. J. Hydrogen Energy, 34, 3436-3444 (2009).
- [4] J. Eller, J. Roth, F. Marone, M. Stampanoni, F.N. Buechi, J. Electrochem. Soc. 164 (2), F115-F126 (2017).
- [5] J. Eller, T. Rosén, F. Marone, M. Stampanoni, A. Wokaun, F. N. Büchi, J. Electrochem. Soc. 158 (8), B963-B970 (2011).
- [6] J. Eller, F. Marone, F. N. Büchi, ECS Trans. 69(17), 523–531 (2015).
- [7] H. Xu, M. Bührer, F. Marone, T. J. Schmidt, F. N. Büchi, J. Eller, ECS Trans. 80(8), 395-402 (2017).

### **SLS related publications of the proposers (within the last 18 months)**

- [1] S. Mueller, J. Eller, M. Ebner, C. Burns, J. Dahn, V. Wood; Quantifying Inhomogeneity of Lithium Ion Battery Electrodes and Its Influence on Electrochemical Performance; J. Electrochem. Soc. 165(2), A339-A344 (2018).
- [2] H. Xu, M. Bührer, F. Marone, T. J. Schmidt, F. N. Büchi, J. Eller; Fighting the Noise: Towards the Limits of Subsecond X-ray Tomographic Microscopy of PEFC, ECS Trans. 80(8), 395-402(2017).
- [3] K. B. Hatzell, J. Eller, S. L. Morelly, M. H. Tang, N. J. Alvarez, Y. Gogotsi; Direct observation of active material interactions in flowable electrodes using X-ray tomography; Faraday Discuss., 199, 511-524 (2017).
- [4] M. A. Safi, N. I. Prasianakis, J. Mantzaras, A. Lamibrac, F. N. Buechi; Experimental and pore-level numerical investigation of water evaporation in gas diffusion layers of polymer electrolyte fuel cells; Int. J. Heat. Mass Transfer, 115 (A), P238-P249 (2017).
- [5] J. Eller, J. Roth, F. Marone, M. Stampanoni, F.N. Buechi; Operando properties of gas diffusion layers: Saturation and liquid permeability; J. Electrochem. Soc. 164 (2), F115-F126 (2017).
- [6] I. V. Zenyuk, A. Lamibrac, J. Eller, D. Y. Parkinson, F. Marone, F. N. Buechi and Adam Z. Weber; Investigating Evaporation in Gas Diffusion Layers for Fuel Cells with X-ray Computed Tomography; J. Phys. Chem. C, 120 (50), F28701–F28711 (2016).
- [7] T. Agaesse, A. Lamibrac, F. N. Buechi, J. Pauchet, M. Prat; Validation of pore network simulations of ex-situ water distributions in a gas diffusion layer of proton exchange membrane fuel cells with X-ray tomographic images; J. Power Sources, 331, 462-474 (2016).
- [8] P. Pietsch, D. Westhoff, J. Feinauer, J. Eller, F. Marone, M. Stampanoni, V. Schmidt and V. Wood; Quantifying microstructural dynamics and electrochemical activity of graphite and silicon-graphite lithium-ion battery anodes; Nature Communications, 7, 12909 (2016)

### **Other publications of the proposers (within the last 18 months)**

- [1] M. Suermann, K. Takanoashi, A. Lamibrac, T. J. Schmidt, F. N. Buechi; Influence of Operating Conditions and Material Properties on the Mass Transport Losses of Polymer Electrolyte Water Electrolysis; J. Electrochem. Soc. 164 (9), F973-F980 (2017).
- [2] M. Suermann, T. Kiupel, T. J. Schmidt, F. N. Buechi; Electrochemical Hydrogen Compression: Efficient Pressurization Concept Derived from an Energetic Evaluation; J. Electrochem. Soc., 164 (12), F1187-F1195 (2017).
- [3] M. Suermann, A. Patru, T. J. Schmidt, F. N. Buechi; High pressure polymer electrolyte water electrolysis: Test bench development and electrochemical analysis; Int. J. Hydrogen Energy, 42(17), P12076-P12086 (2017).
- [4] U. Babic, M. Suermann, F. N. Buechi, L. Gubler, T. J. Schmidt; Critical Review—Identifying Critical Gaps for Polymer Electrolyte Water Electrolysis Development; J. Electrochem. Soc. 164 (4), F387-F399 (2017).
- [5] L. Holzer, O. Pecho, J. Schumacher, Ph. Marmet, O. Stenzel, F.N. Buechi, A. Lamibrac, B. Muench; Microstructure-property relationships in a gas diffusion layer (GDL) for Polymer Electrolyte Fuel Cells, Part I: effect of compression and anisotropy of dry GDL; Electrochimica Acta, 227 F419-434 (2017).

