



ME 1071: Applied Fluids

Lecture 10 Introduction to Compressible Flow

Spring 2021

Weekly Study Plan



Weeks	Dates	Lectures
1	Mar. 9	Course Introduction, Fluids Review
2	Mar. 16	Chapter 8: Internal Incompressible Viscous Flow
3	Mar. 23	Chapter 8: Internal Incompressible Viscous Flow
4	Mar. 30	Chapter 8/Exam I Review
5	Apr. 6	Exam I
6	Apr. 13	Chapter 9: External Incompressible Viscous Flow
7	Apr. 20	Chapter 9: External Incompressible Viscous Flow
8	Apr. 25	Chapter 11: Flow in Open Channels
9	Apr. 27	Chapter 11: Flow in Open Channels
10	May. 11	Exam II Review
11	May. 18	Exam II
12	May. 25	Chapter 12: Introduction to Compressible Flow
13	Jun. 1	Chapter 12: Introduction to Compressible Flow
14	Jun. 8	Chapter 12: Introduction to Compressible Flow
15	Jun. 15	Chapter 5: CFD Related Topics
16	Jun. 22	Final Exam Review (Final Exam at Jun. 26)

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Outlines



- **When is a flow Compressible?**
- **Critical Conditions**
- **Basic Equations for One-Dimensional Compressible Flow**
- **Isentropic Flow**
 - Area Change
 - Subsonic/Supersonic Flow
- **Choked Flow**

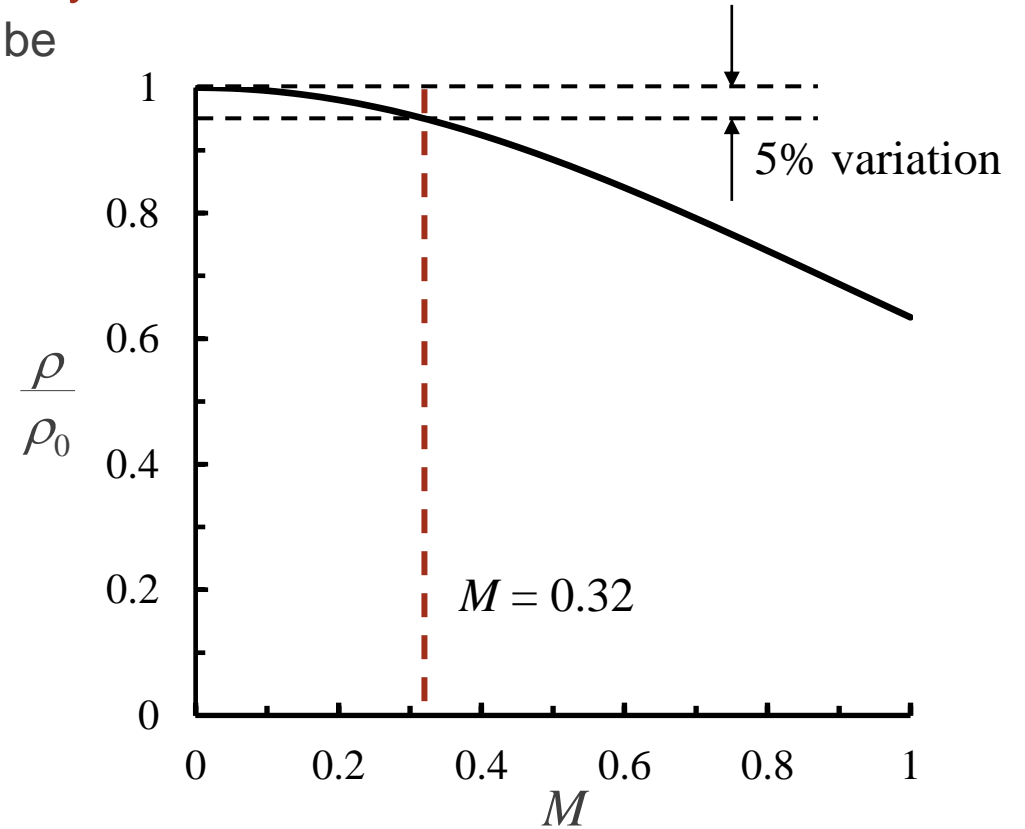
When Is a Flow Compressible?



- Compressible flow: fluid density changes **significantly**.
 - The relation between density and Mach number can be described by:

$$\frac{\rho_0}{\rho} = \left(1 + \frac{k-1}{2} M^2\right)^{1/(k-1)}$$

- To ensure density change $< 5\%$, M must be less than 0.3.
- When $M < 0.3$, the flow can be treated as incompressible; otherwise, the compressibility must be considered.



Isentropic variation of density with Mach number

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When Is a Flow Compressible?



- **Example**

- Consider the flow of air through a nozzle starting in the reservoir at nearly zero velocity and standard sea level values of $p_0 = 1 \text{ atm}$ and $T_0 = 288 \text{ K}$, and expanding to a velocity of 107 m/s at the nozzle exit. Calculate the pressure at the nozzle exit assuming first incompressible flow and then compressible flow.

How about expanding to a velocity of 275 m/s ?

incompressible

From Bernoulli's equation

$$p = p_0 - \frac{1}{2} \rho_0 V^2 = p_0 - \frac{1}{2} \frac{p_0}{RT_0} V^2 = 101325 - 0.5 \frac{101325}{287 \times 288} 107^2 = 94307 \text{ Pa}$$

54972 Pa

compressible

$$T = T_0 - \frac{V^2}{2c_p} = 288 - \frac{107^2}{2(1.4 \times 287 / (1.4 - 1))} = 282.3 \text{ K}$$

250.4 K

$$p = p_0 \left(\frac{T}{T_0} \right)^{k/(k-1)} = 101325 \left(\frac{282.3}{288} \right)^{3.5} = 94478 \text{ Pa}$$

88096 Pa

$$M = V / c = V / \sqrt{kRT} = 107 / \sqrt{1.4 \times 287 \times 282.3} = 0.317$$

0.866

The flow can be treated as incompressible.

