

## Electrochemical Treatment of Tumors

The electrochemical treatment of tumors implies that diseased tissue is treated with direct current through the use of metallic electrodes inserted in the tumor. When tissue is electrolyzed, two competing reactions take place at the anode: oxygen evolution and chlorine production. The oxygen-evolution reaction also produces H<sup>+</sup> ions, which lower the pH close to the anode. It should be stressed that chlorine production also leads to lowered pH through the hydrolysis of chlorine. One effect of low pH is the permanent destruction of hemoglobin in the tissue, which results in destruction of tumor tissue.

$$2Cl^{-} = Cl_{2}(g) + 2e^{-}$$

$$2H_{2}O = 4H^{+} + O_{2}(g) + 4e^{-}$$
(1)

One challenge in developing this method of cancer treatment is in predicting the doses required for tumor destruction. One possible tool for dose planning is by modeling the reactions that take place close to the electrodes.

This example presents a first simple model for the development of dose-planning methods. More advanced models for dose planning, including secondary effects of chlorine, are found in Ref. 1, which also presents and solves models for the cathode.

## Model Definition

This model uses the Tertiary Current Distribution, Nernst-Planck interface to predict the transport and reaction in the electrolysis of tumor tissue in a liver. A needle electrode is placed in the tumor, and transport is assumed to take place radially to and from this electrode. Because you can assume rotational symmetry, the computational domain reduces to a line  $(r_a, r_r)$  where  $r_a$  is 1 mm and  $r_r$  is 6 cm (see Figure 1).

The species you consider in the model are the protons, chloride, and sodium. At the surface of the anode you account for the chlorine and oxygen evolution reactions; see Equation 1.

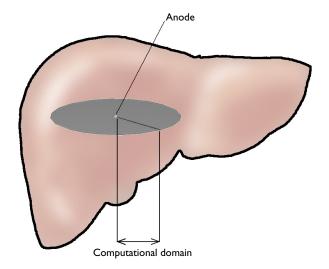


Figure 1: Diagram of the cylindrical modeling domain inside a tumor.

This simplified model considers only a 1D model of the transport between two points, that is, between the two electrodes. The material balance for the species i is given by

$$\frac{\partial c_i}{\partial t} + \nabla \cdot (-D_i \nabla c_i - z_i u_{\text{m}i} F c_i \nabla \phi_l) = R_i$$

where  $c_i$  is the concentration (SI unit: mol/m³),  $D_i$  give the diffusivities (SI unit: m²/s),  $z_i$  equals the charge,  $u_{mi}$  represents the mobility (SI unit: (mol·m²)/(J·s)), and  $R_i$  is the production term for species i (SI unit: mol/(m³·s)), F denotes Faraday's constant (SI unit: C/mol), and  $\phi_l$  is the electrolyte potential (SI unit: V). The mobility,  $u_{mi}$ , can be expressed in terms of  $D_i$ , R, and T as

$$u_{\mathrm{m}i} = \frac{D_i}{RT}$$

The conservation of electric charge is obtained through the divergence of the current density:

$$\nabla \cdot \left( F \sum_{i} z_{i}^{2} (-D_{i} \nabla c_{i} - z_{i} u_{mi} F c_{i} \nabla \phi_{l}) \right) = 0$$

At the electrode surface  $(r = r_a)$  you use the Electrode Surface boundary node to specify the electrode reactions and the resulting fluxes for the ionic species that are included in the electrode reactions, H<sup>+</sup> and Cl<sup>-</sup>. For the inert ionic species, Na<sup>+</sup>, the transport through the electrode surface equals zero. The expressions for molar fluxes at the boundary are based on the electrode reaction currents according to

$$\mathbf{N}_i \cdot \mathbf{n} = \sum_j \frac{\mathbf{v}_{ij} j_j}{n_j F}$$

where  $N_i$  is the flux,  $v_{ij}$  represents the stoichiometric coefficient for the ionic species i in reaction j, and  $n_j$  is the number of electrons in reaction j.

