

Chemical Vapor Deposition of GaAs

This example illustrates the modeling of a reactor for chemical vapor deposition (CVD). CVD is an important process for the electronics industry in which a thin film is grown on a substrate by allowing molecules and molecular fragments to adsorb and react on a surface. Combining detailed chemical reaction kinetics with transport models of a CVD reactor allows for realistic modeling of the deposition process. Such simulations in turn minimize the large number of expensive and time-consuming trial runs typically required for a reactor design.

In the CVD process described here, triethyl-gallium $(Ga(C_2H_5)_3)$ first decomposes into a gas phase. The reaction products, along with arsine (AsH₃), then adsorb and react on a substrate to form GaAs layers. The CVD system is modeled using momentum, energy, and mass balances including a detailed description of the gas phase and adsorption kinetics (Ref. 1).

The model highlights the usability of the Reaction Engineering and Chemistry interfaces together with the Reversible Reaction Group feature for simulation of reaction/transport systems in well-mixed (0D) and space-dependent reactors.

In the Reaction Engineering interface you can easily study the transient behavior of different sets of reactions in a perfectly mixed system. The Chemistry interface collects reaction kinetics and calculates transport and thermal parameters, which can seamlessly be coupled with other interfaces. In this application, you also utilize the Reversible Reaction Group feature for CHEMKIN import and organization of the complex system of bulk and surface reactions that are involved in the CVD process. The space-dependent reactor model accounts for mass transport, heat transfer, and fluid flow in the CVD reactor using the Transport of Diluted Species, Heat Transfer in Fluids, and Laminar Flow interfaces.

Model Definition

CHEMISTRY

In this model, the reaction kinetics together with most species transport and thermal properties are imported from CHEMKIN files using the Reversible Reactions Group feature available in either the Reaction Engineering or Chemistry interface. The CHEMKIN reaction kinetics file includes the following reactions making up the CVD process.

I The gas phase decomposition of $Ga(C_2H_5)_3$:

$$Ga(C_2H_5)_3 \xrightarrow{k_1} Ga(C_2H_5)_2 + C_2H_5^{\bullet}$$
 (1)

$$Ga(C_2H_5)_2 \xrightarrow{k_2} Ga(C_2H_5)H + C_2H_4$$
 (2)

$$Ga(C_2H_5)H \xrightarrow{k_3} GaH_2 + C_2H_4$$
 (3)

2 Gas phase radical reactions:

$$C_2H_5^{\bullet} + H_2 \xrightarrow{k_4^f} C_2H_6 + H^{\bullet}$$
 (4)

$$C_2H_5^{\bullet} + H^{\bullet} \xrightarrow{k_5} 2CH_3^{\bullet}$$
 (5)

$$CH_3^{\bullet} + H_2 \xrightarrow{k_6} CH_4 + H^{\bullet}$$
 (6)

$$2CH_3 \xrightarrow{k_7} C_2H_6 \tag{7}$$

$$C_2H_4 + H^{\bullet} \xrightarrow{k_8} C_2H_5^{\bullet}$$
 (8)

$$2H^{\bullet} + H_2 \xrightarrow{k_9} 2H_2$$
 (9)

3 Growth of GaAs at the surface by the adsorption of gas phase species and the subsequent reaction of the surface-bonded molecular fragments. These surface reactions involve the Ga and As species. S_A and S_G represent surface sites, corresponding to dangling bonds of As or Ga atoms, respectively.

$$Ga(C_2H_5)_3 + S_A \xrightarrow{k_{10}} GaC_2H_5^* + 2C_2H_5^*$$
 (10)

$$Ga(C_2H_5)H + S_A = \frac{k_{11}^f}{k_{11}^r} - Ga(C_2H_5)H^*$$
 (11)

$$GaH_2 + S_A \xrightarrow{k_{12}} Ga^* + 2H^{\bullet}$$
 (12)

$$Ga(C_2H_5)H^* \xrightarrow{k_{13}} Ga^* + C_2H_5^{\bullet} + H^{\bullet}$$
 (13)

$$AsH_3 + S_G \xrightarrow{k_{14}} As^* + 3H^{\bullet}$$
 (14)

4 Surface reactions of carbon and hydrogen fragments:

$$C_2H_5^{\bullet} + S_A = \frac{k_{15}^f}{k_{15}^r} - C_2H_{5A}^{\star}$$
 (15)

$$C_2H_5^{\bullet} + S_G = \frac{k_{16}^f}{k_{16}^r} - C_2H_{5G}^{\star}$$
 (16)

$$C_2H_{5A}^* \xrightarrow{k_{17}} H_A^* + C_2H_4$$
 (17)

$$C_2H_{5G}^* \xrightarrow{k_{18}} H_{G}^* + C_2H_4$$
 (18)

$$H_A^* \xrightarrow{k_{19}} S_A + H^{\bullet}$$
 (19)

$$H_G^* \xrightarrow{k_{20}} S_G + H^{\bullet}$$
 (20)

5 Surface reactions leading to GaAs growth:

$$GaC_2H_5^* + As^* \xrightarrow{k_{21}} GaAs + C_2H_5^* + S_A + S_G$$
 (21)

$$Ga^* + As^* \xrightarrow{k_{22}} GaAs + S_A + S_G$$
 (22)

The reaction rates (SI unit: mol/(m³·s)) corresponding to the chemistry just described involve the mass action law

$$r_j = k_j^f \prod_{i \in \text{react}} c_i^{-v_j} - k_j^r \prod_{i \in \text{prod}} c_i^{v_{ij}}$$

Here, k_j^f and k_j^r denote the forward and reverse rate constants, respectively. The concentration of species i is denoted c_i (SI unit: mol/m³). The stoichiometric coefficients are denoted v_{ij} , and are defined as negative for reactants and positive for products. The temperature dependence of the reaction rates is included through Arrhenius expressions for the rate constants:

$$k = AT^n \exp\left(-\frac{E}{R_g T}\right)$$

In this equation, A denotes the frequency factor, T the temperature (K), n the temperature exponent, E the activation energy (SI unit: J/mol), and R_g the ideal gas constant, 8.314 J/(mol·K). The frequency factor is expressed in the units $(m^3/\text{mol})^{\alpha-1}/\text{s}$, where α is the order of the reaction.

With the CHEMKIN import, the chemical species automatically adapts the following labels, where _1(ads) indicates adsorbed surface species and _Ga_ indicates adsorption at gallium (Ga) sites instead of the more common arsenic (As) sites Figure 1.

$Ga(C_2H_5)_3\\$	GaC6H15	C_2H_6	C2H6
$Ga(C_2H_5)_2$	GaC4HI0	C_2H_5	C2H5
$Ga(C_2H_5)H\\$	GaC2H6	C_2H_4	C2H4
GaH_2	GaH2	CH ₄	CH4
$\text{Ga}(\text{C}_2\text{H}_5)\text{H*}$	GaC2H6_I (ads)	CH₃ •	CH3
GaC ₂ H ₅ *	GaC2H5_I (ads)	H_2	H2
Ga*	Ga_I (ads)	н •	н
AsH ₃	AsH3_I (ads)	C_2H_5*	C2H5_I(ads), C2H5_Ga_I(ads)
As*	As_I (ads)	H*	H_I(ads), H_Ga_I(ads)
GaAs	GaAs		

Figure 1: Species labels used in the model.

