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Appendices of "Heat Transfer 2: Radiation and Exchangers"

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Appendices

A.1. Physical properties of some materials

	ρ	c_p	λ		ρ	c_p	λ
	kg m ⁻³	J kg ⁻¹ K ⁻¹	W m ⁻¹ K ⁻¹		kg m ⁻³	J kg ⁻¹ K ⁻¹	W m ⁻¹ K ⁻¹
Metals and alloys				Construction materials			
Carbon steel	7,833	465	54	Slate	2,400	879	2.2
Stainless steel 15% Cr, 10% Ni	7,864	460	20	Basalt	2,850	881	1.6
Stainless steel 18% Cr, 8% Ni	7,816	460	16.3	Cavernous concrete	1,900	879	1.4
Stainless steel 25% Cr, 20% Ni	7,864	460	13	Solid concrete	2,300	878	1.75
Alumina			29	Bitumen (cardboard)	1,050	1,305	0.23
Aluminum	2,707	896	204	Light hardwoods (dry)	525	1,250	0.15
Silver	10,525	234	407	Medium-heavy hardwoods (dry)	675	1,250	0.23
Bronze 75% Cu, 25%Sn	8,800	377	188	Very light hardwoods (dry)	375	1,250	0.12
Bronze 92% Cu, 8% Al	7,900	377	71	Light softwoods (dry)	375	1,250	0.12
Graphite carbon	2,250	707	147	Medium-weight softwoods (dry)	500	1,250	0.15
Silicon carbide			13	Very light softwoods (dry)	375	1,250	0.12
Bronze 75% Cu, 25%Sn	2,118	7,160	449	Terracotta brick	1,800	878	1.15
Bronze 92% Cu, 8% Al	8,922	410	22.7	Hard limestone	2,450	882	2.4

	ρ	c_p	λ		ρ	c_p	λ
	kg m ⁻³	J kg ⁻¹ K ⁻¹	W m ⁻¹ K ⁻¹		kg m ⁻³	J kg ⁻¹ K ⁻¹	W m ⁻¹ K ⁻¹
Metals and alloys				Construction materials			
Copper	8,954	383	386	Cotta brick	1,650	879	1
Cupronickel 70%Cu, 30% Ni	8,900	377	29.3	Hard limestone	2,400	875	2.4
Duralumin	2,787	883	164	Soft limestone	400	3,000	0.12
Tin	7,304	226	64	Floor tile	500	3,000	0.15
Iron	7,870	452	73	Okoumé plywood	2,600	881	3
Melting	7,849	460	59	Pine plywood	1,800	889	0.7
Brass 70%Cu, 30%Zn	8,522	385	111	Granite	2,500	880	2.6
Magnesium	1,740	1,004	151	Gravel (bulk)	2,350	881	1.1
Gold	19,300	128	312	Sandstone	2,700	881	2.5
Platinum	21,400	140	69	Lava stone	1,440	840	0.48
Lead	11,373	130	35	Marble	2,400	879	2.2
Liquid sodium	930	1,381	84.5	Insulating materials			
Titanium	4,500	523	20.9	Balsa	140		0.054
Tungsten	19,350	134	163	Cotton	80	1,300	0.06
Zinc	7,144	384	112	Kapok			0.035
Miscellaneous materials				Rockwool	20	880	0.047
Asbestos	575	1,046	0.15		55	880	0.038
Asphalt	2,115	920	0.062		135	880	0.041
Rubber (natural)	1,150		0.28	Glass wool	8	875	0.051
Rubber (vulcanized)	1,100	2,010	0.13		10	880	0.045
Cardboard	86	2,030	0.048		15	880	0.041
Leather	998		0.159		40	880	0.035
Ice	920	2,040	1.88	Expanded cork	120	2,100	0.044
Plexiglass	1,190	1,465	0.19	Carpet	200	1,300	0.06
Porcelain	2,400	1,088	1.035	Polyurethane (foam)	32	1,300	0.03
Polyethylene	929	1,830	0.46		50	1,360	0.035
PVC	1,459	930	0.19		85	1,300	0.045
Sand	1,515	800	0.2-1.0	PVC (rigid foam)	30	1,300	0.031
Teflon	2,170	1,004	0.25		40	1,300	0.041
Wet land	1,900	2,000	2	Expanded polystyrene	12	1,300	0.047
Dry land	1,500	1,900	1		14	1,300	0.043
Glass	2,300	837	1.05		18	1,300	0.041
Pyrex glass	2,220	728	1.13	Styrofoam	30		0.032

A.2. Physical properties of air and water

Properties of water at saturation							Properties of air at 1 atm						
<i>T</i>	ρ	c_p	λ	$10^4 \mu$	$10^7 a$	<i>Pr</i>	<i>T</i>	ρ	c_p	λ	$10^4 \mu$	$10^7 a$	<i>Pr</i>
°C	kg m ⁻³	J kg ⁻¹ K ⁻¹	W m ⁻¹ K ⁻¹	Pa s ⁻¹	m ² s ⁻¹		°C	kg m ⁻³	J kg ⁻¹ K ⁻¹	W m ⁻¹ K ⁻¹	Pa s ⁻¹	m ² s ⁻¹	
0	1,002	4,218	0.552	17.90	1.31	13.06	0	1.292	1,006	0.0242	1.72	1.86	0.72
20	1,001	4,182	0.597	10.10	1.43	7.02	20	1.204	1,006	0.0257	1.81	2.12	0.71
40	995	4,178	0.628	6.55	1.51	4.34	40	1.127	1,007	0.0272	1.90	2.40	0.70
60	985	4,184	0.651	4.71	1.55	3.02	60	1.059	1,008	0.0287	1.99	2.69	0.70
80	974	4,196	0.668	3.55	1.64	2.22	80	0.999	1,010	0.0302	2.09	3.00	0.70
100	960	4,216	0.680	2.82	1.68	1.74	100	0.946	1,012	0.0318	2.18	3.32	0.69
120	945	4,250	0.685	2.33	1.71	1.45	120	0.898	1,014	0.0333	2.27	3.66	0.69
140	928	4,283	0.684	1.99	1.72	1.24	140	0.854	1,016	0.0345	2.34	3.98	0.69
160	910	4,342	0.680	1.73	1.73	1.10	160	0.815	1,019	0.0359	2.42	4.32	0.69
180	889	4,417	0.675	1.54	1.72	1.00	180	0.779	1,022	0.0372	2.50	4.67	0.69
200	867	4,505	0.665	1.39	1.71	0.94	200	0.746	1,025	0.0386	2.57	5.05	0.68
220	842	4,610	0.652	1.26	1.68	0.89	220	0.700	1,028	0.0399	2.64	5.43	0.68
240	816	4,756	0.635	1.17	1.64	0.88	240	0.688	1,032	0.0412	2.72	5.80	0.68
260	786	4,949	0.611	1.08	1.58	0.87	260	0.662	1,036	0.0425	2.79	6.20	0.68
280	753	5,208	0.580	1.02	1.48	0.91	280	0.638	1,040	0.0437	2.86	6.59	0.68
300	714	5,728	0.540	0.96	1.32	1.02	300	0.616	1,045	0.0450	2.93	6.99	0.68

Correlations between 0 and 100°C (*T*, temperature in °C).

For air:

$$\rho = \frac{353}{T+273} \text{ (kg m}^{-3}\text{)}$$

$$c_p = 1,008 \text{ (J kg}^{-1} \text{ K}^{-1}\text{)}$$

$$\lambda = 7.57 \times 10^{-5} T + 0.0242 \text{ (W m}^{-1} \text{ K}^{-1}\text{)}$$

$$\mu = 10^{-5}(0.0046 T + 1.7176) \text{ (kg m}^{-1} \text{ s}^{-1}\text{)}$$

$$a = 10^{-5}(0.0146 T + 1.8343) \text{ (m}^2 \text{ s}^{-1}\text{)}$$

$$Pr = -2.54 \times 10^{-4} T + 0.7147$$

$$\beta \approx \frac{1}{T+273} \text{ (K}^{-1}\text{)}$$

For water:

$$\rho = -0.00380 T^2 - 0.0505 T + 1002.6 \text{ (kg m}^{-3}\text{)}$$

$$c_p = 4,180 \text{ (J kg}^{-1} \text{ K}^{-1}\text{)}$$

$$\lambda = -9.87 \times 10^{-6} T^2 + 2.238 \times 10^{-3} T + 0.5536 \text{ (W m}^{-1} \text{ K}^{-1}\text{)}$$

$$\mu = 10^{-4} \times \frac{0.0003354 T^2 - 0.07377 T + 17.9}{8.765 \times 10^{-5} T^2 + 0.03032 T + 1} \text{ (kg m}^{-1} \text{ s}^{-1}\text{)}$$

$$\alpha = 10^{-7} \times (-0.00360 T + 1.340) \text{ (m}^2 \text{ s}^{-1}\text{)}$$

$$Pr = \frac{-0.0037 T^2 + 1.387 T + 13.06}{0.005297 T^2 + 0.1241 T + 1}$$

$$\frac{g\beta\rho^2 c_p}{\lambda\mu} = (0.0105 T^2 + 0.477 T - 0.0363) \times 10^9 \text{ (K}^{-1} \text{ m}^{-3}\text{)}$$

$$\log_{10}[p_{sat}(T + 273)] = 20.3182 - \frac{2,795}{T + 273} - 3.868 \log_{10}(T + 273) \\ \text{(mmHg) - } 50^\circ\text{C} < T < 200^\circ\text{C}$$

$$L_v = 2,495 - 2.346 T \text{ (kJ kg}^{-1}\text{) } 0^\circ\text{C} < T < 100^\circ\text{C}$$

A.3. Bessel equations and functions

A.3.1. Particular Bessel equations and their solutions

$$y'' + \frac{y'}{x} + m^2 y = 0 \Rightarrow y = k_1 J_0(mx) + k_2 Y_0(mx)$$

$$x^2 y'' + x y' + (x^2 - n^2) y = 0 \Rightarrow y = k_1 J_n(x) + k_2 Y_n(x) \text{ (} n \text{ integer)}$$

$$y'' + \frac{y'}{x} - m^2 y = 0 \Rightarrow y = k_1 I_0(mx) + k_2 K_0(mx)$$

$$x^2 y'' + x y' - (x^2 - n^2) y = 0 \Rightarrow y = k_1 I_n(x) + k_2 K_n(x) \text{ (} n \text{ integer)}$$

with:

- J_n , unmodified Bessel function of the first kind of order n .
- I_n , modified Bessel function of the first kind of order n .
- Y_n , unmodified Bessel function of the second kind of order n .
- K_n , modified Bessel function of the second kind of order n .

