

# Water and Carbon Dioxide Co-Electrolysis in a Solid Oxide Electrolyzer Cell

In this tutorial, a solid oxide electrolyzer cell model for co-electrolysis of H<sub>2</sub>O and CO<sub>2</sub> is presented. The model includes the full coupling between the mass balances and gas flow in the H<sub>2</sub> and O<sub>2</sub> gas diffusion electrodes, the momentum balances in the H<sub>2</sub> and O<sub>2</sub> gasflow channels, the energy balance across the cell, the balance of the ionic current carried by the oxide ion, and an electronic-current balance. A reversible water-gas shift reaction is included in the H<sub>2</sub> gas-diffusion electrode and the H<sub>2</sub> gas-flow channel.

The model computes the spatial distributions of the various species across the gas-diffusion electrodes and gas-flow channels. The spatial distribution of the total current density along the electrode length is also evaluated using a general projection operator.

# Model Definition

On the anode, oxygen ions are oxidized to form oxygen gas,

$$2O^{2-} \leftrightarrow O_2(g) + 4e^{-} \tag{1}$$

whereas on the cathode, water vapor is reduced to form hydrogen gas and oxygen ions:

$$H_2O(g) + 2e^- \leftrightarrow H_2(g) + O^{2-}$$
 (2)

A CO<sub>2</sub> electrolysis reaction also occurs on the cathode, where CO<sub>2</sub> gas is reduced to form CO gas and oxygen ions:

$$CO_2(g) + 2e^- \leftrightarrow CO(g) + O^{2-}$$
 (3)

Figure 1 shows the model geometry. Seven computational domains are used in the model: the two interconnects,  $H_2$  and  $O_2$  gas-flow channels,  $H_2$  and  $O_2$  gas-diffusion electrodes, and the membrane.

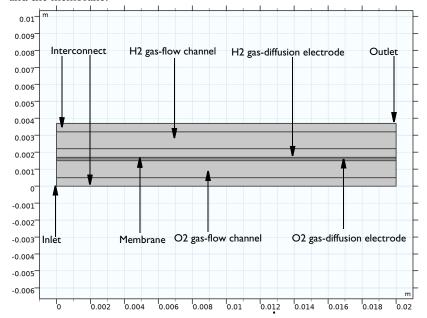


Figure 1: Model geometry. From top: Interconnect,  $H_2$  gas channel,  $H_2$  gas-diffusion electrode, solid oxide electrolyte layer,  $O_2$  gas-diffusion electrode,  $O_2$  gas-flow channel, and interconnect. The inlet and outlet positions are indicated in the figure.

The gas mixture at the cathode consists of  $H_2$ ,  $H_2O$ ,  $CO_2$ , and CO, whereas that at the anode consists of  $O_2$  and  $N_2$ . The composition of the gas mixture will change as a result of the electrochemical reactions and the water–gas shift reaction. The mass transport of the gaseous species is modeled in the gas-flow channels and the gas-diffusion electrodes coupled to the resulting (laminar) flow of the gas mixture.

The current distribution is defined assuming a temperature-dependent electrolyte conductivity of the solid electrolyte. The Water Electrolyzer interface is used to define the electrode reactions and the electrolyte charge transport in the porous gas-diffusion electrodes and the electrolyte layer, as well as the mass transport of the gas mixture. The momentum flow is defined using Darcy's Law in the gas-flow channels and the gas-diffusion electrodes.

On the cathode side, the electrode kinetics depends on the local concentrations of  $H_2O$  and  $H_2$  for the  $H_2O$  electrolysis reaction and on the local concentrations of  $CO_2$  and CO

for the  $CO_2$  electrolysis reaction according to the law of mass action (and the Nernst equation). On the anode side, the electrode kinetics depends on the local concentrations of  $O_2$  for the  $O_2$  evolution reaction according to the law of mass action (and the Nernst equation).

The properties of the gas mixtures at both anode and cathode, as well as the equilibrium potentials of the electrode reactions are automatically defined by the default built-in options of the Water Electrolyzer interface.

## Results and Discussion

Figure 2 shows the  $H_2$  concentration distribution in the  $H_2$  gas-flow channel and the  $H_2$  gas-diffusion electrode for an applied potential of 1.5 V. The  $H_2$  concentration is found to increase along the electrode length due to the  $H_2O$  electrolysis reaction occurring at the  $H_2$  gas diffusion electrode.

