TiO Properties

October 13, 2020

1 MATSE 580 Homework 1

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Thermodynamics of a binary system: Ti - O

Data from: A. Watson and T. Markus, Eds., "Ternary System Fe-Mo-Ti: Datasheet from Landolt-BÃűrnstein - Group IV Physical Chemistry ÂůVolume 19C2: "Ternary Steel Systems: Phase Diagrams and Phase Transition Data' in SpringerMaterials (https://doi.org/10.1007/978-3-540-88154-4_20)." Springer-Verlag Berlin Heidelberg, doi: 10.1007/978-3-540-88154-4_20.

Assignment: a). Calculate the heat capacity, entropy, enthalpy and Gibbs energy of each pure element as a function of temperature. b). Calculate the phase fractions as a function of temperature for the alloy with 50/50 of each element. c). Calculate the enthalpy of formation as a function of composition at 298K. d). Calculate the enthalpy of mixing in the liquid phase at a high temperature of your choice. e). Calculate the binary phase diagram and label all phase regions of one, two, and three phases in equilibrium.

```
[22]: # Set up the database and primary variables

# Load in the database file
from pycalphad import Database
db = Database("TiO_Complete.tdb")
print(sorted(db.elements))
print(sorted(db.phases))

# Composition: copper, oxygen, vacancies
#comp = sorted(db.elements)
# Relevant phases
#phases = sorted(db.phases)
```

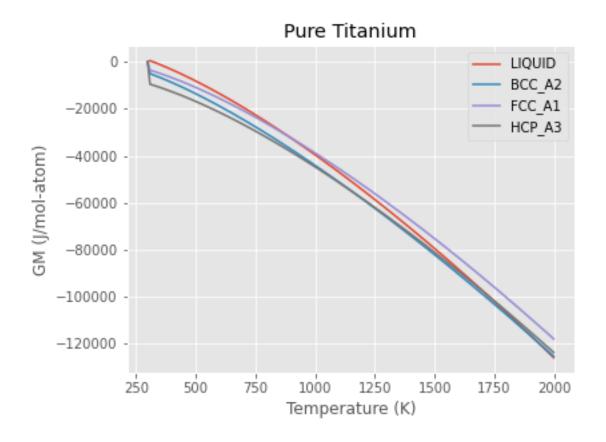
```
['/-', '0', 'TI', 'VA']
['A_TIO', 'BCC_A2', 'FCC_A1', 'GAS', 'HCP_A3', 'I_LIQUID', 'LIQUID', 'TI203',
'TI302', 'TI305', 'TI02', 'TI0X']
```