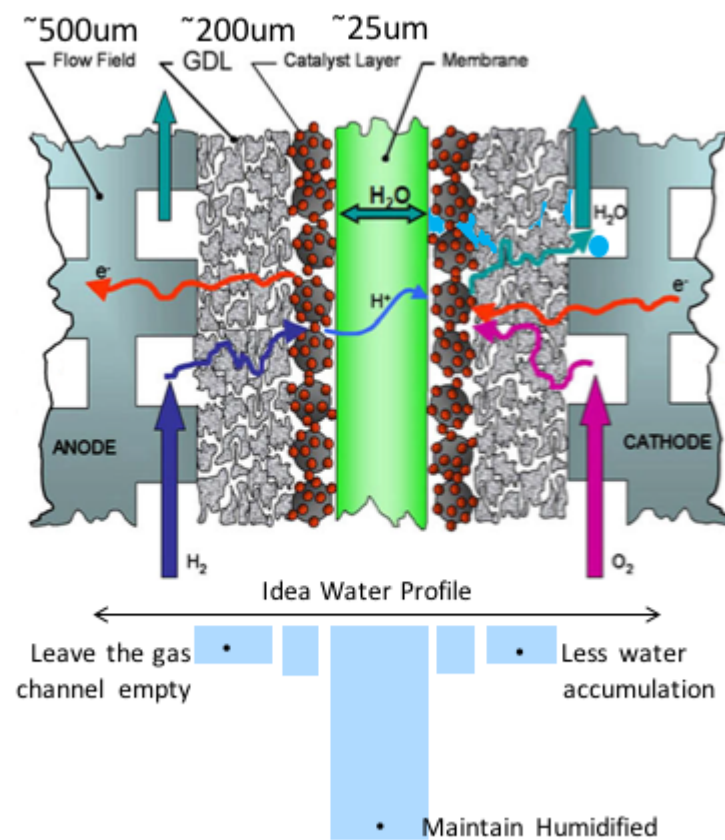
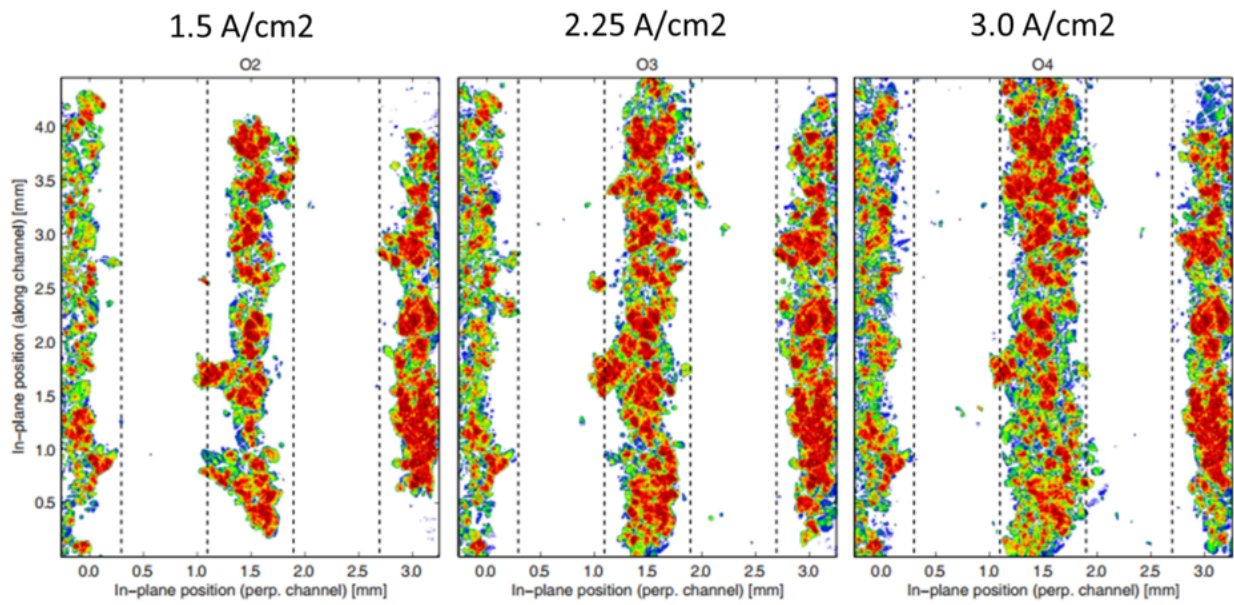