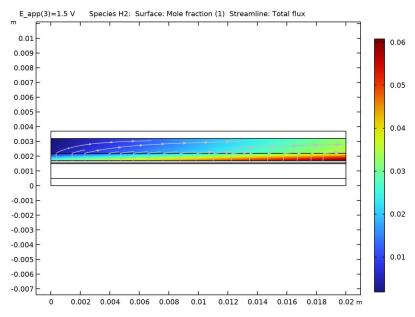


Figure 2:  $H_2$  concentration distribution in the  $H_2$  gas-flow channel and  $H_2$  gas-diffusion electrode for an applied potential of 1.5 V.

Figure 3 shows the CO concentration distribution in the  $H_2$  gas-flow channel and  $H_2$  gas diffusion electrode for applied potential of 1.5 V. CO concentration is found to increase along the electrode length due to the  $CO_2$  electrolysis reaction occurring at the  $H_2$  gas-

diffusion electrode. The difference in the CO concentration between the H2 gas-diffusion electrode and the H<sub>2</sub> gas-flow channel is considerably higher for CO in the downstream when compared to H<sub>2</sub>. This can be attributed to slower diffusion of CO than H<sub>2</sub>.

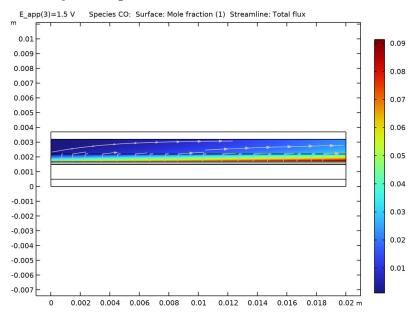


Figure 3: CO concentration distribution in the  $H_2$  gas-flow channel and the  $H_2$  gas-diffusion electrode for an applied potential of 1.5 V.

Figure 4 shows the change in temperature across a solid oxide electrolyzer cell for an applied potential of 1.5 V. Although both the H<sub>2</sub>O and CO<sub>2</sub> electrolysis reactions are endothermic, the cell temperature is increased by about 25 K from the inlet to the outlet for an applied potential of 1.5 V. As this applied potential is higher than the cell thermoneutral potential, the heat generated from overpotential losses is more than the heat required for electrolysis reactions.

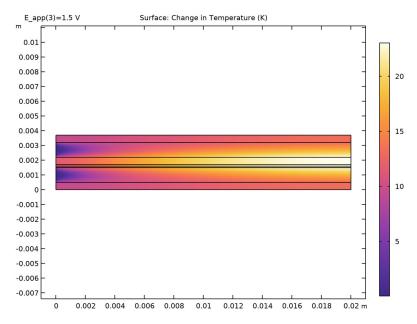


Figure 4: Change in temperature across a solid oxide electrolyzer cell for an applied potential of 1.5 V.

Figure 5 shows the distribution of the water-gas shift reaction rate in the H<sub>2</sub> gas-flow channel and the H<sub>2</sub> gas-diffusion electrode for an applied potential of 1.5 V. The watergas shift reaction rate is found to be higher closer to the H2 gas-diffusion electrodemembrane interface for an applied potential of 1.5 V, which is attributed to the high CO concentration in the region.

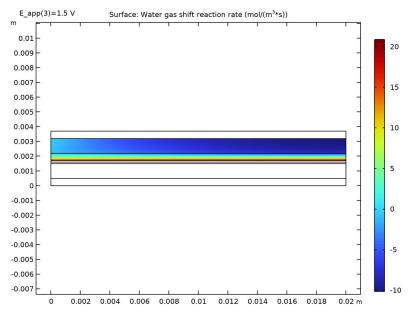


Figure 5: Water–gas shift reaction rate in the  $H_2$  gas-flow channel and the  $H_2$  gas-diffusion electrode for an applied potential of 1.5 V.

Finally, Figure 6 shows that the total cathodic (negative) current density, which is integrated along the y direction for each grid point along the x direction using a general projection operator, decreases for H2O electrolysis and increases for CO2 electrolysis along the electrode length.

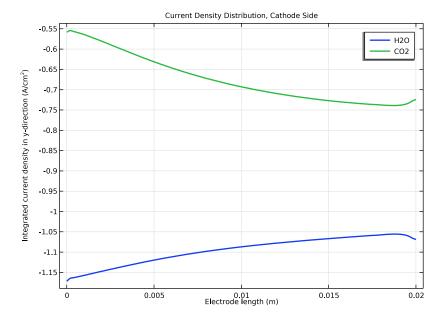


Figure 6: The total cathodic current density for  $H_2O$  and  $CO_2$  electrolysis along the electrode length for an applied potential of 1.5 V.

