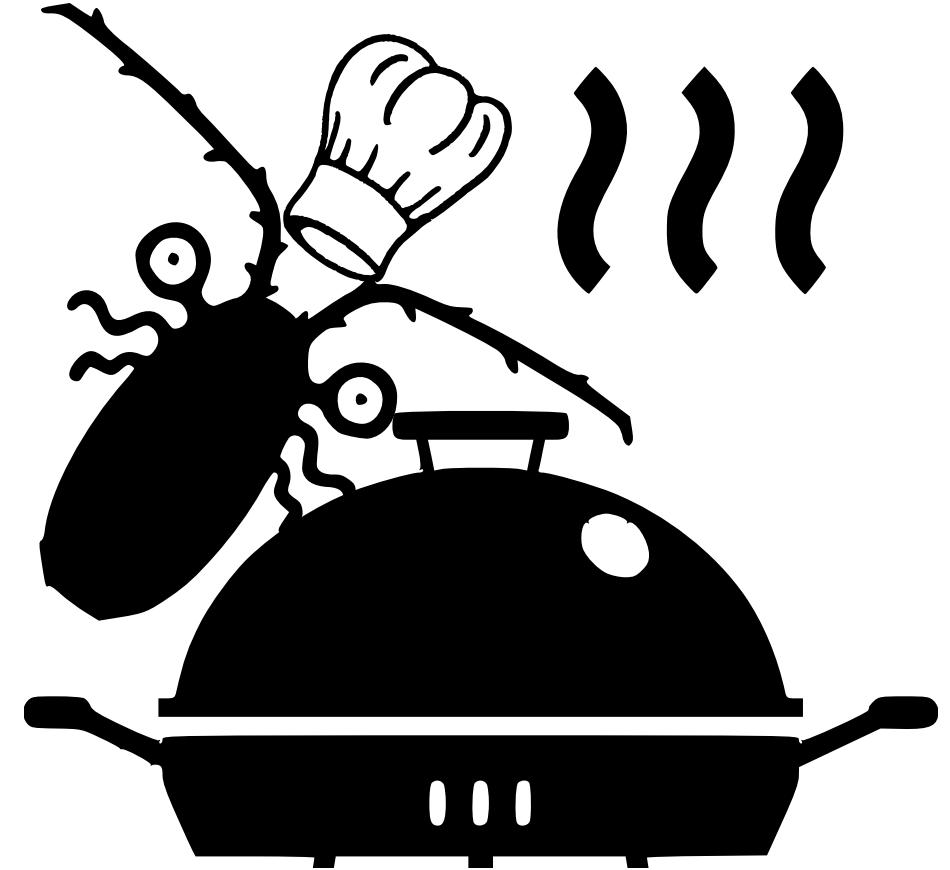


# Plankton Barbecue

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## Introduction

### Natural Thermal Convection

Those plumes coming out from our BBQ grill are caused by a difference in density consequence of temperature variations.

### Governing Equations

#### • ( $\approx$ ) Momentum:

$$\frac{\partial \omega}{\partial t} + \frac{\partial \psi}{\partial y} \frac{\partial \omega}{\partial x} - \frac{\partial \psi}{\partial x} \frac{\partial \omega}{\partial y} = \frac{1}{Re} \nabla^2 \omega + \beta g \frac{\partial T}{\partial x}$$

#### • Stream fnc - Vorticity - Velocity:

$$\nabla^2 \psi = -\omega, \quad u = \frac{\partial \psi}{\partial y}, \quad v = -\frac{\partial \psi}{\partial x}$$

#### • Energy:

$$\frac{\partial T}{\partial t} + (\vec{u} \cdot \nabla T) = \frac{1}{RePr} \nabla^2 T$$

#### • (Bonus!!!) Mass Transfer:

$$\frac{\partial c}{\partial t} + (\vec{u} \cdot \nabla c) = \frac{1}{Pe} \nabla^2 c$$

The last Eq. models a substance moving with the fluid.

## Method

To solve numerically the equations:

- 1 Set up the initial conditions for  $\psi$ ,  $u$  and  $v$ .
- 2 Solve the vorticity equation. (Exp FTCS).
- 3 Solve the Poisson equation for  $\psi$ . (Std. discr.  $\nabla^2$ ).
- 4 Compute the new velocity from  $\psi$ .
- 5 Solve the Energy equation for  $T$ . (Exp FTCS).
- 6 Solve the Mass transfer equation. (Exp FTCS).
- 7 Go to step 2.

