

ID Isothermal Nickel—Cadmium Battery

Nickel-Cadmium (Ni-Cd) batteries are rechargeable batteries with nickel-hydroxide as positive electrode material, cadmium as negative electrode material, and hydroxide ions in an aqueous KOH electrolyte as charge carriers. Historically, they were used in many applications, for example those requiring high power. Today, mainly due to the toxicity of cadmium, their use is restricted. In the European Union, for example, they are only allowed in medical equipment and emergency systems and lighting. Lithium-ion and nickel-metal hydroxide batteries have replaced the Ni-Cd battery in many applications.

The present model shows how a typical sealed Ni-Cd battery cell can be described using the Battery with Binary Electrolyte interface.

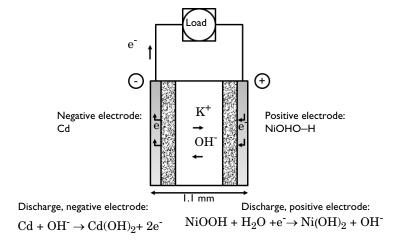


Figure 1: Cross section of a Ni-Cd battery showing the main electrochemical processes that occur during discharge.

The 1D isothermal model includes the following processes:

- Electronic current conduction in the electrodes
- Ionic charge transport in the electrodes and electrolyte/separator
- Material transport in the electrolyte
- Material transport within the cylindrically symmetric particles that form the positive electrode

- Change in porosity of the negative electrode
- Butler-Volmer electrode kinetics using experimentally measured discharge curves for the equilibrium potential. The kinetics for both electrode reactions, as well as for oxygen evolution, are included.

The model is based on a paper by De Vidts and White (Ref. 2) using data for a typical sealed NiCd battery (Ref. 1). In the paper, the authors also included a model for electron transport inside the positive electrode material. However, it was found that this contribution was negligible and it is therefore excluded in the present model.

Model Definition

This example models the battery cross section in 1D, which implies that edge effects in the length and height of the battery are neglected. The example uses the following domains:

- Negative porous electrode (cadmium): 400 μm
- Separator (electrolyte): 250 μm
- Positive porous electrode (nickel oxide): 360 μm

In addition, an extra dimension description of the cylindrically symmetric particles in the positive electrode is included. These particles constitute long "wires", with a central core of inactive support material. The thickness of the inactive core region is $1.5~\mu m$, and the thickness of the active material surrounding it is $1.4~\mu m$.

The electric potential in the electron conducting phase, ϕ_s , is calculated using a charge balance based on Ohm's law, where the charge transfer reactions result in source or sink term. For the porous electrodes effective conductivities, σ_s^{eff} , are used that take porosity and tortuosity into account as given by the following expression:

$$\sigma_s^{\rm eff} = \sigma_s \varepsilon^{\gamma}$$

where γ is the Bruggeman coefficient, which is set to 1.5 in this model, corresponding to a packed bed of spherical particles. Also, the diffusion coefficient for the electrolyte salt is corrected for the tortuosity and the porosity in this way.

The ionic charge balances and material balances are modeled according to the equations for a binary 1:1 electrolyte, with both the anion (OH⁻) and the solvent (H₂O) participating in the electrode reactions (Ref. 2).

Fickian diffusion describes the transport in the cylindrical particles of the positive electrode. The diffusion equation is expressed in cylindrical coordinates for the material balance of protons in the particles.

Butler-Volmer electrode kinetics describes the local charge transfer current density in the electrodes. The Butler-Volmer expressions are introduced as source or sink terms in the charge balances and material balances.

BOUNDARY CONDITIONS

For the electronic current balance, a potential of 0 V is set on the negative electrode's current collector/feeder boundary. At the positive electrode current collector/feeder, the current density is specified. The current density is set to a constant discharge current. The inner boundaries facing the separator are insulating for electric currents.

For the ionic charge balance in the electrolyte, the current collector/feeder boundaries are insulating. Insulating conditions also apply to the material balances.

At the particle surface in the local particle model, the material flux is determined by the local electrochemical reaction rate.

MATERIAL PROPERTIES

The material properties are those of a typical NiCd cell. The electrolyte is KOH, diluted in water to a 30% (wt) solution. The active electrode materials are cadmium for the negative electrode and a nickel oxide (Ni(OH)₂) for the positive electrode.

The model uses constant values for the electrolyte conductivity, the electrolyte diffusivity, and the activity variation with concentration in the electrolyte.

The positive Ni electrode limits, and thus determines, the capacity of the battery cell. For this reason, the solid volume fraction of the Ni electrode is computed as

$$\varepsilon_s = \frac{Q_{\text{cell}}}{Fc_{\text{H, max}}l_{\text{positive}}} \tag{1}$$

where Q_{cell} is the cell capacity (74.16 C/cm² of electrode), F is Faraday's constant, $c_{\text{H.}}$ $_{
m max}$ is the maximum proton concentration in the positive material and $l_{
m positive}$ is the thickness of the positive electrode (400 µm).

Simulations of both the discharge and charge behavior of the cell are performed. In both cases, three increasingly high C-rates of C/10, C/2.1, and C/0.7 are applied. The nominal charge/discharge current density, the 1C rate, is 206 A/m².

DISCHARGE CURVES

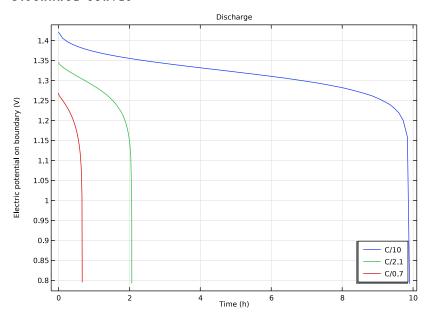


Figure 2: Discharge curves for three C-rates.

Figure 2 shows discharge curves for the three C-rates. The overpotential of the positive electrode reaction increases with increasing C-rate, accounting for most of the difference in cell voltage at the initial time. At the end of discharge, the concentration of protons inside the positive electrode approaches the maximum value and the slopes of the voltage curves decrease drastically.

CHARGE CURVES

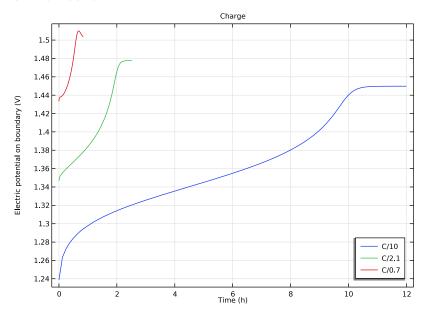


Figure 3: Charge curves for the three C-rates.