Figure 1: PEFC schematic [3] and the ideal water management profile

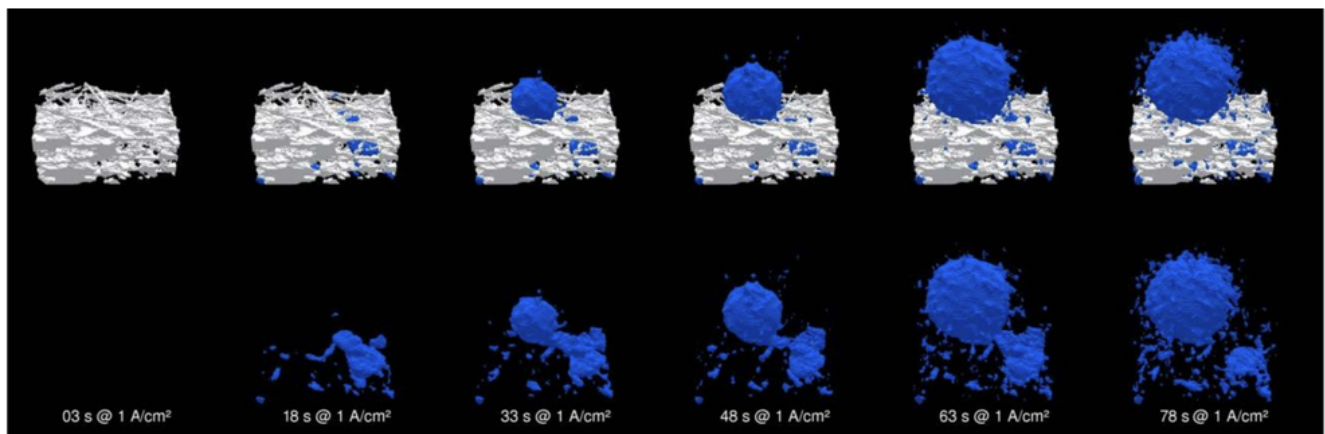


**Figure 5.** 2D projection of the liquid water volume fraction in the analyzed 90  $\mu\text{m}$  thick GDL domain in through-plane direction; black dashed lines indicate the edges of the flow field ribs/channels.

Figure 2: Static water distribution at different current densities [4]



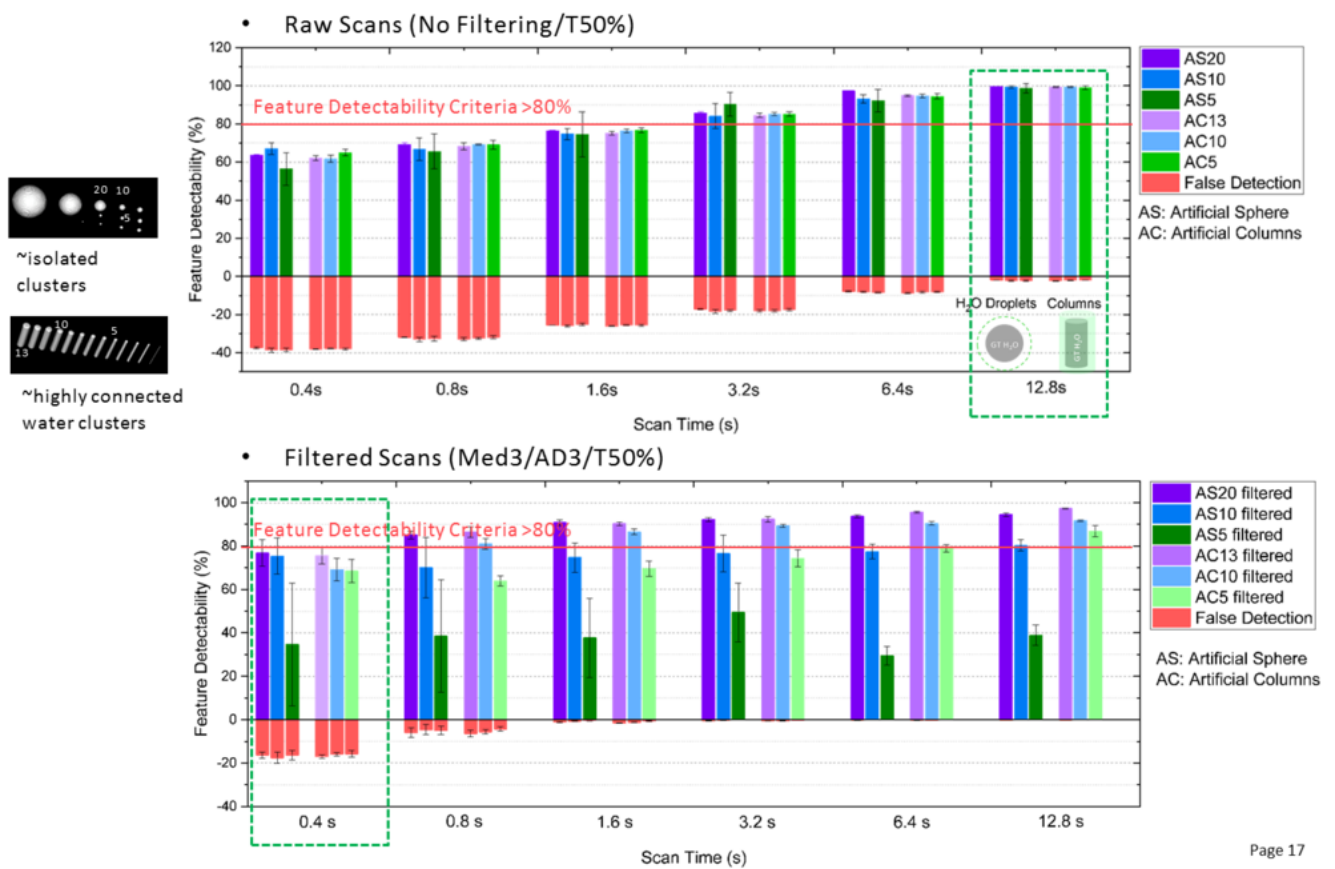
Proof of principle XTM study (0.76s scan time) on water redistribution during PEFC startup with simplified cell and non-realistic operation conditions.