The flow is compressible.

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Critical Conditions



- **Sonic condition (音速状态) / Critical Condition**

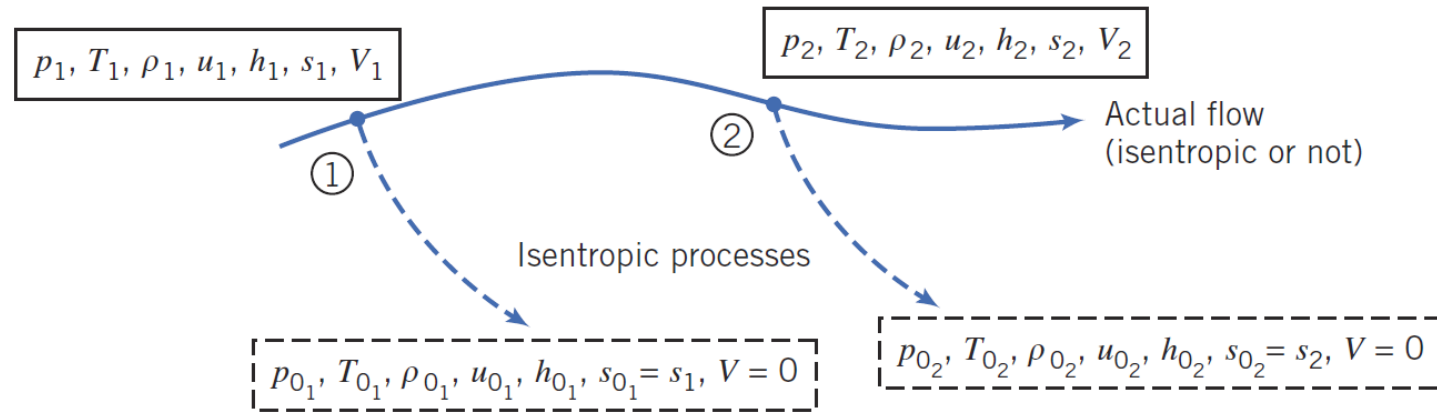
- The condition that the velocity of fluid element **adiabatically or isentropically** approaches to sonic velocity ($M = 1$).

$$\boxed{h, T} \xrightarrow{\text{Approaches adiabatically}} \boxed{h^*, T^*}$$

$$\frac{T^*}{T_0} = \frac{2}{k+1} \quad c^* = \sqrt{kRT^*} = \sqrt{\frac{2k}{k+1} RT_0}$$

$$\boxed{p, \rho} \xrightarrow{\text{Approaches isentropically}} \boxed{p^*, \rho^*}$$

$$\frac{p^*}{p_0} = \left(\frac{2}{k+1}\right)^{k/(k-1)} \quad \frac{\rho^*}{\rho_0} = \left(\frac{2}{k+1}\right)^{1/(k-1)}$$



Local isentropic stagnation properties.

The critical conditions are similar to the stagnation conditions, except that the final velocity is brought to **sonic velocity ($M = 1$)** instead of zero velocity.

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- When is a flow Compressible?
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Introduction

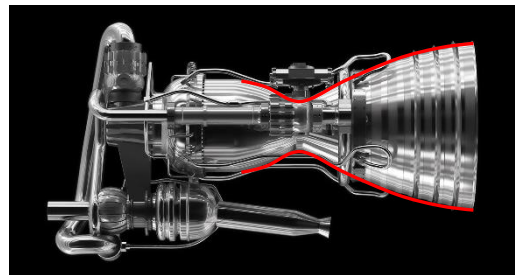


- **Compressible Flow Through Ducts (槽道)**

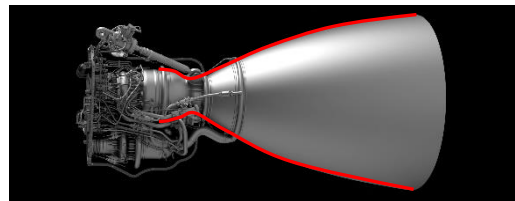
- Nozzle (喷管): A duct to increase the flow velocity in the expense of pressure or internal energy.
- Diffuser (扩压器): A duct to decrease the flow velocity.
- Wind tunnel (风洞): combination of nozzles and diffusers to provide uniform supersonic flow for testing.
- **Quasi-one-dimensional flow (准一维流动)**: one with varied cross-sectional area in which all variables vary primarily along one direction.