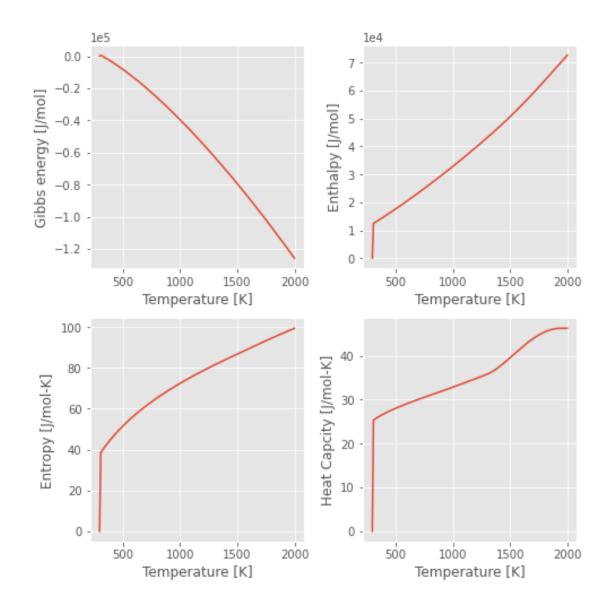
1.1.1 Part a) Pure element properties

Heat capacity, entropy, enthalpy, and Gibbs energy as a function of temperature.

```
[23]: import matplotlib.pyplot as plt
      import numpy as np
      from pycalphad import Database, calculate, equilibrium, variables as v
      #from PT import PT_phase_diagram
      # Conditions
      P = 101325 # [=] Pa, pressure = 1 atm
      T_{lo} = 298 \# [=] K, low temperature bound
      T_hi = 2000 # [=] K, high temperature bound
      N = 1 \# [=] mole
      ## Properties of pure titanium
      # Relevant phases for pure Ti:
      phases_Ti = ['LIQUID', 'BCC_A2', 'FCC_A1', 'HCP_A3']
      # Gibbs energy of different phases
      plt.figure(figsize = [6, 4.5])
      for phase in phases_Ti:
          Ti_GM = calculate(db, ['TI', 'VA'], phase, P=P, T=(T_lo, T_hi, 10), N=N)
          plt.plot(Ti_GM.T, Ti_GM.GM.squeeze(), label = phase)
      plt.legend()
      plt.xlabel('Temperature (K)')
      plt.ylabel('GM (J/mol-atom)')
      plt.title('Pure Titanium')
      plt.show()
      # Equilibrium characteristics
      conditions = { # mapping of state variable to values
          v.N: 1,
          v.P: 101325,
          # for now, only temperature has a range. If multiple variables have ranges, ___
       \rightarrow all combinations are calculated
          v.T: (T_lo, T_hi, 10),
      # Start figure
      fig, ax = plt.subplots(figsize = [7, 7], sharex=True)
      # Gibbs energy
      Ti_gm = equilibrium(db, ['Ti'], phases_Ti, conditions, output='GM')
      plt.subplot(2,2,1)
      plt.plot(Ti_gm.T, Ti_gm.GM.squeeze())
      plt.xlabel("Temperature [K]")
      plt.ylabel("Gibbs energy [J/mol]")
```

```
plt.ticklabel_format(axis = 'y', style = 'sci', scilimits = [-3, 3])
# Heat capacity
Ti_cp = equilibrium(db, ['Ti'], phases_Ti, conditions, output='CPM')
plt.subplot(2,2,4)
plt.plot(Ti_cp.T, Ti_cp.CPM.squeeze())
plt.xlabel("Temperature [K]")
plt.ylabel("Heat Capcity [J/mol-K]")
plt.ticklabel_format(axis = 'y', style = 'sci', scilimits = [-3, 3])
# Entropy
Ti_sm = equilibrium(db, ['Ti'], phases_Ti, conditions, output='SM')
plt.subplot(2,2,3)
plt.plot(Ti_sm.T, Ti_sm.SM.squeeze())
plt.xlabel("Temperature [K]")
plt.ylabel("Entropy [J/mol-K]")
plt.ticklabel_format(axis = 'y', style = 'sci', scilimits = [-3, 3])
# Enthalpy
Ti_hm = equilibrium(db, ['Ti'], phases_Ti, conditions, output='HM')
plt.subplot(2,2,2)
plt.plot(Ti_hm.T, Ti_hm.HM.squeeze())
plt.xlabel("Temperature [K]")
plt.ylabel("Enthalpy [J/mol]")
plt.ticklabel_format(axis = 'y', style = 'sci', scilimits = [-3, 3])
# Space the figure out more for ease of viewing
fig.tight_layout(pad=1.0)
plt.show()
```





```
[24]: # Repeat for oxygen
import matplotlib.pyplot as plt
import numpy as np
from pycalphad import Database, calculate, equilibrium, variables as v
#from PT import PT_phase_diagram

# Conditions
P = 101325 # [=] Pa, pressure = 1 atm
T_lo = 298 # [=] K, low temperature bound
T_hi = 2000 # [=] K, high temperature bound
N = 1 # [=] mole

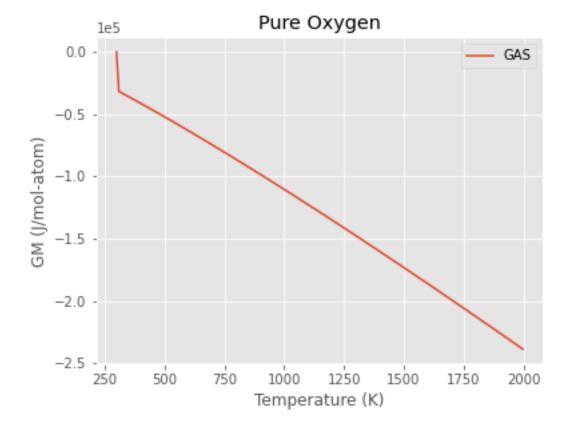
## Properties of pure oxygen
```