- Surface rendering of the liquid water for selected scans. In the top row, the liquid water is shown together with the solid GDL, while the GDL is not shown in the bottom row; droplet is not removed due to low gas speed (approx. 0.8 m/s).

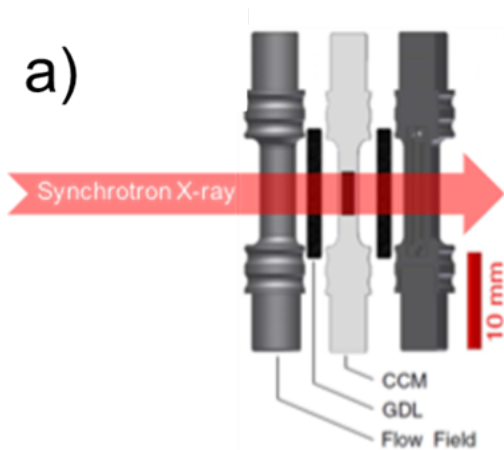
Figure 3: Preliminary operando subsecond XTM experiment [6]





Water feature detectability analysis developed for proposal 20170876

Figure 4: Water feature detectability analysis for different XTM scan time



- Schematic of XTM PEFC components.

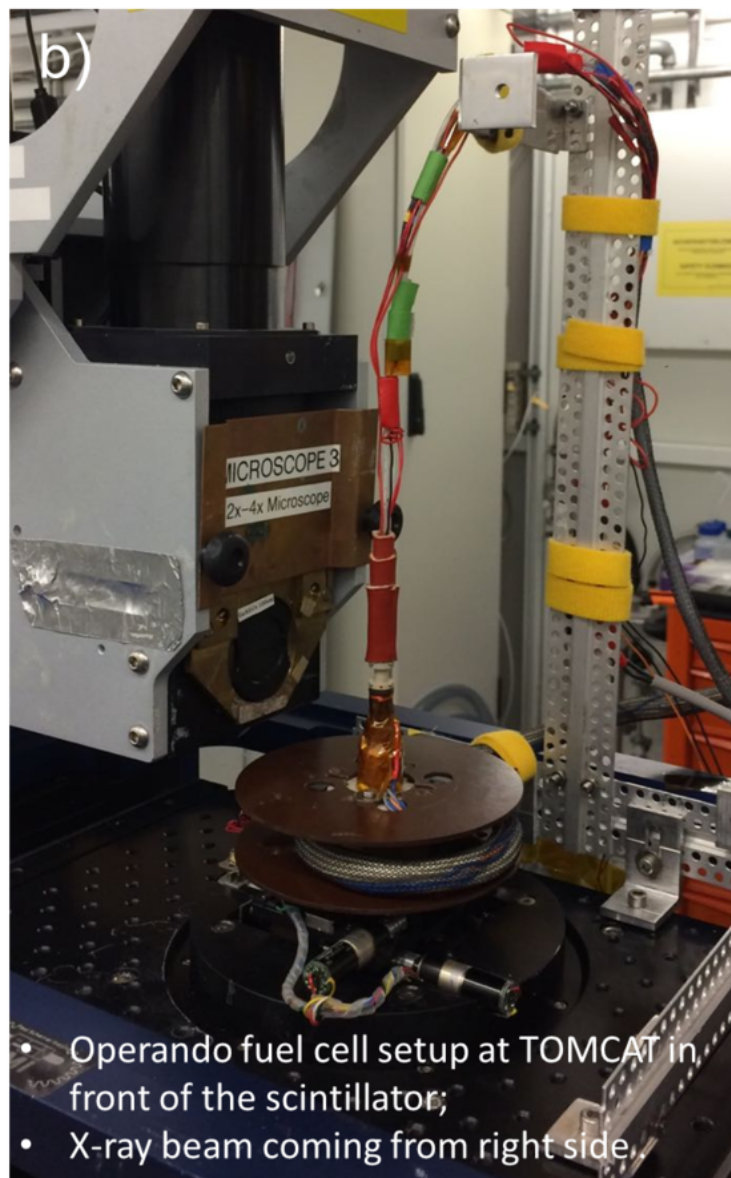


Figure 5: Operando PEFC setup for XTM imaging at TOMCAT

# Sample

Sample #1

Sample and chemical substance to be used in this experiment	
Substance	Carbon fiber; Platinum contained catalyst
Chemical formula	Carbon fiber paper surface-treated with PTFE or FEP; Platinum contained catalyst.
Structure	Multilayer
Size X	5
Size Y	5
Size Z	0.2
Mass	1.6
Container	Vespel cell
High purity	No
After the experiment the sample will be	Removed by user
No ethical issues declared on this sample.	

Sample environment	
Cryojet [K]	270-370
Hotair blower	No
High voltage	No
High pressure	No
High temperature	No
Magnetic field	No
Cryogenic liquid	No
Be window	No

Safety aspects	
<i>Chemical hazards</i>	
Chemical hazards	Gases (CO, H <sub>2</sub> , N <sub>2</sub> , O <sub>2</sub> , CO <sub>2</sub> , noble gases, others) Reactive chemicals
Specification of chemical hazards	In the setup for running the fuel cell, the sample is overflowed with synthetic air and hydrogen with low gas flow up to 200ml/min
Exhaust disposal conditions	The exhausted gas (air and H <sub>2</sub> ) will be first diluted with N <sub>2</sub> and then disposal through TOMCAT exhaust gas pipeline. The disposal gas-diluting set-up has been developed in previous beamtime.

## Experimental Report

### Water feature detectability in subsecond XTM of gas diffusion layer of PEFC

Hong Xu, Minna Bührer, Jens Eller

(Proposal 20170876)