MODEL ANALYSIS

The analysis follows these steps: First, study of the reaction kinetics in an ideal batch reactor using the Reaction Engineering interface. Afterward, setup of a space-dependent

model with the following interfaces to investigate the effects of momentum, heat, and mass transport within the system:

- Chemistry
- Transport of Diluted Species
- Heat Transfer in Fluids
- Laminar Flow

Figure 2 shows the CVD reactor model geometry. The reactor is 40 cm long and 10 cm high. Located in the center is the substrate, 5 cm across and tilted 10° with respect to the vertical position. Gas enters the reactor at the inlet with a velocity of 0.4 m/s and at a pressure of 4000 Pa.

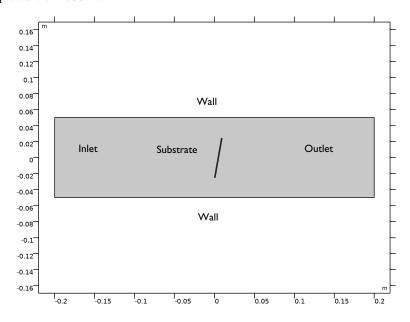


Figure 2: The modeling domain consists of the CVD reactor and the substrate surface.

Results and Discussion

As noted, the first step in the modeling process is to enter the complete set of gas phase reactions, Equation 1 to Equation 9, into the Reaction Engineering interface for analysis. Figure 3 shows the species concentrations as functions of time in a perfectly mixed batch reactor kept at 900 K.

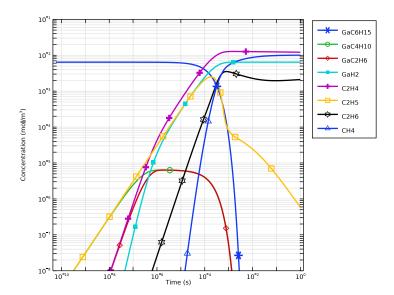


Figure 3: The complete set of gas phase reactions including decomposition reactions of gallium species as well as radical reactions. The chemistry occurs in a perfectly mixed batch reactor held at 900 K. Radical species are not shown in the graph.

As a test, omit the radical reactions given by Equation 4 to Equation 9 from the set of gas phase reactions. Once again analyze the kinetics of the reactions describing gallium species decomposition (Equation 1 to Equation 3) at 900 K. The results appear in Figure 4.

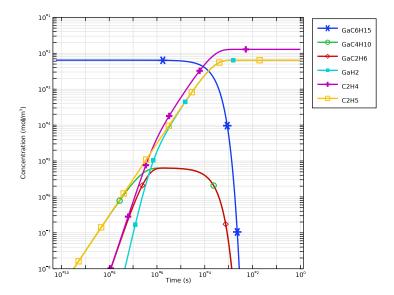


Figure 4: A reduced set of gas phase reactions including only the decomposition reactions of gallium species. Reactions occur in a perfectly mixed system held at 900 K.

Reducing the gas phase reaction set does not affect the reactions of the gallium species. However, excluding the radical reactions has a considerable influence on the carbonspecies distribution. For the reduced reaction set, ethene and ethyl radicals are the main carbon products; for the full reaction set the main products are ethene and methane. The various species have different characteristics with respect to surface adsorption and reaction. Furthermore, the net concentration of carbon species is higher for the full reaction set. Both these factors can significantly influence the growth of surface layers. For a first study of geometrical effects on the reacting system, you can bring the reduced reaction model into the actual geometry of the CVD reactor and then solve the spacedependent problem.

The first results from the space-dependent model are displayed below. Figure 5 shows the fluid velocity and Figure 6 the temperature distribution in the reactor domain. The gas mixture enters the reactor with a velocity of 0.4 m/s and a temperature of 300 K with the substrate held at a constant temperature of 900 K. Notice the large effect that the heating plate has on the temperature and the expansion this causes in the fluid. This effect is seen in the average velocity, which increases downstream after the position of the substrate.

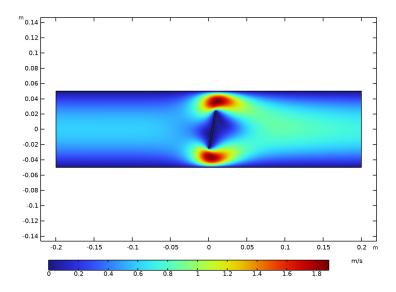


Figure 5: The gas phase velocity in the reactor domain.

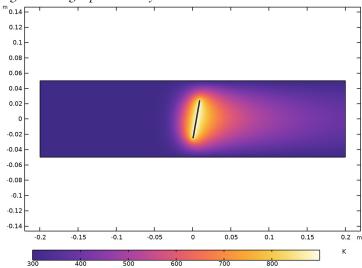


Figure 6: The temperature distribution in the reactor domain.

Figure 7 shows the concentration distribution of the triethyl-gallium species in the reactor domain, while Figure 8 displays the concentration profile along the reactor centerline for

triethyl-gallium together with that of the final product gallium hydride. Triethyl-gallium is stable at the inlet temperature (300 K) and then rapidly decomposes near the hot substrate.

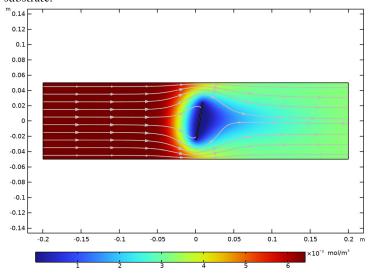


Figure 7: Concentration distribution of triethyl-gallium in the reactor domain.

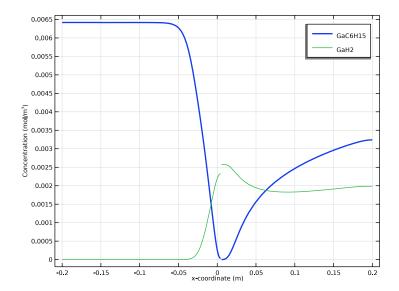


Figure 8: Concentration profiles of triethyl-gallium (blue line) and gallium hydride (green line) along the reactor centerline.

Figure 9 shows the arsine concentration change along the reactor centerline. This species does not decompose in the gas phase. The decrease in concentration at the substrate surface (at the 0 length coordinate) is due to the adsorption of arsine at the surface.

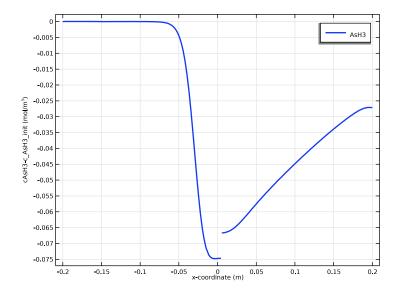


Figure 9: Composition change of arsine along the reactor centerline. Arsine is adsorbed at the substrate surface, which is located at the center of the length scale.