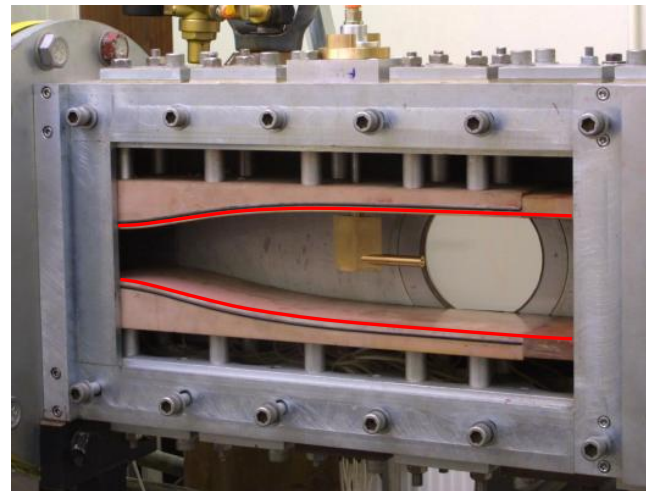
SpaceX's Merlin Engines in Falcon Heavy



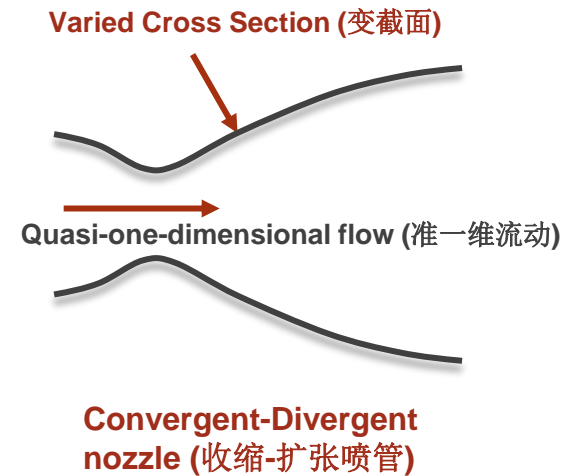
SpaceX's Merlin Engine



SpaceX's Raptor Engine



Supersonic Wind Tunnel of Imperial College London



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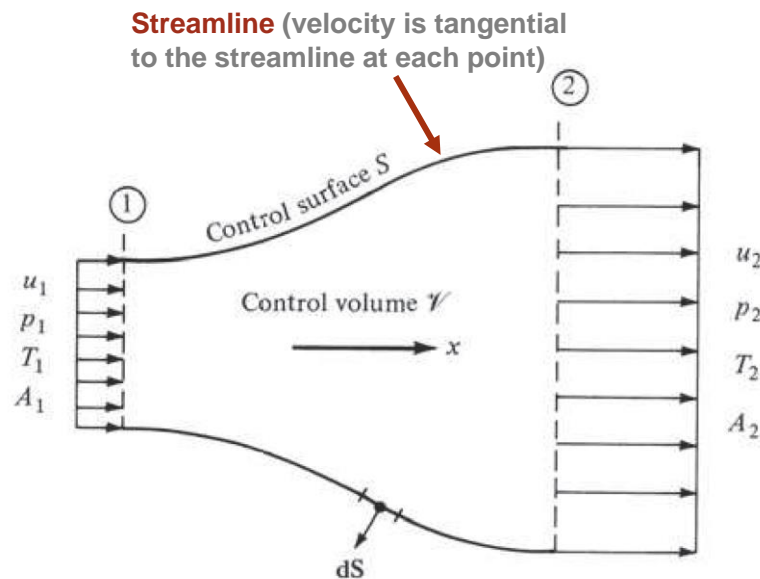
Basic Equations for One-Dimensional Compressible Flow



- **Quasi-one-dimensional flow**

- Flow properties are uniform across any cross section at a given x station.
- The slope/gradient of the changes in area is small and smooth.

- **Continuity Equation**



- **Assumptions**

- Steady flow, $\partial / \partial t = 0$.
- Adiabatic.
- No viscous effects.
- No body forces, $\mathbf{f} = 0$.
- **Quasi-one-dimensional flow**
- ~~$M_1 \geq 1$~~ (not required)

Integration over the surface of the control volume

$$\oint_S \rho \mathbf{V} \cdot d\mathbf{S} = 0$$

$$-\rho_1 u_1 A_1 + 0 + \rho_2 u_2 A_2 + 0 = 0$$

$$\rho_1 u_1 A_1 = \rho_2 u_2 A_2$$

Continuity equation for Quasi-one-dimensional flow

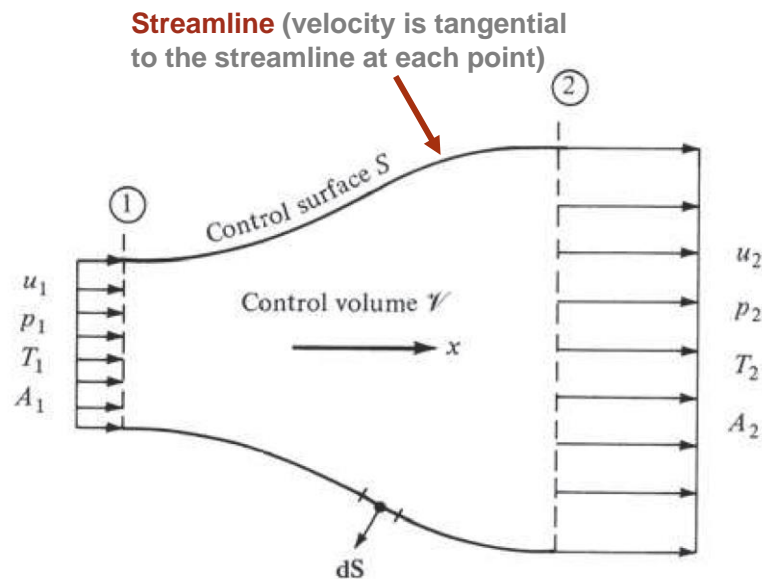
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Basic Equations for One-Dimensional Compressible Flow



• Momentum Equation

- Only one direction, x .
- dA is the x component of the vector $d\mathbf{S}$.
- Additional pressure force term due to area variation.



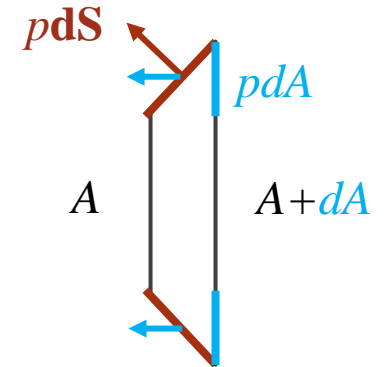
$$\oint_S (\rho \mathbf{V} \cdot d\mathbf{S}) \mathbf{V} = - \oint_S p d\mathbf{S}$$

$$\oint_S (\rho \mathbf{V} \cdot d\mathbf{S}) u = - \oint_S (p dS)_x$$

$$-\rho_1 u_1 A_1 u_1 + 0 + \rho_2 u_2 A_2 u_2 + 0 = -(-p_1 A_1 + p_2 A_2 - \int_{A_1}^{A_2} p dA)$$

$$p_1 A_1 + \rho_1 u_1^2 A_1 + \int_{A_1}^{A_2} p dA = p_2 A_2 + \rho_2 u_2^2 A_2$$