You can express the current densities for the two reactions using the Electrode Reaction nodes. Introducing dimensionless pressure,  $P = p/p_b$ , and concentration,  $C = c/c_b$ , (where b denotes the reference concentration), the current density for the oxygen evolution is

$$j_{\rm I} = j_{\rm I,\,0} \left\{ e^{rac{F\eta_{
m I}}{2RT}} - (P_{
m O_2})^{1/4} C_{
m H^{-1}} e^{-rac{F\eta_{
m I}}{2RT}} 
ight\}$$

where  $j_{I0}$ , is the exchange current density (SI unit: A/m<sup>2</sup>) and  $\eta_I$  is the overpotential for the oxygen evolution reaction, defined as

$$\eta_{\rm I} = \phi_s - \phi_l - E_{\rm eq, I}$$

where  $E_{\rm eq,I}$  (SI unit: V) is the equilibrium potential for the oxygen evolution reaction.

Set the electrode potential to

$$\phi_s(t) = \left(0.4977 + 0.2567 \cdot \ln\left(100 + \frac{t}{1 \text{ s}}\right)\right) \text{ V}$$

where t denotes time.

The chlorine evolution reaction is similarly given by the expression

$$j_{\rm II} = j_{\rm II, \, 0} \left\{ C_{\rm Cl^-} e^{\frac{F \eta_{\rm II}}{2RT}} - (P_{\rm Cl_2})^{1/2} e^{-\frac{F \eta_{\rm II}}{2RT}} \right\}$$

Using the input values  $n_{\rm I} = n_{\rm II} = 1$ ,  $v_{\rm H,I} = -1$ , and  $v_{\rm Cl,II} = 1$ , gives the fluxes at the electrode surface:

$$N_{\rm H} \cdot \mathbf{n} = \frac{-j_{\rm I}}{F}$$

$$N_{\rm Cl} \cdot \mathbf{n} = -\frac{j_{\rm II}}{F}$$

At the exterior boundary, assume the concentration is constant,  $c_i = c_{i0}$ , and ground the electrolyte potential.

The initial concentration is constant:  $c_i = c_{i0}$ .

#### Results and Discussion

The plot in Figure 2 shows the pH for different time steps. You can see that values below pH 2 are reached somewhere between 1800 and 2400 s. A closer examination reveals that

it occurs after 2000 s. At this pH, tumor destruction starts to occur very rapidly according to the experimental and theoretical findings in Ref. 1.

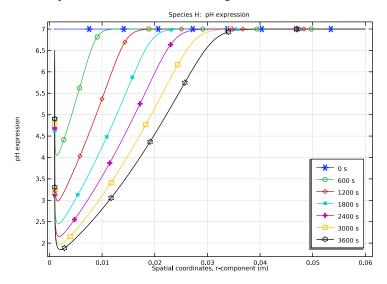


Figure 2: pH-profiles at different time steps during the treatment.

The corresponding H<sup>+</sup> profile in Figure 3 shows that the concentration maximum is not at the anode surface.

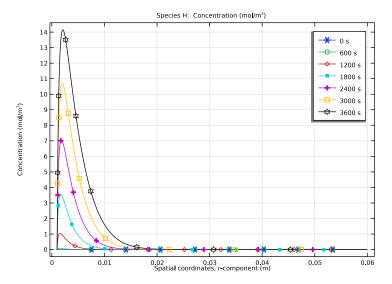


Figure 3: Proton concentration in the domain at different time steps.

This result arises because the current density is not constant over time. At high current densities, large amounts of protons are produced and this front moves inward in the domain as the current density is lowered.

The corresponding plot for chloride (Figure 4) shows a continuous decrease of chloride concentration close to the anode surface. This in turn decreases the production of chlorine and increases oxygen evolution.

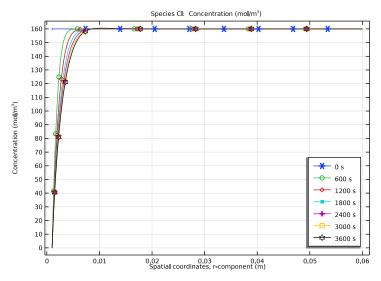


Figure 4: Chloride concentration at different time steps.

The current-density plot in Figure 5 shows that the total current decreases rapidly as the concentration overvoltage for chlorine formation increases, due to lowered chloride

concentration at the anode surface. The potential is then increased, which results in an increase in total current through increased oxygen evolution.

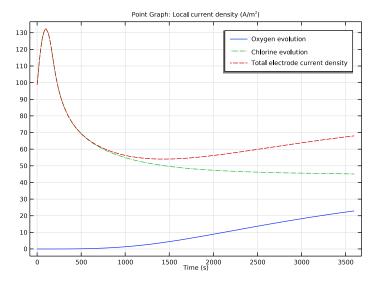


Figure 5: Total current density and current density for the competing reactions on the anode surface. Oxygen evolution is the lowest graph.

