Flow Past a Cylinder

Introduction

The flow of fluid behind a blunt body such as an automobile is difficult to compute due to the unsteady flows. The wake behind such a body consists of unordered eddies of all sizes that create large drag on the body. In contrast, the turbulence in the thin boundary layers next to the streamlined bodies of aircraft and fish create only weak disturbances of flow.

An exception to this occurs when you place a slender body at right angles to a slow flow because the eddies organize; a von Kármán vortex street appears with a predictable frequency and involves the shedding of eddies from alternating sides. Everyday examples of this phenomenon include singing telephone wires and an automobile radio antenna vibrating in an air stream.

From an engineering standpoint, it is important to predict the frequency of vibrations at various fluid speeds and thereby avoid undesirable resonances between the vibrations of the solid structures and the vortex shedding. To help reduce such effects, plant engineers put a spiral on the upper part of high smokestacks; the resulting variation in shape prohibits the constructive interference of the vortex elements that the structure sheds from different positions.

Model Definition

To illustrate how you can study effects of the kind described above, this model examines unsteady, incompressible flow past a long cylinder placed in a channel at right angle to the oncoming fluid. With a symmetric inlet velocity profile, the flow needs some kind of asymmetry to trigger the vortex production. This can be achieved by placing the cylinder with a small offset from the center of the flow.

The simulation time necessary for a periodic flow pattern to appear is difficult to predict. A key predictor is the Reynolds number, which is based on cylinder diameter. For low values (below 100) the flow is steady. In this simulation, the Reynolds number equals 100, which gives a developed von Kármán vortex street, but the flow still is not fully turbulent.

The frequency and amplitude of oscillations are stable features, but flow details are extremely sensitive to perturbations. To gain an appreciation for this sensitivity, you can compare flow images taken at the same time but with such minor differences as are created by different tolerances for the time stepping. It is important to note that this sensitivity is a physical reality and not simply a numerical artifact.

Before calculating the time-varying forces on the cylinder, you can validate the method of computation at a lower Reynolds number using the direct nonlinear solver. This saves time because you can find and correct simple errors and mistakes before the final time-dependent simulation, which requires considerable time.

The viscous forces on the cylinder are proportional to the gradient of the velocity field at the cylinder surface. Evaluating the velocity gradient on the boundary by directly differentiating the FEM solution is possible but not very accurate. The differentiation produces first-order polynomials when second-order elements are used for the velocity field. A far better approach is to use a pair of reaction force operators to compute the integrals of the viscous forces, comparable to second-order accurate integrals of the viscous forces. An alternative approach would be to use a pair of weak-constraint variables to enforce the no-slip condition. Preferably use the reaction force operator instead of weak constraints when computing integrals of reaction forces or fluxes in results processing.

The lift and drag forces themselves are not as interesting as the dimensionless lift and drag coefficients. These depend only on the Reynolds number and an object's shape, not its size. They are defined as

$$C_{\mathrm{L}} \ = \ \frac{2F_{\mathrm{L}}}{\rho U^2_{\mathrm{mean}} A} \tag{1}$$

$$C_{\mathrm{D}} \ = \ \frac{2F_{\mathrm{D}}}{\rho U^2_{\mathrm{mean}} A} \tag{2}$$

where

- F_{L} and F_{D} are the lift and drag forces
- ρ is the fluid density
- U_{mean} is the mean velocity
- A is the projected area (that is, the product of the cylinder diameter and length)

Results and Discussion

Figure 1 shows the flow pattern resulting from the geometry. The points represent massive particles that are released at the inlet boundary; these are used in an animation to further help in visualizing the flow.
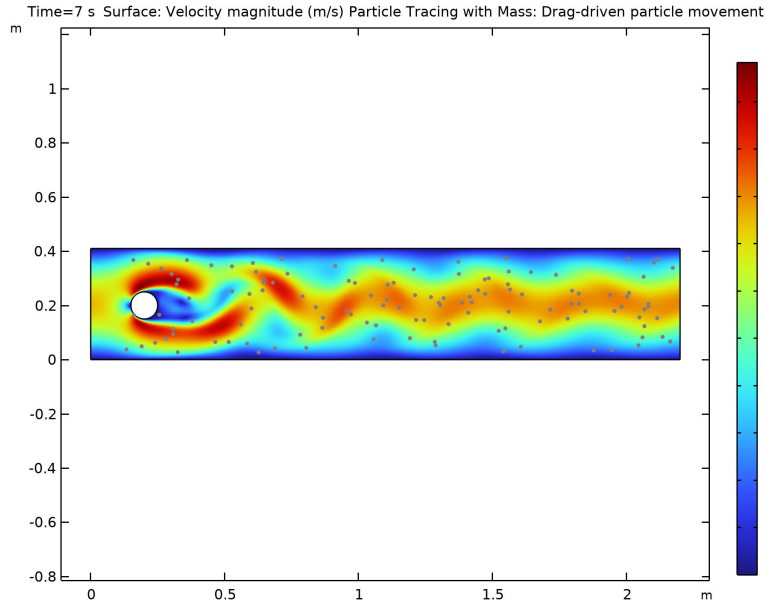

