

# A multiscale method for coupled steady-state heat conduction and

# radiative transfer equations in composite materials

- 3 Zi-Xiang Tong<sup>a</sup>, Ming-Jia Li\*<sup>b</sup>, Yi-Si Yu<sup>b</sup>, Jing-Yu Guo<sup>b</sup>
- 4 a School of Human Settlements and Civil Engineering, Xi'an Jiaotong University, Xi'an, Shaanxi,
- 5 710049, China

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- 6 b Key Laboratory of Thermo-Fluid Science and Engineering of Ministry of Education, School of
- 7 Energy & Power Engineering, Xi'an Jiaotong University, Xi'an, Shaanxi, 710049, China
- 8 \*Corresponding author email: mjli1990@xjtu.edu.cn

# 10 Abstract

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Predictions of coupled conduction-radiation heat transfer processes in periodic composite materials are important for applications of the materials in high-temperature environments. The homogenization method is widely used for the heat conduction equation, but the coupled radiative transfer equation is seldom studied. In this work, the homogenization method is extended to the coupled conduction-radiation heat transfer in composite materials with periodic microscopic structures, in which both the heat conduction equation and the radiative transfer equation are analyzed. Homogenized equations are obtained for the macroscopic heat transfer. Unit cell problems are also derived, which provide the effective coefficients for the homogenized equations and the local temperature and radiation corrections. A second-order asymptotic expansion of the temperature field and a first-order asymptotic expansion of the radiative intensity field are established. A multiscale numerical algorithm is proposed to simulate the coupled conduction-radiation heat transfer in composite materials. According to the numerical examples in this work,

reduced from more than 300 hours to less than 30 minutes. Therefore, the proposed multisca method maintains the accuracy of the simulation and significantly improves the computation	}	compared with the fully-resolved simulations, the relative errors of the multiscale model are less
method maintains the accuracy of the simulation and significantly improves the computation efficiency. It can provide both the average temperature and radiation fields for engineering	ļ	than 13% for the temperature and less than 8% for the radiation. The computational time can be
efficiency. It can provide both the average temperature and radiation fields for engineeri	;	reduced from more than 300 hours to less than 30 minutes. Therefore, the proposed multiscale
	j	method maintains the accuracy of the simulation and significantly improves the computational
applications and the local information in microstructures of composite materials.	,	efficiency. It can provide both the average temperature and radiation fields for engineering
	3	applications and the local information in microstructures of composite materials.

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- Keywords: conduction-radiation heat transfer; homogenization; multiscale simulation; radiative
- 31 transfer equation; composite material

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#### Nomenclature

C	solution of the unit cell	problem for the second-order tem	perature $T_2$ , m <sup>2</sup> K/W

- G incident radiation, W/m<sup>2</sup>
- I radiative intensity, W/m<sup>2</sup>
- $K_{ij}$  effective thermal conductivity tensor, W/m K
- $k_{ij}^{\, arepsilon}$  thermal conductivity tensor, W/m K
- $M_{\alpha\beta}$  solution of the unit cell problem for the second-order temperature  $T_2$ , m<sup>2</sup>
- $N_{\alpha}$  solution of the unit cell problem for the first-order temperature  $T_1$ , m
- **n** outward unit normal
- T temperature, K
- $w_i$  weights in the discrete ordinate method
- X macroscopic structure domain

v	$\mathbf{v} = (\mathbf{r}_1 \ \mathbf{r}_2 \ \mathbf{r}_3)$	macrosconic	coordinate	of the structure
Α	$\mathbf{A} = \{\lambda_1, \lambda_2, \lambda_3\}$	macroscopic	Coordinate	of the structure

|Y| volume of the unit cell, m<sup>3</sup>

 $y = (y_1, y_2, y_3)$  microscopic coordinate of the unit cell

#### **Greek Letters**

ε	absorption coefficient,	/
$\alpha^{\varepsilon}$	ancorntion coefficient	m
a	absorbtion coefficient.	111

 $\overline{\alpha}$  effective absorption coefficient, /m

 $\beta^{\varepsilon}$  extinction coefficient, /m

 $\overline{\beta}$  effective extinction coefficient, /m

 $\Gamma$  boundary of the domain

 $\varepsilon$  ratio of the scales between the macroscopic and microscopic coordinates

 $\sigma^{\varepsilon}$  scattering coefficient, /m

 $\overline{\sigma\Phi}$  effective product of the scattering coefficient and the phase function, /m

 $\sigma_{B}$  Stefan-Boltzmann constant, 5.67×10<sup>-8</sup> W/m<sup>2</sup> K<sup>4</sup>

 $\Phi^{\varepsilon}$  scattering phase function

 $\phi$  volume fraction

 $\Omega = (\Omega_1, \Omega_2, \Omega_3)$  unit vector of a radiation direction

# Subscripts and Superscripts

- 0 homogenized value
- 1 first-order correction
- 2 second-order correction
- b boundary
- F fully-resolved simulation

i, j component of a vector or tensor

M multiscale simulation

ref reference value

 $\alpha, \beta$  component of a vector or tensor

#### 1. Introduction

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Composite materials and porous materials are widely used in high-temperature environments due to their special mechanical and thermal properties. For example, ceramic matrix composites and silica aerogels are used in propulsion systems and thermal protection systems of aerospace vehicles [1-3]. Ceramic foams are used as absorbers of volumetric solar air receivers [4-5]. Predictions of heat transfer processes in these materials are important for their applications. There are two difficulties in the predictions. Firstly, composite materials and porous materials have complex microscopic structures. The local thermal properties fluctuate according to the structures. Secondly, effects of the thermal radiation become important in high-temperature environments. Traditionally, correlations for effective thermal properties are used in these problems, which are obtained from theoretical analyses or experiments [3,6]. The correlations usually depend on the specific structures of the materials and their utilizations are limited. Also, microscopic temperature fluctuations are neglected. In order to accurately predict the thermal performances of composite materials, a multiscale model for the coupled conduction-radiation heat transfer problem is needed [7-8]. Homogenization methods are widely used for analyses of mechanical and thermal properties of composite materials [9-11]. Although homogenization analyses of the heat conduction are well established, homogenization analyses of the coupled conduction-radiation heat transfer still need

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further studies. Some researchers considered the heat radiation in their homogenization analyses. In the existing researches, the heat radiation was treated as a separate heat transfer process, a radiative boundary condition or a heat source in the heat conduction equation. For example, in the multiscale model proposed by Liu and Zhang [12], the heat conduction and radiation equations were solved separately. A homogenization method was firstly applied to the heat conduction equation to obtain the effective conductive thermal conductivity and the temperature field in a unit cell. Then, the effective radiative thermal conductivity was calculated based on the temperature field in the unit cell. Some researches on the multiscale heat transfer in porous media included radiation boundary conditions in the pores. For example, Allaire and El Ganaoui [13] proposed a two-scale homogenization model for heat transfer problems in periodically perforated materials with a radiation boundary condition in the perforations. In the model, the radiative boundary condition was multiplied by a scaling factor  $\varepsilon^{-1}$  and the solution of the temperature field was expanded to the first order of  $\varepsilon$ . Yang et al. [14] developed a second-order two-scale method for steady-state heat transfer problems in porous media with interior surface radiations. The original radiation boundary condition without the scaling factor was used. The solution of the temperature was expanded to the second order of  $\varepsilon$ . The model was extended into transient heat transfer problems [15] and porous materials with three different length scales [16]. The convective heat transfer in the pores was further included in the above models [17-19]. Haymes and Gal [20] used a similar model to study the multiscale heat transfer in porous building materials. Moreover, Huang and Cao [21-22] conducted a homogenization analysis of the transient heat transfer with radiation effects. In their model, the heat radiation was considered as a volumetric heat source, which was proportional to T<sup>4</sup>, in the heat conduction equation.

