### = Shale oil extraction =

Shale oil extraction is an industrial process for unconventional oil production. This process converts kerogen in oil shale into shale oil by pyrolysis, hydrogenation, or thermal dissolution. The resultant shale oil is used as fuel oil or upgraded to meet refinery feedstock specifications by adding hydrogen and removing sulfur and nitrogen impurities.

Shale oil extraction is usually performed above ground (ex situ processing) by mining the oil shale and then treating it in processing facilities. Other modern technologies perform the processing underground (on @-@ site or in situ processing) by applying heat and extracting the oil via oil wells

The earliest description of the process dates to the 10th century . In 1684 , Great Britain granted the first formal extraction process patent . Extraction industries and innovations became widespread during the 19th century . The industry shrank in the mid @-@ 20th century following the discovery of large reserves of conventional oil , but high petroleum prices at the beginning of the 21st century have led to renewed interest , accompanied by the development and testing of newer technologies . As of 2010 , major long @-@ standing extraction industries are operating in Estonia , Brazil , and China . Its economic viability usually requires a lack of locally available crude oil . National energy security issues have also played a role in its development . Critics of shale oil extraction pose questions about environmental management issues , such as waste disposal , extensive water use , waste water management , and air pollution .

# = = History = =

In the 10th century , the Arabian physician Masawaih al @-@ Mardini ( Mesue the Younger ) wrote of his experiments in extracting oil from " some kind of bituminous shale " . The first shale oil extraction patent was granted by the British Crown in 1684 to three people who had " found a way to extract and make great quantities of pitch , tarr , and oyle out of a sort of stone " . Modern industrial extraction of shale oil originated in France with the implementation of a process invented by Alexander Selligue in 1838 , improved upon a decade later in Scotland using a process invented by James Young . During the late 19th century , plants were built in Australia , Brazil , Canada , and the United States . The 1894 invention of the Pumpherston retort , which was much less reliant on coal heat than its predecessors , marked the separation of the oil shale industry from the coal industry . China ( Manchuria ) , Estonia , New Zealand , South Africa , Spain , Sweden , and Switzerland

China (Manchuria), Estonia, New Zealand, South Africa, Spain, Sweden, and Switzerland began extracting shale oil in the early 20th century. However, crude oil discoveries in Texas during the 1920s and in the Middle East in the mid 20th century brought most oil shale industries to a halt. In 1944, the US recommenced shale oil extraction as part of its Synthetic Liquid Fuels Program. These industries continued until oil prices fell sharply in the 1980s. The last oil shale retort in the US, operated by Unocal Corporation, closed in 1991. The US program was restarted in 2003, followed by a commercial leasing program in 2005 permitting the extraction of oil shale and oil sands on federal lands in accordance with the Energy Policy Act of 2005.

As of 2010 , shale oil extraction is in operation in Estonia , Brazil , and China . In 2008 , their industries produced about 930 @,@ 000 metric tonnes ( 17 @,@ 700 barrels per day ) of shale oil . Australia , the US , and Canada have tested shale oil extraction techniques via demonstration projects and are planning commercial implementation ; Morocco and Jordan have announced their intent to do the same . Only four processes are in commercial use : Kiviter , Galoter , Fushun , and Petrosix .

## = = Processing principles = =

Shale oil extraction process decomposes oil shale and converts its kerogen into shale oil? a petroleum @-@ like synthetic crude oil. The process is conducted by pyrolysis, hydrogenation, or thermal dissolution. The efficiencies of extraction processes are often evaluated by comparing their yields to the results of a Fischer Assay performed on a sample of the shale.

The oldest and the most common extraction method involves pyrolysis ( also known as retorting or destructive distillation ) . In this process , oil shale is heated in the absence of oxygen until its kerogen decomposes into condensable shale oil vapors and non @-@ condensable combustible oil shale gas . Oil vapors and oil shale gas are then collected and cooled , causing the shale oil to condense . In addition , oil shale processing produces spent oil shale , which is a solid residue . Spent shale consists of inorganic compounds ( minerals ) and char ? a carbonaceous residue formed from kerogen . Burning the char off the spent shale produces oil shale ash . Spent shale and shale ash can be used as ingredients in cement or brick manufacture . The composition of the oil shale may lend added value to the extraction process through the recovery of by @-@ products , including ammonia , sulfur , aromatic compounds , pitch , asphalt , and waxes .