A.3.2. Main properties of Bessel functions

– Recurrence:

$$J_{n+1}(u) = -J_{n-1}(u) + \frac{2n}{u}J_n(u) \quad Y_{n+1}(u) = -Y_{n-1}(u) + \frac{2n}{u}Y_n(u)$$

$$I_{n+1}(u) = I_{n-1}(u) - \frac{2n}{u}I_n(u) \quad K_{n+1}(u) = K_{n-1}(u) - \frac{2n}{u}K_n(u)$$

– Derivative:

$$\begin{aligned} \frac{dJ_0(u)}{du} &= -J_1(u); & \frac{dI_0(u)}{du} &= I_1(u); & \frac{dK_0(u)}{du} &= -K_1(u); & \frac{dY_0(u)}{du} &= -Y_1(u); \\ \frac{d[uJ_1(u)]}{du} &= uJ_0(u) \end{aligned}$$

– Integrals:

$$\int x^v W_{v-1}(\alpha x) dx = \frac{1}{\alpha} x^v W_v(\alpha x) \text{ for } W = J, Y, I$$

$$\int x^{-v} W_{v+1}(\alpha x) dx = -\frac{1}{\alpha} x^{-v} W_v(\alpha x) \text{ for } W = J, Y, K$$

$$\int_0^R r [J_0(\alpha r)]^2 dr = \frac{R^2}{2} \{ [J_0(\alpha R)]^2 + [J_1(\alpha R)]^2 \}$$

A.3.3. Asymptotic behavior of Bessel functions of order 0 and 1

$$\begin{aligned} \text{If } u \rightarrow 0: \quad & J_0(u) \rightarrow 1; \quad J_1(u) \rightarrow \frac{u}{2}; \quad Y_0(u) \rightarrow \left(\frac{2}{\pi}\right) \left[\ln\left(\frac{u}{2}\right) + \gamma \right]; \quad Y_1(u) \rightarrow \frac{2}{\pi u}; \\ & I_0(u) \rightarrow 1; \quad I_1(u) \rightarrow \frac{u}{2}; \quad K_0(u) \rightarrow -\ln\left(\frac{u}{2}\right) - \gamma; \quad K_1(u) \rightarrow \frac{1}{u} \end{aligned}$$

$$\text{If } u \rightarrow \infty: \quad J_0(u) \rightarrow \sqrt{\frac{2}{\pi u}} \cos\left(u - \frac{\pi}{4}\right); \quad J_1(u) \rightarrow \sqrt{\frac{2}{\pi u}} \cos\left(\frac{u}{2} - \frac{\pi}{4}\right);$$

$$Y_0(u) \rightarrow \sqrt{\frac{2}{\pi u}} \sin\left(u - \frac{\pi}{4}\right); \quad Y_1(u) \rightarrow \sqrt{\frac{2}{\pi u}} \sin\left(\frac{u}{2} - \frac{\pi}{4}\right);$$

$$I_0(u), I_1(u) \rightarrow \sqrt{\frac{2}{\pi u}} \exp(u); \quad K_0(u), K_1(u) \rightarrow \sqrt{\frac{\pi}{2u}} \exp(-u)$$

A.3.4. Useful equations

$$I_v(x)K_{v+1}(x) + I_{v+1}(x)K_v(x) = \frac{1}{x}$$

$$J_{v+1}(x)Y_v(x) - J_v(x)Y_{v+1}(x) = \frac{2}{\pi x}$$

A.4. Main integral transforms: Laplace, Fourier, Hankel

A.4.1. Laplace transform

– Definition:

$$L[T(t)] = \theta(p) = \int_0^\infty \exp(-pt) T(t) dt \quad \text{and:} \quad L^{-1}[\theta(p)] = T(t) \text{ (inverse transform)}$$

– Properties:

- linearity: $L[a_1 T_1(t) + a_2 T_2(t)] = a_1 L[T_1(t)] + a_2 L[T_2(t)]$, same for L^{-1} ;

- translation: $L[\exp(at)T(t)] = \theta(p-a)$; $L^{-1}[\theta(p-a)] = \exp(at)T(t)$:

$$L^{-1}[\exp(-ap)\theta(p)] = T(t-a) \text{ if } t > a$$

$$L^{-1}[\exp(-ap)\theta(p)] = 0 \text{ if } t \leq a$$

– Change of scale:

$$L[T(at)] = \frac{1}{a} \theta\left(\frac{p}{a}\right) L^{-1}[\theta(ap)] = \frac{1}{a} T\left(\frac{t}{a}\right)$$

– Derivation:

$$L[T'(t)] = p\theta(p) - T(0)L^{-1}[\theta^{(n)}(p)] = (-1)^n t^n T(t)$$

$$L[T''(t)] = p^2\theta(p) - pT(0) - T'(0)$$

– Integration:

$$L\left[\int_0^t T(u) du\right] = \frac{\theta(p)}{p} L^{-1}\left[\int_p^\infty \theta(u) du\right] = \frac{T(t)}{t}$$

– Multiplication by t^n :

$$L[t^n T(t)] = (-1)^n \theta^{(n)}(p) L^{-1}[p\theta(p)] = T'(t) - T(0)\delta(t)$$

– Division by t :

$$L\left[\frac{T(t)}{t}\right] = \int_p^\infty \theta(u) du L^{-1}\left[\frac{\theta(p)}{p}\right] = \int_0^t T(u) du$$

– Periodic functions: $L[T(t)] = \frac{\int_0^P \exp(-pt)T(t)dt}{1-\exp(pP)}$.

(Period P).

A.4.2. Complex Fourier transform

– Definition:

$$F[T(x)] = \theta(\omega) = \frac{1}{\sqrt{2\pi}} \int_{-\infty}^{+\infty} e^{i\omega x} T(x) dx$$

$$T(x) = F^{-1}[\theta(\omega)] = \frac{1}{\sqrt{2\pi}} \int_{-\infty}^{+\infty} e^{i\omega x} \theta(\omega) d\omega$$

– Properties:

$$F\left[\frac{\partial T}{\partial x}\right] = -i\omega\theta(\omega); F\left[\frac{\partial^2 T}{\partial x^2}\right] = -\omega^2\theta(\omega)$$

A.4.3. Fourier transform in sine and cosine

– Definitions:

- sine:

$$F_s[T(x)] = \theta_s(\omega) = \sqrt{\frac{2}{\pi}} \int_0^\infty T(x) \sin(\omega x) dx$$

$$T(x) = F_s^{-1}[\theta_s(\omega)] = \sqrt{\frac{2}{\pi}} \int_0^\infty \theta_s(\omega) \sin(\omega x) dx$$

- cosine:

$$F_c[T(x)] = \theta_c(\omega) = \sqrt{\frac{2}{\pi}} \int_0^\infty T(x) \cos(\omega x) dx$$

$$T(x) = F_c^{-1}[\theta_c(\omega)] = \sqrt{\frac{2}{\pi}} \int_0^\infty \theta_c(\omega) \cos(\omega x) dx$$

– Properties:

$$F_s \left[\frac{\partial T}{\partial x} \right] = -\omega \theta_c(\omega); F_c \left[\frac{\partial T}{\partial x} \right] = -\omega \theta_s(\omega) - \sqrt{\frac{2}{\pi}} T(0)$$

$$F_s \left[\frac{\partial^2 T}{\partial x^2} \right] = -\omega^2 \theta_s(\omega) + \omega \sqrt{\frac{2}{\pi}} T(0); F_c \left[\frac{\partial^2 T}{\partial x^2} \right] = -\omega^2 \theta_c(\omega) - \sqrt{\frac{2}{\pi}} \left(\frac{\partial T}{\partial x} \right)_{x=0}$$

A.4.4. Finite Fourier transform in sine and cosine

– Definitions: if the temperature $T(x)$ is only defined on the interval $[0, L]$, we can use a finite Fourier transformation in sine or cosine:

$$F_s[T(x)] = \theta_s(n) = \int_0^L T(x) \sin\left(\frac{n\pi x}{L}\right) dx$$

where $F_c[T(x)] = \theta_c(n) = \int_0^L T(x) \cos\left(\frac{n\pi x}{L}\right) dx.$

$$T(x) = F_s^{-1}[\theta_s(n)] = \frac{2}{L} \sum_{n=1}^\infty \theta_s(n) \sin\left(\frac{n\pi x}{L}\right)$$

where $T(x) = F_c^{-1}[\theta_c(n)] = \frac{1}{L} \theta_c(0) + \frac{2}{L} \sum_{n=1}^\infty \theta_c(n) \cos\left(\frac{n\pi x}{L}\right).$

– Properties:

$$F_s \left[\frac{\partial^2 T}{\partial x^2} \right] = \frac{n\pi}{L} [T(0) - (-1)^n T(L)] - \frac{n^2 \pi^2}{L^2} \theta_s(n)$$

$$F_c \left[\frac{\partial^2 T}{\partial x^2} \right] = (-1)^n \left(\frac{\partial T}{\partial x} \right)_{x=L} - \left(\frac{\partial T}{\partial x} \right)_{x=0} - \frac{n^2 \pi^2}{L^2} \theta_c(n)$$

A.4.5. Hankel transform of order ν

– Definition: for $\nu > -\frac{1}{2}$:

$$H_\nu[T(r)] = \theta_\nu(\sigma) = \int_0^\infty r J_\nu(\sigma r) T(r) dr; \quad T(r) = H_\nu^{-1}[\theta_\nu(\sigma)] = \int_0^\infty \sigma J_\nu(\sigma r) \theta_\nu(\sigma) d\sigma$$

– Property:

$$H_\nu \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) - \frac{\nu^2 T}{r^2} \right] = -\sigma^2 \theta_\nu(\sigma)$$

at order 0:

$$H_0[T(r) = T_i] = T_i \int_0^\infty r J_0(\sigma r) dr = T_i \frac{r}{\sigma} J_1(\sigma r)$$

A.5. Inverse Laplace transform

A.5.1. Analytical method

The Laplace transform $\theta(p)$ of the function $T(t)$ is given by: $L[T(t)] = \theta(p) = \int_0^\infty \exp(-pt) T(t) dt$.

There is no general analytic formula for calculating $T(t)$ knowing $\theta(p)$. However, we know the exact expression of $T(t)$ for some particular functions $\theta(p)$, examples of which can be found in section A.5.4 (see Spiegel (1990) for more complete tables). The use of these tables, associated with the particular properties of the inverse Laplace transform recalled in section A.6, allows us to solve a certain number of cases. We will always try to decompose a complex function into a sum, product, series, etc., of simple functions that are more easily invertible.