#### Overview

The scheduled beamtime on 18<sup>th</sup> Sept 2017 was dedicated to study the influences by decreasing the XTM scan time towards 0.1 s, which paves the way for 4D XTM imaging of the transient water distribution in the gas diffusion layer (GDL) during polymer electrolyte fuel cell (PEFC) operation. Variations of different imaging parameters (beam energy, scan time) are presented and their consequences on the Contrast-to-Noise (CNR) ratio and further on the detectability of the micro-structural water features are discussed.

#### Quality of measurement/data

Followed by the proposed experiment in proposal 20170876, XTM scans for a cathode water filled channel fuel cell were collected at four monochromatic beam energy levels (11 keV, 13.5 keV, 16 keV, 18.5 keV) and polychromatic beam energy with variation of scan time from 12.8s to 0.1s. Several high quality scans were taken between the group of scans for the quality checking and comparison. The reconstructed images with missing pixels mask and ring removal were sufficient for post processing and quantification.

#### Status and progress of evaluation

The data collected at monochromatic beam energy levels are fully reconstructed and processed as presented in the results part. For polychromatic beam data, it is still under optimization of water feature detectability by different reconstruction algorithms. The complete evaluation will be expected to finish before next scheduled beamtime.

#### Results

In order to improve the image quality towards subsecond X-ray tomographic microscopy, it is vital to understand the influence of imaging conditions on the image quality. The CNR(H<sub>2</sub>O/Void) was studied for monochromatic beam energies between 11 keV and 18.5 keV with tomographic scan times ranging from 12.8 s to 0.1 s, which approaches the hardware limitation of image acquisition time 0.05 s at the TOMCAT beamline. The consequences of the time reduction for tomographic scans are shown qualitatively in Figure 1. While the void flow field channels remain visible down to a scan time of 0.1 s in the through-plane slices, the GDL structures can be only seen until 0.8 s scan time in the in-plane view. Some fiber structures are already lost at a scan time of 1.6 s.