Heating the oil shale to pyrolysis temperature and completing the endothermic kerogen decomposition reactions require a source of energy . Some technologies burn other fossil fuels such as natural gas , oil , or coal to generate this heat and experimental methods have used electricity , radio waves , microwaves , or reactive fluids for this purpose . Two strategies are used to reduce , and even eliminate , external heat energy requirements : the oil shale gas and char by @-@ products generated by pyrolysis may be burned as a source of energy , and the heat contained in hot spent oil shale and oil shale ash may be used to pre @-@ heat the raw oil shale .

For ex situ processing , oil shale is crushed into smaller pieces , increasing surface area for better extraction . The temperature at which decomposition of oil shale occurs depends on the time @-@ scale of the process . In ex situ retorting processes , it begins at 300 ° C ( 570 ° F ) and proceeds more rapidly and completely at higher temperatures . The amount of oil produced is the highest when the temperature ranges between 480 and 520 ° C ( 900 and 970 ° F ) . The ratio of oil shale gas to shale oil generally increases along with retorting temperatures . For a modern in situ process , which might take several months of heating , decomposition may be conducted at temperatures as low as 250 ° C ( 480 ° F ) . Temperatures below 600 ° C ( 1 @,@ 110 ° F ) are preferable , as this prevents the decomposition of lime stone and dolomite in the rock and thereby limits carbon dioxide emissions and energy consumption .

Hydrogenation and thermal dissolution (reactive fluid processes) extract the oil using hydrogen donors, solvents, or a combination of these. Thermal dissolution involves the application of solvents at elevated temperatures and pressures, increasing oil output by cracking the dissolved organic matter. Different methods produce shale oil with different properties.

# = = Classification of extraction technologies = =

Industry analysts have created several classifications of the technologies used to extract shale oil from oil shale.

By process principles: Based on the treatment of raw oil shale by heat and solvents the methods are classified as pyrolysis, hydrogenation, or thermal dissolution.

By location: A frequently used distinction considers whether processing is done above or below ground, and classifies the technologies broadly as ex situ (displaced) or in situ (in place). In ex situ processing, also known as above @-@ ground retorting, the oil shale is mined either underground or at the surface and then transported to a processing facility. In contrast, in situ processing converts the kerogen while it is still in the form of an oil shale deposit, following which it is then extracted via oil wells, where it rises in the same way as conventional crude oil. Unlike ex situ processing, it does not involve mining or spent oil shale disposal aboveground as spent oil shale stays underground.

By heating method: The method of transferring heat from combustion products to the oil shale may be classified as direct or indirect. While methods that allow combustion products to contact the oil shale within the retort are classified as direct, methods that burn materials external to the retort to heat another material that contacts the oil shale are described as indirect

By heat carrier: Based on the material used to deliver heat energy to the oil shale, processing technologies have been classified into gas heat carrier, solid heat carrier, wall conduction, reactive fluid, and volumetric heating methods. Heat carrier methods can be sub @-@ classified as direct

or indirect.

The following table shows extraction technologies classified by heating method, heat carrier and location (in situ or ex situ).

By raw oil shale particle size: The various ex situ processing technologies may be differentiated by the size of the oil shale particles that are fed into the retorts. As a rule, gas heat carrier technologies process oil shale lumps varying in diameter from 10 to 100 millimeters ( 0 @.@ 4 to 3 @.@ 9 in ), while solid heat carrier and wall conduction technologies process fines which are particles less than 10 millimeters ( 0 @.@ 4 in ) in diameter.

By retort orientation: " Ex @-@ situ " technologies are sometimes classified as vertical or horizontal. Vertical retorts are usually shaft kilns where a bed of shale moves from top to bottom by gravity. Horizontal retorts are usually horizontal rotating drums or screws where shale moves from one end to the other. As a general rule, vertical retorts process lumps using a gas heat carrier, while horizontal retorts process fines using solid heat carrier.

By complexity of technology: In situ technologies are usually classified either as true in situ processes or modified in situ processes. True in situ processes do not involve mining or crushing the oil shale. Modified in situ processes involve drilling and fracturing the target oil shale deposit to create voids in the deposit. The voids enable a better flow of gases and fluids through the deposit, thereby increasing the volume and quality of the shale oil produced.