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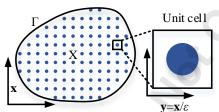
In the above researches, multiscale analyses were mainly applied to the heat conduction equation. Radiation effects were treated as boundary conditions or volumetric heat sources. The radiative transfer equation was not included in the analyses. Meanwhile, homogenizations of the radiative transfer equation was studied in some researches. For example, Mathiaud and Salvarani [23] proposed a homogenization method for transport problems with highly oscillatory coefficients. The derived numerical model was applied to the radiative transfer equation. Homogenizations of linear Boltzmann equation were studied by Goudon and Mellet [24] and Hutridurga et al. [25]. The radiative transfer equation was a special form of the Boltzmann equation. However, the heat conduction was not within the scope of these researches. In this work, the homogenization method will be extended to heat transfer problems with both the heat conduction equation and the radiative transfer equation. Both the temperature field and the radiative intensity field will be considered. The rest of the paper is organized as follows. In Section 2, the homogenization analysis will be applied to the coupled heat conduction and radiative transfer equations. Homogenized equations, unit cell problems and expressions of effective coefficients will be obtained. A multiscale numerical model will be presented in Section 3. In Section 4, the proposed multiscale model will be validated by numerical examples. Finally, some conclusions are summarized in Section 5.

# 2. Homogenization of Heat Conduction and Radiative Transfer Equations

The problem in this work is sketched in Fig. 1. The coupled conduction and radiation heat transfer occurs in a composite material with periodic local structures. The unit cell is the smallest unit that repetitively constitutes the composite material. There are two scales in this problem, which are the macroscale of the material and the microscale of the unit cell. The coordinate in the macroscale is

denoted by  $\mathbf{x}$  and the coordinate in the unit cell is denoted by  $\mathbf{y}$ . Because the characteristic length of the unit cell is much smaller than that of the macroscale, the ratio between  $\mathbf{x}$  and  $\mathbf{y}$  is denoted by a small parameter  $\varepsilon$ , which means  $\mathbf{y}=\mathbf{x}/\varepsilon$  [9]. Based on the homogenization analysis in this section, homogenized equations will be derived for the heat transfer in macroscale. A set of unit cell problems will also be obtained to provide the effective thermal conductivity and radiation coefficients for the homogenized equations, as well as the supplementary temperature and radiation corrections in the unit cells.

conduction and radiation heat transfer



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Fig. 1 A sketch of the problem in this work

The analysis starts from the governing equations of the steady-state conduction-radiation heat transfer [26]:

$$\frac{\partial}{\partial x_{i}} \left( k_{ij}^{\varepsilon} \left( \mathbf{x} \right) \frac{\partial T^{\varepsilon} \left( \mathbf{x} \right)}{\partial x_{j}} \right) - \alpha^{\varepsilon} \left( \mathbf{x} \right) \left( 4\sigma_{\mathrm{B}} \left[ T^{\varepsilon} \left( \mathbf{x} \right) \right]^{4} - \int_{4\pi} I^{\varepsilon} \left( \mathbf{x}, \Omega \right) \mathrm{d}\Omega \right) = 0, \quad \mathbf{x} \in \mathbf{X} \tag{1}$$

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$$\Omega_{i} \frac{\partial I^{\varepsilon}(\mathbf{x}, \Omega)}{\partial x_{i}} = -\beta^{\varepsilon}(\mathbf{x}) I^{\varepsilon}(\mathbf{x}, \Omega) + \frac{\sigma_{B}}{\pi} \alpha^{\varepsilon}(\mathbf{x}) [T^{\varepsilon}(\mathbf{x})]^{4} \\
+ \frac{1}{4\pi} \sigma^{\varepsilon}(\mathbf{x}) \int_{4\pi} I^{\varepsilon}(\mathbf{x}, \Omega') \Phi^{\varepsilon}(\mathbf{x}, \Omega', \Omega) d\Omega', \quad \mathbf{x} \in X$$

109 The boundary conditions are:

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$$\begin{cases} T^{\varepsilon}(\mathbf{x}) = T_{b}(\mathbf{x}), & \mathbf{x} \in \Gamma \\ I^{\varepsilon}(\mathbf{x}, \Omega) = \frac{\sigma_{B}}{\pi} T_{b}^{4}(\mathbf{x}), & \text{for } \Omega \cdot \mathbf{n} < 0, & \mathbf{x} \in \Gamma \end{cases}$$
 (3)

Equation (1) is the heat conduction equation, where the  $T^{\varepsilon}(\mathbf{x})$  is the temperature and the  $\mathbf{x}$  represents the position vector  $(x_1, x_2, x_3)$ . The X represents the whole computational domain. The  $k_{ij}^{\varepsilon}$  is the symmetric thermal conductivity tensor of the material. Equation (2) is the radiative transfer Li et al, HT-21-1051-7

- equation, which describes the radiative intensity  $F(\mathbf{x}, \Omega)$  along the direction  $\Omega$ . The  $\Omega_i$  is the ith cosine of the unit vector of direction  $\Omega$ . The  $\alpha^e$ ,  $\beta^e$  and  $\sigma^e$  are the absorption, extinction and scattering coefficients, which have the relation  $\beta^e = \alpha^e + \sigma^e$ . The  $\Phi^e(\mathbf{x}, \Omega', \Omega)$  is the scattering phase function, which describes the angular distribution of the scattered radiative intensity. The Stefan-Boltzmann constant  $\sigma_B$  is  $5.67 \times 10^{-8}$  W·m<sup>-2</sup>·K<sup>-4</sup>. As for the boundary conditions on  $\Gamma$ , the Dirichlet boundary condition for the temperature is considered in this work. The radiation boundary is assumed to be black, and the inlet radiative intensity is calculated by the black body radiation.
- In the homogenization analysis, the temperature and the radiative intensity are expanded into the
- 122 following series of the small parameter  $\varepsilon$  [9]:

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$$T^{\varepsilon}(\mathbf{x}) = T_{0}(\mathbf{x}, \mathbf{y}) + \varepsilon T_{1}(\mathbf{x}, \mathbf{y}) + \varepsilon^{2} T_{2}(\mathbf{x}, \mathbf{y}) + O(\varepsilon^{3})$$
 (4)

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$$I^{\varepsilon}(\mathbf{x}, \Omega) = I_{0}(\mathbf{x}, \mathbf{y}, \Omega) + \varepsilon I_{1}(\mathbf{x}, \mathbf{y}, \Omega) + O(\varepsilon^{2})$$
 (5)

- It should be mentioned that  $y=x/\varepsilon$ . The thermal conductivities and the radiation coefficients fluctuate
- in the unit cell according to the materials, so the  $k_{ij}^{\varepsilon}$ ,  $\alpha^{\varepsilon}$ ,  $\beta^{\varepsilon}$ ,  $\sigma^{\varepsilon}$  and  $\Phi^{\varepsilon}$  are all functions of  $\mathbf{y}$ .
- 127 The  $(T^{\varepsilon})^4$  can be represented by:

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$$\left[T^{\varepsilon}\left(\mathbf{x}\right)\right]^{4} = T_{0}^{4} + \varepsilon\left(4T_{0}^{3}T_{1}\right) + \varepsilon^{2}\left(6T_{0}^{2}T_{1}^{2} + 4T_{0}^{3}T_{2}\right) + O\left(\varepsilon^{3}\right)$$
 (6)

The spatial derivative is given by [9]:

$$\frac{\partial}{\partial x_i} = \frac{\partial}{\partial x_i} + \frac{1}{\varepsilon} \frac{\partial}{\partial y_i}$$
 (7)

- The above expansions are substituted into Eqs. (1) and (2), and the equations in different orders
- 132 of  $\varepsilon$  can be obtained.
- In the order of  $\varepsilon^{-2}$ , there is only one equation for the heat conduction:

$$\frac{\partial}{\partial y_{i}} \left( k_{ij}^{\varepsilon} \left( \mathbf{y} \right) \frac{\partial T_{0} \left( \mathbf{x}, \mathbf{y} \right)}{\partial y_{j}} \right) = 0 \tag{8}$$

Therefore, the  $T_0$  is independent of **y** and is only a function of **x**:

$$T_0 = T_0(\mathbf{x}) \tag{9}$$

In the order of  $\varepsilon^{-1}$ , the heat conduction and radiative transfer equations are:

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$$\frac{\partial}{\partial x_{i}} \left( k_{ij}^{\varepsilon} \left( \mathbf{y} \right) \frac{\partial T_{0} \left( \mathbf{x} \right)}{\partial y_{j}} \right) + \frac{\partial}{\partial y_{i}} \left( k_{ij}^{\varepsilon} \left( \mathbf{y} \right) \frac{\partial T_{0} \left( \mathbf{x} \right)}{\partial x_{j}} + k_{ij}^{\varepsilon} \left( \mathbf{y} \right) \frac{\partial T_{1} \left( \mathbf{x}, \mathbf{y} \right)}{\partial y_{j}} \right) = 0$$
 (10)

$$\Omega_{i} \frac{\partial I_{0}(\mathbf{x}, \mathbf{y}, \Omega)}{\partial y_{i}} = 0$$
(11)

Equation (11) also demonstrates that the  $I_0$  is not a function of y:

$$I_0 = I_0 \left( \mathbf{x}, \Omega \right) \tag{12}$$

Based on Eq. (9), Eq. (10) can be simplified as:

$$\frac{\partial}{\partial y_{i}} \left( k_{ij}^{\varepsilon} \left( \mathbf{y} \right) \frac{\partial T_{1} \left( \mathbf{x}, \mathbf{y} \right)}{\partial y_{j}} \right) = -\frac{\partial}{\partial y_{i}} \left( k_{ij}^{\varepsilon} \left( \mathbf{y} \right) \frac{\partial T_{0} \left( \mathbf{x} \right)}{\partial x_{j}} \right) \tag{13}$$

According to the form of Eq. (13), it can be assumed that the  $T_1$  is expressed as:

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$$T_{1}(\mathbf{x}, \mathbf{y}) = N_{i}(\mathbf{y}) \frac{\partial T_{0}(\mathbf{x})}{\partial x_{i}}$$
 (14)

By substituting Eq. (14) into Eq. (13), the unit cell problem for  $N_a(\mathbf{y})$  can be obtained:

Next, the heat conduction and radiative transfer equations in the order of  $\varepsilon^0$  are:

$$\frac{\partial}{\partial x_{i}} \left( k_{ij}^{\varepsilon} \frac{\partial T_{0}}{\partial x_{i}} \right) + \frac{\partial}{\partial x_{i}} \left( k_{ij}^{\varepsilon} \frac{\partial T_{1}}{\partial y_{i}} \right) + \frac{\partial}{\partial y_{i}} \left( k_{ij}^{\varepsilon} \frac{\partial T_{1}}{\partial x_{i}} \right) + \frac{\partial}{\partial y_{i}} \left( k_{ij}^{\varepsilon} \frac{\partial T_{2}}{\partial y_{i}} \right) - 4\alpha^{\varepsilon} \sigma_{B} T_{0}^{4} + \alpha^{\varepsilon} \int_{4\pi} I_{0} d\Omega = 0 \quad (16)$$

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$$\Omega_{i} \left( \frac{\partial I_{0}}{\partial x_{i}} + \frac{\partial I_{1}}{\partial y_{i}} \right) = -\beta^{\varepsilon} I_{0} + \frac{\alpha^{\varepsilon} \sigma_{B}}{\pi} T_{0}^{4} + \frac{\sigma^{\varepsilon}}{4\pi} \int_{4\pi} I_{0}(\mathbf{x}, \Omega') \Phi^{\varepsilon}(\mathbf{y}, \Omega', \Omega) d\Omega'$$
 (17)

- 151 Then, the macroscopic homogenized heat conduction and radiative transfer equations can be
- obtained by taking volumetric averages of Eqs. (16) and (17) in the unit cell.
- The homogenized heat conduction equation is the volumetric average of Eq. (16):

$$\begin{cases}
\frac{\partial}{\partial x_{i}} \left( K_{ij} \frac{\partial T_{0}}{\partial x_{j}} \right) - 4 \overline{\alpha} \sigma_{B} T_{0}^{4} + \overline{\alpha} \int_{4\pi} I_{0} d\Omega = 0, \quad \mathbf{x} \in \mathbf{X} \\
T_{0} \left( \mathbf{x} \right) = T_{b} \left( \mathbf{x} \right), \quad \mathbf{x} \in \Gamma
\end{cases}$$
(18)

- where the effective thermal conductivity  $K_{ij}$  and the effective absorption coefficient  $\bar{\alpha}$  are given
- 156 by:

$$K_{ij} = \frac{1}{|Y|} \int \left( k_{ij}^{\varepsilon} \left( \mathbf{y} \right) + k_{ip}^{\varepsilon} \left( \mathbf{y} \right) \frac{\partial N_{j} \left( \mathbf{y} \right)}{\partial y_{p}} \right) d\mathbf{y}$$
(19)

$$\bar{\alpha} = \frac{1}{|Y|} \int \alpha^{\varepsilon} (\mathbf{y}) d\mathbf{y}$$
 (20)

- The terms  $\frac{\partial}{\partial y_i} \left( k_{ij}^{\varepsilon} \frac{\partial T_1}{\partial x_j} \right)$  and  $\frac{\partial}{\partial y_i} \left( k_{ij}^{\varepsilon} \frac{\partial T_2}{\partial y_j} \right)$  are eliminated because the  $T_1$  and  $T_2$  are periodic in
- the unit cell.
- The homogenized radiative transfer equation is the volumetric average of Eq. (17):

$$\begin{cases}
\Omega_{i} \frac{\partial I_{0}}{\partial x_{i}} = -\overline{\beta} I_{0} + \frac{\overline{\alpha} \sigma_{B}}{\pi} T_{0}^{4} + \frac{1}{4\pi} \int_{4\pi} I_{0}(\mathbf{x}, \Omega') \overline{\sigma \Phi}(\Omega', \Omega) d\Omega', & \mathbf{x} \in \mathbf{X} \\
I_{0}(\mathbf{x}, \Omega) = \frac{\sigma_{B}}{\pi} T_{b}^{4}(\mathbf{x}), & \text{for } \Omega \cdot \mathbf{n} < 0, & \mathbf{x} \in \Gamma
\end{cases} \tag{21}$$

- where the effective extinction coefficient and the effective product of scattering coefficient and
- phase function are calculated by:

$$\overline{\beta} = \frac{1}{|Y|} \int \beta^{\varepsilon} (\mathbf{y}) d\mathbf{y}$$
 (22)

$$\overline{\sigma\Phi}(\Omega',\Omega) = \frac{1}{|Y|} \int \sigma^{\varepsilon}(\mathbf{y}) \Phi^{\varepsilon}(\mathbf{y},\Omega',\Omega) d\mathbf{y}$$
 (23)

- In this derivation, it is unnecessary to assume that the  $I_1$  is periodic in the unit cell. It is only assumed
- 168 that:

$$\left\langle \Omega_{i} \frac{\partial I_{1}}{\partial y_{i}} \right\rangle = \frac{1}{|Y|} \int \frac{\partial \left(\Omega_{i} I_{1}\right)}{\partial y_{i}} d\mathbf{y} = \frac{1}{|Y|} \int \Omega_{i} I_{1} n_{i} dS = 0$$
 (24)

- where  $n_i$  is the outward pointing unit normal and dS is the surface element of the unit cell. Equation
- 171 (24) means that there is no net source of  $I_1$  in the unit cell.
- The higher ordered temperature and radiation fields can be obtained by subtracting the Li et al, HT-21-1051-10

- homogenized equations from Eqs. (16) and (17). Subtracting Eq. (18) from Eq. (16) and using
- Eq. (14), the following equation is obtained:

$$\left(k_{ij}^{\varepsilon} - K_{ij} + k_{ip}^{\varepsilon} \frac{\partial N_{j}}{\partial y_{p}} + \frac{\partial \left(k_{pi}^{\varepsilon} N_{j}\right)}{\partial y_{p}}\right) \frac{\partial^{2} T_{0}}{\partial x_{i} \partial x_{j}} + \frac{\partial}{\partial y_{i}} \left(k_{ij}^{\varepsilon} \frac{\partial T_{2}}{\partial y_{j}}\right) - \left(\alpha^{\varepsilon} - \overline{\alpha}\right) \left(4\sigma_{B} T_{0}^{4} - \int_{4\pi} I_{0} d\Omega\right) = 0$$
(25)

According to the form of Eq. (25), it can be assumed that the  $T_2$  is expressed as:

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$$T_{2}(\mathbf{x}, \mathbf{y}) = M_{\alpha\beta}(\mathbf{y}) \frac{\partial^{2} T_{0}(\mathbf{x})}{\partial x_{\alpha} \partial x_{\beta}} + C(\mathbf{y}) \left(4\sigma_{B} T_{0}^{4} - \int_{4\pi} I_{0} d\Omega\right)$$
(26)

178 Thus, Eq. (25) is equivalent to the following two unit cell problems:

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$$\begin{cases} \frac{\partial}{\partial y_i} \left( k_{ij}^{\varepsilon} \frac{\partial C(\mathbf{y})}{\partial y_j} \right) = \alpha^{\varepsilon} - \overline{\alpha} \\ C(\mathbf{y}) \text{ is periodic in Y} \end{cases}$$
 (28)

- 181 It should be mentioned that the periodic boundary conditions in Eqs. (15), (27) and (28) are not sufficient to provide unique solutions for the unit cell problems. In practice, it is also required
- that the volumetric averages of  $N_{\alpha}$ ,  $M_{\alpha\beta}$  and C are zero in the unit cell. Thus, the unit-cell averages
- of  $T_1$  and  $T_2$  also vanish. This is consistent with the definition that the  $T_0$  is the macroscopic average
- 185 temperature.
- Finally, the governing equation for  $I_1$  can be obtained by subtracting Eq. (21) from Eq. (17):

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$$\Omega_{i} \frac{\partial I_{1}}{\partial y_{i}} = -\left(\beta^{\varepsilon} - \overline{\beta}\right) I_{0} + \frac{\left(\alpha^{\varepsilon} - \overline{\alpha}\right) \sigma_{B}}{\pi} T_{0}^{4} + \frac{1}{4\pi} \int_{4\pi} I_{0}(\mathbf{x}, \Omega') \left(\sigma^{\varepsilon} \Phi^{\varepsilon} - \overline{\sigma} \Phi\right) d\Omega'$$
 (29)

- 188 It can be seen that the  $I_1$  in Eq. (29) satisfies Eq. (24). Equation (29) depends on the average
- radiative intensity  $I_0$  and the temperature  $T_0$ . Therefore, Eq. (29) varies in different unit cells and
- the  $I_1$  should be solved in each unit cell. In this work, two different boundary conditions for  $I_1$  are

- considered. The first is similar to the boundary conditions of  $N_a$ ,  $M_{\alpha\beta}$  and C. It is assumed that:
- 192  $I_1$  is periodic in each unit cell (30)
- 193 The second is that:
- 194  $I_1$  is solved in the whole domain with  $I_1(\mathbf{x}, \Omega) = 0$ , for  $\Omega \cdot \mathbf{n} < 0$ ,  $\mathbf{x} \in \Gamma$  (31)
- Boundary condition (31) means that the solutions of  $I_1$  in the upstream unit cells provide the inlet
- boundary conditions of  $I_1$  for the downstream unit cells. Because the right-hand-side of Eq. (29)
- does not contain  $I_1$ , iterations in each unit cell are not necessary if there is no periodic boundary
- 198 condition in the whole domain. The accuracy of the two boundary conditions will be compared in
- the numerical examples in Section 4.2.
- When the  $T_0$ ,  $T_1$ ,  $T_2$ ,  $I_0$  and  $I_1$  are obtained, the approximated temperature field and radiative
- intensity field can be reconstructed by:

$$T^{\varepsilon} = T_{0} + \varepsilon T_{1} + \varepsilon^{2} T_{2} = T_{0} + \varepsilon N_{i} \frac{\partial T_{0}}{\partial x_{i}} + \varepsilon^{2} \left[ M_{\alpha\beta} \frac{\partial^{2} T_{0}}{\partial x_{\alpha} \partial x_{\beta}} + C \left( 4\sigma_{B} T_{0}^{4} - \int_{4\pi} I_{0} d\Omega \right) \right]$$
(32)

$$I^{\varepsilon} = I_0 + \varepsilon I_1 \tag{33}$$

- 204 3. Numerical Algorithm
- A multiscale numerical algorithm is proposed based on the analysis in Section 2. The
- computational procedure is shown in Fig. 2, which contains the following steps.
- 207 1) Identify the geometry of the unit cell and build meshes for both the unit cell problem and the
- 208 macroscopic problem.
- 209 2) Solve Eq. (15) in the unit cell and obtain  $N_a(\mathbf{y})$ . Calculate the effective thermal conductivity,
- 210 the effective absorption and extinction coefficient and the effective product of scattering coefficient
- and phase function by Eqs. (19), (20), (22) and (23).
- 3) Solve the homogenized Eqs. (18) and (21) to obtain the macroscopic  $T_0(\mathbf{x})$  and  $I_0(\mathbf{x})$ .

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- 213 4) Solve Eqs. (27), (28) and (29) to obtain  $M_{\alpha\beta}(\mathbf{y})$ ,  $C(\mathbf{y})$  and  $I_1(\mathbf{y})$ .
  - 5) Reconstruct the temperature field  $T^{\epsilon}$  by the combination of Eqs. (32), (14) and (26).
- Reconstruct the radiative intensity field  $I^{\epsilon}$  by Eq. (33).

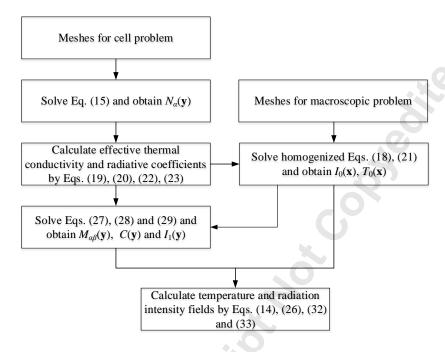


Fig. 2 The computational procedure of the multiscale numerical model

The Cartesian meshes are employed in this work. The material in each control volume is specified and the corresponding thermal properties are determined based on the material. The finite volume method (FVM) is used to solve Eqs. (15), (18), (27) and (28), which are related to the heat conduction equation [27]. The discrete ordinate method (DOM) is used to solve Eqs. (21) and (29), which are related to the radiative transfer equation [26]. For the 2D problems in this work, the S6 DOM with 24 discrete directions is used [26].

In the FVM, the thermal conductivities on the interfaces of a control volume are the harmonic mean values of the thermal conductivities in the neighboring control volumes. The volume integral is conducted in each control volume to derive discrete equations. Therefore, the FVM contains only

first-order derivatives. The finite differences are used to calculate the first-order derivatives.

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228 However, the calculation of  $T_2$  in Eq. (26) contains second-order partial derivatives of  $T_0$ . The 229 second-order finite difference of  $T_0$  can be adopted. For example, if the coordinate **x** is expressed by  $(x_1, x_2)$  in 2D simulations, the derivative  $\frac{\partial^2 T_0}{\partial x_i^2}\Big|_{x_i}$  at a node (i, j) can be calculated by: 230

$$\frac{\partial^2 T_0}{\partial x_1^2} \bigg|_{i,j} = \frac{T_{0,i+1,j} - 2T_{0,i,j} + T_{0,i-1,j}}{\Delta x^2} \tag{34}$$

where  $T_{0,i,j}$  is the  $T_0$  at the node (i, j). However, in practice it is found that the finite difference Eq. 232 (34) has large fluctuations in the computational domain and will lead to large errors in the 233 reconstructed temperature fields. Therefore, the second-order derivatives are calculated by the least 234 square method. For each node (i, j), the coordinates and the  $T_0$  of  $7 \times 7$  neighboring nodes (i+m, j+n), 235 m,  $n=-3\sim3$ , are used to fit a quadric surface by the least square method. The quadric surface is 236 237 expressed as:

expressed as: 
$$T_0(x_1, x_2) = a_{11}x_1^2 + a_{12}x_1x_2 + a_{22}x_2^2 + b_1x_1 + b_2x_1 + c \tag{35}$$

where  $(x_1, x_2)$  is the coordinate and  $a_{11}$ ,  $a_{12}$ ,  $a_{22}$ ,  $b_1$ ,  $b_2$ , c are the fitted parameters. Then, the second-239 order derivatives of  $T_0$  can be obtained by: 240