Time=7 s Surface: Velocity magnitude (m/s) Particle Tracing with Mass: Drag-driven particle movement

Figure 1: A plot of the last time step clearly shows the von Kármán path.

The flow around a cylinder is a common benchmark test for CFD algorithms. Various research teams have tried their strengths on this problem using different techniques. Results from some of these experiments have been collected by Schäfer and Turek (Ref. 1), who also used them to compute a probable value for the "real" answer.

Figure 2 shows how the lift coefficient develops a periodic variation as the von Kármán vortex structure is formed.
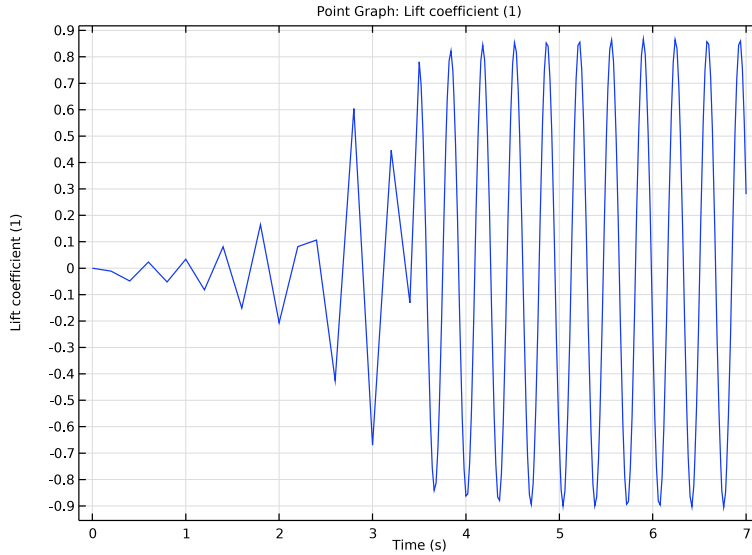
Figure 2: Lift coefficient, C_L*, as a function of time.*
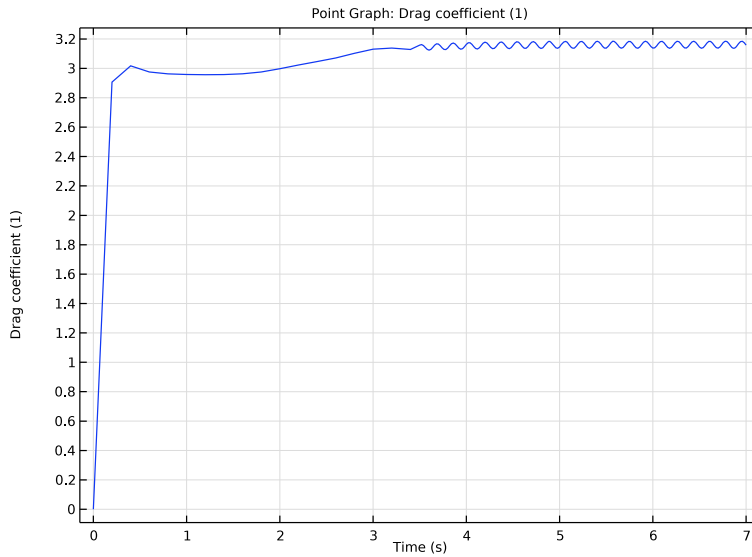
Figure 3: Drag coefficient, C_D*, as a function of time.*

Notes About the COMSOL Implementation

This model uses a Particle Tracing with Mass plot (see *Particle Tracing with Mass* in the *COMSOL Multiphysics Reference Manual* for details) in an Animation feature. More advanced functionality for simulating the trajectories of particles subjected to forces of various kinds is provided with the Particle Tracing Module.