**Application Library path:** Fuel\_Cell\_and\_Electrolyzer\_Module/Electrolyzers/soec\_co2

# Modeling Instructions

From the File menu, choose New.

#### NEW

In the New window, click Model Wizard.

## MODEL WIZARD

- I In the Model Wizard window, click **Q** 2D.
- 2 In the Select Physics tree, select Electrochemistry>Water Electrolyzers>Solid Oxide (we).
- 3 Click Add.

- 4 In the Select Physics tree, select Heat Transfer Heat Transfer in Solids and Fluids (ht).
- 5 Click Add.
- 6 Click Study.
- 7 In the Select Study tree, select Preset Studies for Selected Physics Interfaces> Water Electrolyzer>Stationary with Initialization.
- 8 Click M Done.

#### **GLOBAL DEFINITIONS**

#### Parameters 1

First load the model parameters.

- I In the Model Builder window, under Global Definitions click Parameters I.
- 2 In the Settings window for Parameters, locate the Parameters section.
- 3 Click Load from File.
- **4** Browse to the model's Application Libraries folder and double-click the file soec co2 parameters.txt.

#### GEOMETRY I

Draw the model geometry using a rectangle and six layers.

I In the Sketch toolbar, click Rectangle and choose Rectangle.

Rectangle I (rI)

- I In the Model Builder window, expand the Geometry I node.
- 2 Right-click Component I (compl)>Geometry I and choose Rectangle.
- 3 In the Settings window for Rectangle, locate the Size and Shape section.
- 4 In the Width text field, type L.
- 5 In the **Height** text field, type W.
- 6 Click to expand the Layers section. In the table, enter the following settings:

Layer name	Thickness (m)
Layer 1	di
Layer 2	dg
Layer 3	da
Layer 4	dm

Layer name	Thickness (m)
Layer 5	dc
Layer 6	dg

7 Click Build All Objects.

#### DEFINITIONS

#### Variables 1

Next, add variables.

- I In the Home toolbar, click a= Variables and choose Local Variables.
- 2 In the Settings window for Variables, locate the Variables section.
- 3 Click Load from File.
- 4 Browse to the model's Application Libraries folder and double-click the file soec\_co2\_variables.txt.

General Projection I (gentroil)

Next, add a General Projection coupling.

- I In the Definitions toolbar, click // Nonlocal Couplings and choose General Projection.
- 2 Select Domain 5 only.

## WATER ELECTROLYZER (WE)

Start setting up the electrochemistry part of the model.

- I In the Model Builder window, under Component I (compl) click Water Electrolyzer (we).
- 2 In the Settings window for Water Electrolyzer, locate the H2 Gas Mixture section.
- **3** Select the **CO2** check box.
- 4 Select the **CO** check box.
- **5** Find the **Transport mechanisms** subsection. Select the Use Darcy's Law for momentum transport check box.
- 6 Locate the **02 Gas Mixture** section. Select the **N2** check box.
- 7 Select the Include gas phase diffusion check box.
- 8 Select the Use Darcy's Law for momentum transport check box.

#### Membrane I

- I In the Physics toolbar, click **Domains** and choose **Membrane**.
- 2 Select Domain 4 only.

H2 Gas Diffusion Electrode I

- I In the Physics toolbar, click **Domains** and choose **H2 Gas Diffusion Electrode**.
- 2 Select Domain 5 only.
- 3 In the Settings window for H2 Gas Diffusion Electrode, locate the Effective Electrolyte Charge Transport section.
- **4** In the  $\varepsilon_1$  text field, type eps1.
- 5 Locate the **Gas Transport** section. From the **Effective diffusivity correction** list, choose **Tortuosity**.
- **6** In the  $\varepsilon_g$  text field, type epsg.
- 7 In the  $\tau_g$  text field, type taug.
- 8 In the  $\kappa_g$  text field, type kappag\_GDE.

H2 Gas Diffusion Electrode Reaction: Water Electrolysis

- In the Model Builder window, under Component I (compl)>Water Electrolyzer (we)> H2 Gas Diffusion Electrode I click H2 Gas Diffusion Electrode Reaction I.
- 2 In the Settings window for H2 Gas Diffusion Electrode Reaction, type H2 Gas Diffusion Electrode Reaction: Water Electrolysis in the Label text field.
- **3** Locate the **Electrode Kinetics** section. In the  $i_{0,ref}(T)$  text field, type i0\_ref\_HER.
- **4** In the  $\alpha_a$  text field, type 0.5.
- **5** Locate the **Active Specific Surface Area** section. In the  $a_v$  text field, type S.