## Reference

1. E. Nilsson, Modelling of the Electrochemical Treatment of Tumors, PhD. thesis, Dept. Chemical Engineering and Technology, Royal Inst. of Technology, Stockholm, Sweden, 2000.

## Application Library path: Electrochemistry\_Module/

Electrochemical Engineering/tumor

## Modeling Instructions

From the File menu, choose New.

#### NEW

In the New window, click Model Wizard.

#### MODEL WIZARD

- I In the Model Wizard window, click ID Axisymmetric.
- 2 In the Select Physics tree, select Electrochemistry>Tertiary Current Distribution, Nernst-Planck>Tertiary, Electroneutrality (tcd).
- 3 Click Add.
- 4 In the Number of species text field, type 3.
- 5 In the Concentrations (mol/m³) table, enter the following settings:

Na Н Cl

- 6 Click Study.
- 7 In the Select Study tree, select General Studies>Time Dependent.
- 8 Click Done.

#### **GLOBAL DEFINITIONS**

Start by loading the model parameters and variables from text files.

#### Parameters 1

- I In the Model Builder window, under Global Definitions click Parameters I.
- 2 In the Settings window for Parameters, locate the Parameters section.
- 3 Click Load from File.
- 4 Browse to the model's Application Libraries folder and double-click the file tumor\_parameters.txt.

#### DEFINITIONS

#### Variables 1

- I In the Home toolbar, click a= Variables and choose Local Variables.
- 2 In the Settings window for Variables, locate the Variables section.
- 3 Click Load from File.
- 4 Browse to the model's Application Libraries folder and double-click the file tumor\_variables.txt.

#### GEOMETRY I

Create the geometry as a single interval.

#### Interval I (iI)

- I In the Model Builder window, under Component I (compl) right-click Geometry I and choose Interval.
- 2 In the Settings window for Interval, locate the Interval section.
- **3** In the table, enter the following settings:

Coordinates (m)			
r_a			
r_ext			

- 4 Click Build Selected.
- 5 Click the Zoom Extents button in the Graphics toolbar.

#### TERTIARY CURRENT DISTRIBUTION, NERNST-PLANCK (TCD)

Now start with the physics, begin with the electrolyte settings.

#### Species Charges 1

- I In the Model Builder window, under Component I (compl)>Tertiary Current Distribution, Nernst-Planck (tcd) click Species Charges I.
- 2 In the Settings window for Species Charges, locate the Charge section.
- 3 In the  $z_{\text{Na}}$  text field, type z\_Na.
- 4 In the  $z_H$  text field, type  $z_H$ .
- **5** In the  $z_{Cl}$  text field, type z\_C1.

#### Electrolyte I

- I In the Model Builder window, click Electrolyte I.
- 2 In the Settings window for Electrolyte, locate the Diffusion section.
- 3 In the  $D_{\text{Na}}$  text field, type D\_Na.
- **4** In the  $D_{\rm H}$  text field, type D\_H.
- **5** In the  $D_{\rm Cl}$  text field, type D\_C1.

#### Electrolyte Potential I

Now ground the potential of the exterior end, and then define the concentration at the same location.

- I In the Physics toolbar, click Boundaries and choose Electrolyte Potential.
- 2 Select Boundary 2 only.

#### Concentration 1

- I In the Physics toolbar, click Boundaries and choose Concentration.
- **2** Select Boundary 2 only.
- 3 In the Settings window for Concentration, locate the Concentration section.
- **4** Select the **Species H** check box.
- **5** In the  $c_{0,H}$  text field, type H0.
- **6** Select the **Species CI** check box.
- **7** In the  $c_{0,\text{Cl}}$  text field, type C10.

#### Electrode Surface I

Now set up the anode, and the anode reactions.

- I In the Physics toolbar, click Boundaries and choose Electrode Surface.
- 2 Select Boundary 1 only.
- 3 In the Settings window for Electrode Surface, locate the **Electrode Phase Potential Condition** section.
- 4 In the  $\phi_{s,ext}$  text field, type E\_cell.

