

Thermo HW 6

$$1.) \dot{W}_{s,net} = 300 \text{ MW} \quad \dot{m} = 115000 \frac{\text{kg}}{\text{hr}} \quad \text{HHV} = 29000 \frac{\text{kJ}}{\text{kg}}$$

$$\dot{m} = 31.94 \frac{\text{kg}}{\text{sec}}$$

$$\eta_{\text{overall}} = \frac{\dot{W}_{s,net}}{\text{HHV} \cdot \dot{m}_{\text{fuel}}} = \frac{300000 \text{ kW}}{29000 \frac{\text{kJ}}{\text{kg}} \cdot 31.94 \frac{\text{kg}}{\text{sec}}} = 0.324 = 32.4\%$$

$$2.) \dot{W}_{s,net} = 600 \text{ MW} \quad \eta_{\theta} = 0.40 \quad \eta_{\text{gen}} = 0.100$$

$$\dot{Q}_H - \dot{Q}_C = \dot{W}_{s,net} \quad , \quad \eta_{\theta} = \frac{\dot{W}_{s,net}}{\dot{Q}_H} \rightarrow \dot{Q}_H = \frac{\dot{W}_{s,net}}{\eta_{\theta}}$$

$$\therefore \dot{Q}_C = \dot{W}_{s,net} + \dot{Q}_H \rightarrow \dot{Q}_C = \frac{\dot{W}_{s,net}}{\eta_{\theta}} - \dot{W}_{s,net}$$

$$\dot{Q}_C = \frac{600000 \text{ kW}}{0.40} - 600000 \text{ kW} = 900000 \text{ kW} = 900 \text{ MW}$$

Actual \dot{Q}_C would be lower because $\eta_{\text{gen,actual}} < 0.100$

and $\eta_{\theta} \eta_{\text{boil}} \eta_{\text{gen}} = \frac{\dot{W}_{s,net}}{\text{HHV} \cdot \dot{m}}$ \therefore (assuming HHV and \dot{m} remain unchanged) if η_{gen} decreases, $\dot{W}_{s,net}$ would have to decrease also.

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3.) $W_{s,net} = 100 \text{ kW}$ $Q_H = 400 \text{ kW}$

$$\eta_0 = 1 - \frac{Q_C}{Q_H}$$

$$Q_H - Q_C - W_{s,net} = 0$$

$$\therefore \eta_0 = 1 - \frac{Q_H - W_{s,net}}{Q_H} = 1 - \frac{(400 - 100) \text{ kW}}{400 \text{ kW}} = 1 - \frac{3}{4} = \frac{1}{4} = 0.25 \quad \boxed{25\%}$$

4.) $\eta_0 = 1 - \frac{Q_C}{Q_H} \rightarrow \frac{Q_C}{Q_H} = \frac{T_C}{T_H}$ $T_C = 25^\circ\text{C} = 298.15 \text{ K}$
 $T_H = 450^\circ\text{C} = 723.15 \text{ K}$

$$\eta_{0,max} = 1 - \frac{298.15 \text{ K}}{723.15 \text{ K}} = 1 - 0.412 = 0.588 \quad \boxed{0.588}$$

The actual efficiency might be less than the estimated due to heat lost to the surroundings.

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$$\begin{array}{llll}
 5) \quad T_H = 85^\circ\text{C} & P = 101.3 \text{ kPa} & x_E = 0.45 & C_E = 4.2 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} \\
 T_C = 20^\circ\text{C} & & x_W = 0.55 & C_W = 2.84 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} \\
 \Delta H_W^{\text{vap}} = 2300 \frac{\text{kJ}}{\text{kg}} & & M_E = 46 \frac{\text{kg}}{\text{kmol}} & \\
 \Delta H_E^{\text{vap}} = 844 \frac{\text{kJ}}{\text{kg}} & & M_W = 18 \frac{\text{kg}}{\text{kmol}} &
 \end{array}$$

$$H^{\text{is}} = \sum_i x_i H_i$$

$$H_{1,E} = 0 + \Delta H_E + \Delta H_E^{\text{vap}} = 0 + C_E (\Delta T) + 844 = 0 + 2.84(65) + 844$$

$$H_{1,E} = 1028.6 \frac{\text{kJ}}{\text{kg}} \cdot 46 \frac{\text{kg}}{\text{kmol}} = 47 \times 10^3 \frac{\text{kJ}}{\text{kmol}}$$

$$H_{1,W} = 0 + \Delta H_W + \Delta H_W^{\text{vap}} = 0 + C_W (\Delta T) + 2300 = 4.2(65) + 2300$$

$$H_{1,W} = 2612 \frac{\text{kJ}}{\text{kg}} \cdot 18 \frac{\text{kg}}{\text{kmol}} = 47 \times 10^3 \frac{\text{kJ}}{\text{kmol}}$$

$$H = x_E (H_{1,E}) + x_W (H_{1,W}) = 0.45 (47 \times 10^3) + 0.55 (47 \times 10^3)$$

$$H_1^{\text{is}} = 4.7 \times 10^4$$

$$H_2^{\text{is}} = 0$$

$$Q = H_2 - H_1 = 0 - 4.7 \times 10^4 = -4.7 \times 10^4 \frac{\text{kJ}}{\text{kmol}}$$