H2 Gas Diffusion Electrode I

In the Model Builder window, click H2 Gas Diffusion Electrode 1.

H2 Gas Diffusion Electrode Reaction: CO2 Electrolysis

- I In the Physics toolbar, click Attributes and choose H2 Gas Diffusion Electrode Reaction.
- 2 In the Settings window for H2 Gas Diffusion Electrode Reaction, type H2 Gas Diffusion Electrode Reaction: CO2 Electrolysis in the Label text field.
- **3** Locate the **Stoichiometric Coefficients** section. In the  $v_{CO2}$  text field, type -1.
- 4 In the  $v_{CO}$  text field, type 1.
- **5** Locate the **Electrode Kinetics** section. In the  $i_{0,ref}(T)$  text field, type i0\_ref\_COER.
- **6** Locate the **Active Specific Surface Area** section. In the  $a_v$  text field, type S.

O2 Gas Diffusion Electrode I

In the Physics toolbar, click Domains and choose **02** Gas Diffusion Electrode.

- **2** Select Domain 3 only.
- 3 In the Settings window for O2 Gas Diffusion Electrode, locate the **Effective Electrolyte Charge Transport** section.
- **4** In the  $\varepsilon_1$  text field, type eps1.
- 5 Locate the Gas Transport section. From the Effective diffusivity correction list, choose Tortuosity.
- **6** In the  $\varepsilon_g$  text field, type epsg.
- 7 In the  $\tau_g$  text field, type taug.
- **8** In the  $\kappa_g$  text field, type kappag\_GDE.
- O2 Gas Diffusion Electrode Reaction I
- I In the Model Builder window, click **02** Gas Diffusion Electrode Reaction I.
- 2 In the Settings window for O2 Gas Diffusion Electrode Reaction, locate the **Electrode Kinetics** section.
- **3** In the  $i_{0,ref}(T)$  text field, type i0\_ref\_0ER.
- 4 Locate the Active Specific Surface Area section. In the  $a_{
  m v}$  text field, type S.

H2 Gas Flow Channel I

Next, add the H2 Gas Flow Channel.

- I In the Physics toolbar, click **Domains** and choose **H2 Gas Flow Channel**.
- 2 Select Domain 6 only.
- 3 In the Settings window for H2 Gas Flow Channel, locate the Gas Transport section.
- 4 From the list, choose Straight channels.
- **5** In the *H* text field, type dg.
- **6** In the W text field, type dg.

O2 Gas Flow Channel I

Next, add the **02** Gas Flow Channel.

- I In the Physics toolbar, click **Domains** and choose **O2 Gas Flow Channel**.
- **2** Select Domain 2 only.
- 3 In the Settings window for O2 Gas Flow Channel, locate the Gas Transport section.
- 4 From the list, choose Straight channels.
- **5** In the *H* text field, type dg.
- **6** In the W text field, type dg.

Current Collector I

- I In the Physics toolbar, click **Domains** and choose **Current Collector**.
- **2** Select Domains 1 and 7 only.
- 3 In the Settings window for Current Collector, locate the Electrode Charge Transport section.
- **4** From the  $\sigma_s$  list, choose From material.

Electronic Conducting Phase I

Next, specify the initial values for the oxygen domain to enhance convergence and set the boundary conditions.

I In the Model Builder window, click Electronic Conducting Phase I.

Initial Values, O2 Domains 1

- I In the Physics toolbar, click \_\_\_ Attributes and choose Initial Values, 02 Domains.
- **2** Select Domain 3 only.
- 3 In the Settings window for Initial Values, O2 Domains, locate the Initial Values section.
- **4** In the  $\phi_s$  text field, type E\_app.

Electronic Conducting Phase I

In the Model Builder window, click Electronic Conducting Phase 1.

Electric Ground 1

- I In the Physics toolbar, click Attributes and choose Electric Ground.
- **2** Select Boundary 12 only.

Electronic Conducting Phase I

In the Model Builder window, click Electronic Conducting Phase 1.

Electric Potential I

- I In the Physics toolbar, click \_\_\_ Attributes and choose Electric Potential.
- 2 Select Boundary 6 only.
- 3 In the Settings window for Electric Potential, locate the Electric Potential section.
- 4 In the  $\phi_{s,bnd}$  text field, type E\_app.