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$$\frac{\partial^2 T_0}{\partial x_1^2} \bigg|_{i,j} = 2a_{11}, \quad \frac{\partial^2 T_0}{\partial x_2^2} \bigg|_{i,j} = 2a_{22}, \quad \frac{\partial^2 T_0}{\partial x_1 \partial x_2} \bigg|_{i,j} = a_{12}$$
 (36)

In addition, it should be mentioned that although the small parameter  $\varepsilon$  is important for the analysis in Section 2, its specific value has no influence on the results of numerical simulations. It can be seen that the orders of the partial derivatives with respect to v on the left and right sides of Eqs. (15), (27), (28) and (29) are not equal. Because the coordinate  $\mathbf{v}$  is influenced by  $\varepsilon$  according to  $\mathbf{y}=\mathbf{x}/\varepsilon$ , the values of  $N_{\alpha}$ ,  $M_{\alpha\beta}$ , C and  $I_1$  are also influenced by  $\varepsilon$ . For example, it is assumed that  $\varepsilon_1$ and  $\varepsilon_2$  are used in two numerical simulations for a same problem, and their ratio is  $r=\varepsilon_2/\varepsilon_1$ . Then, the relation for y is  $y_2 = y_1/r$ . Applying  $y_1$  and  $y_2$  in Eq. (15) respectively, it can be found that the results

have a relation  $N_{\alpha,2}=N_{\alpha,1}/r$ , where the subscripts 1 and 2 denote the results which are corresponding to  $\mathbf{y}_1$  and  $\mathbf{y}_2$ . Similarly, relations  $M_{\alpha\beta,2}=M_{\alpha\beta,1}/r^2$ ,  $C_2=C_1/r^2$  and  $I_{1,2}=I_{1,1}/r$  can be obtained from Eqs. (27), (28) and (29). Taking into consideration  $\varepsilon_2=r\varepsilon_1$ , it can be found that  $\varepsilon_2N_{\alpha,2}=\varepsilon_1N_{\alpha,1}$ ,  $\varepsilon_2I_{1,2}=\varepsilon_1I_{1,1}$ ,  $\varepsilon_2^2M_{\alpha\beta,2}=\varepsilon_1^2M_{\alpha\beta,1}$ , and  $\varepsilon_2^2C_2=\varepsilon_1^2C_1$ . Therefore, the  $T^\varepsilon$  and F calculated from Eqs. (32) and (33) are the same for both  $\varepsilon_1$  and  $\varepsilon_2$ . In this work, if the spatial step for the homogenized macroscale simulation is  $\Delta x$  and the spatial step for the unit cell problem is  $\Delta y$ , the  $\varepsilon$  is chosen as  $\varepsilon=\Delta y/\Delta x$ .

#### 4. Numerical Examples

#### 4.1 Effective thermal conductivity

Firstly, the effective thermal conductivities calculated by Eq. (19) are compared with theoretical predictions. The unit cell is the same as that in Fig. 4. The grid size of the unit cell is  $400\times400$ , and a particle of radius R is placed in the center of the unit cell. The dimensionless parameters are used. The R changes from 10 to 140. The thermal conductivity of the base material is  $k_0$ =1, and that of the particle is  $k_1$ =5 or  $k_1$ =10. If the volume fraction of the particle is denoted by  $\phi$ , the effective thermal conductivity K of the unit cell can be predicted by the following equation [28]:

$$\frac{K}{k_0} = 1 + \frac{2\phi}{\left(\frac{k_1 + k_0}{k_1 - k_0}\right) - \phi + \left(\frac{k_1 - k_0}{k_1 + k_0}\right) \left(0.30584\phi^4 + 0.013363\phi^8\right)}$$
(37)

The effective thermal conductivities predicted by Eq. (19) are compared with the values calculated from Eq. (37), and the results are shown in Fig. 3. It can be seen that the predicted thermal conductivities coincide well with that calculated from Eq. (37) for different particle volume fractions and particle thermal conductivities. Therefore, the effective thermal conductivity of the model is validated.

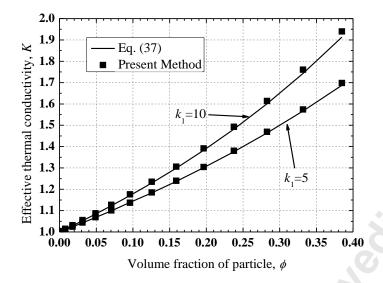


Fig. 3 The comparison between the effective thermal conductivities predicted by the multiscale

### model and the theoretical correlation

## **4.2 Example 1**

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In the following sections, 2D numerical examples are used to validate the proposed multiscale model. The first example is the conduction-radiation heat transfer in SiO<sub>2</sub> aerogel doped with TiO<sub>2</sub> opacifier particles. A sketch of the problem is illustrated in Fig. 4. The computational domain is composed of ten 0.1mm×0.1mm unit cells. A TiO<sub>2</sub> particles is placed at the center of each unit cell and the diameter of the particle is  $20\mu$ m. The thermal conductivities and the absorption and scattering coefficients of the SiO<sub>2</sub> aerogel and the TiO<sub>2</sub> particle are given in Table 1. The scattering is assumed to be isotropic and  $\Phi^e$ =1 is used. The temperature of the left boundary is 900K and the temperature of the right boundary is 500K. The periodic boundary condition is used on the other boundaries.

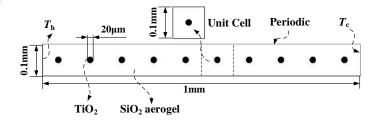


Fig. 4 The computational domain for Example 1 Li et al, HT-21-1051-16

Table 1 Properties of the materials

Material	Thermal conductivity/	Absorption	Scattering	
Material	$Wm^{\text{-}1}K^{\text{-}1}$	coefficient/ m <sup>-1</sup>	Coefficient/ m <sup>-1</sup>	
SiO <sub>2</sub> aerogel	0.0177	15.4	24.8	
$TiO_2$	4.39	7208	0	

The problem is solved by the proposed multiscale numerical model. In order to evaluate the accuracy of the multiscale model, a fully-resolved simulation of the problem is used as the benchmark. A grid independence test of the unit cell problem is conducted first to determine the grid size of the simulation. The grid size of the unit cell changes from  $50\times50$  to  $600\times600$ , and the diameter of the particle is from  $10\Delta x$  to  $120\Delta x$ , respectively. The  $N_{\alpha}$  for each grid size are solved and the corresponding effective thermal conductivities are calculated. The effective thermal conductivities for different grid sizes are given in Figure S1, available in Supplemental Material, part of the ASME Digital Collection. It is found that the variation of the thermal conductivity is relatively small when the grid size is larger than  $200\times200$ . Taking into consideration the computational cost, the  $200\times200$  mesh is adopted for the unit cell problem and the diameter of the particle is  $40\Delta x$ . The corresponding grid size of the fully-resolved problem is  $2000\times200$ . As for the homogenized equations, the grid size is  $500\times50$ . The thermal and radiation properties in each grid node are specified in accordance with the material in that node.

The convergence criterion for  $N_{\alpha}$ ,  $M_{\alpha\beta}$ , C, and  $I_1$  is that the relative error  $E_{\phi}$  between two successive iterations is less than  $10^{-8}$ , which is defined as:

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$$E_{\phi} = \sqrt{\sum_{i,j} \left(\phi_{i,j}^{n+1} - \phi_{i,j}^{n}\right)^{2} / \sum_{i,j} \left(\phi_{i,j}^{n}\right)^{2}}$$
 (38)

The variable  $\phi$  represents  $N_{\alpha}$ ,  $M_{\alpha\beta}$ , or C, and the  $\phi_{i,j}^n$  is the value at node (i,j) after nth iteration.