= = Ex situ technologies = =

= = = Internal combustion = = =

Internal combustion technologies burn materials ( typically char and oil shale gas ) within a vertical shaft retort to supply heat for pyrolysis . Typically raw oil shale particles between 12 millimetres ( 0 @ .@ 5 in ) and 75 millimetres ( 3 @ .@ 0 in ) in size are fed into the top of the retort and are heated by the rising hot gases , which pass through the descending oil shale , thereby causing decomposition of the kerogen at about 500 ° C ( 932 ° F ) . Shale oil mist , evolved gases and cooled combustion gases are removed from the top of the retort then moved to separation equipment . Condensed shale oil is collected , while non @-@ condensable gas is recycled and used to carry heat up the retort . In the lower part of the retort , air is injected for the combustion which heats the spent oil shale and gases to between 700 ° C ( 1 @ ,@ 292 ° F ) and 900 ° C ( 1 @ ,@ 650 ° F ) . Cold recycled gas may enter the bottom of the retort to cool the shale ash . The Union A and Superior Direct processes depart from this pattern . In the Union A process , oil shale is fed through the bottom of the retort and a pump moves it upward . In the Superior Direct process , oil shale is processed in a horizontal , segmented , doughnut @-@ shaped traveling @-@ grate retort .

Internal combustion technologies such as the Paraho Direct are thermally efficient , since combustion of char on the spent shale and heat recovered from the shale ash and evolved gases can provide all the heat requirements of the retort . These technologies can achieve 80 @-@ 90 % of Fischer assay yield . Two well @-@ established shale oil industries use internal combustion technologies : Kiviter process facilities have been operated continuously in Estonia since the 1920s , and a number of Chinese companies operate Fushun process facilities .

Common drawbacks of internal combustion technologies are that the combustible oil shale gas is diluted by combustion gases and particles smaller than 10 millimeters ( 0 @.@ 4 in ) can not be processed. Uneven distribution of gas across the retort can result in blockages when hot spots cause particles to fuse or disintegrate.

= = = Hot recycled solids = = =

Hot recycled solids technologies deliver heat to the oil shale by recycling hot solid particles ? typically oil shale ash . These technologies usually employ rotating kiln or fluidized bed retorts , fed

by fine oil shale particles generally having a diameter of less than 10 millimeters ( 0 @.@ 4 in ); some technologies use particles even smaller than 2 @.@ 5 millimeters ( 0 @.@ 10 in ) . The recycled particles are heated in a separate chamber or vessel to about 800 ° C ( 1 @.@ 470 ° F ) and then mixed with the raw oil shale to cause the shale to decompose at about 500 ° C ( 932 ° F ) . Oil vapour and shale oil gas are separated from the solids and cooled to condense and collect the oil . Heat recovered from the combustion gases and shale ash may be used to dry and preheat the raw oil shale before it is mixed with the hot recycle solids .

In the Galoter and Enefit processes , the spent oil shale is burnt in a separate furnace and the resulting hot ash is separated from the combustion gas and mixed with oil shale particles in a rotating kiln . Combustion gases from the furnace are used to dry the oil shale in a dryer before mixing with hot ash . The TOSCO II process uses ceramic balls instead of shale ash as the hot recycled solids . The distinguishing feature of the Alberta Taciuk Process ( ATP ) is that the entire process occurs in a single rotating multi? chamber horizontal vessel .

Because the hot recycle solids are heated in a separate furnace, the oil shale gas from these technologies is not diluted with combustion exhaust gas. Another advantage is that there is no limit on the smallest particles that the retort can process, thus allowing all the crushed feed to be used. One disadvantge is that more water is used to handle the resulting finer shale ash.

# = = = Conduction through a wall = = =

These technologies transfer heat to the oil shale by conducting it through the retort wall . The shale feed usually consists of fine particles . Their advantage lies in the fact that retort vapors are not combined with combustion exhaust . The Combustion Resources process uses a hydrogen ? fired rotating kiln , where hot gas is circulated through an outer annulus . The Oil @-@ Tech staged electrically heated retort consists of individual inter @-@ connected heating chambers , stacked atop each other . Its principal advantage lies in its modular design , which enhances its portability and adaptability . The Red Leaf Resources EcoShale In @-@ Capsule Process combines surface mining with a lower @-@ temperature heating method similar to in situ processes by operating within the confines of an earthen structure . A hot gas circulated through parallel pipes heats the oil shale rubble . An installation within the empty space created by mining would permit rapid reclamation of the topography . A general drawback of conduction through a wall technologies is that the retorts are more costly when scaled @-@ up due to the resulting large amount of heat conducting walls made of high @-@ temperature alloys .