H2 Gas Phase I

Next, specify initial values, add the water gas shift reaction, and set the hydrogen inlet and outlet boundary conditions.

Initial Values 1

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Composition section.
- 3 In the  $x_{0 \text{ H}20}$  text field, type x0\_H20.
- 4 In the  $x_{0,CO2}$  text field, type x0\_C02.
- **5** In the  $x_{0,CO}$  text field, type x0\_C0.

H2 Gas Phase I

In the Model Builder window, click H2 Gas Phase I.

Water Gas Shift Reaction 1

- I In the Physics toolbar, click Attributes and choose Water Gas Shift Reaction.
- 2 In the Settings window for Water Gas Shift Reaction, locate the Water Gas Shift Reaction Rate section.
- **3** In the  $k_{\text{WGSR}}$  text field, type k\_wgsr.
- **4** In the  $p_{ref}$  text field, type 1[Pa].

H2 Gas Phase I

In the Model Builder window, click H2 Gas Phase I.

H2 Inlet I

- I In the Physics toolbar, click Attributes and choose H2 Inlet.
- 2 Select Boundary 11 only.
- 3 In the Settings window for H2 Inlet, locate the Mixture Specification section.
- 4 From the list, choose Mass flow rates.
- **5** In the  $J_{0.\mathrm{H2O}}$  text field, type Mflux\_in\*w0\_H20.
- **6** In the  $J_{0,CO2}$  text field, type Mflux\_in\*w0\_CO2.
- **7** In the  $J_{0.CO}$  text field, type Mflux\_in\*w0\_C0.
- **8** In the  $\omega_{0.bnd,H2O}$  text field, type w0\_H20.
- **9** In the  $\omega_{0.bnd.CO2}$  text field, type w0\_C02.
- **IO** In the  $\omega_{0,\text{bnd},CO}$  text field, type w0\_CO.
- II Locate the Flow Boundary Condition section. From the list, choose Total mass flow rate.
- 12 In the  $J_0$  text field, type Mflux\_in.

H2 Gas Phase I

In the Model Builder window, click H2 Gas Phase I.

H2 Outlet I

- I In the Physics toolbar, click \_ Attributes and choose H2 Outlet.
- 2 Select Boundary 21 only.

O2 Gas Phase I

Next, set the initial values and the oxygen inlet and outlet boundary conditions.

Initial Values 1

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Composition section.
- **3** In the  $x_{0,N2}$  text field, type x0\_N2.

O2 Gas Phase I

In the Model Builder window, click O2 Gas Phase I.

O2 Inlet I

- I In the Physics toolbar, click Attributes and choose 02 Inlet.
- 2 Select Boundary 3 only.
- 3 In the Settings window for O2 Inlet, locate the Mixture Specification section.
- 4 From the list, choose Mass flow rates.
- **5** In the  $J_{0,\mathrm{N2}}$  text field, type Mflux\_in\*w0\_N2.
- **6** In the  $\omega_{0.bnd,N2}$  text field, type w0\_N2.
- 7 Locate the Flow Boundary Condition section. From the list, choose Total mass flow rate.
- **8** In the  $J_0$  text field, type Mflux\_in.

O2 Gas Phase I

In the Model Builder window, click 02 Gas Phase I.

O2 Outlet I

- I In the Physics toolbar, click Attributes and choose **02 Outlet**.
- 2 Select Boundary 17 only.

## HEAT TRANSFER IN SOLIDS AND FLUIDS (HT)

Next, set the heat transfer physics.

- I In the Model Builder window, under Component I (compl) click Heat Transfer in Solids and Fluids (ht).
- 2 In the Settings window for Heat Transfer in Solids and Fluids, locate the Physical Model section.

**3** In the  $T_{\rm ref}$  text field, type T\_in.

Solid: Interconnects

- I In the Model Builder window, under Component I (compl)> Heat Transfer in Solids and Fluids (ht) click Solid I.
- 2 In the Settings window for Solid, type Solid: Interconnects in the Label text field.

Fluid: Flow Channels

- I In the Model Builder window, under Component I (compl)> Heat Transfer in Solids and Fluids (ht) click Fluid 1.
- 2 In the Settings window for Fluid, type Fluid: Flow Channels in the Label text field.
- **3** Select Domains 2 and 6 only.
- 4 Locate the Model Input section. From the  $p_A$  list, choose User defined. In the associated text field, type we.pA.
- **5** Locate the **Heat Convection** section. Specify the **u** vector as

we.u	x
we.v	у

- **6** Locate the **Heat Conduction, Fluid** section. From the k list, choose **Thermal conductivity**, gas phase (we).
- 7 Locate the Thermodynamics, Fluid section. From the Fluid type list, choose Gas/Liquid.
- 8 From the  $\rho$  list, choose Density of gas phase (we).
- 9 From the  $C_p$  list, choose Heat capacity at constant pressure, gas phase (we).