A.5.2. Numerical methods

When an analytical solution cannot be found, we can use one of the following two numerical methods:

– Stehfest method: the inverse transform of the function $\theta(p)$ can be calculated by (Stehfest 1970):

$$T(t) = \frac{\ln(2)}{t} \sum_{j=1}^N V_j \theta \left[\frac{j \ln(2)}{t} \right]$$

$N = 20$ (double precision):

$$\begin{aligned} V_1 &= -5.511463844797178 \times 10^{-6} & V_2 &= 1.523864638447972 \times 10^{-1} \\ V_3 &= -1.174654761904762 \times 10^2 & V_4 &= 1.734244933862434 \times 10^4 \\ V_5 &= -9.228069289021164 \times 10^5 & V_6 &= 2.377408778710318 \times 10^7 \\ V_7 &= -3.494211661953704 \times 10^8 & V_8 &= 3.241369852231879 \times 10^9 \\ V_9 &= -2.027694830723779 \times 10^{10} & V_{10} &= 8.946482982379724 \times 10^{10} \\ V_{11} &= -2.870209211471027 \times 10^{11} & V_{12} &= 6.829920102815115 \times 10^{11} \\ V_{13} &= -1.219082330054374 \times 10^{12} & V_{14} &= 1.637573800842013 \times 10^{12} \\ V_{15} &= -1.647177486836117 \times 10^{12} & V_{16} &= 1.221924554444226 \times 10^{12} \\ V_{17} &= -6.488065588175326 \times 10^{11} & V_{18} &= 2.333166532137059 \times 10^{11} \\ V_{19} &= -5.091380070546738 \times 10^{10} & V_{20} &= 5.091380070546738 \times 10^9 \end{aligned}$$

$N = 10$ (single precision):

$$\begin{aligned} V_1 &= \frac{1}{12}; V_2 = -\frac{385}{12}; V_3 = 1,279; V_4 = -\frac{46,871}{3}; V_5 = \frac{505,465}{6}; \\ V_6 &= -\frac{473,915}{2}; V_7 = \frac{1,127,735}{3}; V_8 = -\frac{1,020,215}{3}; V_9 = \frac{328,125}{2}; V_{10} = -\frac{65,625}{2} \end{aligned}$$

– Fourier method:

$$\begin{aligned} T(t) &= \frac{\exp(ct)}{t_{\max}} \\ &\left\langle \frac{\theta(c)}{2} + \sum_{k=1}^{\infty} \{ \operatorname{Re}[\theta(c + j\omega_k)] \cos(\omega_k t) - \operatorname{Im}[\theta(c + j\omega_k)] \sin(\omega_k t) \} \right\rangle \end{aligned}$$

$$\text{with: } \omega_k = \frac{k\pi}{t_{\max}}.$$

The infinite sum is in practice calculated for a finite number N of terms; we will generally take $N > 100$. This method requires choosing two parameters: c and t_{\max} . We must ensure a posteriori that $\exp(-2ct_{\max})(2t_{\max}) \approx 0$.

A.5.3. Choosing a method and checking the results

The Stehfest method is simpler to implement, because it does not require choosing certain parameters. The Fourier method can lead to a better result in the case of inversion of certain functions such as periodic functions, for example Maillet et al. (2000), Den Iseger (2006), Toutain et al. (2011). We can also directly use the Matlab subroutine “Invlap” based on De Hoog’s algorithm.

The study of the behavior of the function $\theta(p)$ at long times ($t \rightarrow \infty$ thus $p \rightarrow 0$) and at short times ($t \rightarrow 0$ thus $p \rightarrow \infty$) can lead to approximate formulas of $\theta(p)$ for which we can then find the inverse Laplace transform analytically. The comparison of these analytical solutions with the results of the numerical inversion gives an indication of the accuracy of the numerical inversion.

A.5.4. Table of Laplace transforms

From Spiegel (1990), $q = \sqrt{\frac{p}{a}}$.

$\theta(p) = [T(t)]$	$T(t)$
$\frac{1}{p}$	1
1	$\delta(t)$ Dirac
$\frac{1}{p^2}$	t
$\frac{1}{p^n} \ n = 1, 2, 3 \dots$	$\frac{t^{n-1}}{(n-1)!}$
$\frac{\ln(p)}{p}$	$-\ln(t) - \gamma; \ \gamma = 0.57721$
$\frac{\omega}{p^2 - \omega^2}$	$\sinh(\omega t)$
$\frac{p}{p^2 - \omega^2}$	$\cosh(\omega t)$
$\frac{\omega^2}{p^2 + \omega^2}$	$\sin(\omega t)$
$\frac{p}{p^2 + \omega^2}$	$\cos(\omega t)$

$\frac{1}{\sqrt{p}}$	$\frac{1}{\sqrt{\pi t}}$
$\frac{1}{p\sqrt{p}}$	$\frac{2}{\sqrt{\pi}}\sqrt{t}$
$\frac{b}{p(b + \sqrt{p})}$	$1 - \exp(b^2 t) \operatorname{erfc}(b\sqrt{t})$
$\frac{b}{\sqrt{p}(b + \sqrt{p})}$	$\exp(b^2 t) \operatorname{erf}(b\sqrt{t})$
$\frac{1}{p + \alpha}$	$e^{-\alpha t}$
$\frac{1}{(p + \alpha)(p + \beta)}$	$\frac{e^{-\beta t} - e^{-\alpha t}}{\alpha - \beta}$
$\frac{1}{(p + \alpha)^2}$	$t e^{-\alpha t}$
$\frac{p}{(p + \alpha)^2}$	$(1 - \alpha t) e^{-\alpha t}$
$\frac{p}{(p + \alpha)(p + \beta)}$	$\frac{\alpha e^{-\beta t} - \beta e^{-\alpha t}}{\alpha - \beta}$
$\frac{1}{(p + \alpha)(p + \beta)(p + \gamma)}$	$\frac{(\gamma - \beta) \exp(-\alpha t) + (\alpha - \gamma) \exp(-\beta t) + (\beta - \alpha) \exp(-\gamma t)}{(\alpha - \beta)(\beta - \gamma)(\gamma - \alpha)}$
$\frac{p}{(p + \alpha)(p + \beta)(p + \gamma)}$	$\frac{\alpha(\beta - \gamma) \exp(-\alpha t) + \beta(\gamma - \alpha) \exp(-\beta t) + \gamma(\alpha - \beta) \exp(-\gamma t)}{(\alpha - \beta)(\beta - \gamma)(\gamma - \alpha)}$
e^{-qx}	$\frac{x}{2\sqrt{\pi at^3}} \exp\left(-\frac{x^2}{4at}\right)$
$\frac{e^{-qx}}{q}$	$\sqrt{\frac{a}{\pi t}} \exp\left(-\frac{x^2}{4at}\right)$
$\frac{e^{-qx}}{p}$	$\operatorname{erfc}\left(\frac{x}{2\sqrt{at}}\right)$
$\frac{e^{-qx}}{pq}$	$2\sqrt{\frac{a}{\pi t}} \exp\left(-\frac{x^2}{4at}\right) - x \operatorname{erfc}\left(\frac{x}{2\sqrt{at}}\right)$
$\frac{e^{-qx}}{p^2}$	$\left(t + \frac{x^2}{2a}\right) \operatorname{erfc}\left(\frac{x}{2\sqrt{at}}\right) - x \sqrt{\frac{t}{\pi a}} \exp\left(-\frac{x^2}{4at}\right)$

$\frac{e^{-qx}}{q+h}$	$\sqrt{\frac{a}{\pi t}} \exp\left(-\frac{x^2}{4at}\right) - ha \exp(hx + ath^2) \operatorname{erfc}\left(\frac{x}{2\sqrt{at}} + h\sqrt{at}\right)$
$\frac{e^{-qx}}{q(q+h)}$	$a \exp(hx + ath^2) \operatorname{erfc}\left(\frac{x}{2\sqrt{at}} + h\sqrt{at}\right)$
$\frac{e^{-qx}}{p(q+h)}$	$\frac{1}{h} \operatorname{erfc}\left(\frac{x}{2\sqrt{at}}\right) - \frac{1}{h} \exp(hx + ath^2) \operatorname{erfc}\left(\frac{x}{2\sqrt{at}} + h\sqrt{at}\right)$
$\frac{e^{-qx}}{pq(q+h)}$	$\frac{2}{h} \sqrt{\frac{a}{\pi t}} \exp\left(-\frac{x^2}{4at}\right) - \frac{1+hx}{h^2} \operatorname{erfc}\left(\frac{x}{2\sqrt{at}}\right) + \frac{1}{h^2} \exp(hx + ath^2) \operatorname{erfc}\left(\frac{x}{2\sqrt{at}} + h\sqrt{at}\right)$
$\frac{e^{-qx}}{p-\alpha}$	$\frac{1}{2} \exp(at) \left\{ \exp\left(-\frac{x\sqrt{\alpha}}{\sqrt{a}}\right) \operatorname{erfc}\left(\frac{x}{2\sqrt{at}} - \sqrt{at}\right) + \exp\left(\frac{x\sqrt{\alpha}}{\sqrt{a}}\right) \operatorname{erfc}\left(\frac{x}{2\sqrt{at}} + \sqrt{at}\right) \right\}$
$\frac{e^{-qx}}{q(p-\alpha)}$	$\frac{1}{2} \exp(at) \sqrt{\frac{a}{\alpha}} \left\{ \exp\left(-\frac{x\sqrt{\alpha}}{\sqrt{a}}\right) \operatorname{erfc}\left(\frac{x}{2\sqrt{at}} - \sqrt{at}\right) - \exp\left(\frac{x\sqrt{\alpha}}{\sqrt{a}}\right) \operatorname{erfc}\left(\frac{x}{2\sqrt{at}} + \sqrt{at}\right) \right\}$
$\frac{e^{-qx}}{(q+h)^2}$	$-2h - 2h\left(\frac{a^3 t}{\pi}\right) \exp\left(-\frac{x^2}{4at}\right) + a(1 - hx - 2ah^2 t)$
$\frac{e^{-qx}}{p(q+h)^2}$	$\frac{1}{h^2} \operatorname{erfc}\left(\frac{x}{2\sqrt{at}}\right) - \frac{2}{h} \sqrt{\frac{at}{\pi}} \exp\left(-\frac{x^2}{4at}\right) - \frac{1}{h^2} (1 + hx + 2ah^2 t) \exp(hx + ah^2 t) \times \operatorname{erfc}\left(\frac{x}{2\sqrt{at}} + h\sqrt{at}\right)$
$K_0(qx)$	$\frac{1}{2t} \exp\left(-\frac{x^2}{4at}\right)$
$\frac{1}{p^{1/2}} K_{2n}(qx)$	$\frac{1}{2\sqrt{\pi t}} \exp\left(-\frac{x^2}{8at}\right) K_n\left(\frac{x^2}{8at}\right)$
$p^{n/2} K_n(qx)$	$\frac{x^n}{a^{n/2} (2t)^{n+1}} \exp\left(-\frac{x^2}{4at}\right)$