## = = = Externally generated hot gas = = =

In general , externally generated hot gas technologies are similar to internal combustion technologies in that they also process oil shale lumps in vertical shaft kilns . Significantly , though , the heat in these technologies is delivered by gases heated outside the retort vessel , and therefore the retort vapors are not diluted with combustion exhaust . The Petrosix and Paraho Indirect employ this technology . In addition to not accepting fine particles as feed , these technologies do not utilize the potential heat of combusting the char on the spent shale and thus must burn more valuable fuels . However , due to the lack of combustion of the spent shale , the oil shale does not exceed 500 ° C (  $932\ ^\circ$  F ) and significant carbonate mineral decomposition and subsequent CO2 generation can be avoided for some oil shales . Also , these technologies tend to be the more stable and easier to control than internal combustion or hot solid recycle technologies .

### = = = Reactive fluids = = =

Kerogen is tightly bound to the shale and resists dissolution by most solvents. Despite this constraint, extraction using especially reactive fluids has been tested, including those in a supercritical state. Reactive fluid technologies are suitable for processing oil shales with a low hydrogen content. In these technologies, hydrogen gas (H2) or hydrogen donors (chemicals that

donate hydrogen during chemical reactions ) react with coke precursors ( chemical structures in the oil shale that are prone to form char during retorting but have not yet done so ) . Reactive fluid technologies include the IGT Hytort ( high @-@ pressure H2 ) process , donor solvent processes , and the Chattanooga fluidized bed reactor . In the IGT Hytort oil shale is processed in a high @-@ pressure hydrogen environment . The Chattanooga process uses a fluidized bed reactor and an associated hydrogen @-@ fired heater for oil shale thermal cracking and hydrogenation . Laboratory results indicate that these technologies can often obtain significantly higher oil yields than pyrolysis processes . Drawbacks are the additional cost and complexity of hydrogen production and high @-@ pressure retort vessels .

# = = = Plasma gasification = = =

Several experimental tests have been conducted for the oil @-@ shale gasification by using plasma technologies . In these technologies , oil shale is bombarded by radicals ( ions ) . The radicals crack kerogen molecules forming synthetic gas and oil . Air , hydrogen or nitrogen are used as plasma gas and processes may operate in an arc , plasma arc , or plasma electrolysis mode . The main benefit of these technologies is processing without using water .

## = = In situ technologies = =

In situ technologies heat oil shale underground by injecting hot fluids into the rock formation , or by using linear or planar heating sources followed by thermal conduction and convection to distribute heat through the target area . Shale oil is then recovered through vertical wells drilled into the formation . These technologies are potentially able to extract more shale oil from a given area of land than conventional ex situ processing technologies , as the wells can reach greater depths than surface mines . They present an opportunity to recover shale oil from low @-@ grade deposits that traditional mining techniques could not extract .

During World War II a modified in situ extraction process was implemented without significant success in Germany . One of the earliest successful in situ processes was underground gasification by electrical energy (Ljungström method)? a process exploited between 1940 and 1966 for shale oil extraction at Kvarntorp in Sweden. Prior to the 1980s, many variations of the in situ process were explored in the United States. The first modified in situ oil shale experiment in the United States was conducted by Occidental Petroleum in 1972 at Logan Wash, Colorado. Newer technologies are being explored that use a variety of heat sources and heat delivery systems.

### = = = Wall conduction = = =

Wall conduction in situ technologies use heating elements or heating pipes placed within the oil shale formation . The Shell in situ conversion process ( Shell ICP ) uses electrical heating elements for heating the oil shale layer to between 650 and 700 ° F ( 340 and 370 ° C ) over a period of approximately four years . The processing area is isolated from surrounding groundwater by a freeze wall consisting of wells filled with a circulating super @-@ chilled fluid . Disadvantages of this process are large electrical power consumption , extensive water use , and the risk of groundwater pollution . The process was tested since the early 1980s at the Mahogany test site in the Piceance Basin . 1 @,@ 700 barrels ( 270 m3 ) of oil were extracted in 2004 at a 30 @-@ by @-@ 40 @-@ foot ( 9 @.@ 1 by 12 @.@ 2 m ) testing area .