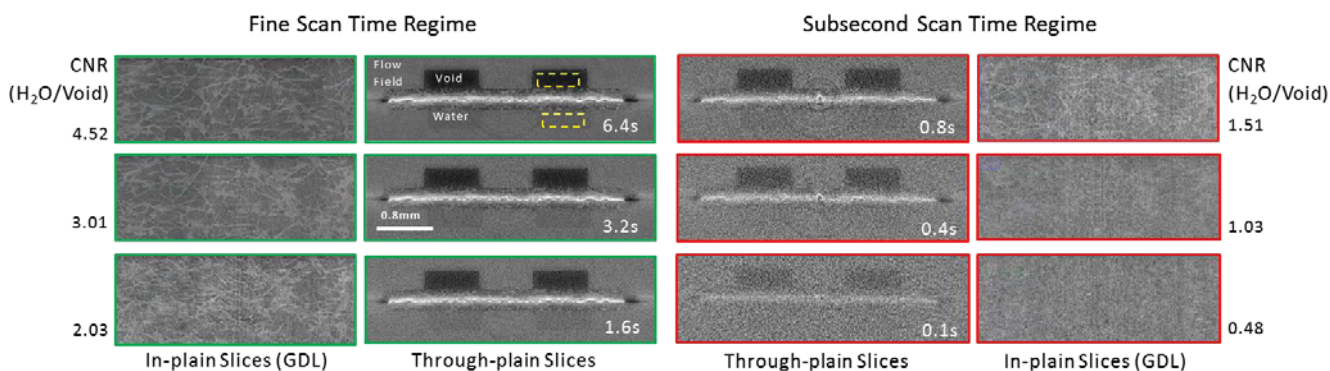


Figure 1: Tomographic in-plane slice and through-plane slice for different tomographic scan times (6.4 s, 3.2 s, 1.6 s, 0.8 s, 0.4 s, 0.1 s) at 13.5 keV; the yellow dashed rectangulars indicate the sampling domains for CNR calculation. The CNR was defined as  $CNR(H_2O/Void) = \frac{\text{mean}(H_2O) - \text{mean}(Void)}{\sqrt{[\text{StdDev}(H_2O)]^2 + [\text{StdDev}(Void)]^2}} / 2$ .

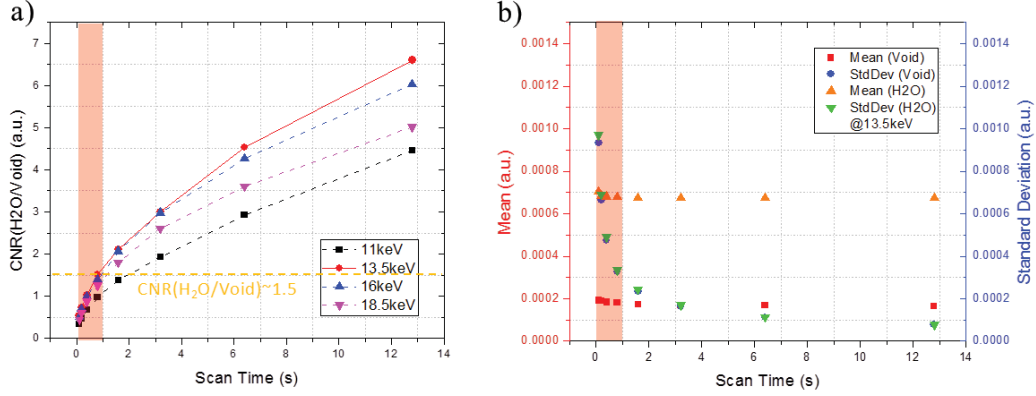


Figure 2: a) Contrast-to-noise ratio between water and void domains for different tomographic scan times at energy levels between 11 keV and 18.5 keV; b) Mean and standard deviation of the H<sub>2</sub>O and void domains versus scan time at 13.5 keV; the red area in plot a) and b) indicates the subsecond scan time regime.