Figure 10 and Figure 11 depict a few of the transport properties calculated in the Chemistry node which are coupled to the physics interfaces of the space-dependent model. Figure 10 shows the diffusivity of triethyl-gallium (bottom) and arsine (top). Figure 11 shows the thermal conductivity of the hydrogen carrier gas. All variables are plotted as functions of temperature.

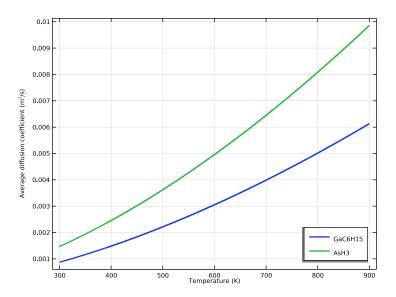


Figure 10: The diffusivities of triethyl-gallium (bottom) and arsine (top) as functions of temperature.

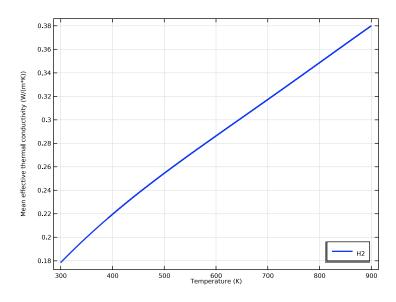


Figure 11: The thermal conductivity of the hydrogen carrier gas.

1. N.K. Ingle, C. Theodoropoulos, T.J. Mountziaris, R.M. Wexler, and F.T.J. Smith, "Reaction kinetics and transport phenomena underlying the low-pressure metalorganic chemical vapor deposition of GaAs", J. Crystal Growth, vol. 167, pp. 543-556, 1996.

Application Library path: Chemical_Reaction_Engineering_Module/ Reactors with Mass and Heat Transfer/gaas cvd

Modeling Instructions

From the File menu, choose New.

NEW

In the New window, click Model Wizard.

MODEL WIZARD

- I In the Model Wizard window, click 0D.
- 2 In the Select Physics tree, select Chemical Species Transport>Reaction Engineering (re).
- 3 Click Add.
- 4 Click 🔵 Study.
- 5 In the Select Study tree, select General Studies>Time Dependent.
- 6 Click **Done**.

GLOBAL DEFINITIONS

Load the model parameters from a text file.

Parameters 1

- I In the Model Builder window, under Global Definitions click Parameters I.
- 2 In the Settings window for Parameters, locate the Parameters section.
- 3 Click Load from File.
- 4 Browse to the model's Application Libraries folder and double-click the file gaas_cvd_parameters.txt.

The 25 reactions describing the GaAs vapor deposition are available in a kinetics CHEMKIN file. Both bulk and surface reactions are present in this process.

REACTION ENGINEERING - GAS PHASE REACTIONS, FULL SET (RE)

Use the Reversible Reaction Group to import the kinetics CHEMKIN file.

- I In the Model Builder window, under Component I (compl) click Reaction Engineering (re).
- 2 In the Settings window for Reaction Engineering, type Reaction Engineering Gas Phase Reactions, Full Set (re) in the Label text field.

Reversible Reaction Group 1

- I In the Reaction Engineering toolbar, click 🚣 Reversible Reaction Group.
- 2 In the Settings window for Reversible Reaction Group, click to expand the **CHEMKIN Import for Kinetics** section.
- 3 Select the Import CHEMKIN data check box.
- 4 Click Browse.
- **5** Browse to the model's Application Libraries folder and double-click the file gaas cvd reaction kinetics.txt.
- 6 Click THI Import.

Delete the imported solid species C because it neither takes part in any reactions nor behaviors as third body.

Species: C

In the Model Builder window, right-click Species: C and choose Delete.

Species Group 1

First, investigate the bulk reactions at 900 K.

- I In the Model Builder window, expand the Component I (compl)>Reaction Engineering -Gas Phase Reactions, Full Set (re) (re)>Species Group I node, then click Component I (compl)>Reaction Engineering - Gas Phase Reactions, Full Set (re) (re).
- 2 In the Settings window for Reaction Engineering, locate the Energy Balance section.
- 3 In the T text field, type 900[K].

Remove the imported reactions associated with surface reactions and move reaction 9 to the model builder tree.

Reversible Reaction Group 1

- I In the Model Builder window, click Reversible Reaction Group I.
- 2 In the Settings window for Reversible Reaction Group, locate the **CHEMKIN Import for Kinetics** section.
- 3 Clear the Import CHEMKIN data check box.

- 4 Click to expand the Move Reaction and Species section. In the Move reaction (with the number) from table text field, type 9.
- 5 In the Move reaction (with the number) from table text field, type 9.

Remove reactions 10 to 25 from the Reaction table by clicking the Delete button.

Reaction 9 contains H2 which is the solvent in this process. When moving the reaction from the table a separate feature for the species H2 is created. This can now be accessed and set as solvent.

Species: H2

- I In the Model Builder window, click Species: H2.
- 2 In the Settings window for Species, locate the Type section.
- **3** From the list, choose **Solvent**.

Initial Values 1

Initially, only GaC6H15 and H2 exist in the reactor.

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Volumetric Species Initial Values section.
- **3** In the table, enter the following settings:

Species	Concentration (mol/m^3)
GaC6H15	c_GaC6H15_init
H2	c_H2_init

STUDY (RE)

- I In the Model Builder window, click Study I.
- 2 In the Settings window for Study, type Study (re) in the Label text field.
- 3 In the Home toolbar, click **Compute**.

RESULTS

Gas Phase Concentrations, Full Set (re)

In the Settings window for ID Plot Group, type Gas Phase Concentrations, Full Set (re) in the Label text field.

Global I

Select the species concentrations that are plotted in Figure 3.

- I In the Model Builder window, expand the Gas Phase Concentrations, Full Set (re) node, then click Global I.
- 2 In the Settings window for Global, click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)> Reaction Engineering - Gas Phase Reactions, Full Set (re)>re.c_GaC6HI5 - Concentration mol/m³.
- 3 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering - Gas Phase Reactions, Full Set (re)>re.c_GaC4H10 - Concentration - mol/m3.
- 4 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering - Gas Phase Reactions, Full Set (re)>re.c_GaC2H6 - Concentration - mol/m3.
- 5 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering - Gas Phase Reactions, Full Set (re)>re.c_GaH2 - Concentration - mol/m3.
- 6 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering - Gas Phase Reactions, Full Set (re)>re.c_C2H4 - Concentration - mol/m3.
- 7 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering - Gas Phase Reactions, Full Set (re)>re.c_C2H5 - Concentration - mol/m3.
- 8 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering - Gas Phase Reactions, Full Set (re)>re.c_C2H6 - Concentration - mol/m3.
- 9 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering - Gas Phase Reactions, Full Set (re)>re.c_CH4 - Concentration - mol/m3.
- 10 Click to expand the Coloring and Style section. From the Width list, choose 2.
- II Find the Line markers subsection. From the Marker list, choose Cycle.
- 12 From the Positioning list, choose Interpolated.
- 13 Click to expand the Legends section. From the Legends list, choose Manual.