Figure 3 shows charge curves for all three C-rates. Again, as for the discharge curves, the difference in initial potential is due mainly to the overpotential of the positive electrode reaction. However, as the cell approaches 100% state of charge (SOC), the oxygen side reaction takes up an increasing fraction of the applied current. The voltage then plateaus, and during overcharging all current goes toward oxygen evolution on the positive Ni electrode and reduction at the negative Cd electrode.

STATE OF CHARGE DURING CHARGING

Figure 4 shows the hydration level of the positive Ni electrode, while Figure 5 shows the volume fraction of the negative Cd electrode, in both cases for charging. The x-axis shows the charge efficiency. Charging should reach completion at t = 1 for 100% charge efficiency. Charging causes protons to exit the positive electrode, and causes Cd hydroxide to be converted into metallic Cd. For this reason, decreasing hydration level and decreasing volume fraction both correspond to increasing SOC.

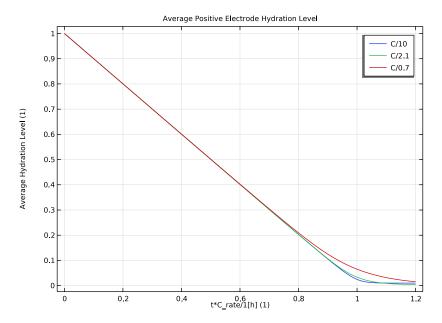


Figure 4: State of charge of the positive Ni electrode during charging at three different Crates.

Both hydration level and volume fraction decrease in the same way during the initial part of charging, when the main electrode reactions consume almost all of the current. As charging approaches completion, after about t = 0.8, increasing C-rates are associated with decreased charge efficiency. Again, at higher C-rates, the oxygen side reaction consumes an increasing fraction of the charging current.

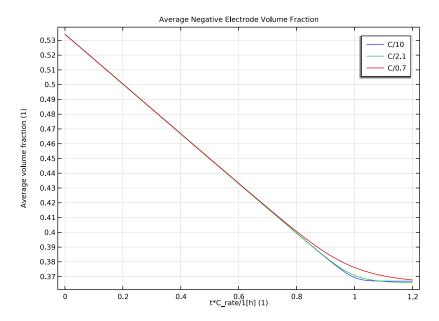


Figure 5: State of charge of the negative Cd electrode during charging at three different Crates.

Notes About the COMSOL Implementation

ELECTROLYTE MOLAR MASS

By default, the Battery with Binary Electrolyte interface assumes a binary aqueous KOH electrolyte, so the default values for molar masses on the main interface node do not need to be changed.

PROTON DIFFUSION IN EXTRA DIMENSION

Proton diffusion inside the positive Ni active material is modeled inside a cylindrically symmetric Extra Dimension. The following continuity equation, which accounts for the cylindrical symmetry, is applied for protons inside the active positive material:

$$2\pi r \left(\frac{\partial c_{\rm H}}{\partial t} + -D_{\rm H} \frac{\partial c_{\rm H}}{\partial r}\right) = 0 \tag{2}$$

Furthermore, at the exterior boundary of the Extra Dimension (the active material particle outer surface), the flux of $c_{\rm H}$ is proportional to the current density of the main Ni electrode reaction. Both expressions are implemented in weak form.

The core of inactive support material is what necessitates the extra dimension description. If the Ni material particles had been assumed to be active throughout the whole radius, the Particle Properties of the Ni electrode could instead have been set to Intercalating Particles, and the diffusion of protons could have been set up in the associated Particle Intercalation child node.

POROUS ELECTRODE ELECTRICAL CONDUCTIVITY

The solid electrical conductivity of each of the two porous electrodes is on the order of 10^5 S/m. However, the electrolyte conductivity is significantly lower, and thus is the main factor limiting the rate of charge transport. This difference in conductivities makes convergence harder to achieve. Using an effective solid phase conductivity of 100 S/m facilitates convergence while having an insignificant effect on the results.

References

- 1. W.R. Scott and D.W. Rusta, Sealed-Cell Nickel Cadmium Battery Applications Manual, 1979.
- 2. P. De Vidts and R.E. White, "Mathematical Modeling of a Nickel-Cadmium Cell: Proton Diffusion in the Nickel Electrode," J. Electrochem. Soc., vol. 142, p. 1509, 1995.

Application Library path: Battery_Design_Module/Batteries,_General/ nicd battery 1d

Modeling Instructions

From the File menu, choose New.

NEW

In the New window, click Model Wizard.

MODEL WIZARD

I In the Model Wizard window, click — ID.

- 2 In the Select Physics tree, select Electrochemistry>Batteries> Battery with Binary Electrolyte (batbe).
- 3 Click Add.
- 4 Click Study.
- 5 In the Select Study tree, select Preset Studies for Selected Physics Interfaces> Time Dependent with Initialization.
- 6 Click M Done.

GLOBAL DEFINITIONS

Define parameters for the model. These include general parameters (for example the geometry), parameters used for each electrode, for the electrode reactions, for initial values of the charging and discharging studies, and finally the different C-rates to use for charge and discharge.

General

- I In the Model Builder window, under Global Definitions click Parameters I.
- 2 In the Settings window for Parameters, type General in the Label text field.
- 3 Locate the Parameters section. Click **Load from File**.
- 4 Browse to the model's Application Libraries folder and double-click the file nicd_battery_1d_general.txt.

Cd Electrode

- I In the Home toolbar, click Pi Parameters and choose Add>Parameters.
- 2 In the Settings window for Parameters, type Cd Electrode in the Label text field.
- 3 Locate the Parameters section. Click **Load from File.**
- 4 Browse to the model's Application Libraries folder and double-click the file nicd battery 1d cd electrode.txt.

Ni Electrode

- I In the Home toolbar, click Pi Parameters and choose Add>Parameters.
- 2 In the Settings window for Parameters, type Ni Electrode in the Label text field.
- 3 Locate the Parameters section. Click **Load from File**.
- 4 Browse to the model's Application Libraries folder and double-click the file nicd_battery_1d_ni_electrode.txt.