A.6. erf function

– Properties:

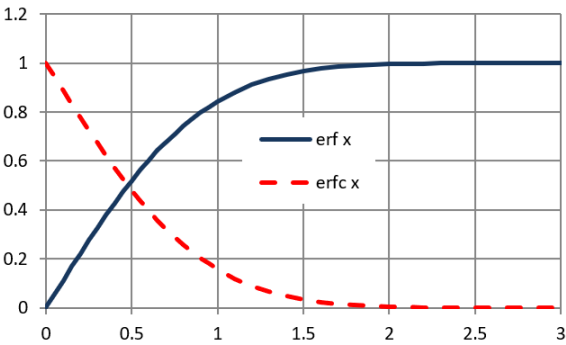
$$\operatorname{erf}(u)=\frac{2}{\sqrt{\pi}} \int_0^u \exp \left(-t^2\right) d t ;$$

$$\operatorname{ierfc}(u)=\frac{1}{\sqrt{\pi}} \exp \left(-u^2\right)-u[1-\operatorname{erf}(u)]$$

$$\operatorname{erfc}(u)=1-\operatorname{erf}(u) ;$$

$$\frac{d}{d x}[\operatorname{erf}(x)]=\frac{2}{\sqrt{\pi}} \exp \left(-x^2\right)$$

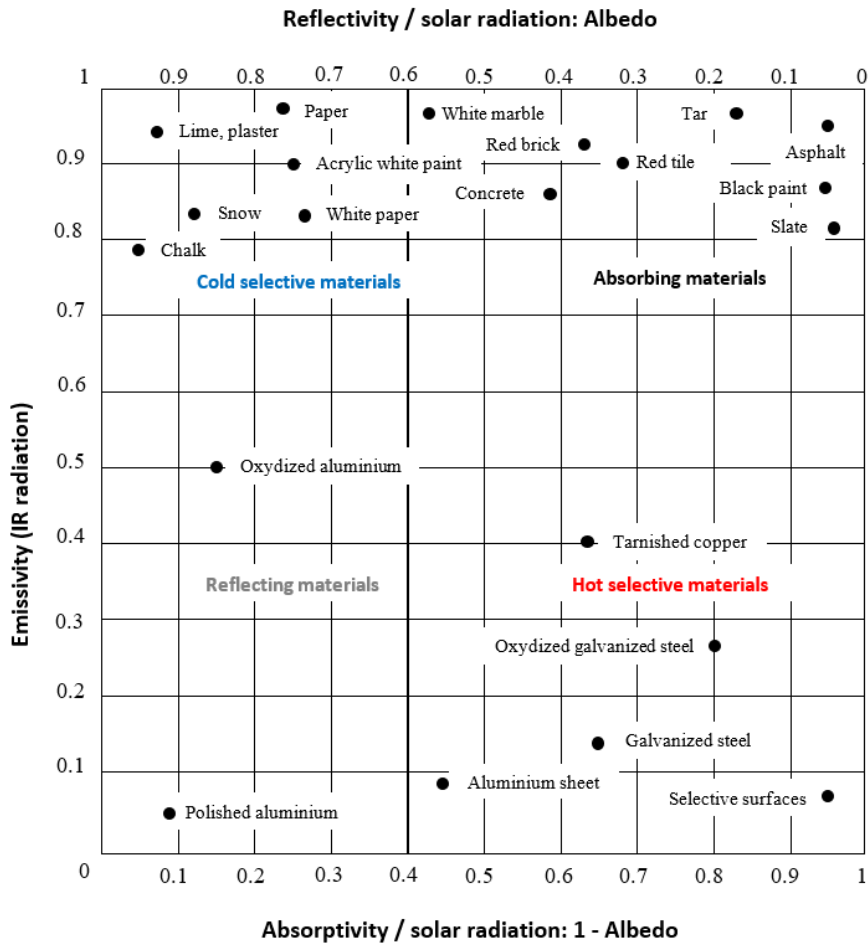
For $x \rightarrow \infty: \operatorname{erfc}(x)=\frac{\exp \left(-x^2\right)}{\sqrt{\pi}}\left[\frac{1}{x}-\frac{1}{2 x^3}+\frac{1.3}{2^2 x^5}-\frac{1.3.5}{2^3 x^7}+\cdots\right]$.



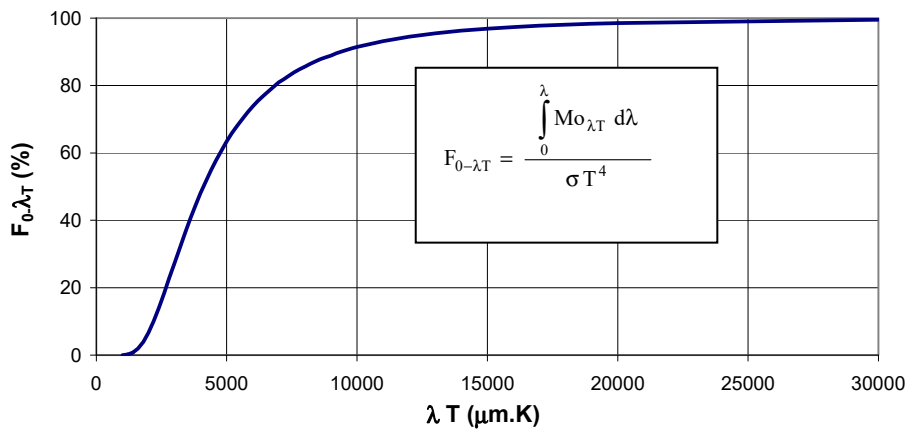
<i>x</i>	<i>erf</i> (<i>x</i>)	<i>erfc</i> (<i>x</i>)	<i>ierfc</i> (<i>x</i>)	<i>x</i>	<i>erf</i> (<i>x</i>)	<i>erfc</i> (<i>x</i>)	<i>ierfc</i> (<i>x</i>)
0	0.000000	1.000000	0.5641896	1.1	0.880205	0.11980	0.036465
0.05	0.056372	0.943628	0.5155995	1.2	0.910314	0.08969	0.026049
0.1	0.112463	0.887537	0.4698221	1.3	0.934008	0.06599	0.018314
0.15	0.167996	0.832004	0.4268365	1.4	0.952285	0.04772	0.012670
0.2	0.222703	0.777297	0.3866080	1.5	0.966105	0.03390	0.008623
0.25	0.276326	0.723674	0.3490886	1.6	0.976378	0.02362	0.005819
0.3	0.328627	0.671373	0.3142186	1.7	0.983790	0.01621	0.003799
0.35	0.379382	0.620618	0.2819256	1.8	0.989091	0.01091	0.002460
0.4	0.428392	0.571608	0.2521274	1.9	0.992790	0.00721	0.001563
0.45	0.475482	0.524518	0.2247329	2	0.995322	0.00468	0.000977
0.5	0.520500	0.479500	0.1996413	2.1	0.997021	0.00298	0.000602
0.55	0.563323	0.436677	0.1767460	2.2	0.998137	0.00186	0.000362
0.6	0.603856	0.396144	0.1559353	2.3	0.998857	0.00114	0.000216
0.65	0.642029	0.357971	0.1370922	2.4	0.999311	0.00069	0.000124
0.7	0.677801	0.322199	0.1200981	2.5	0.999593	0.00041	0.000072

0.75	0.711156	0.288844	0.1048325	2.6	0.999764	0.00024	0.000040
0.8	0.742101	0.257899	0.0911737	2.7	0.999866	0.00013	0.000023
0.85	0.770668	0.229332	0.0790027	2.8	0.999925	0.00008	0.000012
0.9	0.796908	0.203092	0.0682015	2.9	0.999959	0.00004	0.000007
0.95	0.820891	0.179109	0.0586561	3	0.999978	0.00002	0.000004
1	0.842701	0.157299	0.0502547				

A.7. Emissivity of some materials



A.8. Fraction $F_{0-\lambda T}$ of energy radiated by a black body between 0 and λ



$\begin{matrix} b \\ a \end{matrix}$	0	40	80	120	160
1,000	0.03	0.05	0.08	0.11	0.16
1,200	0.21	0.29	0.38	0.49	0.62
1,400	0.78	0.96	1.17	1.41	1.68
1,600	1.97	2.30	2.66	3.06	3.48
1,800	3.94	4.42	4.94	5.49	6.07
2,000	6.68	7.31	7.97	8.65	9.36
2,200	10.09	10.84	11.61	12.40	13.21
2,400	14.03	14.86	15.71	16.57	17.44
2,600	18.32	19.20	20.09	20.99	21.89
2,800	22.79	23.70	24.61	25.51	26.42
3,000	27.33	28.23	29.13	30.03	30.92
3,200	31.81	32.70	33.58	34.45	35.32

$\begin{matrix} b \\ a \end{matrix}$	0	40	80	120	160
7,800	84.80	84.97	85.14	85.30	85.47
8,000	85.63	85.78	85.94	86.10	86.25
8,200	86.40	86.55	86.69	86.83	86.98
8,400	87.12	87.25	87.39	87.52	87.66
8,600	87.80	87.92	88.04	88.17	88.29
8,800	88.41	88.53	88.65	88.77	88.88
9,000	88.89	89.11	89.22	89.33	89.44
9,200	89.55	89.65	89.76	89.86	89.96
9,400	90.06	90.16	90.26	90.35	90.45
9,600	90.54	90.63	90.72	90.81	90.90
9,800	90.99	91.08	91.16	91.25	91.33
10,000	91.42				

