

1) a)  $P_i^{Sat} = 10^A - \frac{B}{T+C}$  H W 6

Toluene  
 $A = 6.95087$   
 $B = 1342.31$   
 $C = 219.187$

$P_i^{Sat} = 244.4 \text{ mmHg} \cdot \frac{0.133 \text{ kPa}}{1 \text{ mmHg}} = 32.6 \text{ kPa}$

$y_1 = \frac{P_i^{Sat} x_1}{P} = \frac{32.6 \cdot 0.7}{30} = 0.76 \rightarrow \boxed{76.0\% = y_1}$

$y_2 = 1 - y_1 = \boxed{24.0\%}$

b)  $P_r = 10^{\left(\frac{7}{3}(1+W)\right) \cdot \left(\frac{1}{1-T_r}\right)}$

$W = 0.264$   
 $T_r = \frac{75+273}{591.8}$   
 $P_c = 4.109 \text{ MPa}$

$P = P_r + P_c$

$P_r = 0.0086 \text{ MPa} \rightarrow P = 0.0086 + 4.109 = 0.0354 \text{ MPa}$

$P = 35.4 \text{ kPa}$   $y_1 = \frac{P_i^{Sat} x_1}{P} = \frac{35.4 \cdot 0.7}{30} = 0.827$   
 $\boxed{y_1 = 82.7\%}$

$y_2 = 1 - y_1 = \boxed{17.3\%}$



# HW 6

- 2) ethyl Bromide : 1  $P_1^{sat} = 0.7569 \text{ Bar}$   $x_1 = 0.4723$   
n-heptane : 2  $P_2^{sat} = 0.0773 \text{ bar}$   $x_2 = 0.5277$

$$BP = P_1 x_1 + P_2 x_2 = 0.7569 \cdot 0.4723 + 0.0773 \cdot 0.5277$$

$$= 0.398 \text{ Bar}$$

$$y_1 = \frac{x_1 \cdot P_1^{sat}}{P} = \frac{0.4723 \cdot 0.7569}{0.398} = 0.8976 \approx 89.8\%$$

$$y_2 = 1 - y_1 = 0.1024 \approx 10.2\%$$

- 3)  $z_1 = 0.07$   $P = 4 \text{ bar}$   
 $z_2 = 0.12$   
 $z_3 = 0.41$   
 $z_4 = 0.40$

$$Pr = 10^{\left(\frac{7}{3}(1+W) \cdot \left(\frac{1}{1-T_r}\right)\right)}$$

excel

a)  $T_{BP}$  :  $P = \sum x_i P_i^{sat}(T) \rightarrow T_{BP} = 279 \text{ K}$

b)  $T_{DP}$  :  ~~$P = \sum x_i P_i^{sat}(T)$~~   $\rightarrow \text{excel} \rightarrow T_{DP} = 304 \text{ K}$

$$P_i = \frac{1}{\sum \frac{y_i}{P_i^{sat}}}$$

c)  $K_i = \frac{P^{sat}}{P} \rightarrow 0 = \sum \frac{z_i (1 - K_i)}{K_i + \frac{1}{R} (1 - K_i)} \rightarrow \text{Excel}$

$$\frac{L}{F} = 0.0688$$




$$\approx 6.88\%$$

$$\therefore 93.1\% \text{ VAP}$$

$$\therefore 93.12\%$$

A7																	
	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q
1	eth	p1sat	w1	tr1	pc		x		x*psat		sum(x*psat)						
2		28.15923	0.099	0.91481	4.88		0.07		1.971146								
3	prop	p2sat									3.999996305						
4		5.732791	0.152	0.755497	4.249		0.12		0.687935								
5	n	p3sat															
6		1.338365	0.193	0.657062	3.797		0.41		0.54873								
7		p4sat															
8		1.980464	0.177	0.684594	3.648		0.4		0.792185								
9																	
10																	
11																	
12																	
13																	
14		T	P														
15		279.383	4														
16																	
17																	
18																	
19																	
20																	
21																	
22																	
23																	
24																	
25																	

F16



	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q
1	eth	p1sat	w1	tr1	pc		y		y/psat		sum(x*psat)						
2		47.08798	0.099	0.993988	4.88		0.07		0.001487								
3	prop	p2sat									3.999998603						
4		11.0098	0.152	0.820887	4.249		0.12		0.010899								
5	n	p3sat															
6		2.911013	0.193	0.713932	3.797		0.41		0.140844								
7	iso	p4sat															
8		4.133526	0.177	0.743847	3.648		0.4		0.09677								
9																	
10																	
11																	
12																	
13																	
14		T	P														
15		303.564	4														
16																	
17																	
18																	
19																	
20																	
21																	
22																	
23																	
24																	
25																	

O2

=SUM(M2:M8)

	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P	Q
1	eth	p1sat	w1	tr1	pc		z		k		L/F		Flash		sum flash		
2		46.70756	0.099	0.992633	4.88		0.07		11.67689		0.068810563		-0.0683027		3.92E-11		
3	prop	p2sat															
4		10.89703	0.152	0.819767	4.249		0.12		2.724257				-0.07940975				
5	n	p3sat															
6		2.875542	0.193	0.712959	3.797		0.41		0.718886				0.156126169				
7	iso	p4sat															
8		4.085818	0.177	0.742833	3.648		0.4		1.021455				-0.00841372				
9																	
10																	
11																	
12																	
13																	
14		T	P														
15		303.15	4														
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# HW 6

4) a) ~~100% P<sub>DP</sub>~~

$$P = 15$$

$$z_1 = 0.45$$

$$z_2 = 0.55$$

$$P_{DP} = \frac{1}{\sum \frac{\gamma_i}{P_i^{sat}(T)}} \rightarrow \text{MM}$$

$$\text{Set } P_{DP} = 15 \rightarrow T = 405 \text{ K} \quad \text{excel}$$

$$x_i = \frac{\gamma_i \cdot P_{DP}}{P_i^{sat}} \rightarrow x_1 = 0.264$$

$$x_2 = 0.735$$

first drop!

26.4% but  
73.6% Pent

$$b) P_{BP} = 15 = \sum x_i \cdot P_i^{sat} \rightarrow \text{excel} \rightarrow T = 395 \text{ K}$$

last drop!

65.7% but  
34.3% Pent



Given xi, P, calculate bubble point temperature								
	A	B	C	Pi_sat (bar)	xi	Pi_sat*xi (bar)	yi	
nbutane	6.80897	935.86	238.73	21.9040854	0.45	9.856838432	0.6571	
npentane	6.85221	1064.63	232	9.351205698	0.55	5.143163134	0.3429	
					$P_1^{sat}(T)$	Iterate T until		
		BP pressure	15.00000157	bar		$P=\sum x_i P_i^{sat}(T)$		
		T	122.1393033	c				
			395.2893033					



Pxy Mehtanol, n-Propanol @ 80C