14 In the table, enter the following settings:

Legends GaC6H15 GaC4H10 GaC2H6 GaH2 C2H4 C2H5 C2H6 CH4

I5 Click the **x-Axis Log Scale** button in the **Graphics** toolbar.

16 Click the **y-Axis Log Scale** button in the **Graphics** toolbar.

Gas Phase Concentrations, Full Set (re)

- I In the Model Builder window, click Gas Phase Concentrations, Full Set (re).
- 2 In the Settings window for ID Plot Group, click to expand the Title section.
- 3 From the Title type list, choose None.
- 4 Locate the Axis section. Select the Manual axis limits check box.
- 5 In the y minimum text field, type 1e-8.
- 6 In the y maximum text field, type 1e-1.
- 7 Locate the Legend section. From the Layout list, choose Outside graph axis area.
- 8 From the Position list, choose Right.

To reduce the model before simulating the process in a 2-dimensional model, study whether it is possible to remove the nongallium species and reactions and yet obtain approximately the same results.

To do so, modify the existing reaction model by first removing reactions of nongallium species from the Reversible Reaction Group. Then solve the mass balances and compare the results with the full reaction model.

REACTION ENGINEERING - GAS PHASE REACTIONS, FULL SET (RE) (RE) In the Model Builder window, under Component I (compl) right-click Reaction Engineering -Gas Phase Reactions, Full Set (re) (re) and choose Copy.

COMPONENT I (COMPI)

In the Model Builder window, right-click Component I (compl) and choose Paste Reaction Engineering.

REACTION ENGINEERING - GAS PHASE REACTIONS, REDUCED SET (RE2)

- I In the Messages from Paste dialog box, click OK.
- 2 In the Model Builder window, click Reaction Engineering Gas Phase Reactions, Full Set (re) 1 (re2).
- 3 In the Settings window for Reaction Engineering, type Reaction Engineering Gas Phase Reactions, Reduced Set (re2) in the Label text field.

Reversible Reaction Group 1

Remove reactions 4 to 8 from the **Reaction table** by clicking the **Delete** button.

$$1: 2 H + H2 => 2 H2$$

- I In the Model Builder window, expand the Component I (compl)>Reaction Engineering Gas Phase Reactions, Reduced Set (re2) (re2) node.
- 2 Right-click I: 2 H + H2 => 2 H2 and choose Disable.

ADD STUDY

- I In the Home toolbar, click Add Study to open the Add Study window.
- 2 Go to the Add Study window.
- 3 Find the Physics interfaces in study subsection. In the table, clear the Solve check box for Reaction Engineering Gas Phase Reactions, Full Set (re) (re).
- 4 Find the Studies subsection. In the Select Study tree, select General Studies>
 Time Dependent.
- 5 Click **Add Study** in the window toolbar.
- 6 In the Home toolbar, click Add Study to close the Add Study window.

STUDY (RE2)

- I In the Model Builder window, click Study 2.
- 2 In the Settings window for Study, type Study (re2) in the Label text field.
- 3 In the Home toolbar, click **Compute**.

RESULTS

Gas Phase Concentrations, Reduced Set (re2)

Select the species concentrations that are plotted in Figure 4.

I In the Settings window for ID Plot Group, type Gas Phase Concentrations, Reduced Set (re2) in the Label text field.

Global I

- I In the Model Builder window, expand the Gas Phase Concentrations, Reduced Set (re2) node, then click Global I.
- 2 In the Settings window for Global, click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)> Reaction Engineering - Gas Phase Reactions, Reduced Set (re2)>re2.c_GaC6HI5 -Concentration - mol/m³.
- 3 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering - Gas Phase Reactions, Reduced Set (re2)>re2.c_GaC4H10 - Concentration - mol/m3.
- 4 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering - Gas Phase Reactions, Reduced Set (re2)>re2.c_GaC2H6 - Concentration - mol/m3.
- 5 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering - Gas Phase Reactions, Reduced Set (re2)>re2.c_GaH2 - Concentration - mol/m³.
- 6 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering - Gas Phase Reactions, Reduced Set (re2)>re2.c_C2H4 - Concentration - mol/m3.
- 7 Click Add Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component I (compl)>Reaction Engineering - Gas Phase Reactions, Reduced Set (re2)>re2.c_C2H5 - Concentration - mol/m3.
- 8 Locate the Coloring and Style section. From the Width list, choose 2.
- 9 Find the Line markers subsection. From the Marker list, choose Cycle.
- 10 From the Positioning list, choose Interpolated.
- II Locate the Legends section. From the Legends list, choose Manual.
- **12** In the table, enter the following settings:

Legends	
GaC6H15	
GaC4H10	
GaC2H6	
GaH2	

Legends	
C2H4	
C2H5	
13 Click the	x-Axis Log Scale button in the Graphics toolbar.
14 Click the	y-Axis Log Scale button in the Graphics toolbar.

Gas Phase Concentrations, Reduced Set (re2)

- I In the Model Builder window, click Gas Phase Concentrations, Reduced Set (re2).
- 2 In the Settings window for ID Plot Group, locate the Title section.
- 3 From the Title type list, choose None.
- 4 Locate the Axis section. Select the Manual axis limits check box.
- **5** In the **y minimum** text field, type 1e-8.
- 6 In the y maximum text field, type 1e-1.
- 7 Locate the Legend section. From the Layout list, choose Outside graph axis area.
- 8 From the Position list, choose Right.
- 9 In the Gas Phase Concentrations, Reduced Set (re2) toolbar, click Plot.

A comparison of Figure 3 and Figure 4 reveals that the gallium-related reactions remain approximately the same. This means that you can go on to set up a space-dependent CVD model based on the reduced model instead of the one comprising all bulk species. Move on to the space-dependent model. This CVD model is in 2D and you set up the necessary reactions using the Chemistry interface and the Reversible Reaction Group feature. Mass transport, heat transfer, and fluid flow are accounted for with Transport of Diluted Species, Heat Transfer in Fluids, and Laminar Flow interfaces, respectively.

ADD COMPONENT

Right-click Results>Gas Phase Concentrations, Reduced Set (re2) and choose Add Component>2D.

First, draw the 2D geometry.

GEOMETRY I

Rectangle I (rI)

- I In the Geometry toolbar, click Rectangle.
- 2 In the Settings window for Rectangle, locate the Size and Shape section.
- 3 In the Width text field, type 0.4.

- 4 In the Height text field, type 0.1.
- 5 Locate the Position section. From the Base list, choose Center.
- 6 Click **P** Build Selected.

