ASAE D271.2 APR1979 (R2010) Psychrometric Data



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Psychrometric Data

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Keywords: Psychrometric

1 Purpose and scope

- 1.1 The purpose of this data is to assemble psychrometric data in chart and equation form in both SI and English units.
- **1.2** Psychrometric charts are presented that give Data for dry bulb temperature ranges of -35 to $600~^\circ\text{F}$ in English units and -10 to $120~^\circ\text{C}$ in SI units.
- 1.3 Many analyses of psychrometric data are made on computers. The equations given in Sections 2 and 3 enable the calculation of all psychrometric data if any two independent psychrometric properties of an air-water vapor mixture are known in addition to the atmospheric pressure. In some cases, iteration procedures are necessary. In some instances, the range of data covered by the equation has been extended beyond that given in the original source. The equations yield results that agree closely with values given by Keenan and Keyes (1936) and existing psychrometric charts.

2 Psychrometric data in SI units

- 2.1 Psychrometric charts; two presented. One for a temperature range of -10 to $55\,^{\circ}\text{C}$ and one for a temperature range of 20 to $120\,^{\circ}\text{C}$.
- $\textbf{2.2 Psychrometric equations, SI units}. \ \textbf{Symbols are defined in Table 1}.$
- 2.2.1 Saturation line. P_s as a function of T

Table 1 - Symbols

h	Enthalpy of air-vapor mixture, J/kg dry air or Btu/lb dry air
h_{fg}	Latent heat of vaporization of water at saturation, J/kg or Btu/lb
h_{fg}'	Latent heat of vaporization of water at T_{wb} , J/kg or Btu/lb
$h_{fq}^{"}$	Latent heat vaporization of water at T_{dp} , J/kg or Btu/lb
h _{ia}	Heat of sublimation of ice, J/kg or Btu/lb
h'_{ig}	Heat of sublimation of ice at T_{wb} , J/kg or Btu/lb
$h_{ig}^{"}$	Heat of sublimation of ice at T_{dp} , J/kg or Btu/lb
H	Humidity ratio, kg water/kg dry air or lb water/lb dry air
In	Natural logarithm (base e)
$P_{\rm atm}$	Atmospheric pressure, Pa or psi
P_s	Saturation vapor pressure at T, Pa or psi
P_{swb}	Saturation vapor pressure at T_{wb} , Pa or psi
P_{v}	Vapor pressure, Pa or psi
rh	Relative humidity, decimal
T	Dry-bulb temperature, kelvin or rankine
T_{dp}	Dew-point temperature, kelvin or rankine
T_{wb}	Wet-bulb temperature, kelvin or rankine
V_{sa}	Air specific volume, m³/kg dry air or ft³/lb dry air

$$\ln P_s = 31.9602 - \frac{6270.3605}{T} - 0.46057 \ln T$$
 Brooker (1967)

255.38≤*T*≤273.16

and

$$\ln(P_s/R) = \frac{A + BT + CT^2 + DT^3 + ET^4}{FT - GT^2}$$

Adapted from Keenan and Keyes (1936)

273.16≤ *T*≤533.16

where

$$R = 22,105,649.25$$
 $D = 0.12558 \times 10^{-3}$
 $A = -27,405.526$ $E = -0.48502 \times 10^{-7}$
 $B = 97.5413$ $F = 4.34903$
 $C = -0.146244$ $G = 0.39381 \times 10^{-2}$

2.2.2 Saturation line. T as a function of P_s

$$T-255.38 = \sum_{i=0}^{i=8} A_i [\ln(0.00145P_s)]^i$$

 $620.52 < P_s < 4,688,396.00$ Steltz and Silvestri (1958)

 $A_0 = 19.5322$

 $A_1 = 13.6626$

 $A_2 = 1.17678$

 $A_3 = -0.189693$

 $A_4 = 0.087453$

 $A_5 = -0.0174053$

 $A_6 = 0.00214768$

 $A_7 = -0.138343 \times 10^{-3}$

 $A_8 = 0.38 \times 10^{-5}$

2.2.3 Latent heat of sublimation at saturation

$$h_{iq} = 2,839,683.144 - 212.56384 \ (T - 255.38)$$

255.38≤ *T*≤273.16 Brooker (1967)

2.2.4 Latent heat of vaporization at saturation

 $h_{fg} = 2,502,535.259 - 2,385.76424 \ (T - 273.16)$

273.16≤ *T*≤338.72 Brooker (1967)

$$h_{fg} = (7,329,155,978,000 - 15,995,964.08 T^2)^{1/2}$$

338.72≤ *T*≤533.16

Brooker (Unpublished)

2.2.5 Wet bulb line

$$P_{swb} - P_v = B'(T_{wb} - T)$$
 Brunt (1941)

where

$$B' = \frac{1006.9254(P_{swb} - P_{atm}) \left(1 + 0.15577 \frac{P_{v}}{P_{atm}}\right)}{0.62194 \ h'_{fg}}$$