Momentum equation for Quasi-one-dimensional flow



For upper and lower surface

$$- \oint_S (p dS)_x = - \int_{A_1}^{A_2} p dA$$

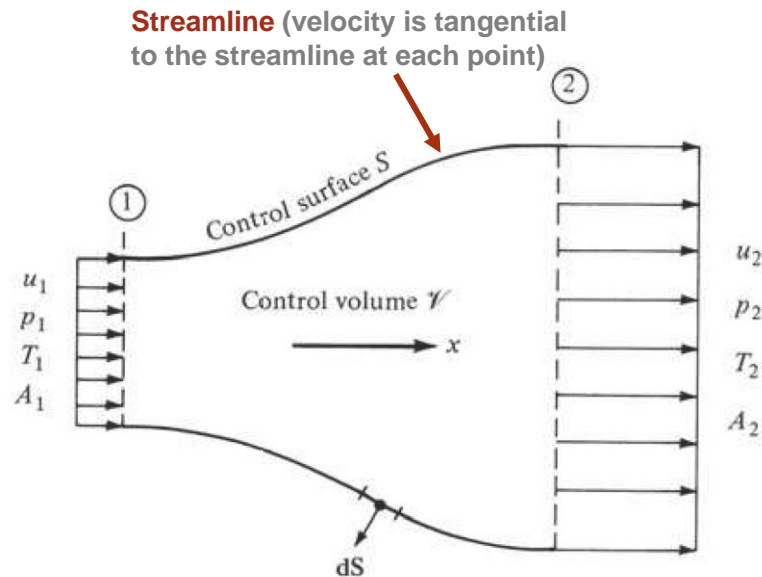
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Basic Equations for One-Dimensional Compressible Flow



• Energy Equation

- The general result for steady, inviscid, adiabatic flow with the total enthalpy being constant.



Energy conservation

$$\oint_S (\rho \mathbf{V} \cdot d\mathbf{S}) \left(e + \frac{V^2}{2} \right) = - \oint_S (p d\mathbf{S}) \cdot \mathbf{V}$$

$$-\rho_1 u_1 A_1 \left(e_1 + \frac{u_1^2}{2} \right) + \rho_2 u_2 A_2 \left(e_2 + \frac{u_2^2}{2} \right) = -(-\rho_1 u_1 A_1 + \rho_2 u_2 A_2)$$

Continuity

$$h_1 + \frac{u_1^2}{2} = h_2 + \frac{u_2^2}{2}$$

Energy equation for Quasi-one-dimensional flow

$$h_{01} = h_{02} \rightarrow T_{01} = T_{02}$$

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Basic Equations for One-Dimensional Compressible Flow



- **Continuity**

$$\rho_1 u_1 A_1 = \rho_2 u_2 A_2$$

- **Momentum**

$$p_1 A_1 + \rho_1 u_1^2 A_1 + \int_{A_1}^{A_2} p dA = p_2 A_2 + \rho_2 u_2^2 A_2$$

- **Energy**

$$h_1 + \frac{u_1^2}{2} = h_2 + \frac{u_2^2}{2}$$

- **Enthalpy**

$$h_2 = c_p T_2$$

- **Equation of state**

$$p_2 = \rho_2 R T_2$$

- **Assumptions**

- Steady flow, $\partial / \partial t = 0$.
- Adiabatic.
- No viscous effects.
- No body forces, $\mathbf{f} = 0$.
- Quasi-one-dimensional flow
- ~~$M_1 > 1$~~ (not required)
- Area changes are prescribed as $A(x)$.

Five equations with five unknowns.

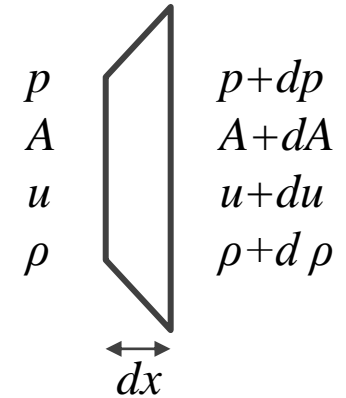
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Basic Equations for One-Dimensional Compressible Flow



• Governing Equations in Differential Form (微分形式的控制方程)

- Convert the five governing equations in integral form to differential form



Momentum

$$p_1 A_1 + \rho_1 u_1^2 A_1 + \int_{A_1}^{A_2} p dA = p_2 A_2 + \rho_2 u_2^2 A_2$$

$$pA + \rho u^2 A + p dA = (p + dp)(A + dA) + (\rho + d\rho)(u + du)^2 (A + dA)$$

$$A dp + Au^2 d\rho + \rho u^2 dA + 2\rho u A du = 0$$

$$d(\rho u A) = 0$$

$$u^2 A d\rho + \rho u A du + \rho u^2 dA = 0$$

$$dp = -\rho u du \quad \text{Euler's equation}$$

Continuity

$$\rho_1 u_1 A_1 = \rho_2 u_2 A_2$$

$$\rho u A = \text{const}$$

$$d(\rho u A) = 0$$

$$d(\rho u) = 0$$

One-dimensional Flow

Energy

$$h_1 + \frac{u_1^2}{2} = h_2 + \frac{u_2^2}{2}$$

$$h + \frac{u^2}{2} = \text{const}$$

$$dh + u du = 0$$

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Isentropic Flow



• Area-velocity relation

- Further simplify the differential equations to obtain some physical insights into the quasi-one-dimensional flow.

Continuity $d(\rho u A) = 0$

$u A d\rho + \rho A du + \rho u dA = 0$

$\frac{d\rho}{\rho} + \frac{du}{u} + \frac{dA}{A} = 0$

$M < 1$

u increasing u decreasing

Euler's equation $dp = -\rho u du$

Isentropic assumption

$\frac{dp}{\rho} = \frac{dp}{d\rho} \frac{d\rho}{\rho} = -u du$

$\frac{dp}{d\rho} \equiv \left(\frac{\partial p}{\partial \rho} \right)_s = a^2$

$\frac{d\rho}{\rho} = -\frac{u^2}{a^2} \frac{du}{u} = -M^2 \frac{du}{u}$

Area-velocity relation

$\frac{dA}{A} = (M^2 - 1) \frac{du}{u}$

- $M < 1$, subsonic flow, $du \propto -dA$
- $M > 1$, supersonic flow, $du \propto dA$
- $M = 1$, $dA = 0$, minimum area
- $M = 0$, incompressible flow, $Au = \text{constant}$.