The lift and drag coefficients (see Equation 1 and Equation 2) are computed using an Integral dataset defined on the cylinder boundaries, with the lift and drag forces, F_L and F_D, evaluated as the reaction-force-operator expressions `-reacf(v)[N/m^2]` and `-reacf(u)[N/m^2]`, respectively (the unit brackets give the correct dimension of force per unit area). Introducing a unit channel width, `W`, in the out-of-plane dimension, which also defines the cylinder length, the full expressions for the integrands read

$$-2*\text{reacf(v)}[\text{N/m\^{}2}]*W/(\text{spf.rho*U\_mean\^{}2*(2*R*W)}) \quad (C_L)$$

and

$$-2*\text{reacf(u)}[\text{N/m\^{}2}]*W/(\text{spf.rho*U\_mean\^{}2*(2*R*W)}) \quad (C_D)$$

For more information about the use of `reacf` to compute reaction forces, see *Computing Accurate Fluxes* in the *COMSOL Multiphysics Reference Manual*. (An alternative is to use the components of the total traction, exterior boundaries auxiliary vector variable, `-spf.T_stressy` and `-spf.T_stressx`, defined in the Single-Phase Flow interface.)

Reference

1. M. Schäfer and S. Turek, "Benchmark Computations of Laminar Flow Around Cylinder", E.H. Hirschel ed., *Flow Simulation with High-Performance Computers II, Volume 52 of Notes on Numerical Fluid Mechanics*, Vieweg, pp. 547–566, 1996.

Application Library path: `COMSOL_Multiphysics/Fluid_Dynamics/cylinder_flow`

Modeling Instructions

From the **File** menu, choose **New**.

NEW

In the **New** window, click **Model Wizard**.

1 In the **Model Wizard** window, click ⚛ **2D**.

2 In the **Select Physics** tree, select **Fluid Flow>Single-Phase Flow>Laminar Flow (spf)**.

3 Click **Add**.

4 Click ➡ **Study**.

5 In the **Select Study** tree, select **General Studies>Time Dependent**.

6 Click ☑ **Done**.

GLOBAL DEFINITIONS

Parameters 1

Define geometry and velocity parameters, including a unit channel width in the out-of-plane dimension that is not included in this 2D model.

1 In the **Model Builder** window, under **Global Definitions** click **Parameters 1**.

2 In the **Settings** window for **Parameters**, locate the **Parameters** section.

3 In the table, enter the following settings:

Name	Expression	Value	Description
H	0.41[m]	0.41 m	Channel height
L	2.2[m]	2.2 m	Channel length
W	1[m]	1 m	Channel width (not modeled)
R	0.05[m]	0.05 m	Cylinder radius
U_mean	1[m/s]	1 m/s	Mean inflow velocity

Next, create a smoothed step function feature that you will use for ramping up the inflow velocity.

Step 1 (step1)

1 In the **Home** toolbar, click f(x) **Functions** and choose **Global>Step**.

2 In the **Settings** window for **Step**, locate the **Parameters** section.

3 In the **Location** text field, type 0.05.

GEOMETRY 1

Rectangle 1 (r1)

1 In the **Geometry** toolbar, click ▭ **Rectangle**.

2 In the **Settings** window for **Rectangle**, locate the **Size and Shape** section.

3 In the **Width** text field, type L.

4 In the **Height** text field, type H.

5 Click ▦ **Build Selected**.

Circle 1 (c1)

1 In the **Geometry** toolbar, click ⊙ **Circle**.

2 In the **Settings** window for **Circle**, locate the **Position** section.

3 In the **x** text field, type 4*R.

4 In the **y** text field, type 4*R.

5 Locate the **Size and Shape** section. In the **Radius** text field, type R.

6 Click ▦ **Build Selected**.

Difference 1 (dif1)