$\begin{smallmatrix} b \\ a \end{smallmatrix}$	0	40	80	120	160
3,400	36.18	37.03	37.88	38.71	39.54
3,600	40.36	41.18	41.98	42.78	43.56
3,800	44.34	45.11	45.87	46.62	47.36
4,000	48.09	48.81	49.53	50.23	50.92
4,200	51.60	52.28	52.94	53.60	54.25
4,400	54.88	55.51	56.13	56.74	57.34
4,600	57.93	58.51	59.09	59.65	60.21
4,800	60.66	61.30	61.83	62.35	62.87
5,000	63.38	63.88	64.37	64.85	65.33
5,200	65.80	66.26	66.72	67.16	67.60
5,400	68.04	68.46	68.88	69.30	69.70
5,600	70.11	70.50	70.89	71.27	71.65
5,800	72.02	72.38	72.74	73.09	73.44
6,000	73.78	74.12	74.45	74.78	75.10
6,200	75.41	75.72	76.03	76.33	76.63
6,400	76.92	77.21	77.49	77.77	78.05
6,600	78.32	78.59	78.85	79.11	79.36
6,800	79.61	79.86	80.10	80.34	80.58
7,000	80.90	81.04	81.26	81.47	81.70
7,200	81.92	82.13	82.34	82.55	82.75
7,400	82.95	83.15	83.34	83.53	83.72
7,600	83.91	84.09	84.27	84.45	84.62

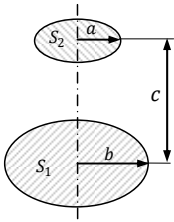
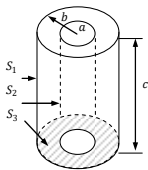
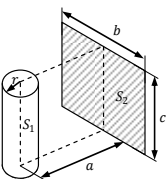
$\begin{smallmatrix} b \\ a \end{smallmatrix}$	0	40	80	120	160
$\begin{smallmatrix} b \\ a \end{smallmatrix}$	0	200	400	600	800
10,000	91.42	91.81	92.19	92.54	92.87
11,000	93.18	93.48	93.76	94.02	94.27
12,000	94.50	94.73	94.94	95.14	95.33
13,000	95.51	95.68	95.84	96.00	96.14
14,000	96.29	96.42	96.54	96.67	96.78
15,000	96.89	97.00	97.10	97.19	97.29
16,000	97.37	97.46	97.54	97.62	97.69
17,000	97.77	97.83	97.90	97.96	98.02
18,000	98.08	98.14	98.19	98.24	98.29
19,000	98.34	98.38	98.43	98.47	98.51
20,000	98.55	Use: $\lambda T = a + b$			
30,000	99.53				
40,000	99.78				
50,000	99.89	Example: $\lambda T = 2,720 \text{ }\mu\text{m K}$ Reads at $2,600 + 120$ hence: $F_{0-\lambda T} = 20.99\%$			
60,000	99.93				
70,000	99.96				
80,000	99.97				
90,000	99.98				
100,000	99.98				

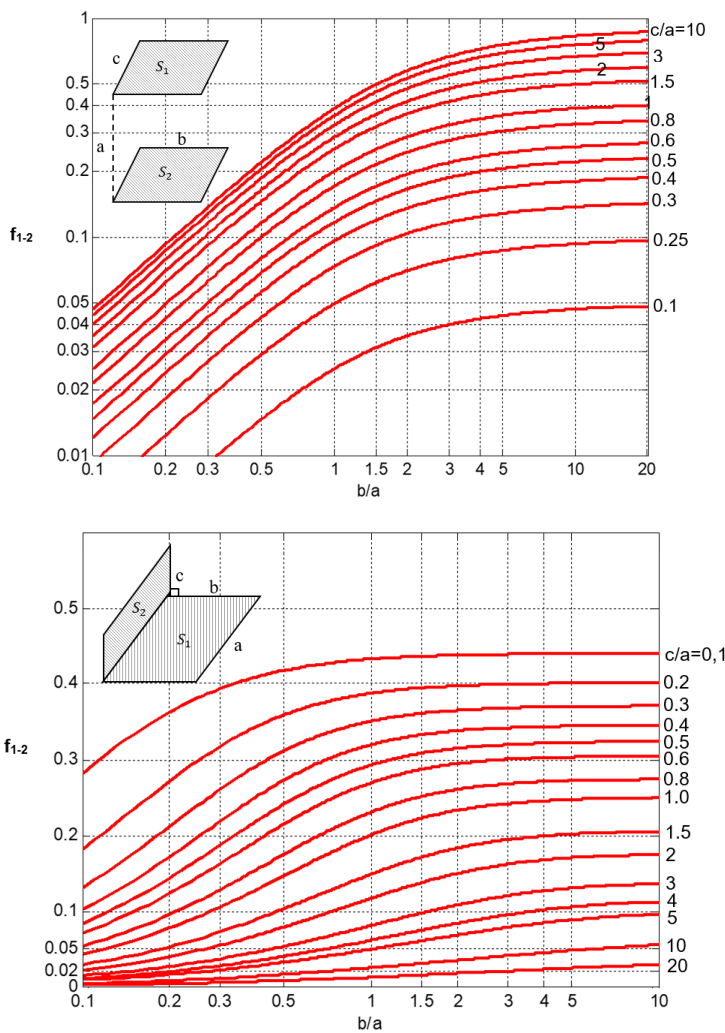
A.9. Radiation shape factors

Adapted from Siegel and Howell (1992)

Configuration	Diagram	Shape factor
Elementary surface parallel to a rectangular plane		$f_{1-2} = \frac{1}{2\pi} \left[\frac{B}{\sqrt{1+B^2}} \tan^{-1} \left(\frac{C}{\sqrt{1+B^2}} \right) + \frac{C}{\sqrt{1+C^2}} \tan^{-1} \left(\frac{B}{\sqrt{1+C^2}} \right) \right]$ $B = \frac{b}{a}; C = \frac{c}{a}$
Linear source parallel to a rectangular plane		$f_{1-2} = \frac{1}{\pi B} \left[\sqrt{1+B^2} \tan^{-1} \left(\frac{C}{\sqrt{1+B^2}} \right) - \tan^{-1}(C) + \frac{BC}{\sqrt{1+C^2}} \tan^{-1} \left(\frac{B}{\sqrt{1+C^2}} \right) \right]$ $B = \frac{b}{a}; C = \frac{c}{a}$
Linear source parallel to a rectangular plane, intersecting at an angle ϕ		$f_{1-2} = \frac{1}{\pi} \times \left\{ \begin{aligned} &\tan^{-1}(B) + \frac{\sin^2(\phi)}{2B} \ln \left[\frac{B^2 + X^2}{(1+B^2)X^2} \right] \\ &- \frac{\sin(2\phi)}{2B} \left\{ \frac{\pi}{2} - \phi + \tan^{-1} \left[\frac{C - \cos(\phi)}{\sin(\phi)} \right] \right\} \\ &+ \frac{Y}{B} \left[\tan^{-1} \left(\frac{C - \cos(\phi)}{\sin(\phi)} \right) + \tan^{-1} \left(\frac{\cos(\phi)}{Y} \right) \right] \cos(\phi) \\ &+ \frac{C \cos(\phi) - 1}{X} \tan^{-1} \left(\frac{B}{X} \right) \end{aligned} \right\}$ $B = \frac{b}{a}; C = \frac{c}{a}; X = \sqrt{C^2 - 2C \cos(\phi) + 1}; Y = \sqrt{B^2 + \sin^2(\phi)}$
Two rectangular parallel planes with the same area		$f_{1-2} = \frac{1}{\pi} \left[\frac{1}{BC} \ln \left(\frac{XY}{X+Y-1} \right) + \frac{2\sqrt{X}}{B} \tan^{-1} \left(\frac{C}{\sqrt{X}} \right) + \frac{2\sqrt{Y}}{C} \tan^{-1} \left(\frac{B}{\sqrt{Y}} \right) - \frac{2}{C} \tan^{-1}(B) - \frac{2}{B} \tan^{-1}(C) \right]$ $B = \frac{b}{a}; C = \frac{c}{a}; X = 1 + B^2; Y = 1 + C^2$
Two infinite parallel strips of different widths		$f_{1-2} = \frac{1}{2B} \left[\sqrt{(B+C)^2 + 4} - \sqrt{(B-C)^2 + 4} \right]$ $f_{2-1} = \frac{1}{2C} \left[\sqrt{(B+C)^2 + 4} - \sqrt{(B-C)^2 + 4} \right]$ $f_{1-2} = f_{2-1} = \frac{1}{b} \left[\sqrt{B^2 + 1} - 1 \right] \text{ si } b = c$ $B = \frac{b}{a}; C = \frac{c}{a}$

Two perpendicular rectangular planes having a common side		$f_{1-2} = \frac{1}{\pi B} \left[\frac{1}{4} \ln \left\{ \left[\frac{(1+B^2)(1+C^2)}{1+B^2+C^2} \right] \left[\frac{B^2(1+B^2+C^2)}{(1+B^2)(B^2+C^2)} \right]^{B^2} \right. \right. \\ \left. \left. \times \left[\frac{C^2(1+B^2+C^2)}{(1+C^2)(B^2+C^2)} \right]^{C^2} \right. \right. \\ \left. \left. + B \tan^{-1} \left(\frac{1}{B} \right) + C \tan^{-1} \left(\frac{1}{C} \right) \right. \right. \\ \left. \left. - \sqrt{B^2+C^2} \tan^{-1} \left(\frac{1}{\sqrt{B^2+C^2}} \right) \right] \right]$ $B = \frac{b}{a}; C = \frac{c}{a}; f_{1-2} = \frac{1}{2} \left[1 + \frac{c}{b} - \sqrt{1 + \left(\frac{c}{b} \right)^2} \right] \text{ si } a \rightarrow \infty$
Two identical planes having a common side		$f_{1-2} = f_{2-1} = 1 - \sin \left(\frac{\theta}{2} \right)$
Two perpendicular rectangles		$f_{1-6} = \frac{1}{2A_1} \left\{ (A_1 + A_2 + A_3 + A_4) f_{1234-56} - A_6 f_{6-24} - A_5 f_{5-13} \right. \\ \left. - (A_3 + A_4) f_{34-56} - A_6 f_{6-4} - A_5 f_{5-3} \right\}$
Two parallel rectangles		$f_{1-7} = \frac{1}{4A_1} \left(\begin{aligned} &A_{1234} f_{1234-5678} + A_1 f_{1-5} + A_2 f_{2-6} \\ &+ A_3 f_{3-7} + A_4 f_{4-8} - A_{12} f_{12-56} \\ &- A_{14} f_{14-58} - A_{34} f_{34-78} - A_{23} f_{23-67} \end{aligned} \right)$
Elementary surface perpendicular to a surface		$f_{1-2} = \frac{1}{2\pi} \left[\tan^{-1} \left(\frac{1}{X} \right) - \frac{1}{\sqrt{1-\frac{Y}{X}}} \tan^{-1} \left(\frac{1}{\sqrt{X^2+Y^2}} \right) \right]$ $X = \frac{c}{a}; Y = \frac{a}{b}$
Two infinite cylinders with parallel axes		$f_{1-2} = \frac{2}{\pi} \left[\sqrt{X^2-1} - X + \frac{\pi}{2} - \cos^{-1} \left(\frac{1}{X} \right) \right]$ $X = 1 + \frac{a}{b}$