Electrode Reactions

I In the Home toolbar, click P Parameters and choose Add>Parameters.

- 2 In the Settings window for Parameters, type Electrode Reactions in the Label text field
- 3 Locate the Parameters section. Click **Load from File.**
- **4** Browse to the model's Application Libraries folder and double-click the file nicd_battery_1d_electrode_reactions.txt.

Charge/Discharge Cases

- I In the Home toolbar, click P Parameters and choose Add>Parameters.
- 2 In the Settings window for Parameters, type Charge/Discharge Cases in the Label text field.
- **3** Locate the **Parameters** section. In the table, enter the following settings:

Name	Expression	Value	Description
c_H_init	c_H_max/500	104.2 mol/m³	Initial H concentration in positive electrode
epsilon_3_init	epsilon_3_max	0.6365	Initial porosity of the negative electrode
sign	-1	-1	Sign of applied current, 1 for charge, -1 for discharge

- 4 In the Home toolbar, click Pi Parameter Case.
- **5** Right-click **Case I** and choose **Rename**.
- 6 In the Rename Case dialog box, type Discharge in the New label text field.
- 7 Click OK.
- 8 In the Home toolbar, click Pi Parameter Case.
- 9 In the Settings window for Case, type Charge in the Label text field.
- **10** Locate the **Parameters** section. In the table, enter the following settings:

Name	Expression	Description
c_H_init	c_H_max	Initial H concentration in positive electrode
epsilon_3_init	epsilon_3_min+0.05	Initial porosity of the negative electrode
sign	1	Sign of applied current, I for charge, - I for discharge

C-rate Cases

- I In the Home toolbar, click Pi Parameters and choose Add>Parameters.
- 2 In the Settings window for Parameters, type C-rate Cases in the Label text field.
- 3 Locate the Parameters section. In the table, enter the following settings:

Name	Expression	Value	Description
C_rate	1	I	Charge/discharge rate

- 4 In the Home toolbar, click Pi Parameter Case.
- 5 In the Settings window for Case, locate the Parameters section.
- **6** In the table, enter the following settings:

Name	Expression	Description
C_rate	1/10	Charge/discharge rate

- 7 In the Home toolbar, click Pi Parameter Case.
- 8 In the Settings window for Case, locate the Parameters section.
- **9** In the table, enter the following settings:

Name	Expression	Description
C_rate	1/2.1	Charge/discharge rate

- 10 In the Home toolbar, click Pi Parameter Case.
- II In the Settings window for Case, locate the Parameters section.
- **12** In the table, enter the following settings:

Name	Expression	Description	
C_rate	1/0.7	Charge/discharge rate	

Define the cylindrical geometry of the electrode particles in the positive electrode in an Extra Dimension.

- 13 Click the Show More Options button in the Model Builder toolbar.
- 14 In the Show More Options dialog box, select Physics>Extra Dimensions in the tree.
- **I5** In the tree, select the check box for the node **Physics>Extra Dimensions**.
- 16 Click OK.

ADD COMPONENT

In the Model Builder window, right-click Global Definitions and choose Extra Dimensions> ID Axisymmetric.

EXTRA DIMENSION: POSITIVE ELECTRODE

- I In the Settings window for Extra Dimension, type Extra Dimension: Positive Electrode in the Label text field.
- **2** Locate the **Frames** section. Find the **Spatial frame coordinates** subsection. In the table, enter the following settings:

First	Second	Third
rxd	phi1	z1

GEOMETRY 2

Interval I (iI)

- In the Model Builder window, expand the Global Definitions>
 Extra Dimension: Positive Electrode (xdim1)>Definitions node.
- 2 Right-click Global Definitions>Extra Dimension: Positive Electrode (xdim1)>Geometry 2 and choose Interval.

The geometry of the positive electrode particles consists of an inner core of inactive substrate surrounded by active battery material.

- 3 In the Settings window for Interval, locate the Interval section.
- 4 From the Specify list, choose Interval lengths.
- **5** In the **Left endpoint** text field, type y_positive_substrate.
- **6** In the table, enter the following settings:

Le	Lengths (m)				
٧	positive	active			

7 Click **Build Selected**.

Define two integration operators to allow integration of variables in the extra dimension. These will be used later to compute the particle surface proton concentration as well as the average proton concentration inside the particle.

DEFINITIONS (XDIMI)

Extra Dimension Surface Integral

- I In the Model Builder window, under Global Definitions> Extra Dimension: Positive Electrode (xdim I) right-click Definitions and choose Extra Dimensions>Integration over Extra Dimension.
- 2 In the Settings window for Integration over Extra Dimension, type Extra Dimension Surface Integral in the Label text field.
- 3 Locate the Operator Name section. In the Operator name text field, type xdsurfop.
- 4 Locate the Source Selection section. From the Geometric entity level list, choose Boundary.
- **5** Select Boundary 2 only.
- 6 Locate the Advanced section. Clear the Compute integral in revolved geometry check box.

Extra Dimension Domain Integral

- I In the Model Builder window, right-click Extra Dimensions and choose Integration over Extra Dimension.
- 2 In the Settings window for Integration over Extra Dimension, type Extra Dimension Domain Integral in the Label text field.
- 3 Locate the Operator Name section. In the Operator name text field, type xdintopDomain.
- 4 Select Domain 1 only.
- 5 Locate the Advanced section. Clear the Compute integral in revolved geometry check box.

Make the mesh finer close to the left and right boundaries of the extra dimension.

MESH 2

- I In the Model Builder window, under Global Definitions> Extra Dimension: Positive Electrode (xdim1) click Mesh 2.
- 2 In the Settings window for Mesh, locate the Sequence Type section.
- 3 From the list, choose User-controlled mesh.

Distribution 1

- I Right-click Global Definitions>Extra Dimension: Positive Electrode (xdim I)>Mesh 2 and choose Distribution.
- 2 Drag and drop Distribution I below Size.
- **3** Select Domain 1 only.

- 4 In the Settings window for Distribution, locate the Distribution section.
- 5 From the Distribution type list, choose Predefined.
- 6 In the Number of elements text field, type 31.
- 7 In the Element ratio text field, type 0.1.
- 8 Click Build All.

Next, define the geometry for the battery cell.