Initial Values 1

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- 3 In the T text field, type T in.

Porous Medium: Cathode GDE

Next, add thermal conductivities for the gas diffusion electrode domains.

- I In the Physics toolbar, click **Domains** and choose Porous Medium.
- 2 In the Settings window for Porous Medium, type Porous Medium: Cathode GDE in the **Label** text field.
- 3 Select Domain 5 only.

#### Fluid 1

- I In the Model Builder window, click Fluid I.
- 2 In the Settings window for Fluid, locate the Model Input section.
- **3** From the  $p_A$  list, choose **User defined**. In the associated text field, type we.pA.
- 4 Locate the **Heat Convection** section. Specify the  ${\bf u}$  vector as

we.u	x
we.v	у

- 5 Locate the Heat Conduction, Fluid section. From the  $k_f$  list, choose Thermal conductivity, gas phase (we).
- **6** Locate the **Thermodynamics, Fluid** section. From the  $\rho_f$  list, choose Density of gas phase (we).
- 7 From the  $C_{p,f}$  list, choose Heat capacity at constant pressure, gas phase (we).

#### Porous Matrix I

- I In the Model Builder window, click Porous Matrix I.
- 2 In the Settings window for Porous Matrix, locate the Matrix Properties section.
- **3** From the  $\varepsilon_p$  list, choose **User defined**. In the associated text field, type epsg.
- 4 Locate the Heat Conduction, Porous Matrix section. From the  $k_{\rm b}$  list, choose User defined. In the associated text field, type kc.
- 5 Locate the Thermodynamics, Porous Matrix section. From the  $\rho_b$  list, choose User defined. From the  $C_{\rm p,b}$  list, choose **User defined**.

## Porous Medium: Anode GDE

- I In the Physics toolbar, click **Domains** and choose Porous Medium.
- 2 In the Settings window for Porous Medium, type Porous Medium: Anode GDE in the Label text field.
- **3** Select Domain 3 only.

#### Fluid 1

- I In the Model Builder window, click Fluid I.
- 2 In the Settings window for Fluid, locate the Model Input section.
- **3** From the  $p_A$  list, choose **User defined**. In the associated text field, type we.pA.

**4** Locate the **Heat Convection** section. Specify the **u** vector as

we.u	х
we.v	y

- 5 Locate the Heat Conduction, Fluid section. From the  $k_f$  list, choose Thermal conductivity, gas phase (we).
- **6** Locate the **Thermodynamics, Fluid** section. From the  $\rho_f$  list, choose Density of gas phase (we).
- 7 From the  $C_{p,\mathrm{f}}$  list, choose Heat capacity at constant pressure, gas phase (we).

Porous Matrix I

- I In the Model Builder window, click Porous Matrix I.
- 2 In the Settings window for Porous Matrix, locate the Matrix Properties section.
- **3** From the  $\varepsilon_{\rm p}$  list, choose **User defined**. In the associated text field, type epsg.
- 4 Locate the Heat Conduction, Porous Matrix section. From the  $k_{\rm b}$  list, choose User defined. In the associated text field, type ka.
- **5** Locate the **Thermodynamics, Porous Matrix** section. From the  $\rho_b$  list, choose **User defined**. From the  $C_{\mathrm{p,b}}$  list, choose User defined.

Solid: Membrane

Next, add thermal conductivity for the membrane domains.

- I In the Physics toolbar, click **Domains** and choose **Solid**.
- 2 In the Settings window for Solid, type Solid: Membrane in the Label text field.
- **3** Select Domain 4 only.
- 4 Locate the **Heat Conduction, Solid** section. From the k list, choose **User defined**. In the associated text field, type km.
- **5** Locate the **Thermodynamics, Solid** section. From the ρ list, choose **User defined**. From the  $C_p$  list, choose User defined.

Inflow I

Next, add the inflow, outflow, and periodic condition boundary conditions.

- I In the Physics toolbar, click Boundaries and choose Inflow.
- **2** Select Boundaries 3 and 11 only.
- 3 In the Settings window for Inflow, locate the Upstream Properties section.
- **4** In the  $T_{\rm ustr}$  text field, type T\_in.