Substitute h'_{ia} for h'_{fa} where $T_{wb} \leq 273.16$

2.2.6 Humidity ratio

$$H = \frac{0.6219 P_v}{P_{atm} - P_v}$$

$$P_{v} < P_{atm}$$

2.2.7 Specific volume

$$V_{sa} = \frac{287 T}{P_{atm} - P_{v}}$$

$$P_v < P_{atm}$$

2.2.8 Enthalpy

Enthalpy=enthalpy of air+enthalpy of water (or ice) at dew-point temperature+enthalpy of evaporation (or sublimation) at dew-point temperature+enthalpy added to the water vapor (super-heat) after vaporization.

$$h = 1006.92540 \ (T - 273.16)$$

$$-H[333,\!432.1\!+\!2030.5980(273.16\!-\!T_{dp})]\!+\!h_{ig}''H$$

$$+ 1875.6864H(T-T_{dp})$$

$$255.38 \le T_{dp} \le 273.16$$

and

2

$$h = 1006.92540 \ (T - 273.16)$$

$$+\,4186.8\ H(T_{dp}\!-\!273.16) + h_{fg}''\,H + 1875.6864\ H(T\!-\!T_{dp})$$

$$273.16 \le T_{dp} \le 373.16$$

2.2.9 Relative humidity

$$rh = P_v/P_s$$

3 Psychrometric data in English Units

- 3.1 Three psychrometric charts are presented with temperature ranges of -35 to $50\,^\circ\text{F}$, 32 to $120\,^\circ\text{F}$ and 32 to $600\,^\circ\text{F}$, respectively.
- ${f 3.2}$ Psychrometric equations, English units. Symbols are defined in Table 1.
- 3.2.1 Saturation line. P_s as a function of T

$$\ln P_s = 23.3924 - \frac{11286.6489}{T} - 0.46057 \ln T$$

Brooker (1967)

459.69≤ *T*≤491.69

$$\ln(P_s/R) = \frac{A + BT + CT^2 + DT^3 + ET^4}{FT - GT^2}$$

Adapted from Keenan and Keyes (1936)

where

$$R = 3206.18$$

$$A = -27405.5$$

$$B = 54.1896$$

$$C = -0.045137$$

$$D = 0.215321 \times 10^{-4}$$

$$E = -0.462027 \times 10^{-8}$$

$$F = 2.41613$$

$$G = 0.00121547$$

3.2.2 Saturation line. T as a function of P_s

$$T - 459.69$$

$$= \sum_{i=0}^{i=8} A_i [\ln(10P_s)]^i$$
 Steltz and Silvestri (1958)

$$0.09 \le P_s \le 680$$

where

$$A_0 = 35.1579$$

$$A_1 = 24.5926$$

$$A_2 = 2.11821$$

$$A_3 = -0.341447$$

$$A_4 = 0.157416$$

$$A_5 = -0.0313296$$

$$A_6 = 0.00386583$$

$$A_7 = -0.249018 \times 10^{-3}$$

$$A_8 = 0.684016 \times 10^{-5}$$

3.2.3 Latent heat of sublimation at saturation

$$h_{ia} = 1220.844 - 0.05077 \ (T - 459.69)$$

3.2.4 Latent heat of vaporization at saturation

$$h_{fa} = 1075.8965 - 0.56983 \quad (T - 491.69)$$
 Brooker (1967)

$$h_{fq} = (1354673.214 - 0.9125275587 \ T^2)^{1/2}$$
 Brooker (Unpublished)

3.2.5 Wet bulb line

$$P_{swb} - P_v = B'(T_{wb} - T)$$

Brunt (1941)

$$B' = \frac{0.2405(P_{swb} - P_{atm})(1 + 0.15577P_v/P_{atm})}{0.62194 \ h'_{fg}}$$

Substitute h'_{ig} for h'_{fg} when $T_{wb} \leq 491.69$

3.2.6 Absolute humidity (humidity ratio)

$$H = \frac{0.6219 \ P_{v}}{P_{atm} - P_{v}}$$

459.69≤ *T*≤959.69

$$P_v < P_{atm}$$

3.2.7 Specific volume

$$V_{sa} = \frac{53.35 \times T}{144(P_{atm} - P_v)}$$

459.69≤ *T*≤959.69

$$P_v < P_{atm}$$

3.2.8 Enthalpy

Enthalpy=enthalpy of air+enthalpy of water (or ice) at dew-point temperature+enthalpy of evaporation (or sublimation) at dew-point temperature+enthalpy added to the water vapor (super-heat) after vaporization.

$$\begin{split} h &= 0.2405(\,T - 459.69) - H[\,143.35 + 0.485(\,491.69 - T_{dp})\,] \\ &+ h_{ig}'' H + 0.448 H(\,T - T_{dp}) \end{split}$$

$$459.69 \le T_{dp} \le 491.69$$

$$h = 0.2405(T - 459.69) + H(T_{dp} - 491.69)$$
$$+ h''_{fa}H + 0.448H(T - T_{dp})$$

$$491.69 \le T_{dp} \le 671.69$$

3.2.9 Relative humidity

$$rh = P_v/P_s$$

Note: Psychrometric charts are printed with permission from the American Society of Heating, Refrigerating and Airconditioning Engineers, Inc., 345 E. 47th St., New York, NY; Proctor & Schwartz, Inc., 7th St. and Tabor Rd., Philadelphia, PA; and Carrier Corp., Carrier Parkway, Syracuse, NY.

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