GEOMETRY I

Interval I (i1)

- I In the Model Builder window, expand the Component I (compl)>Geometry I node.
- 2 Right-click Geometry I and choose Interval.
- 3 In the Settings window for Interval, locate the Interval section.
- 4 From the Specify list, choose Interval lengths.
- **5** In the table, enter the following settings:

Lengths (m)		
l_neg		
l_sep		
l_pos		

6 Click **Build All Objects**.

Define the connection between the battery cell geometry and the extra dimension used for the cylindrical battery particles.

DEFINITIONS (COMPI)

Attached Dimensions I

- I In the Model Builder window, expand the Component I (compl)>Definitions node.
- 2 Right-click Component I (compl)>Definitions and choose Extra Dimensions> Attached Dimensions.
- 3 In the Settings window for Attached Dimensions, locate the Geometric Entity Selection section.
- 4 From the Geometric entity level list, choose Domain.
- **5** Select Domain 3 only.

- 6 Locate the Attached Dimensions section. Under Extra dimensions to attach, click
- 7 In the Add dialog box, select Extra Dimension: Positive Electrode (xdim1) in the Extra dimensions to attach list.
- 8 Click OK.

Define the variables needed for the SOC of the negative electrode, the SOC and diffusive flux of protons inside the positive electrode, and the surface and average proton concentration and SOC at the positive electrode.

Negative Electrode

- I Right-click **Definitions** and choose **Variables**.
- 2 In the Settings window for Variables, type Negative Electrode in the Label text field.
- 3 Locate the Geometric Entity Selection section. From the Geometric entity level list, choose Domain.
- 4 Select Domain 1 only.
- **5** Locate the **Variables** section. In the table, enter the following settings:

Name	Expression	Unit	Description
theta_N	<pre>(batbe.eps1- epsilon_3_min)/ (epsilon_3_max- epsilon_3_min)</pre>		SOC, negative electrode

Positive Electrode (Intraparticle)

- I Right-click **Definitions** and choose **Variables**.
- 2 In the Settings window for Variables, type Positive Electrode (Intraparticle) in the Label text field.
- 3 Locate the Geometric Entity Selection section. From the Geometric entity level list, choose Domain.
- 4 Select Domain 3 only.
- 5 From the Extra dimension attachment list, choose Attached Dimensions 1.

6 Locate the **Variables** section. In the table, enter the following settings:

Name	Expression	Unit	Description
theta_P	cH[mol/m^3]/ c_H_max		SOC, positive electrode
particle_diffusiv e_flux	-D_H*d(cH[mol/ m^3],rxd)		Fickian diffusive flux in positive electrode

Positive Electrode (Particle Surface)

- I Right-click **Definitions** and choose **Variables**.
- 2 In the **Settings** window for **Variables**, type Positive Electrode (Particle Surface) in the **Label** text field.
- 3 Locate the Geometric Entity Selection section. From the Geometric entity level list, choose Domain.
- 4 Select Domain 3 only.
- **5** Locate the **Variables** section. In the table, enter the following settings:

Name	Expression	Unit	Description
cH_surf	<pre>xdim1.xdsurfop(cH)[mol/m^3]</pre>		Particle surface H concentration, positive electrode
cH_average	<pre>xdim1.xdintopDomain(rxd* cH[mol/m^3])/ xdim1.xdintopDomain(rxd)</pre>		Average H concentration, positive electrode
soc_average	cH_average/c_H_max		Average SOC, positive electrode

At this point, all the entries are shown in yellow since further settings are needed to fully define the variables.

Define three operators: one for the positive electrode current collector, one for positive electrode averages, and one for negative electrode averages.

Integration Operator for Positive Electrode Current Collector

- I In the Definitions toolbar, click / Nonlocal Couplings and choose Integration.
- 2 In the **Settings** window for **Integration**, type Integration Operator for Positive Electrode Current Collector in the **Label** text field.

- 3 In the Operator name text field, type intop posCC.
- 4 Locate the Source Selection section. From the Geometric entity level list, choose Boundary.
- **5** Select Boundary 4 only.

Positive Electrode Average Operator

- I In the Definitions toolbar, click Nonlocal Couplings and choose Average.
- 2 In the Settings window for Average, type Positive Electrode Average Operator in the Label text field.
- 3 In the Operator name text field, type ave pos.
- 4 Select Domain 3 only.

Negative Electrode Average Operator

- I In the **Definitions** toolbar, click Monlocal Couplings and choose Average.
- 2 In the Settings window for Average, type Negative Electrode Average Operator in the Label text field.
- 3 In the Operator name text field, type ave_neg.
- 4 Select Domain 1 only.

The next step is to set up the description of the chemical processes inside the battery. Begin with the Battery with Binary Electrolyte interface.

BATTERY WITH BINARY ELECTROLYTE (BATBE)

By default, the **Battery with Binary Electrolyte** interface assumes a KOH binary electrolyte, so the default values for the **Species** section will be kept. However, properties for the KOH electrolyte for the porous electrodes and separator need to be specified. These are available in the Material Library.

ADD MATERIAL

- I In the Home toolbar, click # Add Material to open the Add Material window.
- 2 Go to the Add Material window.
- 3 In the tree, select Battery>Electrolytes>KOH (Liquid).
- **4** Click **Add to Component** in the window toolbar.
- 5 In the Home toolbar, click Radd Material to close the Add Material window.

Continue by defining the separator.

BATTERY WITH BINARY ELECTROLYTE (BATBE)

Separator I

- I In the Model Builder window, under Component I (compl)>
 Battery with Binary Electrolyte (batbe) click Separator I.
- 2 In the Settings window for Separator, locate the Porous Matrix Properties section.
- **3** In the ε_1 text field, type epsilon_2.

Initial Values 1

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- **3** In the *cl* text field, type cl init.

Continue by setting up the description for the Ni (positive) electrode.

Porous Electrode: Ni (Positive)

- I In the Physics toolbar, click **Domains** and choose **Porous Electrode**.
- 2 In the Settings window for Porous Electrode, type Porous Electrode: Ni (Positive) in the Label text field.
- **3** Select Domain 3 only.
- **4** Locate the **Electrode Properties** section. In the σ_s text field, type sigma_electrode.
- 5 Locate the Particle Properties section. From the list, choose Nonintercalating particles.
- **6** Locate the **Porous Matrix Properties** section. In the ε_s text field, type epss.
- 7 In the ε_1 text field, type epsilonO_P-epss.
- 8 Locate the Effective Transport Parameter Correction section. From the Electrical conductivity list, choose No correction.