## Outflow I

- I In the Physics toolbar, click Boundaries and choose Outflow.
- 2 Select Boundaries 17 and 21 only.

#### Periodic Condition I

- I In the Physics toolbar, click Boundaries and choose Periodic Condition.
- 2 Select Boundaries 2 and 15 only.

#### MULTIPHYSICS

Next, add an electrochemical heating multiphysics coupling.

Electrochemical Heating I (ech I)

In the Physics toolbar, click Multiphysics Couplings and choose Domain> Electrochemical Heating.

#### MATERIALS

Now, add materials from the Material Library.

#### ADD MATERIAL

- I In the Home toolbar, click **‡ Add Material** to open the **Add Material** window.
- 2 Go to the Add Material window.
- 3 In the tree, select Fuel Cell and Electrolyzer>Solid Oxides>Yttria-Stabilized Zirconia, 8YSZ, (ZrO2)0.92-(Y2O3)0.08.
- 4 Click Add to Component in the window toolbar.

#### MATERIALS

Yttria-Stabilized Zirconia, 8YSZ, (ZrO2)0.92-(Y2O3)0.08 (mat1)

- I In the Settings window for Material, locate the Geometric Entity Selection section.
- 2 Click Clear Selection.
- **3** Select Domains 3–5 only.

### ADD MATERIAL

- I Go to the Add Material window.
- 2 In the tree, select Built-in>Steel AISI 4340.
- **3** Click **Add to Component** in the window toolbar.
- 4 In the Home toolbar, click **‡** Add Material to close the Add Material window.

#### MATERIALS

Steel AISI 4340 (mat2)

Select Domains 1 and 7 only.

## MESH I

Next, set up a user-controlled mesh.

#### Distribution I

- I In the Model Builder window, under Component I (compl) right-click Mesh I and choose Distribution.
- **2** Select Boundaries 2, 4, 6, 8, 10, 12, 14, and 15 only.
- 3 In the Settings window for Distribution, locate the Distribution section.
- 4 In the Number of elements text field, type 100.

#### Distribution 2

- I In the Model Builder window, right-click Mesh I and choose Distribution.
- 2 Select Boundaries 1, 13, 16, and 22 only.
- 3 In the Settings window for Distribution, locate the Distribution section.
- 4 In the Number of elements text field, type 2.

#### Distribution 3

- I Right-click Mesh I and choose Distribution.
- 2 Select Boundaries 3, 11, 17, and 21 only.
- 3 In the Settings window for Distribution, locate the Distribution section.
- 4 In the Number of elements text field, type 10.

#### Distribution 4

- I Right-click Mesh I and choose Distribution.
- **2** Select Boundaries 7 and 19 only.
- 3 In the Settings window for Distribution, locate the Distribution section.
- 4 In the Number of elements text field, type 2.

#### Distribution 5

- I Right-click Mesh I and choose Distribution.
- 2 Select Boundaries 9 and 20 only.
- 3 In the Settings window for Distribution, locate the Distribution section.
- 4 From the Distribution type list, choose Predefined.

- 5 In the Number of elements text field, type 20.
- 6 In the Element ratio text field, type 10.
- 7 From the Growth rate list, choose Exponential.

## Distribution 6

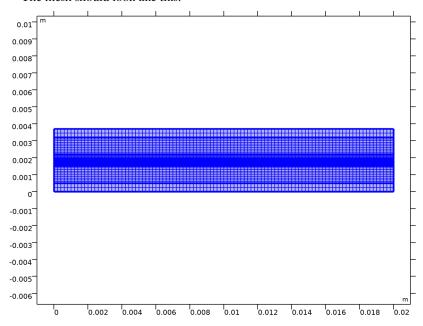
- I Right-click Mesh I and choose Distribution.
- 2 Select Boundaries 5 and 18 only.
- 3 In the Settings window for Distribution, locate the Distribution section.
- 4 From the Distribution type list, choose Predefined.
- 5 In the Number of elements text field, type 10.
- **6** In the **Element ratio** text field, type 5.
- 7 From the Growth rate list, choose Exponential.
- 8 Select the Reverse direction check box.

## Mapped I

- I In the Mesh toolbar, click Mapped.
- 2 In the Settings window for Mapped, click **Build All**.

3 Click the Zoom Extents button in the Graphics toolbar.

The mesh should look like this:



#### STUDY I

Finally, set the study settings using an auxiliary sweep for the applied potential to complete the model setup.