$M > 1$

u increasing u decreasing

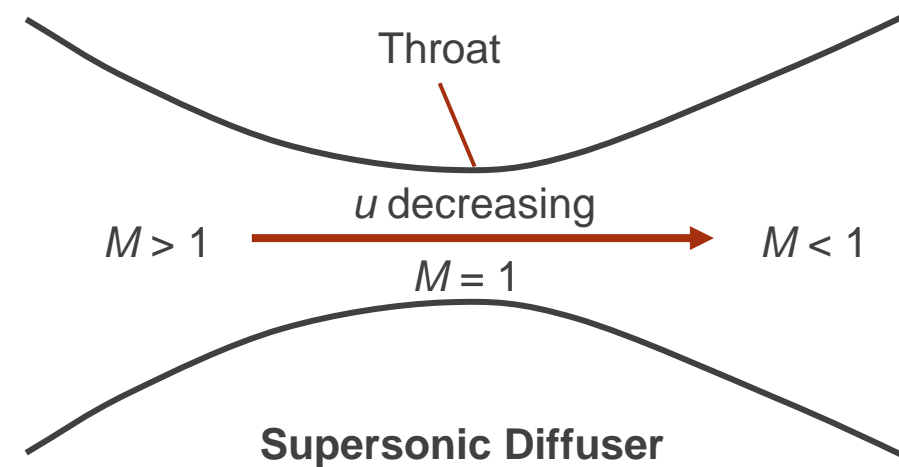
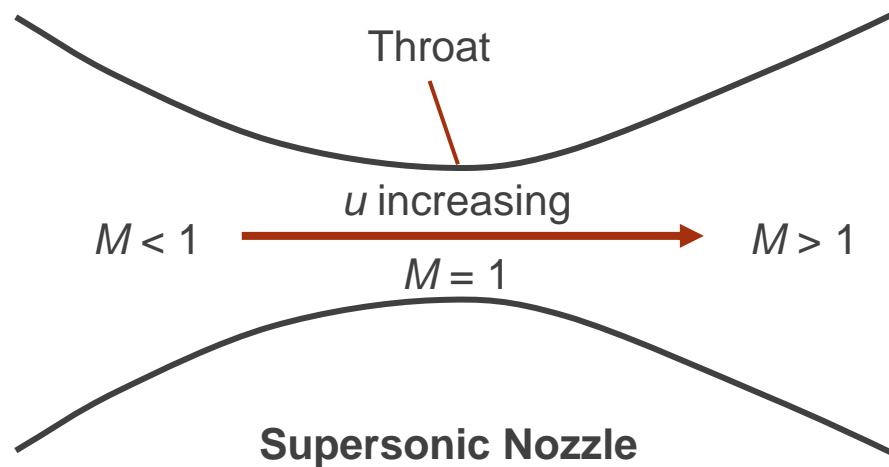
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Governing Equations for Quasi-One-Dimensional Flow



- **Operation of Convergent-Divergent duct**

- Throat (喉道): the minimum area of the convergent-divergent duct.
- Supersonic Nozzle : convergent-divergent duct operated with a subsonic inflow ($M < 1$).
- Supersonic Diffuser: convergent-divergent duct operated with a supersonic inflow ($M > 1$).
- Supersonic nozzle or supersonic diffuser **depends on inflow Mach number**.



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Isentropic Flows



• Area-Mach number relation

- The ratio of A^* and A can be express as a function of Mach number in nozzle flows (inflow Mach number $M < 1$).

$$\rho^* u^* A^* = \rho u A$$

$$\frac{A}{A^*} = \frac{\rho^*}{\rho} \frac{u^*}{u} = \frac{\rho^*}{\rho_0} \frac{\rho_0}{\rho} \frac{c^*}{u}$$

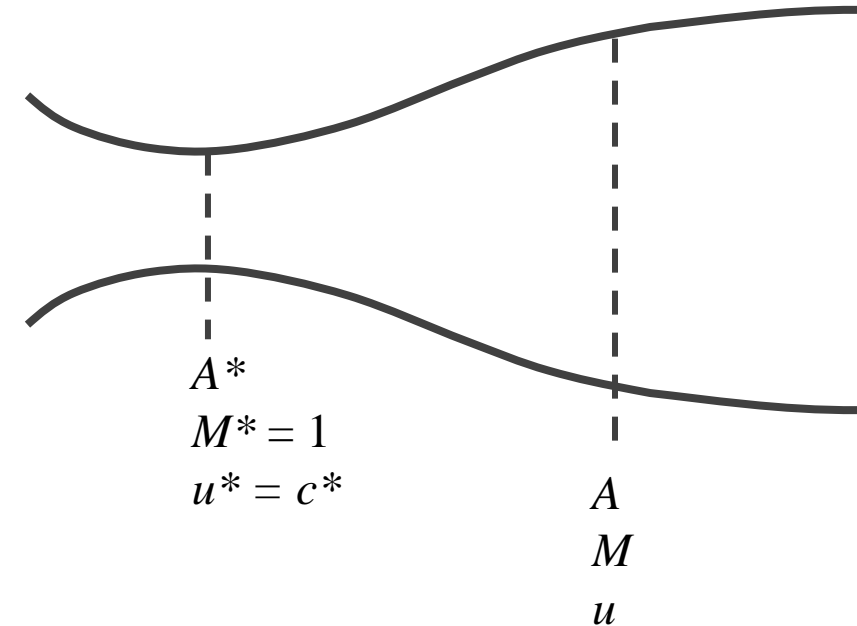
$$\left(\frac{A}{A^*}\right)^2 = \left(\frac{\rho^*}{\rho_0}\right)^2 \left(\frac{\rho_0}{\rho}\right)^2 \left(\frac{c^*}{u}\right)^2$$

$$\left(\frac{A}{A^*}\right)^2 = \frac{1}{M^2} \left[\frac{2}{k+1} \left(1 + \frac{k-1}{2} M^2 \right) \right]^{(k+1)/(k-1)}$$