#### Electrode Reaction I

- I In the Model Builder window, click Electrode Reaction I.
- 2 In the Settings window for Electrode Reaction, locate the Stoichiometric Coefficients section.
- 3 In the  $v_H$  text field, type -1.
- **4** Locate the **Equilibrium Potential** section. In the  $E_{\rm eq,ref}(T)$  text field, type E\_eqI.
- 5 Click to expand the **Reference Concentrations** section. In the table, enter the following settings:

Electrolyte species	Reference concentrations (mol/m^3)	
Н	но	

**6** Locate the **Electrode Kinetics** section. In the  $i_{0,ref}(T)$  text field, type j\_I0.

#### Electrode Surface 1

In the Model Builder window, click Electrode Surface 1.

#### Electrode Reaction 2

I In the Physics toolbar, click — Attributes and choose Electrode Reaction.

- 2 In the Settings window for Electrode Reaction, locate the Stoichiometric Coefficients section.
- 3 In the  $v_{Cl}$  text field, type 1.
- **4** Locate the **Equilibrium Potential** section. In the  $E_{\text{eq.ref}}(T)$  text field, type **E\_eqII**.
- **5** Locate the **Reference Concentrations** section. In the table, enter the following settings:

Electrolyte species	Reference concentrations (mol/m^3)	
CI	C10	

**6** Locate the **Electrode Kinetics** section. In the  $i_{0,ref}(T)$  text field, type j\_II0.

#### Initial Values 1

- I In the Model Builder window, under Component I (compl)>Tertiary Current Distribution, Nernst-Planck (tcd) click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- 3 In the H text field, type H0.
- **4** In the Cl text field, type C10.

#### **GLOBAL DEFINITIONS**

#### Default Model Inputs

Set up the temperature value used in the entire model.

- I In the Model Builder window, under Global Definitions click Default Model Inputs.
- 2 In the Settings window for Default Model Inputs, locate the Browse Model Inputs section.
- 3 In the tree, select General>Temperature (K) minput.T.
- 4 Find the Expression for remaining selection subsection. In the Temperature text field, type T.

#### MESH I

Create a user defined mesh with a very fine resolution close to the anode.

- I In the Model Builder window, under Component I (compl) click Mesh I.
- 2 In the Settings window for Mesh, locate the Sequence Type section.
- **3** From the list, choose **User-controlled mesh**.

#### Size

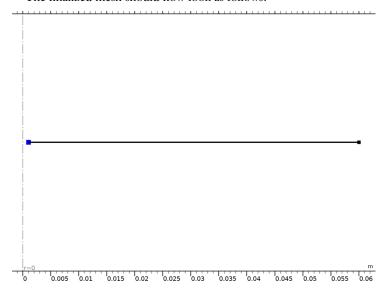
- I In the Model Builder window, under Component I (compl)>Mesh I click Size.
- 2 In the Settings window for Size, locate the Element Size section.

3 From the Predefined list, choose Extra fine.

Size 1

- I In the Model Builder window, right-click Edge I and choose Size.
- 2 In the Settings window for Size, locate the Geometric Entity Selection section.
- 3 From the Geometric entity level list, choose Boundary.
- 4 Select Boundary 1 only.
- **5** Locate the **Element Size** section. Click the **Custom** button.
- **6** Locate the **Element Size Parameters** section.
- 7 Select the Maximum element size check box. In the associated text field, type 1e-8.
- **8** Select the **Maximum element growth rate** check box. In the associated text field, type 1.1.
- 9 Click **Build All**.

The finalized mesh should now look as follows:



#### STUDY I

Step 1: Time Dependent

Modify the default solver to store all steps taken by the solver, and solve the problem.

- I In the Model Builder window, under Study I click Step I: Time Dependent.
- 2 In the Settings window for Time Dependent, locate the Study Settings section.

3 In the Output times text field, type 0 3600.

Solution I (soll)

- I In the **Study** toolbar, click **Show Default Solver**.

  Store the actual steps taken by the solver to avoid interpolation issues in the stored solution.
- 2 In the Model Builder window, expand the Solution I (soll) node, then click Time-Dependent Solver I.
- 3 In the Settings window for Time-Dependent Solver, locate the General section.
- 4 From the Times to store list, choose Steps taken by solver.
- 5 In the Study toolbar, click **Compute**.

#### RESULTS

Concentration, H (tcd)

The following instructions show how to create the plots shown in Figure 3 to Figure 5.