- As for the simulation of conduction and radiation heat transfer, the relative error E is defined as:
- 303  $E = \sqrt{\sum_{i,j} \left(T_{i,j}^{n+1} T_{i,j}^{n}\right)^{2} / \sum_{i,j} \left(T_{i,j}^{n} T_{\text{ref}}\right)^{2}} + \sqrt{\sum_{i,j,k} \left(I_{i,j,k}^{n+1} I_{i,j,k}^{n}\right)^{2} / \sum_{i,j,k} \left(I_{i,j,k}^{n} I_{\text{ref}}\right)^{2}}$ (39)
- 304 where the k represents the kth direction of the DOM. The reference temperature is  $T_{\text{ref}} = (T_h + T_c)/2$
- and the reference radiative intensity is  $I_{\text{ref}} = \sigma_{\text{B}} T_{\text{ref}}^4 / \pi$ . The convergence criterion is  $E < 10^{-8}$ .
- Incident radiations G are shown in the figures of this paper instead of the individual radiative
- intensities  $I_i$ . In DOM, the G is calculated by  $G = \sum_k w_k I_k$ , where the  $w_k$  are the weights of the
- 308 discrete directions [26].
- The solutions of  $N_{\alpha}$ ,  $M_{\alpha\beta}$  and C in the unit cell are shown in Fig. 5. Because of the symmetric
- structure of the unit cell, the effective thermal conductivity is isotropic and the value is 0.0218 Wm
- $^{1}$ K<sup>-1</sup> according to the solution of  $N_{\alpha}$ . The effective absorption coefficient and scattering coefficient
- are 242.7m<sup>-1</sup> and 24.02m<sup>-1</sup>. These parameters are used in Eqs. (18) and (21) to calculate the
- 313 homogenized temperature and radiative intensity fields, which are shown in Fig. 6 (b) and Fig. 7 (b)
- separately. Then, the multiscale temperature field can be reconstructed and the result is given in Fig.
- 315 6 (c). The relative errors of the temperature and radiative intensity fields are defined as:

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$$E_{T} = \sqrt{\sum_{i,j} \left(T_{i,j}^{\varepsilon} - T_{i,j}^{F}\right)^{2} / \sum_{i,j} \left(T_{i,j}^{F} - T_{ref}\right)^{2}}, \quad E_{I} = \sqrt{\sum_{i,j,k} \left(I_{i,j,k}^{\varepsilon} - I_{i,j,k}^{F}\right)^{2} / \sum_{i,j,k} \left(I_{i,j,k}^{F} - I_{ref}\right)^{2}}$$
(40)

- 317 where the superscripts  $\varepsilon$  and F represent the multiscale results and the fully-resolved results,
- respectively. The relative errors of the homogenized temperature  $T_0$  and the reconstructed multiscale
- temperature  $T^{\epsilon}$  are 0.90% and 0.48%.

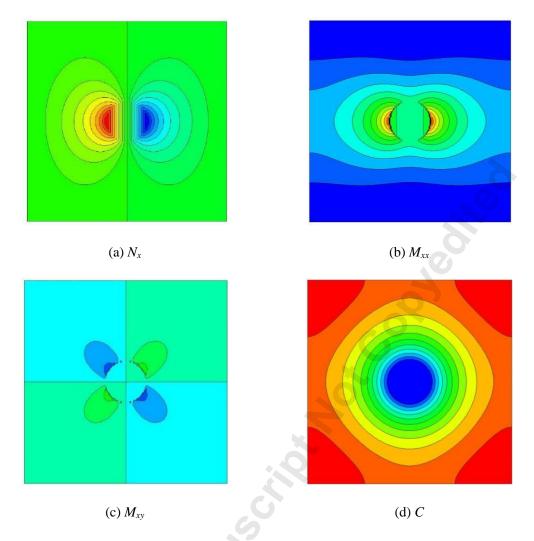


Fig. 5 The results of  $N_{\alpha}$ ,  $M_{\alpha\beta}$  and C in the unit cell for Example 1

Then, the multiscale radiative intensity fields are reconstructed. The  $T_0$  is used in Eq. (29) to calculate  $I_1$ , and the boundary conditions (30) and (31) for  $I_1$  are compared. The results of the reconstructed multiscale incident radiation fields  $G^e$  are shown in Fig. 7 (c) and Fig. 7 (d). The corresponding first-order corrections  $G_1$  are also given in Figure S2, available in Supplemental Material, part of the ASME Digital Collection. Because the  $I_1$  in each unit cell is solved individually under the boundary condition (30), the radiative intensity is discontinuous between different unit cells and the discontinuity is more significant near the left boundary. In addition, the periodic boundary condition for  $I_1$  in the individual unit cell leads to large fluctuations near the four corners of the unit cell. The result with the boundary condition (31) is smoother because the  $I_1$  is solved in Li et al, HT-21-1051-19

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the whole domain. Finally, the reconstructed multiscale incident radiations are compared with the result of the fully-resolved simulation. The relative error of  $I_0$  is 12%, but the relative error of  $I^F$  with boundary condition (30) is 19%, which is even higher. On the contrary, the relative error of  $I^F$  with boundary condition (31) drops to 7.3%. The relative errors of  $I^F$  in each individual unit cell are also calculated and shown in Table 2. It can be seen that with the boundary condition (31), the error of  $I^F$  in each unit cell is reduced. With boundary condition (30), the relative errors in all the unit cells are large because of the fluctuations near the corners. In conclusion, boundary condition (31) is better than boundary condition (30). Therefore, boundary condition (31) will be chosen in the following simulations of this work, and the  $I_1$  will be solved in the whole domain.

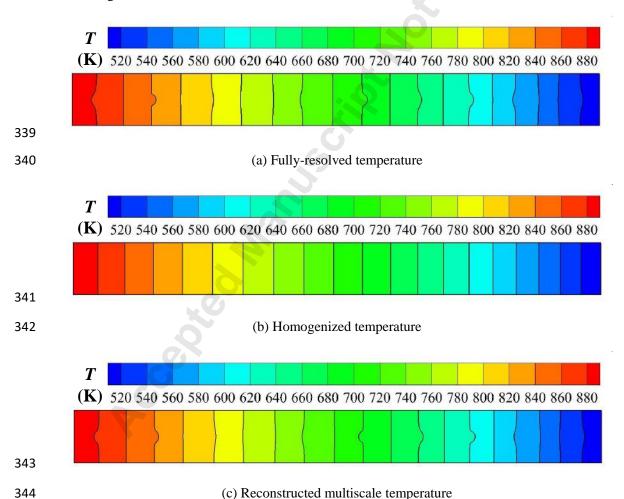
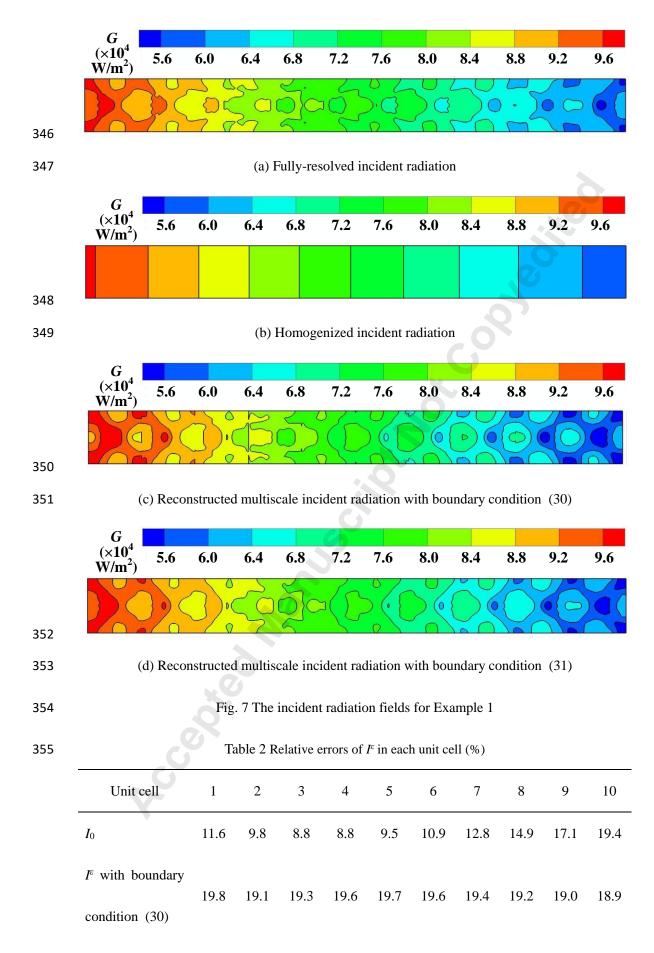