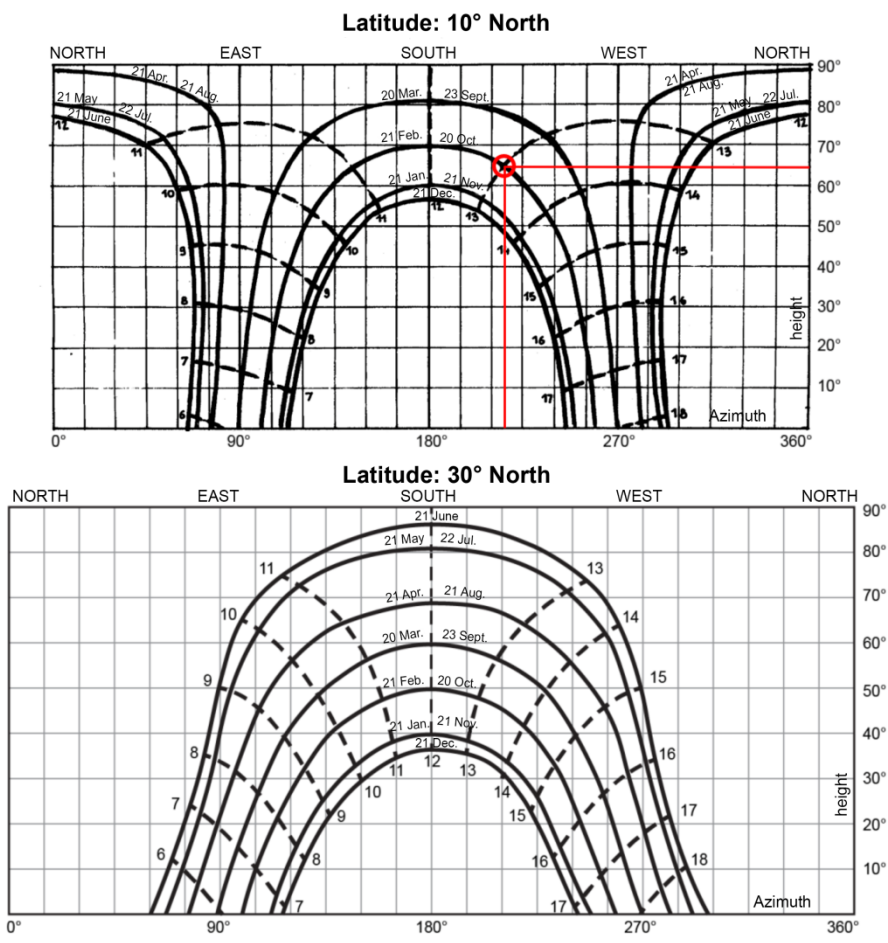
<p>Two parallel disks</p>		$f_{1-2} = \frac{1}{2} \left[Z - \sqrt{Z^2 - 4X^2Y^2} \right]$ $X = \frac{a}{c}; Y = \frac{c}{b}; Z = 1 + (1 + X^2)Y^2$
<p>Two finite coaxial cylinders</p>		$f_{1-2} = \frac{1}{X} - \frac{1}{\pi X} \left\{ \cos^{-1} \left(\frac{B}{A} \right) - \frac{1}{2Y} \left[\sqrt{(A+2)^2 - 4X^2} \cos^{-1} \left(\frac{B}{XA} \right) + B \sin^{-1} \left(\frac{1}{X} \right) - \frac{\pi A}{2} \right] \right\}$ $f_{1-1} = 1 - \frac{1}{X} + \frac{2}{\pi X} \tan^{-1} \left(\frac{2\sqrt{X^2 - 1}}{Y} \right) - \frac{Y}{2\pi X} \left\{ \frac{\sqrt{4X^2 + Y^2}}{Y} \sin^{-1} \left[\frac{4(X^2 - 1) + \frac{Y^2}{X^2}(X^2 - 2)}{Y^2 + 4(X^2 - 1)} \right] - \sin^{-1} \left(\frac{X^2 - 2}{X^2} \right) + \frac{\pi}{2} \left(\frac{\sqrt{4X^2 + Y^2}}{Y} - 1 \right) \right\}$ $f_{1-3} = \frac{1}{2} (1 - f_{1-1} - f_{1-2})$ $X = \frac{b}{a}; Y = \frac{c}{a}; A = X^2 + Y^2 - 1; B = Y^2 - X^2 + 1$
<p>A plane rectangle and a cylinder with axis located in the middle plane rectangle</p>		$f_{1-2} = \frac{2}{Y} \int_0^{Y/2} \left\{ \frac{X}{X^2 + \beta^2} - \frac{X}{\pi(X^2 + \beta^2)} \left[\cos^{-1} \left(\frac{W}{V} \right) - \frac{1}{2Z} \sqrt{V^2 + 4Z} \right] \times \cos^{-1} \left(\frac{W}{V\sqrt{X^2 + \beta^2}} \right) + W \sin^{-1} \left(\frac{1}{\sqrt{X^2 + \beta^2}} \right) - \frac{\pi V}{2} \right\} d\beta$ $X = \frac{a}{r}; Y = \frac{b}{r}; Z = \frac{c}{r};$ $V = X^2 + Z^2 + \beta^2 - 1; W = Z^2 - X^2 - \beta^2 + 1$



A.10. Cylindrical solar diagram

The diagram enables the calculation of the azimuth a and the height h of the Sun according to the latitude L .

Example: on October 20 at 1 p.m. in a place of latitude 10°N , the azimuth is $a = 217^\circ$ and the height of the Sun is $h = 65^\circ$.



A.11. Albedo values

Surface	Albedo	Surface (various materials)	Albedo
Earth (planet)	0.20–0.60	Polished silver	0.94
Ground		Oxidized silver	0.50
Cover of fresh snow	0.80–0.90	Polished aluminum	0.97
Aged, packed snow cover	0.50–0.70	Oxidized aluminum	0.85
Bare cultivated land	0.08–0.25	Concrete	0.50
Meadow and green grass	0.12–0.25	Carbon	0.15

Surface	Albedo	Surface (various materials)	Albedo
Sandy soil	0.15–0.25	Gravels	0.25
Light sand, dry or wet	0.25–0.45	Asphalt	0.18
Forests of deciduous trees in summer	0.10–0.20	White lime	0.75
Evergreen forests in summer	0.05–0.15	Papier blanc	0.85
Forest and snow	0.25–0.50	White paints	0.90
Grass and dry vegetation	0.28–0.33	Black matt paints	0.07
Bodies of water (seas, lakes)		Window glass	0.10
Perfectly calm water, $h > 30^\circ$	0.06–0.02	Dry white plaster	0.90
Perfectly calm water, $h < 10^\circ$	0.35–0.60	Asbestos cement	0.20
Seas and oceans, $h > 30^\circ$	0.02–0.05	Clouds	
Seas and oceans, $h < 10^\circ$	0.02–0.20	Stratiforms	0.40–0.75
Vast icy surfaces	0.25–0.40	Cumuliforms	0.60–0.85

A.12. Integral exponential functions

The integral exponential function of order n , with a positive argument x , is defined by:

$$E_n(x) = \int_0^1 \mu^{n-2} e^{-\frac{x}{\mu}} d\mu \tag{a}$$

All the following properties are only valid for n integer.

– For $x = 0$, equation (a) becomes:

$$E_n(0) = \int_0^1 \mu^{n-2} d\mu$$

thus:

$$E_n(0) \rightarrow \infty \tag{b}$$

for $n = 1$, and:

$$E_n(0) = \frac{1}{n-1} \text{ for } n \geq 2 \tag{c}$$

– By differentiating relation (a), we obtain:

$$\frac{dE_n(x)}{dx} = -\frac{1}{x} e^{-x} \tag{d}$$

for $n = 1$, and:

$$\frac{dE_n(x)}{dx} = -E_{n-1}(x) \quad (e)$$

For $n \geq 2$.

From where:

$$\int E_n(x) dx = -E_{n+1}(x) \quad (f)$$

– An integration by parts leads to the recurrence:

$$n E_{n+1}(x) = e^{-x} - x E_n(x) \quad (g)$$

– We frequently encounter the integral:

$$\int_0^x x^m E_n(x) dx \quad (h)$$

Integrating by parts and using relations (d) and (e), this integral can be written as:

$$\begin{aligned} \int_0^x x^m E_n(x) dx = & \frac{x^{m+1}}{m+1} E_n(x) + \frac{x^{m+2}}{(m+1)(m+2)} E_{n-1}(x) + \dots + \frac{x^{m+n}}{(m+1)(m+2)\dots(m+n)} E_1(x) + \\ & \frac{1}{(m+1)(m+2)\dots(m+n)} \int_0^1 x^{m+n-1} e^{-x} dx \end{aligned} \quad (i)$$

– According to the recurrence relation (f), $E_1(x)$ can be put in the form:

$$E_1(x) = \int_1^\infty e^{-xt} \frac{dt}{t} = \int_x^\infty e^{-t} \frac{dt}{t} \quad (j)$$

– For large values of x , the expansion to infinity of $E_n(x)$ is:

$$E_n(x) = \frac{e^{-x}}{x} \left(1 - \frac{n}{x} + \frac{n(n+1)}{x^2} - \frac{n(n+1)(n+2)}{x^3} + \dots \right) \quad (k)$$

and therefore: $E_n(x) = \frac{e^{-x}}{x}$ when $x \rightarrow \infty$.

– When $x \rightarrow 0$, $E_1(x)$ presents a logarithmic singularity point and can be developed in series, i.e.:

$$E_1(x) = -\gamma - \log(x) + \sum_{n=1}^{\infty} (-1)^{n+1} \frac{x^n}{n!n} \quad (l)$$

where $\gamma = 0.5772156$ is Euler's constant.

Approximation of integral exponential functions:

We seek to approach the integral exponentials by classical exponentials, in particular:

$$E_2(x) \approx a \exp(-bx)$$

$$E_3(x) \approx c \exp(-dx)$$

There are several methods to determine the constants a , b , c and d ; the most used is that of Lick:

– we keep the derivation property of the exponential integrals:
 $\frac{d}{dx} E_3(ax) \approx -a E_2(ax)$, which imposes $E_3(x) \approx \frac{a}{b} \exp(-bx)$;

– we impose the moments of order 0 and order 1 of the function E : $a = \frac{3}{4}$ and $b = \frac{1}{2}$.