At an energy level of 13.5 keV the CNR(H<sub>2</sub>O/Void) is the highest for all scan settings (see Figure 2 a). At the lowest energy of 11 keV the X-ray flux and the transmission are lowest and therefore the CNR is smallest for the all scan settings. The reduction of CNR for energies above 13.5 keV is due to the decreasing of the attenuation coefficient of water. For subsecond scan times below 0.8 s the CNR(H<sub>2</sub>O/Void) reduces to below 1.5, which challenges the segmentation of the liquid water in the cell. To reveal the reason behind this, a detailed analysis of the contributions of mean and standard deviation levels to the CNR at 13.5 keV is shown in Figure 2 b. The mean gray scale value of both H<sub>2</sub>O and void domain remains stable, as the attenuation coefficients are not affected by the scan time. The standard deviations increase as the scan time decreases, especially in the subsecond scan time regime, with similar values for the water and void domains. When the scan time reduces to 0.5 s and below, the standard deviations are almost the same as the mean level of the H<sub>2</sub>O domain, and as the noise level reaches the signal level the CNR drops below 1.

The low CNR requires appropriate image denoising before segmentation in order to increase the detection level of the true water domains and to minimize the amount of falsely assigned water domains. Median filter (13) and anisotropic diffusion filter (14) are applied to reduce noise while preserving the edges of the water boundaries. The influence of the number of iterations of the anisotropic diffusion (AD) filter was analyzed for the noise level of 1.6 s scan time. When increasing the number of iterations, the noise in the background decreases (see Figure 3 c). The CNR between water domain and background increases from 2.2 (no AD iteration) to 7.7 (5 AD iterations), which exceeds even the CNR(H<sub>2</sub>O/Void) of a 12.8 s scan. This leads to reduction of the falsely segmented water from almost 12 % (no AD iteration) below 1 % (5 AD iterations). The drawback of the strong filtering is a loss of feature detectability which starts already for sphere with a diameter of 10 pixels and cylinder with a diameter of 9 pixels. For larger diameter structures, the anisotropic diffusion filter increases the feature detectability. At cylinder diameters of 5-7 pixels the 5 AD iterations prior to segmentation start to show clearly lower feature detectability levels compared to fewer iterations. This effect becomes more pronounced for even smaller features. 1 pixel diameter cylinders are completely removed by 5 AD iterations, while they can be detected at least partially after 1 AD iteration. Generally, the cylindrical domains show higher feature detectability levels than the spherical domains at the same diameter, as their connectivity is higher (see Figure 3 a-b). 3 AD iterations are identified as a compromise between the detection of small diameter features and the reduction of falsely detected water in the background.

In the following feature detectability analysis, the subtracted image has therefore been filtered with a 3D median filter (radius 1 pixel) and a 3D anisotropic diffusion filter (3 iterations) before segmentation through thresholding. The influence of the scan time on the feature detectability when denoising with 3 AD iterations is presented in Figure 4. A clearly better detection level can be found



for the 3.2 s scan, where feature detectability levels of more than 80 % are observed for cylinders with diameters of 5 pixels and the amount of false water does not exceed 1 %. For the 0.4 s scan, the feature detectability is kept above 60 % with the diameter down to 4 pixels. Due to sampling the virtual water structures only once, fluctuations of feature detectability can be observed for both spherical and cylindrical water clusters with diameter below 8 pixels. Detectability level of subsecond scans needs to be improved. Further studies on threshold level as well as denoising filter combinations are needed. The application of phase retrieval and iterative reconstructions schemes are expected to improve feature detectability further.