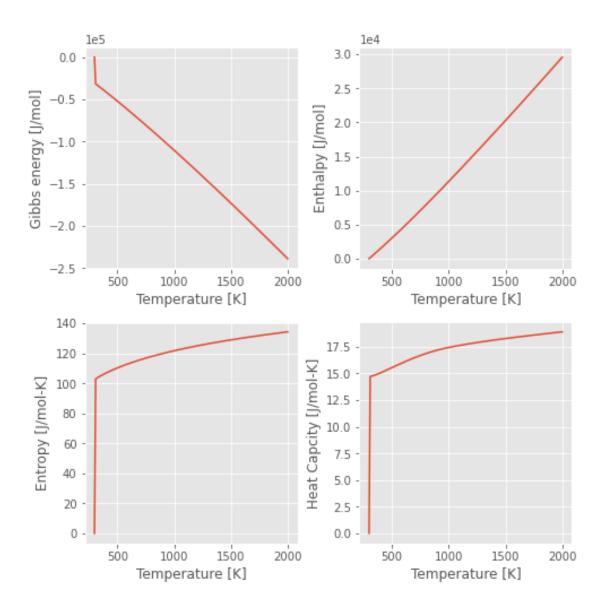
```
# Relevant phases for pure 0:
phases 0 = ['GAS']
# Gibbs energy of different phases
plt.figure(figsize = [6, 4.5])
for phase in phases_0:
    O_GM = calculate(db, ['O', 'VA'], phase, P=P, T=(T_lo, T_hi, 10), N=N)
    plt.plot(O_GM.T, O_GM.GM.squeeze(), label = phase)
plt.legend()
plt.xlabel('Temperature (K)')
plt.ylabel('GM (J/mol-atom)')
plt.title('Pure Oxygen')
plt.ticklabel_format(axis = 'y', style = 'sci', scilimits = [-3, 3])
plt.show()
# Equilibrium characteristics
conditions = { # mapping of state variable to values
    v.N: 1,
   v.P: 101325,
    # for now, only temperature has a range. If multiple variables have ranges, u
\rightarrowall combinations are calculated
   v.T: (T_lo, T_hi, 10),
# Start figure
fig, ax = plt.subplots(figsize = [7, 7], sharex=True)
# Gibbs energy
O_gm = equilibrium(db, ['O'], phases_O, conditions, output='GM')
plt.subplot(2,2,1)
plt.plot(O_gm.T, O_gm.GM.squeeze())
plt.xlabel("Temperature [K]")
plt.ylabel("Gibbs energy [J/mol]")
plt.ticklabel_format(axis = 'y', style = 'sci', scilimits = [-3, 3])
# Heat capacity
O_cp = equilibrium(db, ['O'], phases_O, conditions, output='CPM')
plt.subplot(2,2,4)
plt.plot(O_cp.T, O_cp.CPM.squeeze())
plt.xlabel("Temperature [K]")
plt.ylabel("Heat Capcity [J/mol-K]")
plt.ticklabel_format(axis = 'y', style = 'sci', scilimits = [-3, 3])
# Entropy
0_sm = equilibrium(db, ['0'], phases_0, conditions, output='SM')
plt.subplot(2,2,3)
plt.plot(O_sm.T, O_sm.SM.squeeze())
plt.xlabel("Temperature [K]")
```

```
plt.ylabel("Entropy [J/mol-K]")
plt.ticklabel_format(axis = 'y', style = 'sci', scilimits = [-3, 3])

# Enthalpy
O_hm = equilibrium(db, ['0'], phases_0, conditions, output='HM')
plt.subplot(2,2,2)
plt.plot(O_hm.T, O_hm.HM.squeeze())
plt.xlabel("Temperature [K]")
plt.ylabel("Enthalpy [J/mol]")
plt.ticklabel_format(axis = 'y', style = 'sci', scilimits = [-3, 3])

# Space the figure out more for ease of viewing
fig.tight_layout(pad=1.0)
plt.show()
```





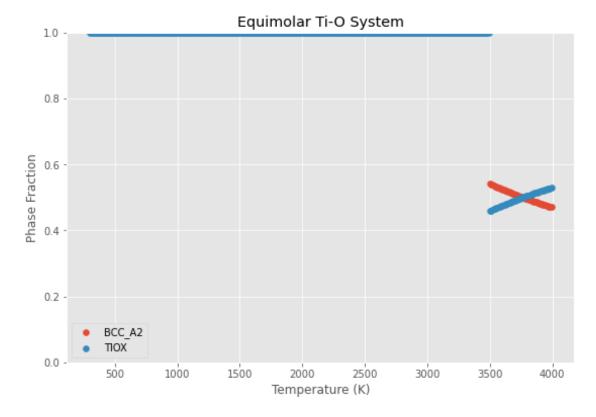
1.1.2 Part b) Equimolar mixture phase fractions

as a function of temperature

```
[25]: import matplotlib.pyplot as plt
import numpy as np
from pycalphad import Database, calculate, equilibrium, variables as v

# Equilibrium characteristics
conditions = { # mapping of state variable to values
    v.N: 1,
    v.P: 101325,
```