Set up the intercalation process for protons at the Ni electrode.

Porous Electrode Reaction: NiOOH + H2O + e- <=> Ni(OH)2 + OH-

- I In the Model Builder window, under Component I (compl)>
 Battery with Binary Electrolyte (batbe)>Porous Electrode: Ni (Positive) click
 Porous Electrode Reaction I.
- 2 In the Settings window for Porous Electrode Reaction, type Porous Electrode Reaction: NiOOH + H2O + e- <=> Ni(OH)2 + OH- in the Label text field.
- 3 Locate the Equilibrium Potential section. From the $E_{\rm eq}$ list, choose Nernst equation.
- **4** In the $E_{\text{eq.ref}}(T)$ text field, type E_ref_pos.
- **5** In the C_R text field, type (cl/c_ref)*(cH_surf/c_H_ref).

- **6** In the C_O text field, type (c_H_max-cH_surf)/(c_H_max-c_H_ref).
- 7 Locate the Electrode Kinetics section. From the Kinetics expression type list, choose Butler-Volmer.
- 8 From the Exchange current density type list, choose From Nernst Equation.
- **9** In the $i_{0,ref}(T)$ text field, type i0_1_ref.
- **IO** In the α_a text field, type alpha_a_1.
- II Locate the Active Specific Surface Area section. From the Active specific surface area list, choose **User defined**. In the a_v text field, type a_Ni.
- 12 Click to expand the Heat of Reaction section. From the list, choose User defined.

Add the OER/ORR reaction on the Ni electrode. The mass transport of oxygen inside the battery cell will be set up later.

Porous Electrode: Ni (Positive)

In the Model Builder window, click Porous Electrode: Ni (Positive).

Porous Electrode Reaction: 1/2 O2 + H2O + 2e- <=> 2 OH-

- I In the Physics toolbar, click Attributes and choose Porous Electrode Reaction.
- 2 In the Settings window for Porous Electrode Reaction, type Porous Electrode Reaction: 1/2 02 + H20 + 2e- <=> 2 0H- in the Label text field.
- 3 Locate the Equilibrium Potential section. From the $E_{\rm eq}$ list, choose Nernst equation.
- **4** In the $E_{\text{eq,ref}}(T)$ text field, type E_ref_0ER.
- **5** In the $C_{\rm R}$ text field, type 1.
- **6** In the C_0 text field, type c_02/c_02_ref.
- 7 Locate the **Electrode Kinetics** section. From the **Kinetics expression type** list, choose Butler-Volmer.
- 8 From the Exchange current density type list, choose From Nernst Equation. Use a max() operator to numerically stabilize the kinetics expression.
- **9** In the $i_{0,ref}(T)$ text field, type i0_2_ref*max(cl/c_ref,1e-20)^2.
- **10** In the α_a text field, type alpha_a_2.
- II Locate the Active Specific Surface Area section. From the Active specific surface area list, choose **User defined**. In the a_v text field, type a_Ni.
- 12 Locate the Stoichiometric Coefficients section. In the n text field, type 4.
- 13 Locate the Heat of Reaction section. From the list, choose User defined. Set up the diffusion of protons inside the positive electrode. Add one weak expression for the

diffusive flux and one weak expression for the boundary flux due to the NiOOH/Ni(OH)2 electrode reaction.

- 14 Click the Show More Options button in the Model Builder toolbar.
- 15 In the Show More Options dialog box, select Physics>Stabilization in the tree.
- **16** In the tree, select the check box for the node **Physics>Stabilization**.
- 17 In the tree, select Physics>Stabilization.
- **18** In the tree, clear the check box for the node **Physics>Stabilization**.
- 19 In the tree, select Physics>Equation-Based Contributions.
- **20** In the tree, select the check box for the node **Physics>Equation-Based Contributions**.
- 21 Click OK.
- H+ Diffusion Inside Positive Electrode
- I In the Physics toolbar, click Domains and choose Weak Contribution.
- 2 In the Settings window for Weak Contribution, type H+ Diffusion Inside Positive Electrode in the Label text field.
- **3** Select Domain 3 only.
- 4 Locate the Domain Selection section. From the Extra dimension attachment list, choose Attached Dimensions 1.
- **5** Click to select the **Activate Selection** toggle button.
- 6 Select Domain 1 only.
- 7 Locate the **Weak Contribution** section. In the **Weak expression** text field, type 2*pi*rxd* (particle_diffusive_flux*test(cHrxd)-cHt*test(cH)).

Intraparticle H+ Concentration

- I In the Physics toolbar, click Attributes and choose Auxiliary Dependent Variable.
- 2 In the Settings window for Auxiliary Dependent Variable, type Intraparticle H+ Concentration in the Label text field.
- 3 Locate the Domain Selection section. From the Extra dimension attachment list, choose Attached Dimensions 1.
- **4** Click to select the **Activate Selection** toggle button.
- **5** Select Domain 1 only.
- 6 Locate the Auxiliary Dependent Variable section. In the Field variable name text field, type cH.
- 7 In the Initial value text field, type c_H_init.

Boundary Condition for Concentration at Particle Outer Surface

- I In the Physics toolbar, click **Domains** and choose **Weak Contribution**.
- 2 In the Settings window for Weak Contribution, type Boundary Condition for Concentration at Particle Outer Surface in the Label text field.
- **3** Select Domain 3 only.
- 4 Locate the Domain Selection section. From the Extra dimension attachment list, choose Attached Dimensions I.
- 5 From the Geometric entity level list, choose Boundary.
- 6 Select Boundary 2 only.
- 7 Locate the Weak Contribution section. In the Weak expression text field, type -2* batbe.pce1.per1.iloc*test(cH)*pi*rxd/(1[m]*F const).

Boundary Condition for Concentration at Particle Outer Surface, H+ Diffusion Inside Positive Electrode

- I In the Model Builder window, under Component I (compl)>Battery with Binary Electrolyte (batbe), Ctrl-click to select H+ Diffusion Inside Positive Electrode and **Boundary Condition for Concentration at Particle Outer Surface.**
- **2** Right-click and choose **Group**.

Intraparticle Diffusion of H+

- I In the Model Builder window, right-click Group I and choose Rename.
- 2 In the Rename Group dialog box, type Intraparticle Diffusion of H+ in the New label text field.
- 3 Click OK.