In the CCR Process proposed by American Shale Oil , superheated steam or another heat transfer medium is circulated through a series of pipes placed below the oil shale layer to be extracted . The system combines horizontal wells , through which steam is passed , and vertical wells , which provide both vertical heat transfer through refluxing of converted shale oil and a means to collect the produced hydrocarbons . Heat is supplied by combustion of natural gas or propane in the initial phase and by oil shale gas at a later stage .

The Geothermic Fuels Cells Process (IEP GFC) proposed by Independent Energy Partners

extracts shale oil by exploiting a high @-@ temperature stack of fuel cells . The cells , placed in the oil shale formation , are fueled by natural gas during a warm @-@ up period and afterward by oil shale gas generated by its own waste heat .

## = = = Externally generated hot gas = = =

Externally generated hot gas in situ technologies use hot gases heated above @-@ ground and then injected into the oil shale formation . The Chevron CRUSH process , which was researched by Chevron Corporation in partnership with Los Alamos National Laboratory , injects heated carbon dioxide into the formation via drilled wells and to heat the formation through a series of horizontal fractures through which the gas is circulated . General Synfuels International has proposed the Omnishale process involving injection of super @-@ heated air into the oil shale formation . Mountain West Energy 's In Situ Vapor Extraction process uses similar principles of injection of high @-@ temperature gas .

### = = = ExxonMobil Electrofrac = = =

ExxonMobil 's in situ technology ( ExxonMobil Electrofrac ) uses electrical heating with elements of both wall conduction and volumetric heating methods . It injects an electrically conductive material such as calcined petroleum coke into the hydraulic fractures created in the oil shale formation which then forms a heating element . Heating wells are placed in a parallel row with a second horizontal well intersecting them at their toe . This allows opposing electrical charges to be applied at either end .

## = = = Volumetric heating = = =

The Illinois Institute of Technology developed the concept of oil shale volumetric heating using radio waves ( radio frequency processing ) during the late 1970s . This technology was further developed by Lawrence Livermore National Laboratory . Oil shale is heated by vertical electrode arrays . Deeper volumes could be processed at slower heating rates by installations spaced at tens of meters . The concept presumes a radio frequency at which the skin depth is many tens of meters , thereby overcoming the thermal diffusion times needed for conductive heating . Its drawbacks include intensive electrical demand and the possibility that groundwater or char would absorb undue amounts of the energy . Radio frequency processing in conjunction with critical fluids is being developed by Raytheon together with CF Technologies and tested by Schlumberger .

Microwave heating technologies are based on the same principles as radio wave heating, although it is believed that radio wave heating is an improvement over microwave heating because its energy can penetrate farther into the oil shale formation. The microwave heating process was tested by Global Resource Corporation. Electro @-@ Petroleum proposes electrically enhanced oil recovery by the passage of direct current between cathodes in producing wells and anodes located either at the surface or at depth in other wells. The passage of the current through the oil shale formation results in resistive Joule heating.

## = = Economics = =

The dominant question for shale oil production is under what conditions shale oil is economically viable . According to the United States Department of Energy , the capital costs of a 100 @,@ 000 barrels per day ( 16 @,@ 000 m3 / d ) ex @-@ situ processing complex are \$ 3 ? 10 billion . The various attempts to develop oil shale deposits have succeeded only when the shale @-@ oil production cost in a given region is lower than the price of petroleum or its other substitutes . According to a survey conducted by the RAND Corporation , the cost of producing shale oil at a hypothetical surface retorting complex in the United States ( comprising a mine , retorting plant , upgrading plant , supporting utilities , and spent oil shale reclamation ) , would be in a range of US \$

70 ? 95 per barrel ( \$ 440 ? 600 / m3 ) , adjusted to 2005 values . Assuming a gradual increase in output after the start of commercial production , the analysis projects a gradual reduction in processing costs to \$ 30 ? 40 per barrel ( \$ 190 ? 250 / m3 ) after achieving the milestone of 1 billion barrels (  $160 \times 10 ^6 \text{ m3}$ ) . The United States Department of Energy estimates that the ex @-@ situ processing would be economic at sustained average world oil prices above US \$ 54 per barrel and in @-@ situ processing would be economic at prices above \$ 35 per barrel . These estimates assume a return rate of 15 % . Royal Dutch Shell announced in 2006 that its Shell ICP technology would realize a profit when crude oil prices are higher than \$ 30 per barrel ( \$ 190 / m3 ) , while some technologies at full @-@ scale production assert profitability at oil prices even lower than \$ 20 per barrel ( \$ 130 / m3 ) .