Rectangle 2 (r2)

- I In the Geometry toolbar, click Rectangle.
- 2 In the Settings window for Rectangle, locate the Position section.
- 3 In the y text field, type -0.025.
- 4 Locate the Size and Shape section. In the Width text field, type 1e-3.
- 5 In the **Height** text field, type 0.05.
- 6 Locate the Rotation Angle section. In the Rotation text field, type -10.
- 7 Click | Build Selected.

Difference I (dif1)

- I In the Geometry toolbar, click Booleans and Partitions and choose Difference.
- 2 Select the object rl only.
- 3 In the Settings window for Difference, locate the Difference section.
- 4 Click to clear the Activate Selection toggle button for Objects to add.
- 5 Click to select the Activate Selection toggle button for Objects to subtract.
- **6** Select the object **r2** only.

Form Union (fin)

In the Geometry toolbar, click **Build All**.

Select the Chemistry interface and the Reversible Reaction Group feature to set up all necessary reaction kinetics and define some species parameters.

ADD PHYSICS

- I In the Home toolbar, click open the Add Physics window.
- 2 Go to the Add Physics window.
- 3 In the tree, select Chemical Species Transport>Chemistry (chem).
- 4 Click Add to Component 2 in the window toolbar.
- 5 In the Home toolbar, click of Add Physics to close the Add Physics window.

CHEMISTRY (CHEM)

Reversible Reaction Group 1

I Right-click Component 2 (comp2)>Chemistry (chem) and choose Reversible Reaction Group.

Aside from CHEMKIN import of reaction kinetics, also use CHEMKIN import of transport and thermal properties. In this manner, several thermal and transport properties available in the **Chemistry** interface can be utilized in the other interfaces.

- 2 In the Settings window for Reversible Reaction Group, click to expand the **CHEMKIN Import for Kinetics** section.
- 3 Select the Import CHEMKIN data check box.
- 4 Click **Browse**.
- 5 Browse to the model's Application Libraries folder and double-click the file gaas_cvd_reaction_kinetics.txt.
- 6 Click | Import.

Species: C

- I In the Model Builder window, right-click Species: C and choose Delete.
- 2 In the Model Builder window, click Chemistry (chem).
- 3 In the Settings window for Chemistry, click to expand the Calculate Transport Properties section.

Species Group 1

- I In the Model Builder window, under Component 2 (comp2)>Chemistry (chem) click Species Group 1.
- 2 In the Settings window for Species Group, click to expand the CHEMKIN section.
- 3 Click **Browse**.
- **4** Browse to the model's Application Libraries folder and double-click the file gaas_cvd_transp.txt.
- 5 Click | Import.

Species Thermodynamics I

- I In the Model Builder window, expand the Species Group I node, then click Species Thermodynamics 1.
- 2 In the Settings window for Species Thermodynamics, click to expand the CHEMKIN Import for Thermodynamic Data section.
- 3 Click Browse.

- **4** Browse to the model's Application Libraries folder and double-click the file gaas cvd thermo.txt.
- 5 Click | Import.

Remove the bulk reactions that were considered redundant in the 0D model investigation of the system.

Reversible Reaction Group 1

- I In the Model Builder window, under Component 2 (comp2)>Chemistry (chem) click Reversible Reaction Group 1.
- 2 In the Settings window for Reversible Reaction Group, locate the **CHEMKIN Import for Kinetics** section.
- 3 Clear the Import CHEMKIN data check box.

Remove reactions 4 to 8 from the Reaction table by clicking the **Delete** button.

Continue with moving the reactions containing surface species to the model builder tree. This enables access to all surface species. Additionally, do the same with the hydrogen reaction (reaction 17).

- 4 Click to expand the Move Reaction and Species section. In the Move reaction (with the number) from table text field, type 9.
- 5 In the Move reaction (with the number) from table text field, type 9.
- 6 Click Create Reaction.

Repeat this with reactions 10 to 25.

Disable reaction 17 (Ga_1(ads)+As_Ga_1(ads)=>GaAs) and select H2 as solvent.

In the Model Builder window, right-click 17: Surface: Ga_I(ads) + As_Ga_I(ads) => GaAs and choose Disable.

Species: H2

- I In the Model Builder window, right-click Species: H2 and choose Enable.
- 2 In the Settings window for Species, locate the Type section.
- **3** From the list, choose **Solvent**.

The surface species concentrations are considered constant. To account for this, lock the concentrations for these.

Species: GaAs

I In the Model Builder window, click Species: GaAs.

- 2 In the Settings window for Species, click to expand the Constant Concentration/Activity section.
- 3 Select the Keep concentration/activity constant check box.

```
Repeat the same lock operation for GaC2H5 1 surf, GaC2H6 1 surf, Ga 1 surf,
As_Ga_1_surf, C2H5_1_surf, C2H5_Ga_1_surf, H_1_surf, and H_Ga_1_surf.
```

4 In the Model Builder window, collapse the Chemistry (chem) node.

COMPONENT 2 (COMP2)

Add a Transport of Diluted Species interface to model the mass transport of the bulk species diluted in solvent. When available, use the transport parameters from the **Chemistry** interface. Additionally, show the **Advanced physics option**. This is needed to choose the conservative form for the convective term in the mass transfer interface. The conservative form should be used for systems including convection and nonnegligible changes in density.

ADD PHYSICS

- I In the Physics toolbar, click Add Physics to open the Add Physics window.
- 2 Go to the Add Physics window.
- 3 In the tree, select Chemical Species Transport>Transport of Diluted Species (tds).
- 4 Click Add to Component 2 in the window toolbar.
- 5 In the Physics toolbar, click Add Physics to close the Add Physics window.
- 6 Click the Show More Options button in the Model Builder toolbar.
- 7 In the Show More Options dialog box, select Physics>Advanced Physics Options in the tree.
- 8 In the tree, select the check box for the node Physics>Advanced Physics Options.
- 9 Click OK.

TRANSPORT OF DILUTED SPECIES (TDS)

- I In the Settings window for Transport of Diluted Species, click to expand the Advanced Settings section.
- 2 From the Convective term list, choose Conservative form.
- 3 Click to expand the **Dependent Variables** section. In the **Number of species** text field, type 8.

4 In the Concentrations (mol/m³) table, enter the following settings:

cGaC4H10
cC2H5
сН
cC2H4
cAsH3
cGaH2
cGaC2H6
cGaC6H15

Set the constant (locked) concentrations in the **Chemistry** interface main node.