Continue by setting up the Cd (Negative) electrode.

Porous Electrode: Cd (Negative)

- I In the Physics toolbar, click Domains and choose Porous Electrode.
- 2 In the Settings window for Porous Electrode, type Porous Electrode: Cd (Negative) in the Label text field.
- **3** Select Domain 1 only.
- **4** Locate the **Electrode Properties** section. From the σ_s list, choose **User defined**. In the associated text field, type sigma electrode.
- 5 Locate the Particle Properties section. From the list, choose Nonintercalating particles.
- 6 Locate the Porous Matrix Properties section. In the $\varepsilon_{\rm s}$ text field, type 1 epsilon 3 init.

- 7 In the ε_1 text field, type epsilon_3_init.
- 8 Locate the Effective Transport Parameter Correction section. From the **Electrical conductivity** list, choose **No correction**.
- **9** Click to expand the **Dissolving-Depositing Species** section. Click + Add.
- **10** In the table, enter the following settings:

Species	Density (kg/m^3)	Molar mass (kg/mol)
Cd	rho_Cd	M_Cd

II Click + Add.

12 In the table, enter the following settings:

Species	Density (kg/m^3)	Molar mass (kg/mol)
Cd02H2	rho_CdO2H2	M_Cd02H2

Porous Electrode Reaction: Cd + 2 OH- <=> Cd(OH)2 + 2e-

- I In the Model Builder window, under Component I (compl)> Battery with Binary Electrolyte (batbe)>Porous Electrode: Cd (Negative) click Porous Electrode Reaction 1.
- 2 In the Settings window for Porous Electrode Reaction, type Porous Electrode Reaction: Cd + 2 OH- <=> Cd(OH)2 + 2e- in the Label text field.
- 3 Locate the Equilibrium Potential section. From the $E_{\rm eq}$ list, choose Nernst equation.
- **4** In the $E_{\text{eq.ref}}(T)$ text field, type E_ref_neg.
- **5** In the C_R text field, type $(c1/c_ref)^2$.
- 6 Locate the Electrode Kinetics section. From the Kinetics expression type list, choose Butler-Volmer.
- 7 From the Exchange current density type list, choose From Nernst Equation.
- **8** In the $i_{0,ref}(T)$ text field, type theta_N*i0_3_ref.
- **9** In the α_a text field, type alpha_a_3.
- 10 Locate the Active Specific Surface Area section. From the Active specific surface area list, choose **User defined**. In the a_v text field, type a_Cd.
- II Locate the **Stoichiometric Coefficients** section. In the n text field, type 2.

12 In the Stoichiometric coefficients for dissolving-depositing species: table, enter the following settings:

Species	Stoichiometric coefficient (I)
Cd	1
CdO2H2	-1

13 Locate the Heat of Reaction section. From the list, choose User defined.

The oxygen reduction reaction is mass-transport limited at the Cd electrode. Model it using an Internal Electrode Surface, with the local current density being given by an oxygen flux at the Cd electrode. In turn, the flux will be obtained from a Transport of Diluted **Species** interface, where the diffusion of oxygen in the battery is also modeled.

Oxygen Recombination at Cd Electrode

- I In the Physics toolbar, click Boundaries and choose Internal Electrode Surface.
- 2 In the Settings window for Internal Electrode Surface, type Oxygen Recombination at Cd Electrode in the Label text field.
- **3** Select Boundary 2 only.

Electrode Reaction: 1/2 O2 + H2O + 2e- <=> 2 OH-

- I In the Model Builder window, under Component I (compl)> Battery with Binary Electrolyte (batbe)>Oxygen Recombination at Cd Electrode click Electrode Reaction 1.
- 2 In the Settings window for Electrode Reaction, type Electrode Reaction: 1/2 02 + H20 + 2e- <=> 2 OH- in the Label text field.
- 3 Locate the Equilibrium Potential section. From the E_{eq} list, choose User defined. Locate the **Electrode Kinetics** section. From the $i_{loc.expr}$ list, choose **User defined**. In the associated text field, type tds.tflux_c_02x*4*F_const.
- 4 Click to expand the Heat of Reaction section. From the list, choose User defined.

Define the boundary conditions for the battery cell.

Electric Ground 1

- I In the Physics toolbar, click Boundaries and choose Electric Ground.
- 2 Select Boundary 1 only.

Electrode Current I

- I In the Physics toolbar, click Boundaries and choose Electrode Current.
- **2** Select Boundary 4 only.

- 3 In the Settings window for Electrode Current, locate the Electrode Current section.
- 4 From the list, choose Average current density.
- **5** In the $i_{s,average}$ text field, type sign*i_app.

Set up the description of the oxygen transport and reaction.

ADD PHYSICS

- I In the Physics toolbar, click open the Add Physics window.
- 2 Go to the Add Physics window.
- 3 In the tree, select Chemical Species Transport>Transport of Diluted Species (tds).
- 4 Click Add to Component I in the window toolbar.
- 5 In the Physics toolbar, click add Physics to close the Add Physics window.

TRANSPORT OF DILUTED SPECIES (TDS)

- In the Settings window for Transport of Diluted Species, locate the Transport Mechanisms section.
- **2** Clear the **Convection** check box.
- 3 Select the Mass transfer in porous media check box.
- 4 Click to expand the **Dependent Variables** section. In the **Concentrations (mol/m³)** table, enter the following settings:

c_02

5 Select Domains 2 and 3 only.

Transport Properties 1

- I In the Model Builder window, under Component I (compl)>
 Transport of Diluted Species (tds) click Transport Properties I.
- 2 In the Settings window for Transport Properties, locate the Diffusion section.
- **3** In the $D_{\rm cO2}$ text field, type D_02.

Initial Values 1

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- **3** In the c_{O2} text field, type c_O2_init.

Porous Electrode Coupling: Positive Electrode

I In the Physics toolbar, click — Domains and choose Porous Electrode Coupling.

- 2 In the Settings window for Porous Electrode Coupling, type Porous Electrode Coupling: Positive Electrode in the Label text field.
- **3** Select Domain 3 only.