To increase the efficiency of oil shale retorting and by this the viability of the shale oil production, researchers have proposed and tested several co @-@ pyrolysis processes, in which other materials such as biomass, peat, waste bitumen, or rubber and plastic wastes are retorted along with the oil shale. Some modified technologies propose combining a fluidized bed retort with a circulated fluidized bed furnace for burning the by @-@ products of pyrolysis ( char and oil shale gas ) and thereby improving oil yield, increasing throughput, and decreasing retorting time.

Other ways of improving the economics of shale oil extraction could be to increase the size of the operation to achieve economies of scale , use oil shale that is a by @-@ product of coal mining such as at Fushun China , produce specialty chemicals as by Viru Keemia Grupp in Estonia , co @-@ generate electricity from the waste heat and process high grade oil shale that yields more oil per shale processed .

A possible measure of the viability of oil shale as an energy source lies in the ratio of the energy in the extracted oil to the energy used in its mining and processing ( Energy Returned on Energy Invested , or EROEI ) . A 1984 study estimated the EROEI of the various known oil shale deposits as varying between 0 @.@ 7 ? 13 @.@ 3 ; Some companies and newer technologies assert an EROEI between 3 and 10 . According to the World Energy Outlook 2010 , the EROEI of ex @-@ situ processing is typically 4 to 5 while of in @-@ situ processing it may be even as low as 2 .

To increase the EROEI, several combined technologies were proposed. These include the usage of process waste heat, e.g. gasification or combustion of the residual carbon (char), and the usage of waste heat from other industrial processes, such as coal gasification and nuclear power generation.

The water requirements of extraction processes are an additional economic consideration in regions where water is a scarce resource .

### = = Environmental considerations = =

Objections to its potential environmental impact have stalled governmental support for extraction of shale oil in some countries , such as Australia . Shale oil extraction may involve a number of different environmental impacts that vary with process technologies . Depending on the geological conditions and mining techniques , mining impacts may include acid drainage induced by the sudden rapid exposure and subsequent oxidation of formerly buried materials , the introduction of metals into surface water and groundwater , increased erosion , sulfur gas emissions , and air pollution caused by the production of particulates during processing , transport , and support activities . Surface mining for ex situ processing , as with in situ processing , requires extensive land use and ex situ thermal processing generates wastes that require disposal . Mining , processing , spent oil shale disposal , and waste treatment require land to be withdrawn from traditional uses . Depending on the processing technology , the waste material may contain pollutants including sulfates , heavy metals , and polycyclic aromatic hydrocarbons , some of which are toxic and carcinogenic . Experimental in situ conversion processes may reduce some of these impacts , but may instead cause other problems , such as groundwater pollution .

The production and usage of oil shale usually generates more greenhouse gas emissions, including carbon dioxide, than conventional fossil fuels. Depending on the technology and the oil shale composition, shale oil extraction processes may also emit sulfur dioxide, hydrogen sulfide,

carbonyl sulfide, and nitrogen oxides. Developing carbon capture and storage technologies may reduce the processes 'carbon footprint.

Concerns have been raised over the oil shale industry 's use of water , particularly in arid regions where water consumption is a sensitive issue . Above @-@ ground retorting typically consumes between one and five barrels of water per barrel of produced shale oil , depending on technology . Water is usually used for spent oil shale cooling and oil shale ash disposal . In situ processing , according to one estimate , uses about one @-@ tenth as much water . In other areas , water must be pumped out of oil shale mines . The resulting fall in the water table may have negative effects on nearby arable land and forests .

A 2008 programmatic environmental impact statement issued by the United States Bureau of Land Management stated that surface mining and retort operations produce 2 to 10 U.S. gallons ( 7 @.@ 6 to 37 @.@ 91; 1 @.@ 7 to 8 @.@ 3 imp gal ) of waste water per 1 short ton ( 0 @.@ 91t ) of processed oil shale .