CHEMISTRY (CHEM)

- I In the Model Builder window, under Component 2 (comp2) click Chemistry (chem).
- 2 In the Settings window for Chemistry, locate the Species Matching section.
- 3 From the Species solved for list, choose Transport of Diluted Species.
- **4** Find the **Bulk species** subsection. In the table, enter the following settings:

Species	Туре	Molar concentration	Value (mol/m^3)
AsH3	Variable	cAsH3	Solved for
C2H4	Variable	cC2H4	Solved for
C2H5	Variable	cC2H5	Solved for
GaAs	Constant	User defined	0
GaC2H6	Variable	cGaC2H6	Solved for
GaC4H10	Variable	cGaC4H10	Solved for
GaC6H15	Variable	cGaC6H15	Solved for
GaH2	Variable	cGaH2	Solved for
Н	Variable	cH	Solved for
H2	Solvent	User defined	c_H2_init

5 Find the **Surface species** subsection. In the table, enter the following settings:

Species	Species concentration type	Surface concentration (mol/m^2)
As_Ga_I (ads)	Constant	c_Assurf_Ga
C2H5_I (ads)	Constant	c_C2H5surf

Species	Species concentration type	Surface concentration (mol/m^2)
C2H5_Ga_I (ads)	Constant	c_C2H5surf_Ga
GaC2H5_I (ads)	Constant	c_GaC2H5surf
GaC2H6_I (ads)	Constant	0
Ga_I (ads)	Constant	c_Gasurf
H_I (ads)	Constant	c_Hsurf
H_Ga_I (ads)	Constant	c_Hsurf_Ga

TRANSPORT OF DILUTED SPECIES (TDS)

Transport Properties 1

- In the Model Builder window, under Component 2 (comp2)>
 Transport of Diluted Species (tds) click Transport Properties 1.
- 2 In the Settings window for Transport Properties, locate the Diffusion section.
- **3** From the **Source** list, choose **Chemistry**.
- 4 From the $D_{cGaC4H10}$ list, choose Diffusion coefficient, GaC4H10 in H2 (solvent) (chem).
- 5 From the $D_{
 m cC2H5}$ list, choose Diffusion coefficient , C2H5 in H2 (solvent) (chem).
- 6 From the $D_{\rm cH}$ list, choose Diffusion coefficient , H in H2 (solvent) (chem).
- 7 From the $D_{\rm cC2H4}$ list, choose Diffusion coefficient, C2H4 in H2 (solvent) (chem).
- 8 From the D_{cAsH3} list, choose Diffusion coefficient , AsH3 in H2 (solvent) (chem).
- 9 From the D_{cGaH2} list, choose Diffusion coefficient, GaH2 in H2 (solvent) (chem).
- 10 From the $D_{\rm cGaC2H6}$ list, choose Diffusion coefficient, GaC2H6 in H2 (solvent) (chem).
- II From the $D_{\rm cGaC6H15}$ list, choose Diffusion coefficient , GaC6H15 in H2 (solvent) (chem).

Reactions 1

- I In the Physics toolbar, click **Domains** and choose Reactions.
- 2 In the Settings window for Reactions, locate the Domain Selection section.
- 3 From the Selection list, choose All domains.
- 4 Locate the Reaction Rates section. From the $R_{\rm cGaC4H10}$ list, choose Reaction rate for species GaC4H10 (chem).
- **5** From the $R_{\rm cC2H5}$ list, choose Reaction rate for species C2H5 (chem).
- 6 From the $R_{\rm cH}$ list, choose Reaction rate for species H (chem).
- 7 From the $R_{
 m cC2H4}$ list, choose Reaction rate for species C2H4 (chem).
- 8 From the R_{cAsH3} list, choose Reaction rate for species AsH3 (chem).

- 9 From the $R_{\rm cGaH2}$ list, choose Reaction rate for species GaH2 (chem).
- 10 From the $R_{\rm cGaC2H6}$ list, choose Reaction rate for species GaC2H6 (chem).
- II From the $R_{cGaC6H15}$ list, choose Reaction rate for species GaC6H15 (chem).

Surface Reactions 1

Create a Surface Reactions feature and apply it at the substrate surface. Then prescribe the surface reaction rates to model the deposition on the substrate.

- I In the Physics toolbar, click Boundaries and choose Surface Reactions.
- **2** Select Boundaries 4–7 only.
- 3 In the Settings window for Surface Reactions, locate the Surface Reaction Rate section.
- 4 From the $J_{0,{
 m cGaC4H10}}$ list, choose Surface reaction rate for species GaC4H10 (chem).
- 5 From the $J_{0,{
 m cC2H5}}$ list, choose Surface reaction rate for species C2H5 (chem).
- **6** From the $J_{0,\mathrm{cH}}$ list, choose Surface reaction rate for species H (chem).
- 7 From the $J_{0,cC2H4}$ list, choose Surface reaction rate for species C2H4 (chem).
- 8 From the $J_{0,cAsH3}$ list, choose Surface reaction rate for species AsH3 (chem).
- 9 From the $J_{0,{
 m cGaH2}}$ list, choose Surface reaction rate for species GaH2 (chem).
- 10 From the $J_{0,{
 m cGaC2H6}}$ list, choose Surface reaction rate for species GaC2H6 (chem).
- II From the $J_{0,{
 m cGaC6H15}}$ list, choose Surface reaction rate for species GaC6H15 (chem).

Inflow I

- I In the Physics toolbar, click Boundaries and choose Inflow.
- 2 Select Boundary 1 only.
- 3 In the Settings window for Inflow, locate the Concentration section.
- **4** In the $c_{0,{\rm cAsH3}}$ text field, type c_AsH3_in.
- **5** In the $c_{0.{
 m cGaC6H15}}$ text field, type c_GaC6H15_in.

Outflow I

- I In the Physics toolbar, click Boundaries and choose Outflow.
- 2 Select Boundary 8 only.

Initial Values 1

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- **3** In the cAsH3 text field, type c AsH3 in.
- **4** In the cGaC6H15 text field, type c GaC6H15 in.

COMPONENT 2 (COMP2)

Add a Heat Transfer in Fluids interface to model the heat transfer and heat generation in the reactor. When available, use the thermal parameters from the **Chemistry** interface.

ADD PHYSICS

- I In the Physics toolbar, click and Physics to open the Add Physics window.
- **2** Go to the **Add Physics** window.
- 3 In the tree, select Heat Transfer>Heat Transfer in Fluids (ht).
- 4 Click Add to Component 2 in the window toolbar.
- 5 In the Physics toolbar, click and Physics to close the Add Physics window.

HEAT TRANSFER IN FLUIDS (HT)

- I In the Model Builder window, under Component 2 (comp2)>Heat Transfer in Fluids (ht) click Fluid 1.
- 2 In the Settings window for Fluid, locate the Heat Conduction, Fluid section.
- **3** From the k list, choose Thermal conductivity (chem).
- 4 Locate the Thermodynamics, Fluid section. From the Fluid type list, choose Gas/Liquid.
- **5** From the ρ list, choose **Density (chem)**.
- 6 From the C_p list, choose Heat capacity at constant pressure (chem).
- **7** From the γ list, choose **User defined**.

Heat Source 1

- I In the Physics toolbar, click **Domains** and choose **Heat Source**.
- 2 Select Domain 1 only.
- 3 In the Settings window for Heat Source, locate the Heat Source section.
- 4 From the Q_0 list, choose Heat source of reactions (chem).

Temperature I

- I In the Physics toolbar, click Boundaries and choose Temperature.
- 2 Select Boundaries 1–3 only.
- 3 In the Settings window for Temperature, locate the Temperature section.
- **4** In the T_0 text field, type T_in.

Temberature 2

I In the Physics toolbar, click — Boundaries and choose Temperature.