From where:

$$E_2(x) \approx \frac{3}{4} \exp\left(-\frac{1}{2}x\right)$$

$$E_3(x) \approx \frac{1}{2} \exp\left(-\frac{3}{2}x\right)$$

A.13. Fredholm singular integral equation

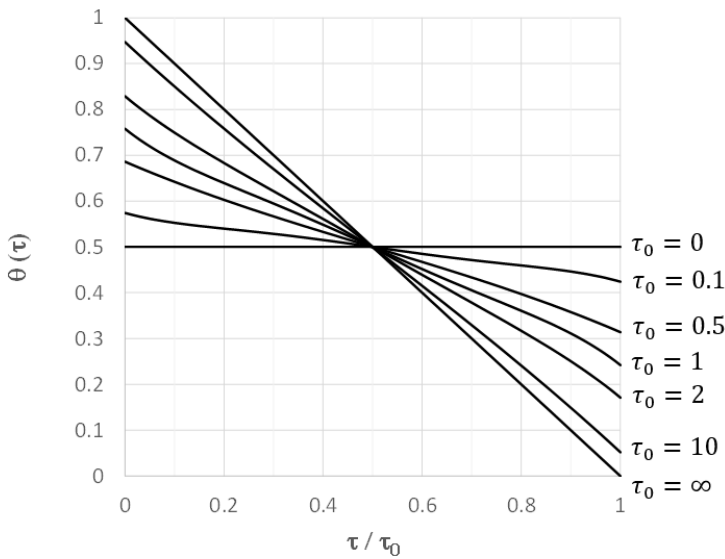
The reduced temperature is given by the equation:

$$\theta(\tau) = \frac{1}{2} \left[E_2(\tau) + \int_0^{\tau_0} \theta(\tau') E_1(|\tau - \tau'|) d\tau' \right]$$

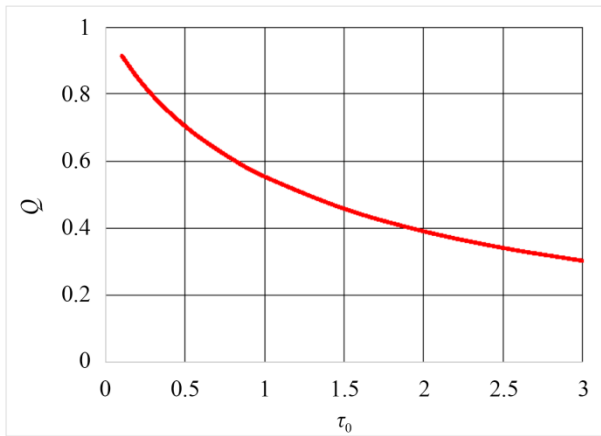
which is the singular Fredholm integral equation whose numerically calculated values for different values of τ are given by the following graph.

The reduced radiation flux is expressed by:

$$Q = 1 - 2 \int_0^{\tau_0} \theta(\tau') E_2(\tau') d\tau'$$

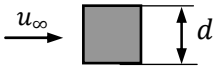
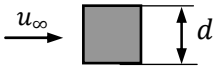
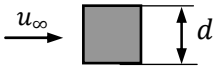


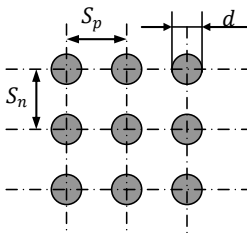
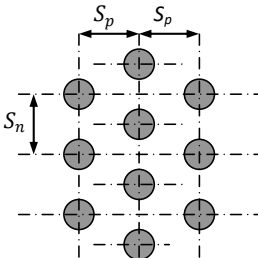
τ_0	Q
0.1	0.9157
0.2	0.8491
0.3	0.7934
0.4	0.7458
0.5	0.7040
0.6	0.6672
0.8	0.6045
1.0	0.5532
1.5	0.4572
2.0	0.3900
2.5	0.3401
3.0	0.3016



A.14. Correlations for heat transfer coefficients in forced convection

The characteristics of the fluid calculated at $T_f = \frac{T_p + T_\infty}{2}$.

Geometry	Correlation																		
Flow on a plane	$Nu(x)$: Nu at the distance x from the edge of the plane \overline{Nu}_L : average Nu over the length L of the plane <i>Turbulent flow</i> : ($Re > 5 \cdot 10^5$ and $Pr > 0.5$) $Nu(x) = 0.0288 Re(x)^{0.8} Pr^{1/3}$ $\overline{Nu}_L = 0.035 Re_L^{0.8} Pr^{1/3}$ <i>Laminar flow</i> : ($Re < 5 \cdot 10^5$ and $10 > Pr > 0.5$) $Nu(x) = 0.324 Re(x)^{0.5} Pr^{1/3}$ $\overline{Nu}_L = 0.628 Re_L^{0.5} Pr^{1/3}$																		
Flow in a tube	<i>Turbulent flow</i> : ($Re > 5,000$ and $100 > Pr > 0.6$) $Nu = 0.023 Re^{0.8} Pr^n$ $n = 0.3$ if $T_{fluid} > T_{wall}$ $n = 0.4$ if $T_{fluid} < T_{wall}$ Re calculated for $D_h = \frac{4S}{P}$, where S is the fluid passage section and P is the fluid/wall contact perimeter <i>Laminar flow</i> : $Nu = 1.86(RePr)^{1/3} \left(\frac{D}{L}\right)^{1/3} \left(\frac{\mu}{\mu_p}\right)^{0.14}$ Valid for $Pr \frac{D}{L} > 10$, μ_p calculated at T_p																		
Flow perpendicular to a circular cylinder (Jakob 1949)	$Nu = C Re^n Pr^{1/3}$, velocity u_∞ calculated upstream of the tube <table><tr><th>Re</th><th>C</th><th>n</th></tr><tr><td>0.4–4</td><td>0.989</td><td>0.330</td></tr><tr><td>4–40</td><td>0.911</td><td>0.385</td></tr><tr><td>40–4,000</td><td>0.683</td><td>0.466</td></tr><tr><td>4,000–40,000</td><td>0.193</td><td>0.618</td></tr><tr><td>40,000–250,000</td><td>0.0266</td><td>0.805</td></tr></table>	Re	C	n	0.4–4	0.989	0.330	4–40	0.911	0.385	40–4,000	0.683	0.466	4,000–40,000	0.193	0.618	40,000–250,000	0.0266	0.805
Re	C	n																	
0.4–4	0.989	0.330																	
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40–4,000	0.683	0.466																	
4,000–40,000	0.193	0.618																	
40,000–250,000	0.0266	0.805																	
Flow perpendicular to a non-circular cylinder (Jakob 1949)	<table><tr><th>Geometry</th><th>Re</th><th>C</th><th>n</th></tr><tr><td rowspan="2"></td><td>$5 \cdot 10^3$–10^5</td><td>0.102</td><td>0.675</td></tr><tr><td>$4 \cdot 10^3$–$1.5 \cdot 10^4$</td><td>0.228</td><td>0.731</td></tr></table>	Geometry	Re	C	n		$5 \cdot 10^3$ – 10^5	0.102	0.675	$4 \cdot 10^3$ – $1.5 \cdot 10^4$	0.228	0.731							
Geometry	Re	C	n																
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	$4 \cdot 10^3$ – $1.5 \cdot 10^4$	0.228	0.731																

Geometry	Correlation																																																																																																																																																																
Flow perpendicular to a bundle of 10 tubes (Grimson 1937)	<table><tr><td></td><td colspan="8">$\frac{S_n}{d}$</td></tr><tr><td rowspan="2">$\frac{S_p}{d}$</td><td colspan="2">1.25</td><td colspan="2">1.5</td><td colspan="2">2.0</td><td colspan="2">3.0</td></tr><tr><td>C</td><td>n</td><td>C</td><td>n</td><td>C</td><td>n</td><td>C</td><td>n</td></tr><tr><td colspan="9">In-line arrangement</td></tr><tr><td>1.25</td><td>0.386</td><td>0.592</td><td>0.305</td><td>0.608</td><td>0.111</td><td>0.704</td><td>0.070</td><td>0.752</td></tr><tr><td>1.5</td><td>0.407</td><td>0.586</td><td>0.278</td><td>0.620</td><td>0.112</td><td>0.702</td><td>0.075</td><td>0.744</td></tr><tr><td>2.0</td><td>0.464</td><td>0.570</td><td>0.332</td><td>0.602</td><td>0.254</td><td>0.632</td><td>0.220</td><td>0.648</td></tr><tr><td>3.0</td><td>0.322</td><td>0.601</td><td>0.396</td><td>0.584</td><td>0.415</td><td>0.581</td><td>0.317</td><td>0.608</td></tr><tr><td colspan="9">Staggered arrangement</td></tr><tr><td>0.16</td><td>-</td><td>-</td><td>-</td><td>-</td><td>-</td><td>-</td><td>0.236</td><td>0.636</td></tr><tr><td>0.9</td><td>-</td><td>-</td><td>-</td><td>-</td><td>0.495</td><td>0.571</td><td>0.445</td><td>0.581</td></tr><tr><td>1.0</td><td>-</td><td>-</td><td>0.552</td><td>0.558</td><td>-</td><td>-</td><td>-</td><td>-</td></tr><tr><td>1.125</td><td>-</td><td>-</td><td>-</td><td>-</td><td>0.531</td><td>0.565</td><td>0.575</td><td>0.560</td></tr><tr><td>1.25</td><td>0.575</td><td>0.556</td><td>0.561</td><td>0.554</td><td>0.576</td><td>0.556</td><td>0.579</td><td>0.562</td></tr><tr><td>1.5</td><td>0.501</td><td>0.568</td><td>0.511</td><td>0.562</td><td>0.502</td><td>0.568</td><td>0.542</td><td>0.568</td></tr><tr><td>2.0</td><td>0.448</td><td>0.572</td><td>0.462</td><td>0.568</td><td>0.535</td><td>0.556</td><td>0.498</td><td>0.570</td></tr><tr><td>3.0</td><td>0.344</td><td>0.592</td><td>0.395</td><td>0.580</td><td>0.488</td><td>0.562</td><td>0.467</td><td>0.574</td></tr></table>										$\frac{S_n}{d}$								$\frac{S_p}{d}$	1.25		1.5		2.0		3.0		C	n	C	n	C	n	C	n	In-line arrangement									1.25	0.386	0.592	0.305	0.608	0.111	0.704	0.070	0.752	1.5	0.407	0.586	0.278	0.620	0.112	0.702	0.075	0.744	2.0	0.464	0.570	0.332	0.602	0.254	0.632	0.220	0.648	3.0	0.322	0.601	0.396	0.584	0.415	0.581	0.317	0.608	Staggered arrangement									0.16	-	-	-	-	-	-	0.236	0.636	0.9	-	-	-	-	0.495	0.571	0.445	0.581	1.0	-	-	0.552	0.558	-	-	-	-	1.125	-	-	-	-	0.531	0.565	0.575	0.560	1.25	0.575	0.556	0.561	0.554	0.576	0.556	0.579	0.562	1.5	0.501	0.568	0.511	0.562	0.502	0.568	0.542	0.568	2.0	0.448	0.572	0.462	0.568	0.535	0.556	0.498	0.570	3.0	0.344	0.592	0.395	0.580	0.488	0.562	0.467	0.574
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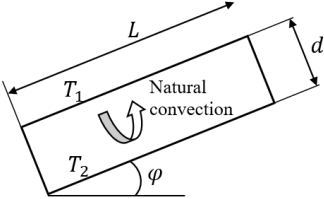
Geometry	Correlation										
Flow perpendicular to a bundle of n rows of tubes ($n \leq 10$) (Grimson 1937)	$N = \frac{h_n}{h_{10}}$										
	Number of rows n	1	2	3	4	5	6	7	8	9	10
	N in-line	0.64	0.80	0.87	0.90	0.92	0.94	0.96	0.98	0.99	1.0
	N staggered	0.68	0.75	0.83	0.89	0.92	0.95	0.97	0.98	0.99	1.0