- I In the Model Builder window, under Results click Concentration, H (tcd).
- 2 In the Settings window for ID Plot Group, locate the Data section.
- **3** From the **Time selection** list, choose **Interpolated**.
- 4 In the Times (s) text field, type range (0,600,3600).

Line Graph I

- I In the Model Builder window, expand the Concentration, H (tcd) node, then click Line Graph 1.
- 2 In the Settings window for Line Graph, click to expand the Legends section.
- 3 Select the Show legends check box.
- 4 Click to expand the Coloring and Style section. Find the Line markers subsection. From the Marker list, choose Cycle.
- 5 From the Positioning list, choose Interpolated.
- 6 In the Concentration, H (tcd) toolbar, click  **Plot**.

Compare the plot with that shown in Figure 3.

Concentration, CI (tcd)

- I In the Model Builder window, under Results click Concentration, CI (tcd).
- 2 In the Settings window for ID Plot Group, locate the Data section.
- 3 From the Time selection list, choose Interpolated.

- 4 In the Times (s) text field, type range (0,600,3600).
- 5 Locate the Legend section. From the Position list, choose Lower right.

#### Line Graph 1

- I In the Model Builder window, expand the Concentration, CI (tcd) node, then click Line Graph 1.
- 2 In the Settings window for Line Graph, locate the Legends section.
- **3** Select the **Show legends** check box.
- 4 Locate the Coloring and Style section. Find the Line markers subsection. From the Marker list, choose Cycle.
- 5 From the Positioning list, choose Interpolated.
- 6 In the Concentration, CI (tcd) toolbar, click Plot. Compare with the plot in Figure 4.

#### Concentration. H (tcd)

In the Model Builder window, under Results right-click Concentration, H (tcd) and choose Duplicate.

#### bН

- I In the Model Builder window, under Results click Concentration, H (tcd) I.
- 2 In the Settings window for ID Plot Group, type pH in the Label text field.
- 3 Locate the Legend section. From the Position list, choose Lower right.

#### Line Graph 1

- I In the Model Builder window, expand the pH node, then click Line Graph I.
- 2 In the Settings window for Line Graph, locate the y-Axis Data section.
- **3** In the **Expression** text field, type pH.
- 4 In the pH toolbar, click Plot. The plot should look like that in Figure 2.

#### Electrode reaction current densities

- I In the Home toolbar, click **Add Plot Group** and choose ID Plot Group. Finally, reproduce the plot shown in Figure 5.
- 2 In the Settings window for ID Plot Group, type Electrode reaction current densities in the Label text field.

#### Point Graph 1

I Right-click Electrode reaction current densities and choose Point Graph.

- 2 Select Boundary 1 only.
- 3 In the Settings window for Point Graph, click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)> Tertiary Current Distribution, Nernst-Planck>Electrode kinetics>tcd.iloc\_erl Local current density A/m².
- 4 Click to expand the **Legends** section. Select the **Show legends** check box.
- 5 From the Legends list, choose Manual.
- **6** In the table, enter the following settings:

# Legends Oxygen evolution

7 Right-click Point Graph I and choose Duplicate.

#### Point Graph 2

- I In the Model Builder window, click Point Graph 2.
- 2 In the Settings window for Point Graph, locate the y-Axis Data section.
- **3** In the **Expression** text field, type tcd.iloc\_er2.
- 4 Click to expand the **Title** section. From the **Title type** list, choose **None**.
- 5 Click to expand the Coloring and Style section. Find the Line style subsection. From the Line list, choose Dash-dot.
- **6** Locate the **Legends** section. In the table, enter the following settings:

Legends	
Chlorine	evolution

- 7 In the Electrode reaction current densities toolbar, click **Tool** Plot.
- 8 Right-click Point Graph 2 and choose Duplicate.

#### Point Graph 3

- I In the Model Builder window, click Point Graph 3.
- 2 In the Settings window for Point Graph, click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)> Tertiary Current Distribution, Nernst-Planck>Electrode kinetics>tcd.itot Total interface current density A/m².
- **3** Locate the **Coloring and Style** section. Find the **Line style** subsection. From the **Line** list, choose **Dashed**.

**4** Locate the **Legends** section. In the table, enter the following settings:

Legend	ls			
Total	electrode	current	density	

Concentrations, All Species (tcd)

In the Model Builder window, under Results right-click Concentrations, All Species (tcd) and choose Delete.