$$\frac{\rho^*}{\rho_0} = \left(\frac{2}{k+1} \right)^{1/(k-1)}$$

$$\frac{\rho_0}{\rho} = \left(1 + \frac{k-1}{2} M^2 \right)^{1/(k-1)}$$

$$M^{*2} = \frac{(k+1)M^2}{2+(k-1)M^2}$$



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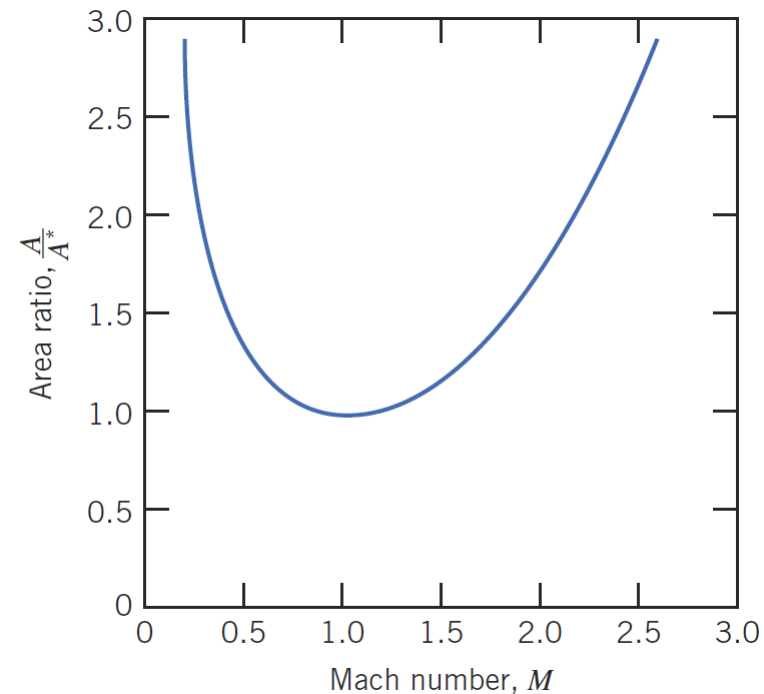
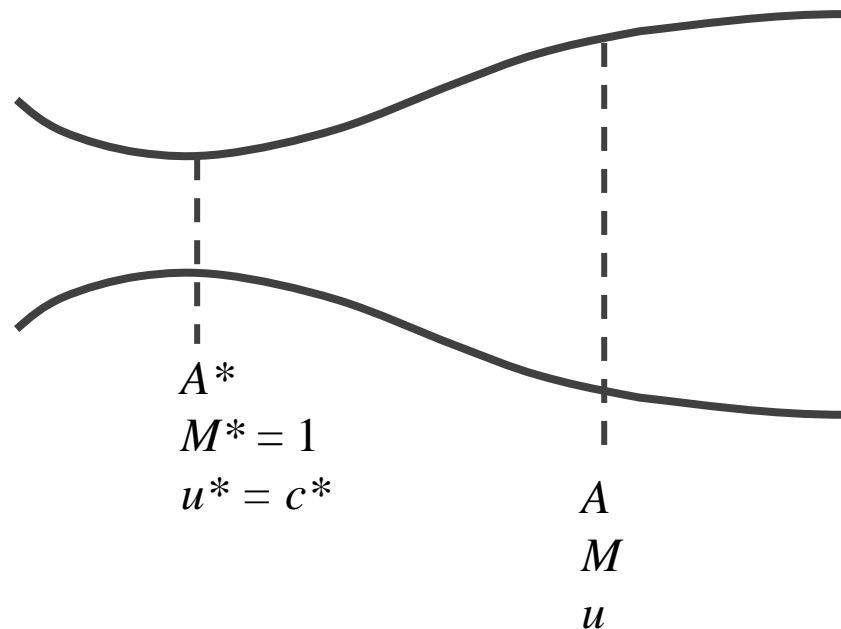
Isentropic Flows



- **Area-Mach number relation**

- The ratio of A^* and A can be expressed as a function of Mach number in nozzle flows (inflow Mach number $M < 1$).

$$\left(\frac{A}{A^*}\right)^2 = \frac{1}{M^2} \left[\frac{2}{k+1} \left(1 + \frac{k-1}{2} M^2 \right) \right]^{(k+1)/(k-1)}$$



The Mach number inside a supersonic nozzle is a function of area ratio only!

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Isentropic Flows



Example

Air flows isentropically in a channel. At section (1) the Mach number is 0.3, the area is 0.001 m², and the absolute pressure and the temperature are 650 kPa and 62°C, respectively. At section (2), the Mach number is 0.8. Evaluate the properties at section (2).

$$T_{0_1} = T_1 \left(1 + \frac{k-1}{2} M_1^2 \right) = T_{0_2}$$

$$p_{0_1} = p_1 \left[1 + \frac{k-1}{2} M_1^2 \right]^{k(k-1)} = p_{0_2} \quad p_2 = \frac{p_{0_2}}{\left[1 + \frac{k-1}{2} M_1^2 \right]^{k(k-1)}}$$

$$T_2 = \frac{T_{0_2}}{\left(1 + \frac{k-1}{2} M_1^2 \right)}$$

$$\rho_2 = \frac{p_2}{RT_2} \quad V_2 = M_2 c_2 = M_2 \sqrt{kRT_2}$$

$$\frac{A_2}{A_1} = \frac{A_2 A^*}{A^* A_1} = \left\{ \frac{1}{M_2} \frac{\left[1 + \frac{k-1}{2} M_2^2 \right]^{\frac{k+1}{2(k-1)}}}{\frac{k+1}{2}} \right\} / \left\{ \frac{1}{M_1} \frac{\left[1 + \frac{k-1}{2} M_1^2 \right]^{\frac{k+1}{2(k-1)}}}{\frac{k+1}{2}} \right\}$$

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Choked Flow



• The Flow Rate of an Isentropic Flow with Area Variation

- The limiting of the mass flow rate is called choking of the flow, this happens when the Mach number at the throat equals to 1.