## BBQ Grill: Air Thermal Convection

As benchmark parameters we chose:

$$Re = 4365.30, \quad Pr = 0.72, \quad Pe = 0.07$$

For a rectangular cavity width dimensions: 0.65m height, and 2.6m wide, and normalized temperatures  $T_c = 292.5^\circ K$ ,  $T_h = 293.5^\circ K$ .

The Figure 2 the fluid shows the normalized velocities, temperature and concentration evolution for several times, some remarkable facts are:

- Buoyancy force makes rise the warmer water from the bottom.
- Cell formations even for early times.
- Iso-thermal and Iso-concentration regions.

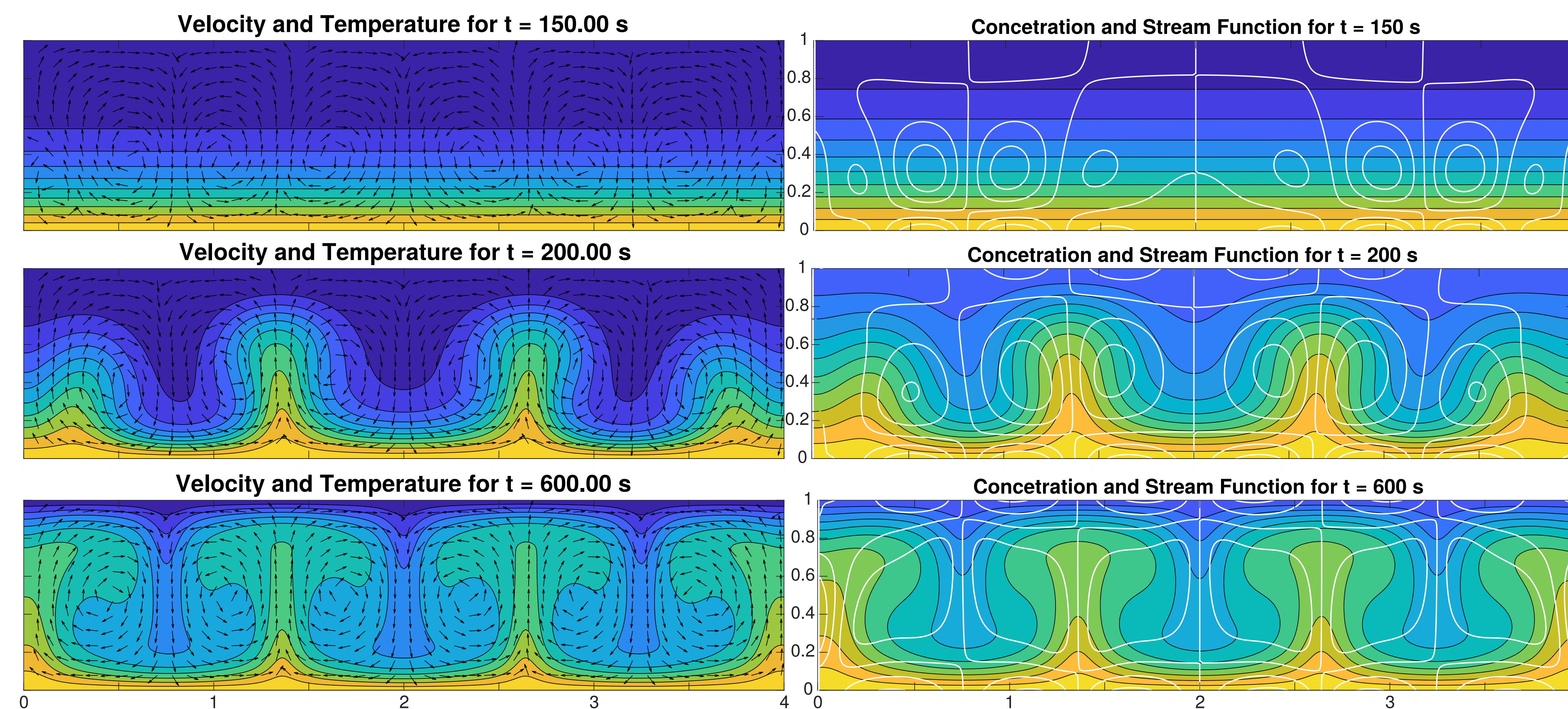


Figure 2: Air thermal convection and mass transfer in normalized velocity, temperature and mass concentration for different times.