Reaction Coefficients 1

- I In the Model Builder window, click Reaction Coefficients I.
- 2 In the Settings window for Reaction Coefficients, locate the Model Inputs section.
- 3 From the i_v list, choose Local current source, Porous Electrode Reaction: 1/2 02 + H2O + 2e- <=> 2 OH- (batbe/pcel/per2).
- **4** Locate the **Stoichiometric Coefficients** section. In the *n* text field, type 4.
- 5 In the v_{cO2} text field, type -1.

Oxygen Recombination at Cd Electrode

- I In the Physics toolbar, click Boundaries and choose Concentration.
- 2 In the Settings window for Concentration, type Oxygen Recombination at Cd Electrode in the Label text field.
- **3** Select Boundary 2 only.
- 4 Locate the Concentration section. Select the Species c_02 check box.

Initial Values 2

- I In the Physics toolbar, click **Domains** and choose **Initial Values**. Add a suitable initial value for the oxygen concentration in the separator.
- 2 Select Domain 2 only.
- 3 In the Settings window for Initial Values, locate the Initial Values section.
- **4** In the c_{O2} text field, type c_02_init*((x-l_neg)/l_sep).

The battery model, including the oxygen transport and reaction, has now been set up. Now, configure the study to simulate both discharging, and charging, of the battery.

DISCHARGE AND CHARGE

- I In the Model Builder window, click Study I.
- 2 In the Settings window for Study, type Discharge and Charge in the Label text field.

Parametric Sweep

- I In the Study toolbar, click Parametric Sweep.
- 2 In the Settings window for Parametric Sweep, locate the Study Settings section.
- 3 From the Sweep type list, choose Parameter switch.

- 4 Click + Add.
- **5** In the table, enter the following settings:

Switch	Cases	Case numbers
Charge/Discharge Cases	All	range(I,I,2)

- 6 Click + Add.
- **7** In the table, enter the following settings:

Switch	Cases	Case numbers
C-rate Cases	All	range(1,1,3)

Current Distribution Initialization: Primary

- I In the Model Builder window, click Step I: Current Distribution Initialization.
- 2 In the Settings window for Current Distribution Initialization, type Current Distribution Initialization: Primary in the Label text field.

Current Distribution Initialization: Secondary

- I In the Study toolbar, click Study Steps and choose Other>
 Current Distribution Initialization.
- 2 Right-click Step 3: Current Distribution Initialization 2 and choose Move Up.
- 3 In the Settings window for Current Distribution Initialization, type Current Distribution Initialization: Secondary in the Label text field.

Use an additional **Current Distribution Initialization** step, solving for a secondary current distribution, to improve the initial guess further.

4 Locate the Study Settings section. From the Current distribution type list, choose Secondary.

Step 3: Time Dependent

- I In the Model Builder window, click Step 3: Time Dependent.
- 2 In the Settings window for Time Dependent, locate the Study Settings section.
- **3** From the **Time unit** list, choose **h**.
- 4 In the Output times text field, type range(0,t_charge_limit/100, t_charge_limit).

Before starting to solve, to make convergence easier to achieve, manually set the scaling for the oxygen concentration, and the proton concentration in the extra dimension. The corresponding reference concentrations are suitable values for scaling.

Solution I (soll)

- I In the Study toolbar, click Show Default Solver.
- 2 In the Model Builder window, expand the Solution I (soll) node.
- 3 In the Model Builder window, expand the Discharge and Charge>Solver Configurations> Solution I (soll)>Dependent Variables 3 node, then click Concentration (compl.c_02).
- 4 In the Settings window for Field, locate the Scaling section.
- 5 From the Method list, choose Manual.
- 6 In the Scale text field, type c_02_ref.
- 7 In the Model Builder window, under Discharge and Charge>Solver Configurations> Solution I (soll)>Dependent Variables 3 click Auxiliary dependent variable cH (compl.cH).
- 8 In the Settings window for Field, click to collapse the Scaling section.
- 9 Click to expand the Scaling section. From the Method list, choose Manual.
- 10 In the Scale text field, type c H ref.

Additionally, set up two **Stop** conditions, signaling the solver to stop if the cell voltage gets below 0.8 V or above 1.6 V.

- II In the Model Builder window, under Discharge and Charge>Solver Configurations> Solution I (soll) right-click Time-Dependent Solver I and choose Stop Condition.
- 12 In the Settings window for Stop Condition, locate the Stop Expressions section.
- 13 Click + Add.
- **14** In the table, enter the following settings:

Stop expression	Stop if	Active	Description
<pre>comp1.intop_posCC(co mp1.phis)<0.8</pre>	True (>=I)	V	Stop expression 1

15 Click + Add.

16 In the table, enter the following settings:

Stop expression	Stop if	Active	Description
<pre>comp1.intop_posCC(co mp1.phis)>1.6</pre>	True (>=I)	V	Stop expression 2

Store the solution just after the stop condition to include the data at the lowest and highest voltages reached in the results.

17 Locate the Output at Stop section. From the Add solution list, choose Step after stop. Now, run the study for discharge and charge of the battery.

18 In the **Study** toolbar, click **Compute**.

RESULTS

Discharge: Boundary Electrode Potential with Respect to Ground (batbe) Plot the cell voltage for discharge at the three different C-rates.

- I In the **Settings** window for **ID Plot Group**, type Discharge: Boundary Electrode Potential with Respect to Ground (batbe) in the **Label** text field.
- 2 Locate the Data section. From the Parameter selection (c_H_init, epsilon_3_init, sign, C_rate) list, choose From list.
- 3 In the Parameter values list, choose 1: c_H_init=104.2, epsilon_3_init=0.6365, sign=-1, C_rate=0.1, 2: c_H_init=104.2, epsilon_3_init=0.6365, sign=-1, C_rate=0.47619, and 3: c_H_init=104.2, epsilon_3_init=0.6365, sign=-1, C_rate=1.4286.
- 4 In the Discharge: Boundary Electrode Potential with Respect to Ground (batbe) toolbar, click Plot.

Global I

- I In the Model Builder window, expand the

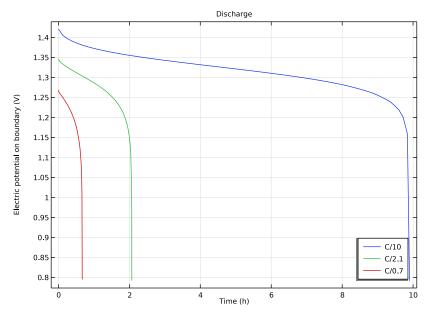
 Discharge: Boundary Electrode Potential with Respect to Ground (batbe) node, then click

 Global I.
- 2 In the Settings window for Global, locate the x-Axis Data section.
- 3 From the Parameter list, choose Expression.
- 4 In the Expression text field, type t.
- **5** From the **Unit** list, choose **h**.
- 6 Click to expand the Legends section. From the Legends list, choose Evaluated.
- 7 In the **Legend** text field, type C/eval(1/C_rate).