Fig. 6 The temperature fields for Example 1

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$I^{\varepsilon}$ with boundary										
	6.7	5.4	4.5	4.1	4.6	5.8	7.5	9.3	11.3	13.3
condition (31)										

Finally, as for the CPU time, the fully-resolved simulation takes 84229s (23.4h) to reach the  $10^{-8}$  convergence criterion. Using the same computer resources, the multiscale simulation consumes 1641s (27.4 min) in total with boundary condition (30) for  $I_1$ , which includes 98.2s for  $N_a$ , 234.5s for  $M_{\alpha\beta}$ , 70.7s for C, 476.7s for the homogenized conduction-radiation equations, 19.0s for the reconstruction of the multiscale temperature field, and 742.1s for the calculation of  $I_1$  and the reconstruction of the radiative intensity field. In addition, the boundary condition (31) consumes only 130.5s for the  $I_1$  and the reconstruction of the radiation field, which is more efficient. The reason is that this boundary condition prevents the iteration in each individual unit cell, compared with the boundary condition (30). Therefore, the proposed multiscale model can significantly

#### **4.3 Example 2**

Example 2 is similar to example 1, but the computational domain is composed of  $7\times7$  unit cells, and the temperatures of the up and bottom boundaries are specified as  $T_c$ , as shown in Fig. 8. The solutions of the unit cell problems are the same as those in Fig. 5. The temperature fields and the incident radiation fields of the fully-resolved simulation and the multiscale simulation are given in Fig. 9 and Fig. 10. For the calculation of  $I_1$ , the boundary condition (31) is used. It can be seen that the multiscale numerical model can reproduce the local temperature and radiation fluctuations caused by the TiO<sub>2</sub> particles.

improve the efficiency of the simulation and maintain the accuracy.

The relative error of the homogenized temperature field is 1.57%, and that of the reconstructed

second-order temperature field is 0.93%. It should be mentioned that the relative error of the first-order temperature field ( $T_0+\varepsilon T_1$ ) is only 0.66%, which is even lower. The reason is that the second-order derivatives near the top-left and bottom-left corners have large fluctuations due to the steep temperature gradient. The errors in each unit cell are also compared. It is found that the second-order temperature has lower errors except in the unit cells near the top-left and bottom-left corners. The plots of the errors are given in Figure S3, available in Supplemental Material, part of the ASME Digital Collection. These errors near the corners result in a higher error of the overall temperature field. As for the radiation field, the error of the homogenized radiation field is 10.6% and the error of the reconstructed multiscale radiation field drops to 6.6%. In addition, the computational time is reduced from 238.9h to 15.6min.

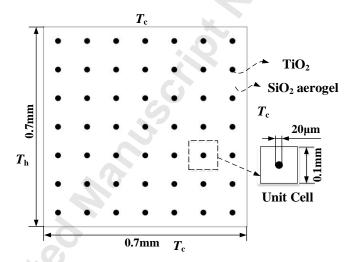
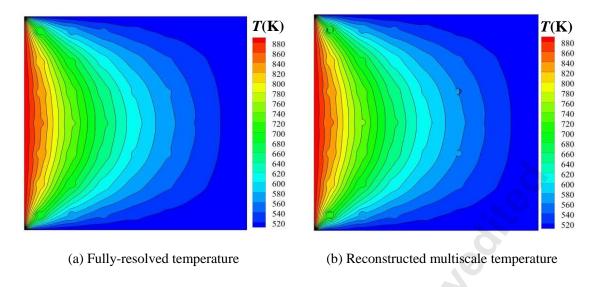


Fig. 8 The computational domain for Example 2



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Fig. 9 The temperature fields for Example 2

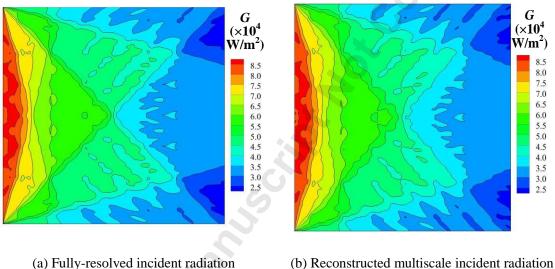


Fig. 10 The incident radiation fields for Example 2

## **4.4 Example 3**

In this example, anisotropic structures are generated by changing the circular TiO<sub>2</sub> particle in example 2 into elliptical particles. The lengths of the major axis and the minor axis of the elliptical particle are 95µm and 9µm. The particles are either horizontally aligned or 45° tilted, as shown in Fig. 11.

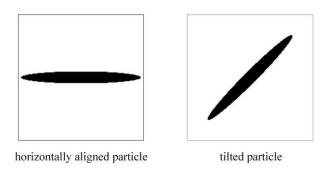


Fig. 11 The unit cells for Example 3

For the horizontally aligned particle, the solution of  $N_{\alpha}$  in the unit cell provides an effective thermal conductivity tensor:

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$$K_{ij} = \begin{bmatrix} 0.0567 & 0\\ 0 & 0.0301 \end{bmatrix} \text{Wm}^{-1} \text{K}^{-1}$$
 (41)

The tensor demonstrates that the heat conduction along the *x*-direction is stronger than that along the *y*-direction because the high-thermal-conductivity TiO<sub>2</sub> particle is elongated along the *x*-direction. The temperature and incident radiation fields of the fully-resolved simulation and the multiscale simulation are given in Fig. 12 and Fig. 13, respectively. The relative errors of the temperature and radiation fields are 12.4% and 5.6%. In addition, the multiscale numerical model reduces the computational time from 314.6h to 21.0min.

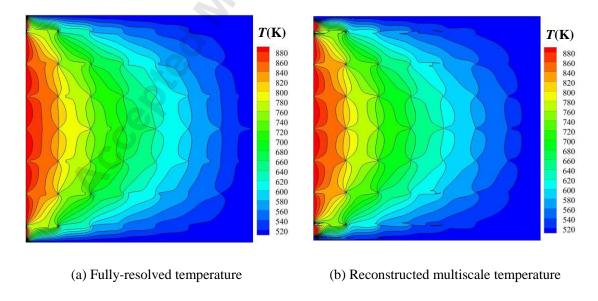


Fig. 12 The temperature fields for Example 3 with horizontally aligned particles

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(a) Fully-resolved incident radiation

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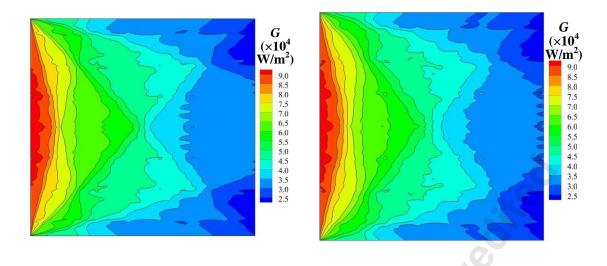


Fig. 13 The incident radiation fields for Example 3 with horizontally aligned particles

(b) Reconstructed multiscale incident radiation

As for the tiled particle, the effective thermal conductivity tensor calculated from the unit cell problem is:

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$$K_{ij} = \begin{bmatrix} 0.0343 & 0.0067 \\ 0.0067 & 0.0343 \end{bmatrix} \text{Wm}^{-1} \text{K}^{-1}$$
 (42)

It can be found that the principal directions of the thermal conductivity are 45° and 135°, which are consistent with the structure of the unit cell. The corresponding principal values of the thermal conductivity are 0.0410 Wm<sup>-1</sup>K<sup>-1</sup> and 0.0276 Wm<sup>-1</sup>K<sup>-1</sup>. The simulation results of the temperature and incident radiation fields are given in Fig. 14 and Fig. 15. The relative errors of the temperature and radiation fields are 10.1% and 3.0%. The computational time of the multiscale simulation is 14.7min while the fully-resolved simulation costs 364h. Finally, it can be seen that the multiscale simulation can reproduce the anisotropic effects of the elliptical particles in this problem. It can provide the detailed temperature and radiation information in the local structures and save the computational time.