## Numerical Convergence

Due to the high Reynolds number the experimental study for the convergence rates presents some challenges:

- Variations in the grid size cause variation in the direction of rotation in the cells.

## Cells and Spatial Resolution

The Figure 1 shows that the simulation results depend on the discretization size. In the coarse discretization only 4 cells Rayleigh-Benard cells form, compared to 6 in the fine discretization. This indicates that some discretizations cannot completely resolve the structure of the flow.

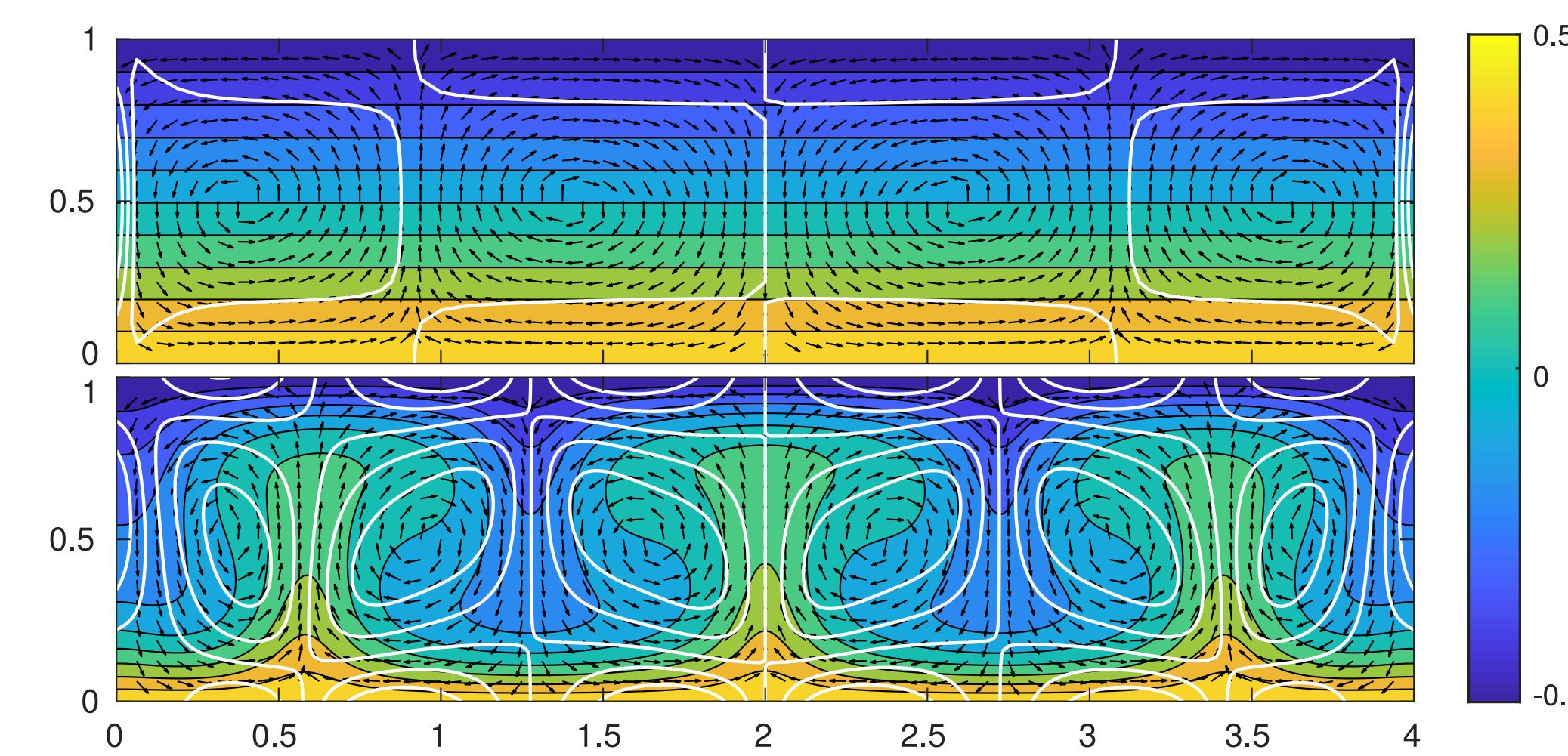


Figure 1: Cell on grids: (top)  $\Delta x = 156 \times 10^{-3}$ ,  $\Delta y = 62.5 \times 10^{-3}$  (bottom)  $\Delta x = 39 \times 10^{-3}$ ,  $\Delta y = 15.4 \times 10^{-3}$ .

## And the plankton?

- Phytoplankton is the base of the oceanic food chain, it sinks in the oceans up to 160m per year (passive swimmers).
- The temperature in the ocean varies up to  $10^\circ K$  in a year.
- The buoyancy forces keep them in specific regions in the ocean.