1 In the **Geometry** toolbar, click ▦ **Booleans and Partitions** and choose **Difference**.

2 Select the object **r1** only.

3 In the **Settings** window for **Difference**, locate the **Difference** section.

4 Click to select the ▭ **Activate Selection** toggle button for **Objects to subtract**.

5 Select the object **c1** only.

6 In the **Geometry** toolbar, click ▦ **Build All**.

7 Click the ⊹ **Zoom Extents** button in the **Graphics** toolbar.

8 In the **Model Builder** window, click **Geometry 1**.
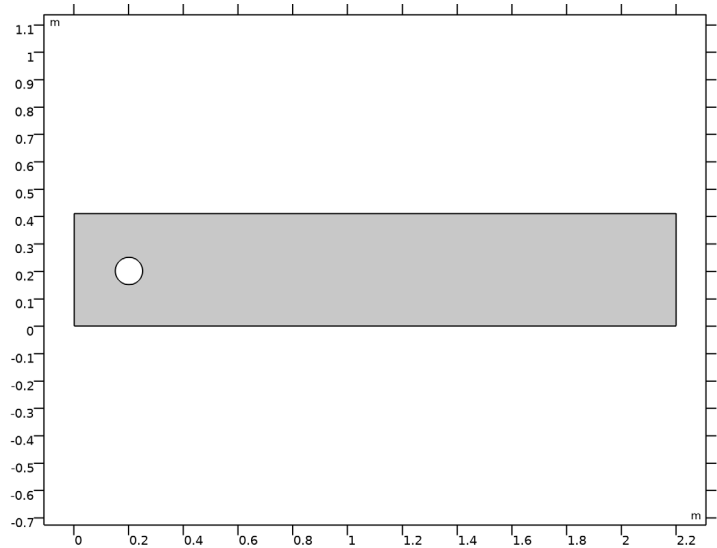
MATERIALS

Specify the relevant fluid properties: the density and the dynamic viscosity.

Material 1 (mat1)

1 In the **Model Builder** window, under **Component 1 (comp1)** right-click **Materials** and choose **Blank Material**.

2 In the **Settings** window for **Material**, locate the **Material Contents** section.

3 In the table, enter the following settings:

Property	Variable	Value	Unit	Property group
Density	rho	1	kg/m³	Basic
Dynamic viscosity	mu	1e-3	Pa·s	Basic

LAMINAR FLOW (SPF)

Inlet 1

1 In the **Model Builder** window, under **Component 1 (comp1)** right-click **Laminar Flow (spf)** and choose **Inlet**.

2 Select Boundary 1 only.

Define a parabolic velocity profile using the predefined parameters and ramp up the velocity using the previously defined step function.

3 In the **Settings** window for **Inlet**, locate the **Velocity** section.

4 In the U_0 text field, type `6*U_mean*y*(H-y)/H^2*step1(t[1/s])`.

By appending the inverse unit bracket `[1/s]` to the time variable `t` you get a dimensionless argument, as the step function expects.

Outlet 1

1 In the **Physics** toolbar, click ⬭ **Boundaries** and choose **Outlet**.
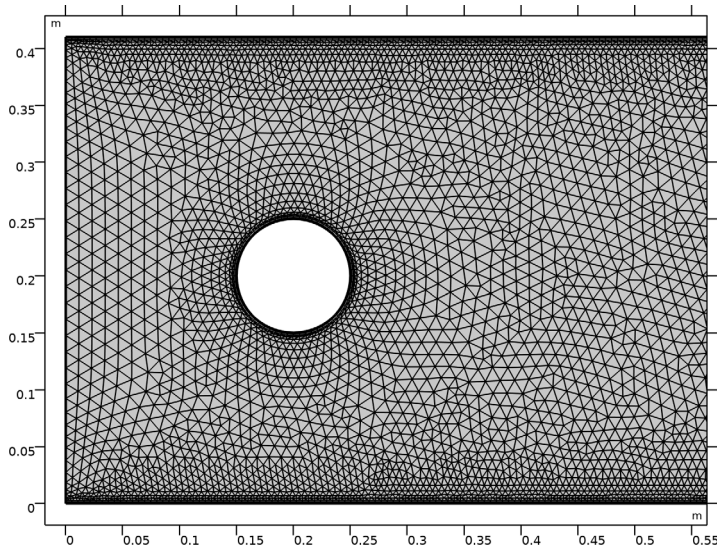
2 Select Boundary 4 only.

MESH 1

1 In the **Model Builder** window, under **Component 1 (comp1)** click **Mesh 1**.

2 In the **Settings** window for **Mesh**, locate the **Physics-Controlled Mesh** section.

3 From the **Element size** list, choose **Finer**.

4 Click ⊞ **Build All**.

If you zoom in on the inlet and the cylinder you can see the boundary layers that the physics-controlled mesh gives.

5 Click the ⌖ **Zoom Extents** button in the **Graphics** toolbar.

Step 1: Time Dependent

1 In the **Model Builder** window, under **Study 1** click **Step 1: Time Dependent**.

2 In the **Settings** window for **Time Dependent**, locate the **Study Settings** section.

3 In the **Output times** text field, type `range(0,0.2,3.4) range(3.5,0.02,7)`.

Solution 1 (sol1)

1 In the **Study** toolbar, click ▐▊▄ **Show Default Solver**.

2 In the **Model Builder** window, expand the **Solution 1 (sol1)** node, then click **Time-Dependent Solver 1**.

3 In the **Settings** window for **Time-Dependent Solver**, click to expand the **Time Stepping** section.

4 From the **Steps taken by solver** list, choose **Intermediate**.

5 In the **Study** toolbar, click ▬ **Compute**.

RESULTS

Velocity (spf)

Click the ┼ **Zoom Extents** button in the **Graphics** toolbar.