A.15. Correlations for heat transfer coefficients in natural convection

According to Holman (1990). $Ra = GrPr = \frac{c\beta g\Delta T\rho^2 d^3}{\lambda\mu}$

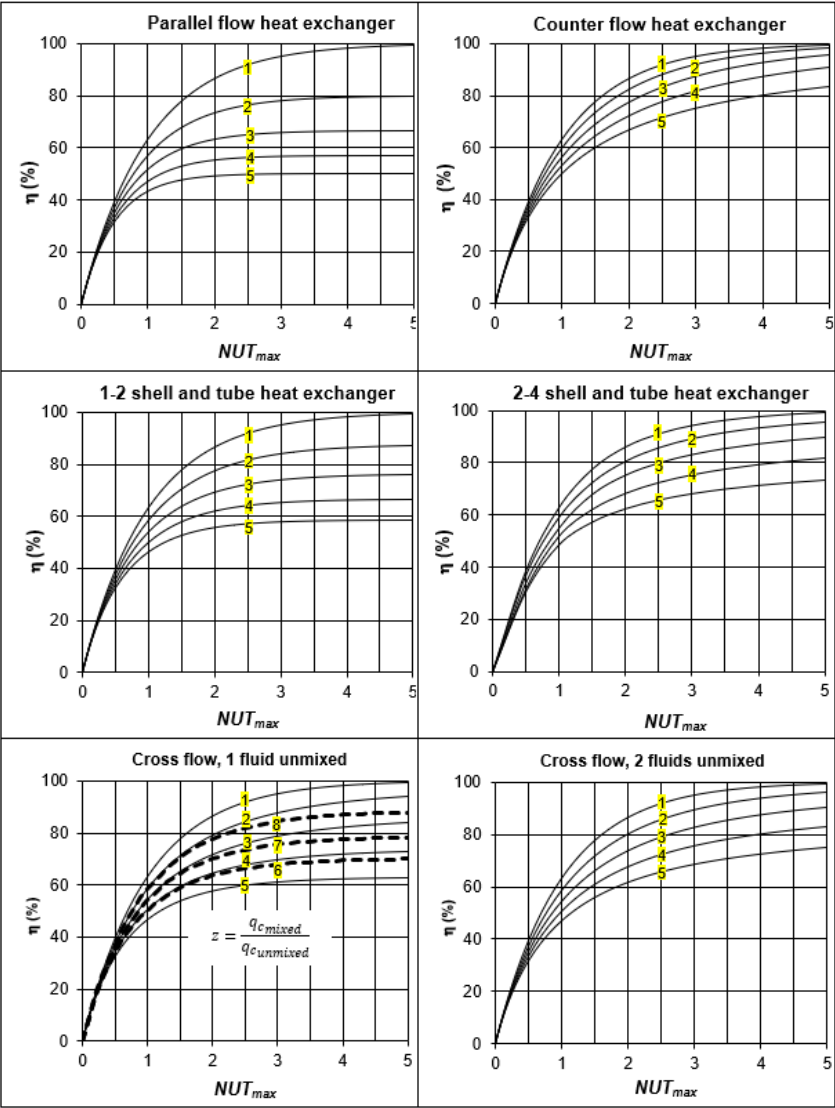
Correlations valid for all fluids: $Nu = C(GrPr)^m$			
Geometry	$GrPr$	C	m
Vertical plates and cylinders	$10^4\text{--}10^9$	0.59	1/4
	$10^9\text{--}10^{13}$	0.021	2/5
Horizontal cylinders	$10^{-10}\text{--}10^{-2}$	0.675	0.058
	$10^{-2}\text{--}10^2$	1.02	0.148
	$10^2\text{--}10^4$	0.850	0.188
	$10^4\text{--}10^7$	0.480	0.25
	$10^7\text{--}10^{12}$	0.125	0.33
Upper face of a hot plate or lower face of a cold plate	$2\times10^4\text{--}8\times10^6$	0.54	0.25
	$8\times10^6\text{--}10^{11}$	0.15	0.33
Lower face of a hot plate or upper side of a cold plate	$10^5\text{--}10^{11}$	0.27	0.25
Simplified relations for air at atmospheric pressure and at $T \approx 20^\circ\text{C}$			
Geometry	Laminar $10^4 < GrPr < 10^9$	Turbulent $GrPr > 10^9$	
Vertical plate or cylinder	$h = 1.54 \left(\frac{\Delta T}{L}\right)^{1/4}$	$h = 1.22(\Delta T)^{1/3}$	
Horizontal cylinder	$h = 1.26 \left(\frac{\Delta T}{D}\right)^{1/4}$	$h = 1.52(\Delta T)^{1/3}$	
Upper face of a hot horizontal plate or lower face of a cold plate	$h = 1.41 \left(\frac{\Delta T}{L}\right)^{1/4}$	$h = 1.83(\Delta T)^{1/3}$	

Lower face of a hot plate or upper face of a cold plate	$h = 0.71 \left(\frac{\Delta T}{L} \right)^{1/4}$	$h = 0.71 \left(\frac{\Delta T}{L} \right)^{1/4}$
---	--	--

Enclosed rectangular cell	
	<p>Correlation of Hollands et al. (1976)</p> $Nu = 1 + 1.44 \left[1 - \frac{1,708}{Ra_d \cos(\varphi)} \right]^* \left\{ 1 - \frac{1,708 [\sin(1.8\varphi)^{1.6}]}{Ra_d \cos(\varphi)} \right\} + \left\{ \left[\frac{Ra_d \cos(\varphi)}{5,830} \right]^{1/3} - 1 \right\}^*$ <p>If $0 < \varphi < \tan^{-1}(4,800 Pr)$, $\frac{L}{d} > 12$</p> <p>The quantities * are taken equal to 0 if the result of their calculation leads to a negative number.</p> <p>$0 < \varphi < 90^\circ$ if the hot plate is down.</p>
	<p>Correlation of El Sherbiny et al. (1982):</p> <p>Valid for $\frac{L}{d} < 100$ and $Ra_d < 10^6$</p> $Nu = \max[Nu_1, Nu_2, Nu_3]$ <p>with:</p> $Nu_1 = 0.0605 Ra_d^{0.33}$ $Nu_2 = \left\{ 1 + \left[\frac{0.104 Ra_d^{0.293}}{1 + \left(\frac{5310}{Ra_d} \right)^{1.36}} \right]^3 \right\}^{\frac{1}{3}}$ $Nu_3 = 0.242 \left(\frac{Ra_d d}{L} \right)^{0.272}$

A.16. NUT charts = f(η) for heat exchangers

$z = \frac{q_{cmin}}{q_{cmax}}$	0	0.25	0.5	0.75	1	1.33	2	4
Point	1	2	3	4	5	6	7	8



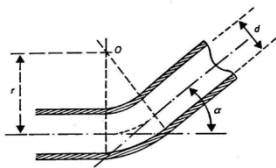
A.17. Calculation formulas for singular pressure drops

A.17.1. Pressure drops by change of direction

$$\Delta P = R \frac{\rho u^2}{2}$$

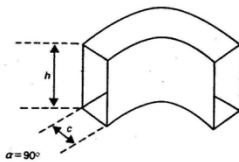
with:

- ρ , fluid density;
- u , fluid velocity;
- R , coefficient given in the tables below.
- Circular pipes:



α $\frac{r}{d}$	10°	20°	45°	60°	90°	120°
0.5	0.18	0.33	0.59	0.70	0.86	0.97
0.6	0.13	0.26	0.48	0.55	0.68	0.72
0.8	0.10	0.19	0.33	0.39	0.48	0.52
1	0.07	0.15	0.27	0.32	0.38	0.43
2	0.04	0.09	0.17	0.19	0.23	0.26
5	0.03	0.05	0.12	0.13	0.14	0.16
10	0.03	0.05	0.09	0.10	0.12	0.14

- Rectangular pipes:



r/d h/c	0.5	0.6	0.7	0.8	1.0	1.5
0.5	1.3	0.8	0.55	0.41	0.3	0.2
1	1	0.65	0.44	0.35	0.25	0.16
2	0.8	0.5	0.35	0.28	0.2	0.13

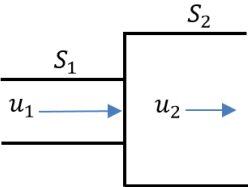
Multiplier coefficient k to be applied to R for $\alpha \neq 90^\circ$

α	15°	30°	45°	60°	90°	135°	180°
k	0.31	0.53	0.69	0.81	1.00	1.21	1.34

A.17.2. Pressure drops by sudden change of cross-section

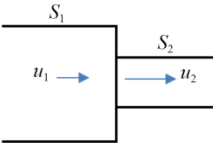
- Abrupt enlargement:

$$\Delta P = \rho \frac{(u_1 - u_2)^2}{2} = \rho \left(1 - \frac{S_1}{S_2}\right) \frac{u_1^2}{2}$$



– Abrupt narrowing:

$$\Delta P = R \frac{\rho u_1^2}{2}$$



S_1/S_2	0.01	0.1	0.2	0.4	0.5	0.6	0.8	1
R	1.5	1.45	1.35	1.2	1.1	0.9	0.5	0