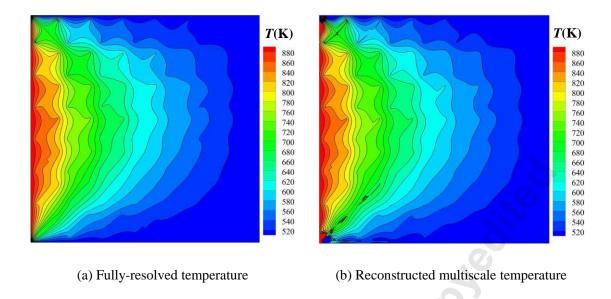


Fig. 14 The temperature fields for Example 3 with tilted particles

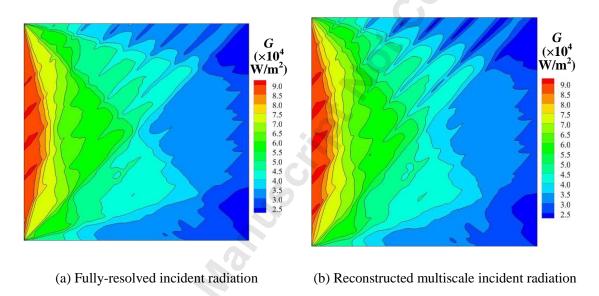


Fig. 15 The incident radiation fields for Example 3 with tilted particles

#### 5. Conclusions

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In the above sections, the homogenization analysis has been extended to the steady-state heat conduction and radiative transfer equations. Both the macroscopic homogenized equations and the unit cell problems are obtained. The multiscale algorithm is also proposed for the coupled conduction-radiation heat transfer problems in periodic composite materials. The main conclusions are as follows.

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1) The macroscopic homogenized heat conduction and radiative transfer equations have the same forms as the traditional equations. The effective thermal conductivity is related to the solution of  $N_{\alpha}$ in the unit cell. As for the radiation, the effective absorption and extinction coefficients and the effective product of scattering coefficient and phase function are the volumetric averages of the corresponding coefficients in the unit cell. 2) The analysis provides a second-order approximation of the temperature field and a first-order approximation of the radiative intensity field, which can be reconstructed from the results of the homogenized equations and the unit cell problems. 3) The heat transfer processes in the SiO<sub>2</sub> aerogel doped with TiO<sub>2</sub> particles are simulated by the proposed multiscale method. It is demonstrated that the method can be used in both the isotropic and anisotropic unit cell geometries. The reconstructed temperature and radiative intensity fields can reproduce the local fluctuations due to the microscale structures. 4) Compared with the results of the fully-resolved simulations, the multiscale method can provide accurate temperature and radiative intensity fields, and can significantly increase the efficiency of the simulations. 5) It is also found that for the unit cell problem of radiative transfer, solving  $I_1$  in the whole domain can provide better multiscale radiation results than solving  $I_1$  in each unit cell individually with periodic boundary condition. As for applications of the model, microscale visualization methods such as the X-ray computed tomography or the scanning electron microscope can be used to reconstruct unit cells of composite materials [5]. The thermal conductivities and radiation coefficients can be obtained from

experiments or existing literature. Then, the proposed method is used to model the coupled

- 450 conduction-radiation heat transfer in the materials.
- The present research extends the homogenization of heat conduction equation into the coupled
- 452 heat conduction and radiative transfer equations. Further researches are still needed to improve the
- proposed multiscale method. Some of the considerations are as follows.
- 1) The present analysis focuses on the steady-state conduction and radiation heat transfer
- 455 problems with constant thermal properties. The unit cell problems of the temperature need to be
- 456 solved only once during multiscale simulations. When the multiscale model is used in unsteady
- 457 problems with temperature-related material properties, the unit cell problems need to be repetitively
- 458 solved under different temperatures. The speed-up of the multiscale method should be further
- 459 studied.
- 460 2) To calculate  $I_1$  in a whole domain is inconvenient for applications because a fully-resolved
- mesh is needed. More researches on the boundary conditions of the unit cell problems for  $I_1$  should
- 462 be carried out.
- 463 3) Although the  $T_0$  satisfies the boundary condition Eq. (3), the  $T_1$  and  $T_2$  will introduce errors to
- 464 the boundary. Therefore, the present asymptotic expansion of  $T^{\epsilon}$  does not exactly satisfy the
- boundary condition. In order to solve this problem, boundary layer solutions should be included in
- 466 the future [17,21,22].

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545	List of Figure Captions
546	Fig. 1 A sketch of the problem in this work
547	Fig. 2 The computational procedure of the multiscale numerical model
548	Fig. 3 The comparison between the effective thermal conductivities predicted by the multiscale
549	model and the theoretical correlation
550	Fig. 4 The computational domain for Example 1
551	Fig. 5 The results of $N_{\alpha}$ , $M_{\alpha\beta}$ and $C$ in the unit cell for Example 1
552	Fig. 6 The temperature fields for Example 1
553	Fig. 7 The incident radiation fields for Example 1
554	Fig. 8 The computational domain for Example 2
555	Fig. 9 The temperature fields for Example 2
556	Fig. 10 The incident radiation fields for Example 2
557	Fig. 11 The unit cells for Example 3
558	Fig. 12 The temperature fields for Example 3 with horizontally aligned particles
559	Fig. 13 The incident radiation fields for Example 3 with horizontally aligned particles
560	Fig. 14 The temperature fields for Example 3 with tilted particles
561	Fig. 15 The incident radiation fields for Example 3 with tilted particles
562	Figure S1 The effective thermal conductivities for different grid sizes
563	Figure S2 The first-order corrections of the incident radiation, $G_1$ , for Example 1
564	Figure S3 The comparison between the errors of the reconstructed first-order and second-order
565	temperatures in different unit cells (The location of the unit cell is numbered as (column, row) for
566	convenience)

567	List of Table Captions
568	Table 1 Properties of the materials
569	Table 2 Relative errors of $I^{\epsilon}$ in each unit cell (%)
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# **Supplementary Material** 572 573 A multiscale method for coupled steady-state heat conduction and radiative 574 transfer equations in composite materials 575 576 Zi-Xiang Tonga, Ming-Jia Li\*b, Yi-Si Yub, Jing-Yu Guob 577 <sup>a</sup> School of Human Settlements and Civil Engineering, Xi'an Jiaotong University, Xi'an, Shaanxi, 578 710049, China 579 <sup>b</sup> Key Laboratory of Thermo-Fluid Science and Engineering of Ministry of Education, School of 580 Energy & Power Engineering, Xi'an Jiaotong University, Xi'an, Shaanxi, 710049, China 581 \*Corresponding author email: mjli1990@xjtu.edu.cn 582

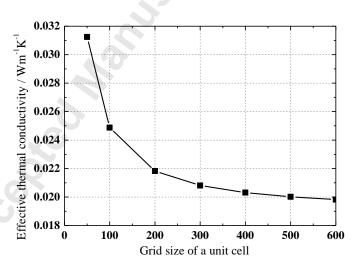


Figure S1 The effective thermal conductivities for different grid sizes

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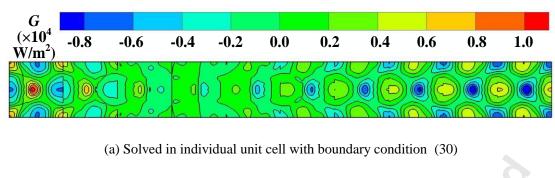
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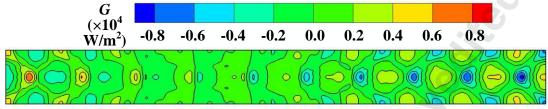
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(b) Solved in the whole domain with boundary condition (31)

Figure S2 The first-order corrections of the incident radiation,  $G_1$ , for Example 1

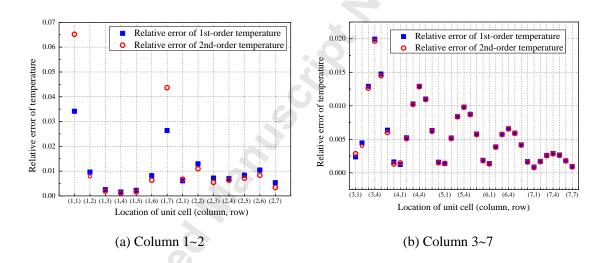


Figure S3 The comparison between the errors of the reconstructed first-order and second-order temperatures in different unit cells (The location of the unit cell is numbered as (column, row) for convenience)

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