- 2 Select Boundaries 4–7 only.
- 3 In the Settings window for Temperature, locate the Temperature section.
- **4** In the T_0 text field, type T_surf.

Outflow I

- I In the Physics toolbar, click Boundaries and choose Outflow.
- 2 Select Boundary 8 only.

Initial Values 1

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- **3** In the *T* text field, type T in.

COMPONENT 2 (COMP2)

Add a Laminar Flow interface to model the fluid flow. When available, use the fluid parameters from the **Chemistry** interface.

ADD PHYSICS

- I In the Physics toolbar, click Add Physics to open the Add Physics window.
- 2 Go to the Add Physics window.
- 3 In the tree, select Fluid Flow>Single-Phase Flow>Laminar Flow (spf).
- 4 Click Add to Component 2 in the window toolbar.
- 5 In the Physics toolbar, click Add Physics to close the Add Physics window.

LAMINAR FLOW (SPF)

- I In the Settings window for Laminar Flow, locate the Physical Model section.
- 2 From the Compressibility list, choose Compressible flow (Ma<0.3).
- 3 In the p_{ref} text field, type 0[atm].

Fluid Properties 1

- I In the Model Builder window, under Component 2 (comp2)>Laminar Flow (spf) click Fluid Properties 1.
- 2 In the Settings window for Fluid Properties, locate the Fluid Properties section.
- **3** From the ρ list, choose **Density (chem)**.
- 4 From the μ list, choose Dynamic viscosity (chem).

Inlet I

- I In the Physics toolbar, click Boundaries and choose Inlet.
- 2 Select Boundary 1 only.
- 3 In the Settings window for Inlet, locate the Boundary Condition section.
- 4 From the list, choose Fully developed flow.
- **5** Locate the **Fully Developed Flow** section. In the U_{av} text field, type u_in.

Outlet I

- I In the Physics toolbar, click Boundaries and choose Outlet.
- 2 Select Boundary 8 only.
- 3 In the Settings window for Outlet, locate the Pressure Conditions section.
- **4** In the p_0 text field, type p_0 .
- 5 Select the Normal flow check box.

Initial Values 1

- I In the Model Builder window, click Initial Values I.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- **3** In the *p* text field, type p_0.

CHEMISTRY (CHEM)

Finish the space-dependent model setup by coupling the interfaces.

- I In the Model Builder window, under Component 2 (comp2) click Chemistry (chem).
- 2 In the Settings window for Chemistry, locate the Model Input section.
- **3** From the T list, choose **Temperature** (ht).
- **4** From the *p* list, choose **Absolute pressure (spf)**. Set the density dependent on both pressure and temperature.
- 5 Locate the Mixture Properties section. From the Density list, choose User defined.
- 6 In the ρ text field, type chem.p/R const/chem.T*chem.M H2.

MULTIPHYSICS

Nonisothermal Flow I (nitf1)

In the Physics toolbar, click Multiphysics Couplings and choose Domain>

Reacting Flow, Diluted Species 1 (rfd1)

In the Physics toolbar, click Aultiphysics Couplings and choose Domain>Reacting Flow, **Diluted Species.**

MESH I

- I In the Model Builder window, under Component 2 (comp2) click Mesh I.
- 2 In the Settings window for Mesh, locate the Physics-Controlled Mesh section.
- **3** From the **Element size** list, choose **Finer**.
- 4 Click III Build All.

STUDY (RE)

Step 1: Time Dependent

- I In the Model Builder window, under Study (re) click Step 1: Time Dependent.
- 2 In the Settings window for Time Dependent, locate the Physics and Variables Selection section.
- 3 In the table, clear the Solve for check boxes for Reaction Engineering -Gas Phase Reactions, Reduced Set (re2) (re2), Chemistry (chem), Transport of Diluted Species (tds), and Heat Transfer in Fluids (ht).

ROOT

Solve the model for stationary conditions by selecting the **Stationary** study type.

ADD STUDY

- I In the Home toolbar, click Add Study to open the Add Study window.
- 2 Go to the Add Study window.
- **3** Find the **Physics interfaces in study** subsection. In the table, clear the **Solve** check boxes for Reaction Engineering - Gas Phase Reactions, Full Set (re) (re) and Reaction Engineering -Gas Phase Reactions, Reduced Set (re2) (re2).
- 4 Find the Studies subsection. In the Select Study tree, select General Studies>Stationary.
- 5 Click Add Study in the window toolbar.
- 6 In the Home toolbar, click Add Study to close the Add Study window.

STUDY 2D MODEL

- I In the Model Builder window, click Study 3.
- 2 In the Settings window for Study, type Study 2D Model in the Label text field.
- 3 In the Home toolbar, click **Compute**.

RESULTS

Velocity (spf)

To create Figure 5, follow these steps:

- I In the Model Builder window, under Results click Velocity (spf).
- 2 In the Settings window for 2D Plot Group, click to expand the Title section.
- **3** From the **Title type** list, choose **None**.
- **4** Locate the **Color Legend** section. Select the **Show units** check box.
- **5** From the **Position** list, choose **Bottom**.
- 6 In the Velocity (spf) toolbar, click **Plot**.
- 7 Click the **Zoom Extents** button in the **Graphics** toolbar.

Temperature (ht)

To reproduce Figure 6, do the following:

- I In the Model Builder window, click Temperature (ht).
- 2 In the Settings window for 2D Plot Group, locate the Title section.
- **3** From the **Title type** list, choose **None**.
- 4 Locate the Color Legend section. From the Position list, choose Bottom.
- **5** Select the **Show units** check box.
- 6 In the Temperature (ht) toolbar, click Plot.
- 7 Click the **Zoom Extents** button in the **Graphics** toolbar.

Concentration, GaC6H15 (tds)

You can reproduce Figure 7 as follows:

- I In the Model Builder window, click Concentration, GaC6H15 (tds).
- 2 In the Settings window for 2D Plot Group, locate the Title section.
- **3** From the **Title type** list, choose **None**.
- 4 Locate the Color Legend section. From the Position list, choose Bottom.
- **5** Select the **Show units** check box.

Streamline 1

- I In the Model Builder window, expand the Concentration, GaC6H15 (tds) node, then click Streamline 1.
- 2 In the Settings window for Streamline, locate the Streamline Positioning section.
- 3 From the Positioning list, choose On selected boundaries.

- 4 In the Number text field, type 10.
- **5** Locate the **Selection** section. Click to select the **Selection** toggle button.
- **6** Select Boundary 1 only.
- 7 Locate the Coloring and Style section. Find the Line style subsection. From the Type list, choose Tube.
- 8 Select the Radius scale factor check box. In the associated text field, type 0.0005.
- **9** Find the **Point style** subsection.
- 10 Select the Scale factor check box. In the associated text field, type 5.
- II Click the **Zoom Extents** button in the **Graphics** toolbar.
- 12 In the Concentration, GaC6H15 (tds) toolbar, click Plot.

The pressure variation in this model is small. For clarity, plot the relative pressure instead of the total pressure.