We wanted to study the effects of a variation of  $2^\circ K$  in a big rectangular area in the sea (160m deep, 1.6km wide) with planktonic organisms in the bottom, getting as parameters:

$$Re = 184269, \quad Pr = 7.56, \quad Pe = 6965.39$$

Although the Reynolds number is enormous, some general structure of this phenomena may be preserved as the number of cells or the average concentration in specific areas.

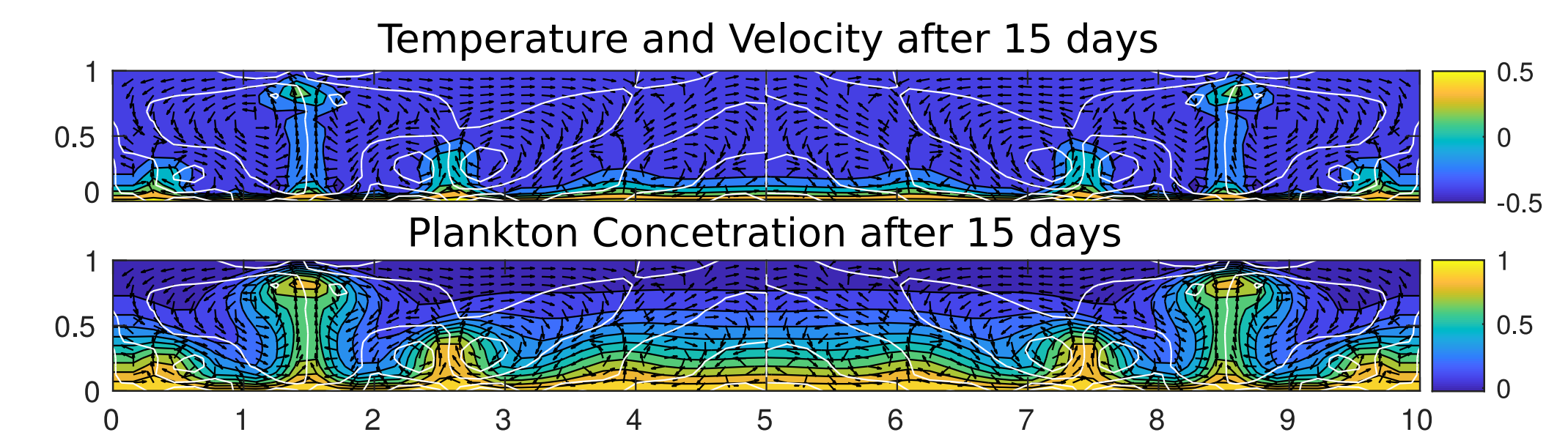


Figure 3: Thermal convection with planktonic mass transfer in the sea.

## Final Thoughts!

### Conclusions

- The behavior of the thermal cells depends on the size of the spatial discretization.
- Even with high Reynolds numbers the implemented method seems to show properly the general structure of the fluid.

### Pendings

- A solver using the projection method was considered, however, the staggered grid was an issue for the energy equation.
- An implementation using the second order FTBS scheme will help to deal with higher Reynolds numbers.

### Spatial Convergence order

$u$	1.5339	$v$	1.3119	$T$	0.3145
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