$$\dot{m}_{\text{choked}} = \rho^* c^* A_e$$

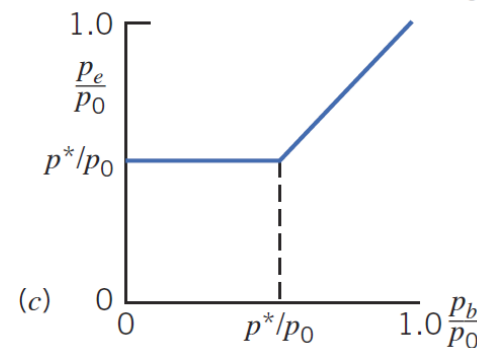
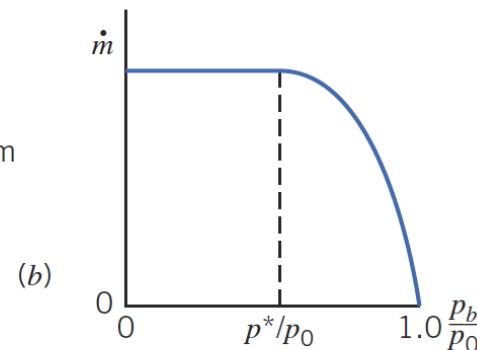
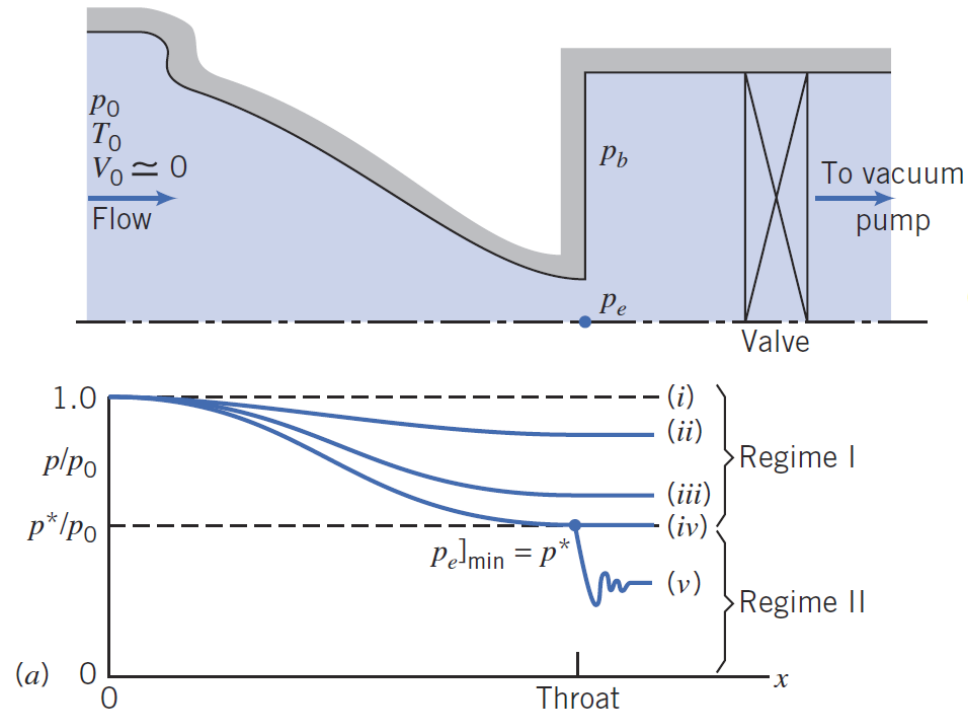
$$c^* = \sqrt{kRT^*} = \sqrt{\frac{2k}{k+1} RT_0}$$

$$\dot{m}_{\text{choked}} = A_e p^* \sqrt{\frac{k}{RT^*}}$$

$$\left. \frac{p_e}{p_0} \right|_{\text{choked}} = \frac{p^*}{p_0} = \left(\frac{2}{k+1} \right)^{k/(k-1)}$$

$$\frac{T^*}{T_0} = \frac{2}{k+1}$$

$$\dot{m}_{\text{choked}} = A_e p_0 \sqrt{\frac{k}{RT_0}} \left(\frac{2}{k+1} \right)^{(k+1)/2(k-1)}$$