Discharge: Boundary Electrode Potential with Respect to Ground (batbe)

- I In the Model Builder window, click
 Discharge: Boundary Electrode Potential with Respect to Ground (batbe).
- 2 In the Settings window for ID Plot Group, click to expand the Title section.
- 3 From the Title type list, choose Manual.
- **4** In the **Title** text area, type **Discharge**.
- 5 Locate the Legend section. From the Position list, choose Lower right.

6 In the Discharge: Boundary Electrode Potential with Respect to Ground (batbe) toolbar, click **Plot**.



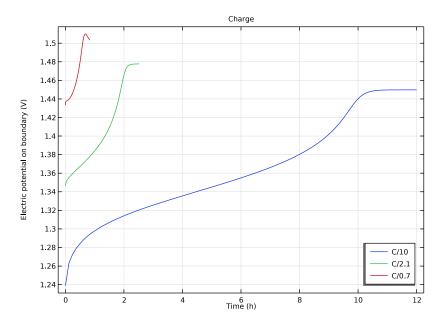
Plot the cell voltage for charging. Then, plot the average positive electrode hydration level (SOC) and the average negative electrode volume fraction (SOC).

7 Right-click Discharge: Boundary Electrode Potential with Respect to Ground (batbe) and choose **Duplicate**.

Charge: Boundary Electrode Potential with Respect to Ground (batbe)

- I In the Model Builder window, under Results click Discharge: Boundary Electrode Potential with Respect to Ground (batbe) I.
- 2 In the Settings window for ID Plot Group, type Charge: Boundary Electrode Potential with Respect to Ground (batbe) in the Label text field.
- 3 Locate the Data section. In the Parameter values list, choose 4: c_H_init=52098, epsilon_3_init=0.46587, sign=1, C_rate=0.1, 5: c_H_init=52098, epsilon_3_init=0.46587, sign=1, C_rate=0.47619, and 6: c_H_init=52098, epsilon_3_init=0.46587, sign=1, C rate=1.4286.
- 4 Locate the Title section. In the Title text area, type Charge.

5 In the Charge: Boundary Electrode Potential with Respect to Ground (batbe) toolbar, click Plot.



Charge: Average Positive Electrode Hydration Level

- I In the Home toolbar, click Add Plot Group and choose ID Plot Group.
- 2 In the Settings window for ID Plot Group, type Charge: Average Positive Electrode Hydration Level in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Discharge and Charge/Parametric Solutions 1 (sol4).
- 4 From the Parameter selection (c_H_init, epsilon_3_init, sign, C_rate) list, choose From list.
- 5 In the Parameter values list, choose 4: c_H_init=52098, epsilon_3_init=0.46587, sign=1, C_rate=0.1, 5: c_H_init=52098, epsilon_3_init=0.46587, sign=1, C_rate=0.47619, and 6: c_H_init=52098, epsilon_3_init=0.46587, sign=1, C_rate=1.4286.
- **6** Locate the **Title** section. From the **Title type** list, choose **Manual**.
- 7 In the Title text area, type Average Positive Electrode Hydration Level.

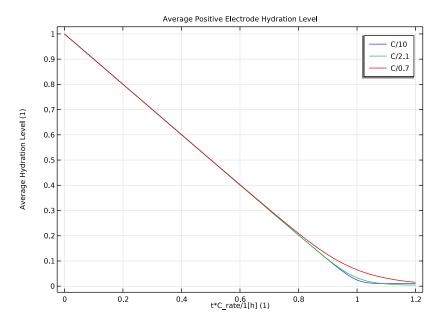
Global I

- I Right-click Charge: Average Positive Electrode Hydration Level and choose Global.
- 2 In the Settings window for Global, locate the y-Axis Data section.

3 In the table, enter the following settings:

Expression	Unit	Description
comp1.ave_pos(cH_average/ c_H_max)	1	Average Hydration Level

- 4 Locate the x-Axis Data section. From the Parameter list, choose Expression. Normalize the time by the C-rate to enable comparing hydration levels for increasing C-rates.
- 5 In the Expression text field, type t*C_rate/1[h].
- 6 Locate the Legends section. From the Legends list, choose Evaluated.
- 7 In the **Legend** text field, type C/eval(1/C rate).
- 8 In the Charge: Average Positive Electrode Hydration Level toolbar, click on Plot.



Charge: Average Negative Electrode Volume Fraction

- I In the Home toolbar, click Add Plot Group and choose ID Plot Group.
- 2 In the Settings window for ID Plot Group, type Charge: Average Negative Electrode Volume Fraction in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Discharge and Charge/ Parametric Solutions I (sol4).

- 4 From the Parameter selection (c_H_init, epsilon_3_init, sign, C_rate) list, choose From list.
- 5 In the Parameter values list, choose 4: c H init=52098, epsilon_3 init=0.46587, sign=1, C_rate=0.1, 5: c_H_init=52098, epsilon_3_init=0.46587, sign=1, C_rate=0.47619, and 6: c_H_init=52098, epsilon_3_init=0.46587, sign=1, C_rate=1.4286.
- 7 Locate the Title section. From the Title type list, choose Manual.
- 8 In the Title text area, type Average Negative Electrode Volume Fraction.

Global I

- I Right-click Charge: Average Negative Electrode Volume Fraction and choose Global.
- 2 In the Settings window for Global, locate the y-Axis Data section.
- **3** In the table, enter the following settings:

Expression	Unit	Description
comp1.ave_neg(batbe.epss)	1	Average volume fraction

- 4 Locate the x-Axis Data section. From the Parameter list, choose Expression.
- 5 In the Expression text field, type t*C_rate/1[h].
- 6 Locate the Legends section. From the Legends list, choose Evaluated.
- 7 In the Legend text field, type C/eval(1/C rate).

8 In the Charge: Average Negative Electrode Volume Fraction toolbar, click on Plot.