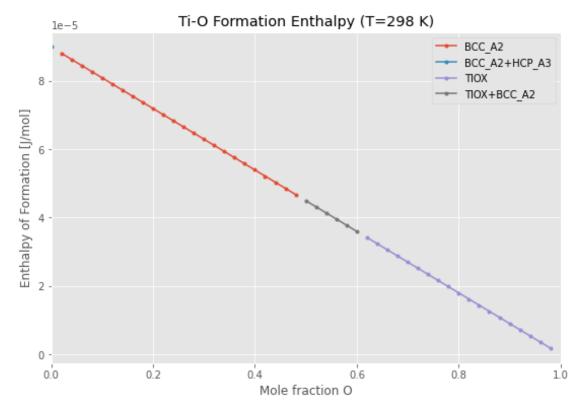
```
v.T: (300, 4000, 10), # Database is limited to about 4000 K for its equations
    v.X('TI'): 0.5
}
phases_mix = ['A_TIO', 'BCC_A2', 'FCC_A1', 'GAS', 'HCP_A3', 'I_LIQUID',
→ 'LIQUID', 'TI203', 'TI302', 'TI305', 'TI02', 'TI0X']
phase_eq = equilibrium(db, ['TI', 'O', 'VA'], phases_mix, conditions)
fig = plt.figure(figsize=(9,6))
ax = fig.gca()
for phase in phases_mix:
    # Phase indices for plotting
    phase_indices = np.nonzero(phase_eq.Phase.values == phase)
    # Many phases are not present in any appreciable amount; omit if empty so \Box
 → the legend is not too large
    if len(phase_eq.NP.values[phase_indices]) > 0:
        plt.scatter(np.take(phase_eq['T'].values, phase_indices[2]), phase_eq.NP.
→values[phase_indices], label = phase)
plt.legend(loc = 'lower left')
plt.title('Equimolar Ti-O System')
plt.ylabel('Phase Fraction')
plt.ylim(0, 1)
plt.xlabel('Temperature (K)')
plt.show()
```



1.1.3 Part c) Enthalpy of formation

T = 298 K as a function of composition

```
[26]: from pycalphad import Database, equilibrium, Model, ReferenceState, variables as
      import matplotlib.pyplot as plt
      import numpy as np
      # Load data and phases
      db = Database("TiO_Complete.tdb")
      comps = ["TI", "O", "VA"]
      phases = ['A_TIO', 'BCC_A2', 'FCC_A1', 'GAS', 'HCP_A3', 'TI203', 'TI302', '
      →'TI305', 'TI02', 'TI0X']
      # Omit liquid phases, which should not be stable at T = 298K
      # Single element reference state phase for Ti and O
      Ti_ref = ReferenceState("TI", "HCP_A3", {v.T: 298.15, v.P: 101325})
      O_ref = ReferenceState("0", "GAS",
                                             {v.T: 298.15, v.P: 101325})
      # Create the models for each phase and shift them all by the same reference,
       \rightarrowstates.
      eq models = {}
      for phase_name in phases:
          mod = Model(db, comps, phase_name)
          mod.shift_reference_state([Ti_ref, O_ref], db)
          eq_models[phase_name] = mod
      # Calculate HMR at 298 K from X(0)=0 to X(0)=1
      conds = \{v.P: 101325, v.T: 298, v.X("0"): (0, 1, 0.02)\}
      result = equilibrium(db, comps, phases, conds, output="HMR", model=eq_models)
      # Find the groups of unique phases in equilibrium
      unique_phase_sets = np.unique(result.Phase.values.squeeze(), axis=0)
      # Plot
      fig = plt.figure(figsize=(9,6))
      ax = fig.gca()
      for phase_set in unique_phase_sets:
          label = '+'.join([ph for ph in phase_set if ph != ''])
          # Composition indices with the same unique phase
          unique_phase_idx = np.nonzero(np.all(result.Phase.values.squeeze() ==__
       →phase_set, axis=1))[0]
          masked_result = result.isel(X_0=unique_phase_idx)
```



1.1.4 Part d) Enthalpy of mixing, liquid phase

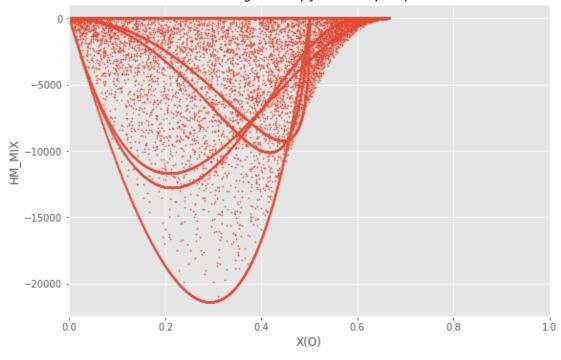
Based on the phase fractions above, use T = 6500 K

```
[27]: from pycalphad import Database, calculate
import matplotlib.pyplot as plt

dbf = Database("TiO_Complete.tdb")
comps = ["TI", "O", "VA"]

# Calculate HMR for the Chi at 2800 K from X(RE) = 0 to X(RE) = 1
```





1.1.5 Part e) Binary phase diagram

Label all phase regions of 1, 2, and 3, phase equilibrium

```
[28]: import matplotlib.pyplot as plt
from pycalphad import Database, binplot
import pycalphad.variables as v
```