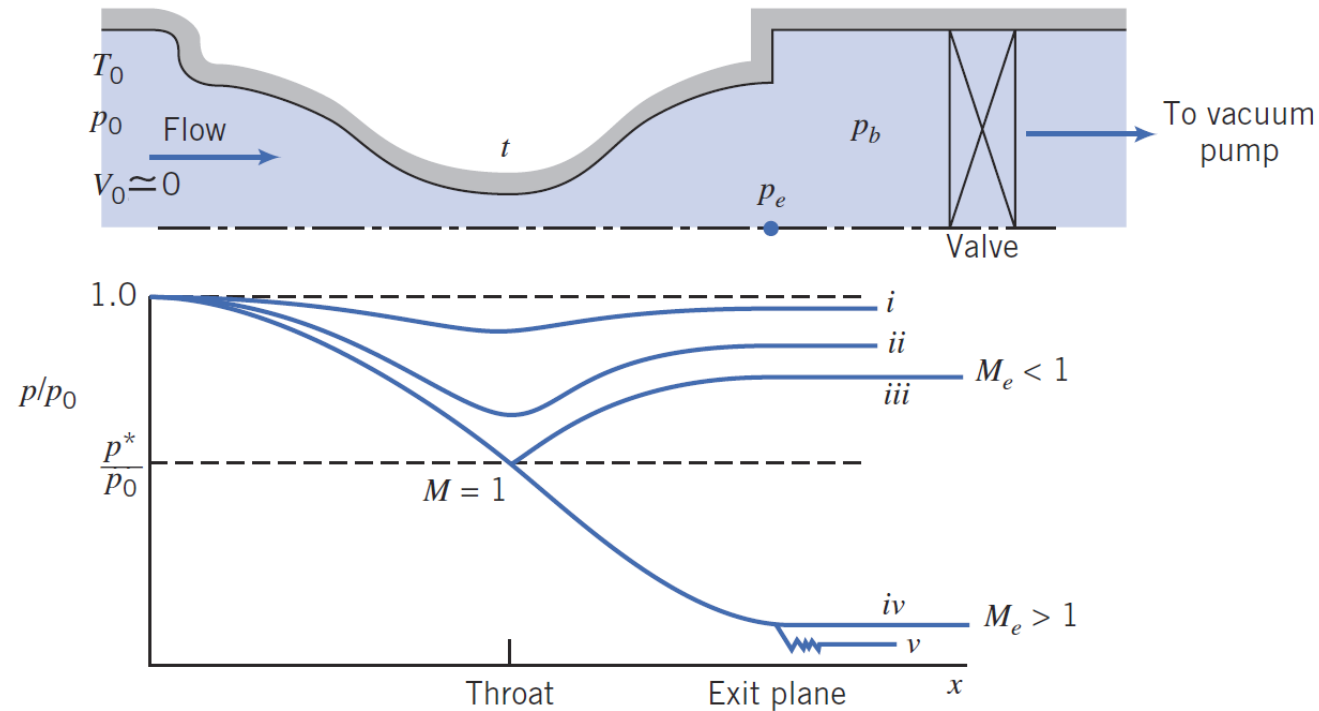


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Choked Flow



- **Throat:** the minimum area of the convergent-divergent duct.



$$\dot{m}_{\text{choked}} = A_t p_0 \sqrt{\frac{k}{RT_0} \left(\frac{2}{k+1} \right)^{(k+1)/2(k-1)}}$$

Pressure distributions for isentropic flow in a converging-diverging nozzle.

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Homework



Problem 12.34

Consider steady, adiabatic flow of air through a long straight pipe with $A = 0.05 \text{ m}^2$. At the inlet the air is at 200 kPa, 60°C and 146 m/s. Downstream at section 2, the air is at 95.6 kPa and 280 m/s. Determine $p_{01}, p_{02}, T_{01}, T_{02}$ and the entropy change for the flow.

$$\frac{dQ}{dm} = h_{02} - h_{01} = 0$$
$$h_{02} - h_{01} = c_p(T_{02} - T_{01}) = 0$$

$$h_1 + \frac{V_1^2}{2} = h_2 + \frac{V_2^2}{2} = h_{01} = h_{02}$$
$$\rho_1 V_1 A = \rho_2 V_2 A$$

$$s_2 - s_1 = c_p \ln \frac{T_2}{T_1} - R \ln \frac{P_2}{P_1}$$
$$s_{02} - s_{01} = -R \ln \frac{P_{02}}{P_{01}}$$

$$\frac{p_0}{p} = \left[1 + \frac{k-1}{2} M^2 \right]^{k/(k-1)}$$

$$\frac{T_0}{T} = 1 + \frac{k-1}{2} M^2$$

$$\frac{\rho_0}{\rho} = \left[1 + \frac{k-1}{2} M^2 \right]^{1/(k-1)}$$

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Homework



Problem 12.38

Air flows from the atmosphere into an evacuated tank through a convergent nozzle of 38 *mm* tip diameter. If atmospheric pressure and temperature are 101.3 kPa and 15 °C, respectively, what vacuum must be maintained in the tank to produce sonic velocity in the jet? What is the flow rate? What is the flow rate when the vacuum is 254 *mm* of mercury?

$$Vac = (P_0 - P) \times \frac{760 \text{ mm}}{101.3 \text{ kPa}}$$

$$c = \sqrt{kRT} = V$$

$$\dot{m} = \rho VA$$

$$h_0 = h + \frac{1}{2} V^2$$

$$\dot{m} = \rho VA$$

$$\frac{p_0}{p} = \left[1 + \frac{k-1}{2} M^2 \right]^{k/(k-1)}$$

$$\frac{T_0}{T} = 1 + \frac{k-1}{2} M^2$$

$$\frac{\rho_0}{\rho} = \left[1 + \frac{k-1}{2} M^2 \right]^{1/(k-1)}$$

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Homework



Problem 12.43

Nitrogen flows through a diverging section of duct with $A_1 = 0.15 \text{ m}^2$ and $A_2 = 0.45 \text{ m}^2$. If $M_1 = 0.7$ and $P_1 = 450 \text{ kPa}$, find M_2 and P_2 .

$$p_{0_1} = p_{0_2}$$

$$A_1^* = A_2^*$$

$$\frac{p_0}{p} = \left[1 + \frac{k-1}{2} M^2 \right]^{k/(k-1)}$$

$$\frac{T_0}{T} = 1 + \frac{k-1}{2} M^2$$

$$\frac{\rho_0}{\rho} = \left[1 + \frac{k-1}{2} M^2 \right]^{1/(k-1)}$$

$$\frac{A}{A^*} = \frac{1}{M} \left[\frac{1 + \frac{k-1}{2} M^2}{\frac{k+1}{2}} \right]^{(k+1)/2(k-1)}$$

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Homework



Problem 12.46

Air, at an absolute pressure of 60.0 kPa and 27°C enters a passage at 486 m/s, where $A = 0.02 \text{ m}^2$. At section 2 downstream, $p = 78.8 \text{ kPa}$. Assuming isentropic flow, calculate the Mach number at section 2. Sketch the flow passage.

$$p_{0_1} = p_{0_2}$$

$$c = \sqrt{kRT}$$

$$M_1 = \frac{V_1}{c_1}$$

$$\frac{p_0}{p} = \left[1 + \frac{k-1}{2} M^2 \right]^{k/(k-1)}$$

$$\frac{T_0}{T} = 1 + \frac{k-1}{2} M^2$$

$$\frac{\rho_0}{\rho} = \left[1 + \frac{k-1}{2} M^2 \right]^{1/(k-1)}$$

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Homework



This assignment is due by **6pm on June 3rd**.

- Upload your solution to BB.
- You can either type your solution out using a word editor like Microsoft Word or clearly hand write the information and then copy/scan your solution to a digital file.