Step 1: Current Distribution Initialization

- I In the Model Builder window, under Study I click Step 1: Current Distribution Initialization.
- 2 In the Settings window for Current Distribution Initialization, locate the Study Settings section.
- 3 From the Current distribution type list, choose Secondary.

Step 2: Stationary

- I In the Model Builder window, click Step 2: Stationary.
- 2 In the Settings window for Stationary, click to expand the Study Extensions section.
- 3 Select the Auxiliary sweep check box.
- 4 Click + Add.

**5** In the table, enter the following settings:

Parameter name	Parameter value list	Parameter unit
E_app (SOEC operating potential)	0.5 1 1.5	V

**6** In the **Home** toolbar, click **Compute**.

#### RESULTS

Some plots are added by default. Follow the instructions below to reproduce the figures in the Results and Discussion section.

Mole Fraction, H2 (we)

- I In the Model Builder window, under Results click Mole Fraction, H2 (we).

The plot should look like Figure 2.

Mole Fraction, CO (we)

- I In the Model Builder window, click Mole Fraction, CO (we).
- 2 In the Mole Fraction, CO (we) toolbar, click Plot.

The plot should look like Figure 3.

Surface I

- I In the Model Builder window, expand the Temperature (ht) node, then click Surface I.
- 2 In the Settings window for Surface, locate the Expression section.
- 3 In the Expression text field, type T-T in.

Temperature (ht)

- I In the Model Builder window, click Temperature (ht).
- 2 In the Settings window for 2D Plot Group, click to expand the Title section.
- 3 From the Title type list, choose Manual.
- 4 In the Title text area, type Surface: Change in Temperature (K).
- 5 In the Temperature (ht) toolbar, click  **Plot**.

The plot should look like Figure 4.

Water Gas Shift Reaction Rate

Next, plot the water gas shift reaction rate over the hydrogen gas diffusion electrode and flow channel domains.

- I In the Home toolbar, click Add Plot Group and choose 2D Plot Group.
- 2 In the Settings window for 2D Plot Group, type Water Gas Shift Reaction Rate in the Label text field.

#### Surface 1

- I In the Water Gas Shift Reaction Rate toolbar, click
- 2 In the Settings window for Surface, locate the Expression section.
- 3 In the Expression text field, type we.r wgsr.
- 4 In the Water Gas Shift Reaction Rate toolbar, click Plot.

The plot should look like Figure 5.

## Current Density Distribution

Finally, add a plot for the total integrated current density across the electrode length.

- I In the Home toolbar, click **Add Plot Group** and choose ID Plot Group.
- 2 In the Settings window for ID Plot Group, type Current Density Distribution in the Label text field.
- 3 Locate the Data section. From the Parameter selection (E\_app) list, choose Last.
- 4 Click to expand the Title section. From the Title type list, choose Manual.
- 5 In the Title text area, type Current Density Distribution, Cathode Side.
- 6 Locate the Plot Settings section.
- 7 Select the x-axis label check box. In the associated text field, type Electrode length (m).
- 8 Select the y-axis label check box. In the associated text field, type Integrated current density in y-direction (A/cm<sup>2</sup>).

## Line Graph 1

- I In the Current Density Distribution toolbar, click \times Line Graph.
- **2** Select Boundary 10 only.
- 3 In the Settings window for Line Graph, locate the y-Axis Data section.
- 4 In the Expression text field, type genproj1(we.iv h2gder1).
- 5 In the Unit field, type A/cm<sup>2</sup>.
- 6 Click to expand the Coloring and Style section. From the Width list, choose 2.
- 7 Click to expand the **Legends** section. Select the **Show legends** check box.
- 8 From the Legends list, choose Manual.

**9** In the table, enter the following settings:

Legends	
H20	

Current Density Distribution

In the Model Builder window, click Current Density Distribution.

## Line Graph 2

- I In the Current Density Distribution toolbar, click \times Line Graph.
- **2** Select Boundary 10 only.
- 3 In the Settings window for Line Graph, locate the y-Axis Data section.
- 4 In the Expression text field, type genproj1 (we.iv h2gder2).
- 5 In the **Unit** field, type A/cm^2.
- 6 Locate the Coloring and Style section. From the Width list, choose 2.
- 7 Locate the Legends section. Select the Show legends check box.
- 8 From the Legends list, choose Manual.
- **9** In the table, enter the following settings:



## Current Density Distribution

- I In the Model Builder window, click Current Density Distribution.
- 2 In the Current Density Distribution toolbar, click  **Plot**.

The plot should look like Figure 6.