Add a **Particle Tracing with Mass** node to the first default plot group to reproduce the plot in Figure 1.

Particle Tracing with Mass 1

1 In the **Velocity (spf)** toolbar, click ▇ **More Plots** and choose **Particle Tracing with Mass**.

2 In the **Settings** window for **Particle Tracing with Mass**, click to expand the **Mass and Velocity** section.

3 In the **Mass** text field, type `4*pi/3*1e-9`.

4 Find the **Initial velocity** subsection. In the **x-component** text field, type `u`.

5 In the **y-component** text field, type `v`.

6 Locate the **Particle Positioning** section. In the **y** text field, type `range(0.05,0.025, 0.35)`.

7 In the **x** text field, type `0`.

8 Click to expand the **Release** section. From the **Release particles** list, choose **At intervals**.

9 Select the **Start time** check box. In the associated text field, type `3.2`.

10 In the **Time between releases** text field, type `0.2`.

11 Click to expand the **Coloring and Style** section. Find the **Line style** subsection. From the **Type** list, choose **None**.

12 Find the **Point style** subsection. From the **Type** list, choose **Point**.

13 Select the **Radius scale factor** check box. In the associated text field, type `7.5`.

14 From the **Color** list, choose **Custom**.

15 Click **Define custom colors**.

16 Set the RGB values to 128, 128, and 128, respectively.

17 Click **Add to custom colors**.

18 Click **Show color palette only** or **OK** on the cross-platform desktop.

19 Find the **Point motion** subsection. From the **When particle leaves domain** list, choose **Disappear**.

20 In the **Velocity (spf)** toolbar, click 🔲 **Plot**.

Next, use the plot you just set up in an animation.

Animation 1

1 In the **Results** toolbar, click ▦ **Animation** and choose **Player**.

2 In the **Settings** window for **Animation**, locate the **Frames** section.

3 In the **Number of frames** text field, type 50. Increasing the number of frames results in a smoother animation.

4 Click the ▶ **Play** button in the **Graphics** toolbar.

To reproduce Figure 2 and Figure 3 of the lift and drag coefficients, first add an **Integral** dataset for computing the total reaction force on the cylinder.

Integral 1

In the **Results** toolbar, click ▦ **More Datasets** and choose **Evaluation>Integral**.

Selection

1 In the **Results** toolbar, click 🗏 **Attributes** and choose **Selection**.

2 In the **Settings** window for **Selection**, locate the **Geometric Entity Selection** section.

3 From the **Geometric entity level** list, choose **Boundary**.

4 Select Boundaries 5–8 only.

Lift Coefficient

First, create a plot of the lift coefficient using the following steps:

1 In the **Results** toolbar, click 〰 **1D Plot Group**.

2 In the **Settings** window for **ID Plot Group**, type Lift Coefficient in the **Label** text field.

3 Locate the **Data** section. From the **Dataset** list, choose **Integral 1**.

Point Graph 1

1 Right-click **Lift Coefficient** and choose **Point Graph**.

2 In the **Settings** window for **Point Graph**, locate the **y-Axis Data** section.

3 In the **Expression** text field, type -2*reacf(v)[N/m^2]*W/(spf.rho*U_mean^2*(2* R*W)).

In this expression, reacf(v)[N/m^2] is the vertical component of the outward reaction force on the exterior cylinder boundaries; multiplying by the nonmodeled channel unit width W gives a dimensionless lift coefficient.

4 Select the **Description** check box. In the associated text field, type Lift coefficient.

5 In the **Lift Coefficient** toolbar, click ▣ **Plot**.

Compare the graph with that shown in Figure 2.

Lift Coefficient

Finally, visualize the drag coefficient:

In the **Model Builder** window, right-click **Lift Coefficient** and choose **Duplicate**.

Drag Coefficient

1 In the **Model Builder** window, expand the **Results>Lift Coefficient 1** node, then click **Lift Coefficient 1**.

2 In the **Settings** window for **ID Plot Group**, type Drag Coefficient in the **Label** text field.

Point Graph 1

1 In the **Model Builder** window, click **Point Graph 1**.

2 In the **Settings** window for **Point Graph**, locate the **y-Axis Data** section.

3 In the **Expression** text field, type -2*reacf(u)[N/m^2]*W/(spf.rho*U_mean^2*(2* R*W)). That is, just replace v by u as the argument for reacf.

4 In the **Description** text field, type Drag coefficient.

5 In the **Drag Coefficient** toolbar, click ▣ **Plot**.

Compare with Figure 3.