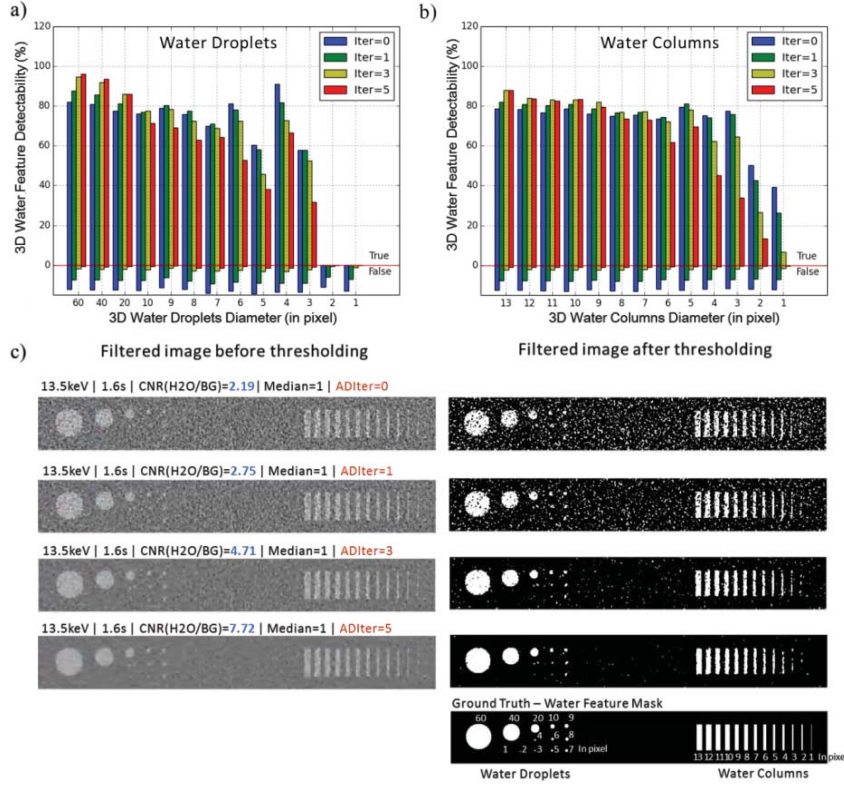


Figure 3: Feature detectability of artificial water droplets a) and water columns b) with various diameters for different number of anisotropic diffusion iterations for a tomographic scan time of 1.6 s at 13.5 keV; bar height above the red line is the percentage of true water voxels in the ground truth domain, bar height below the red line is the percentage of false voxels outside the ground truth within 10 pixels from the surface of the ground truth; c) 2D representation of 3D filtered images and the corresponding segmented images for different number of anisotropic diffusion iterations. The ground truth is shown below as a reference.

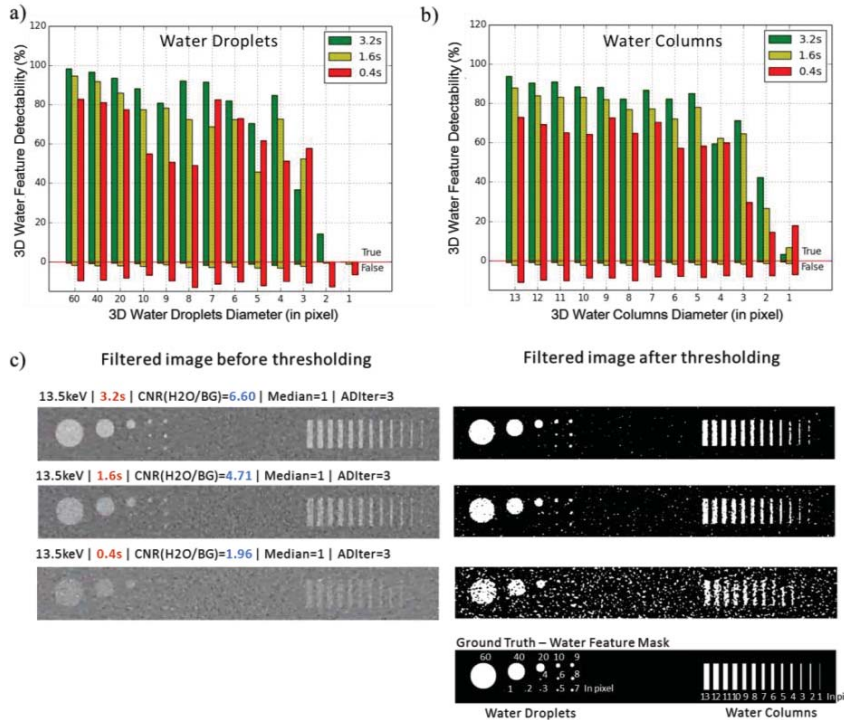


Figure 4: Feature detectability of artificial water droplets a) and water columns b) with different diameters for tomographic scan times 3.2 s, 1.6 s and 0.4 s at 13.5 keV; bar height above the red line is the percentage of true water voxels in the ground truth domain, bar height below the red line is the percentage of false voxels outside the ground truth within 10 pixels from the surface of the ground truth; c) 2D representation of 3D filtered images (left) and the corresponding segmented images (right) for scan times 3.2 s, 1.6 s and 0.4 s. The ground truth is shown below as a reference.

Publications linked to this proposal

**Fighting the Noise: Towards the Limits of Subsecond X-ray Tomographic Microscopy of PEFC**

Xu H, Bührer M, Marone F, Schmidt Thomas J, Büchi F, Eller J

ECS TRANSACTIONS 80 395 (2017)

DOI : [10.1149/08008.0395ecst](https://doi.org/10.1149/08008.0395ecst)



*Experimental Report*

**Fundamental understanding of dominating water transport mode in PEFC gas diffusion layers**

Hong Xu, Minna Bührer, Jens Eller

*(Proposal 20171538)*

**Overview**

This report will be updated after the scheduled beamtime on 14.06.2018 for proposal 20171538...

**Quality of measurement/data**

**Status and progress of evaluation**

**Results**