Contour

- I In the Model Builder window, expand the Results>Pressure (spf) node, then click Contour.
- 2 In the Settings window for Contour, locate the Expression section.
- 3 In the Expression text field, type p-p_0.
- 4 In the Pressure (spf) toolbar, click **Plot**.

To produce the remaining figures, illustrating various results along the reactor centerline, use a **Cut Line 2D** dataset.

Cut Line 2D I

- I In the Results toolbar, click Cut Line 2D.
- 2 In the Settings window for Cut Line 2D, locate the Line Data section.
- **3** In row **Point I**, set **x** to -0.2.
- 4 In row **Point 2**, set **x** to 0.2.
- 5 Click Plot.

Concentration Profiles GaC6H15 and GaH2

- I In the Results toolbar, click \to ID Plot Group.
- 2 In the Settings window for ID Plot Group, type Concentration Profiles GaC6H15 and GaH2 in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Cut Line 2D 1.
- 4 Locate the Legend section. From the Position list, choose Upper right.

GaC6H15

- I Right-click Concentration Profiles GaC6H15 and GaH2 and choose Line Graph.
- 2 In the Settings window for Line Graph, type GaC6H15 in the Label text field.
- 3 Click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component 2 (comp2)>Transport of Diluted Species>Species cGaC6H15> cGaC6H15 - Concentration - mol/m3.
- 4 Click Replace Expression in the upper-right corner of the x-Axis Data section. From the menu, choose Component 2 (comp2)>Geometry>Coordinate>x - x-coordinate.
- 5 Click to expand the Coloring and Style section. From the Width list, choose 2.
- **6** Click to expand the **Legends** section. Select the **Show legends** check box.
- **7** Find the **Include** subsection. Select the **Label** check box.
- 8 Clear the Solution check box.

GaH2

- I In the Model Builder window, right-click Concentration Profiles GaC6H15 and GaH2 and choose Line Graph.
- 2 In the Settings window for Line Graph, type GaH2 in the Label text field.
- 3 Click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component 2 (comp2)>Transport of Diluted Species>Species cGaH2> cGaH2 - Concentration - mol/m3.
- 4 Click Replace Expression in the upper-right corner of the x-Axis Data section. From the menu, choose Component 2 (comp2)>Geometry>Coordinate>x - x-coordinate.
- **5** Locate the **Legends** section. Select the **Show legends** check box.
- **6** Find the **Include** subsection. Select the **Label** check box.
- 7 Clear the **Solution** check box.

Concentration Profiles GaC6H15 and GaH2

- I In the Model Builder window, click Concentration Profiles GaC6H15 and GaH2.
- 2 In the Settings window for ID Plot Group, locate the Title section.
- **3** From the **Title type** list, choose **None**.
- 4 In the Concentration Profiles GaC6H15 and GaH2 toolbar, click Plot.
- **5** Click the **Zoom Extents** button in the **Graphics** toolbar.

Concentration Profile AsH3 Change

I In the Home toolbar, click **Add Plot Group** and choose ID Plot Group.

- 2 In the Settings window for ID Plot Group, type Concentration Profile AsH3 Change in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Cut Line 2D 1.
- 4 Locate the Legend section. From the Position list, choose Upper right.

Line Graph 1

- I Right-click Concentration Profile AsH3 Change and choose Line Graph.
- 2 In the Settings window for Line Graph, click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component 2 (comp2)> Transport of Diluted Species>Species cAsH3>cAsH3 - Concentration - mol/m3.
- 3 Locate the y-Axis Data section. In the Expression text field, type cAsH3-c_AsH3_init.
- 4 Click to expand the Title section. From the Title type list, choose Manual.
- 5 In the Title text area, type Change in arsine, AsH₃, concentration compared to initial conditions in the reactor.
- 6 Click Replace Expression in the upper-right corner of the x-Axis Data section. From the menu, choose Component 2 (comp2)>Geometry>Coordinate>x - x-coordinate.
- 7 Locate the Coloring and Style section. From the Width list, choose 2.
- **8** Locate the **Legends** section. Select the **Show legends** check box.
- 9 From the Legends list, choose Manual.
- **10** In the table, enter the following settings:

Legends AsH3

II In the Concentration Profile AsH3 Change toolbar, click **Tool** Plot.

The Chemistry node calculates the diffusivities, the thermal conductivity, and other fluid properties, including their temperature dependence. Next, plot the diffusivities along the reactor centerline for two of the species as functions of the temperature.

Diffusivities vs. Temperature

- I In the Home toolbar, click **Add Plot Group** and choose ID Plot Group.
- 2 In the Settings window for ID Plot Group, type Diffusivities vs. Temperature in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Cut Line 2D 1.
- 4 Locate the Legend section. From the Position list, choose Lower right.

GaC6H15

- I Right-click Diffusivities vs. Temperature and choose Line Graph.
- 2 In the Settings window for Line Graph, type GaC6H15 in the Label text field.
- 3 Click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component 2 (comp2)>Transport of Diluted Species>Species cGaC6H15> tds.Day cGaC6H15 Average diffusion coefficient m²/s.
- 4 Locate the x-Axis Data section. From the Parameter list, choose Expression.
- 5 Click Replace Expression in the upper-right corner of the x-Axis Data section. From the menu, choose Component 2 (comp2)>Heat Transfer in Fluids>Temperature>T Temperature K.
- 6 Locate the Coloring and Style section. From the Width list, choose 2.
- 7 Locate the Legends section. Select the Show legends check box.
- 8 Find the Include subsection. Select the Label check box.
- **9** Clear the **Solution** check box.

AsH3

- I In the Model Builder window, right-click Diffusivities vs. Temperature and choose Line Graph.
- 2 In the Settings window for Line Graph, type AsH3 in the Label text field.
- 3 Click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component 2 (comp2)>Transport of Diluted Species>Species cAsH3> tds.Dav_cAsH3 Average diffusion coefficient m²/s.
- 4 Locate the x-Axis Data section. From the Parameter list, choose Expression.
- 5 Click Replace Expression in the upper-right corner of the x-Axis Data section. From the menu, choose Component 2 (comp2)>Heat Transfer in Fluids>Temperature>T Temperature K.
- 6 Locate the Coloring and Style section. From the Width list, choose 2.
- 7 Locate the Legends section. Select the Show legends check box.
- 8 Find the Include subsection. Select the Label check box.
- **9** Clear the **Solution** check box.

Diffusivities vs. Temperature

- I In the Model Builder window, click Diffusivities vs. Temperature.
- 2 In the Settings window for ID Plot Group, locate the Title section.

- 3 From the Title type list, choose None.
- 4 Locate the Grid section. Select the Manual spacing check box.
- 5 In the x spacing text field, type 100.
- 6 In the y spacing text field, type 1e-3.
- 7 Locate the Legend section. From the Position list, choose Lower right.
- 8 In the Diffusivities vs. Temperature toolbar, click **Plot**.

Thermal Conductivity H2

- I In the Home toolbar, click Add Plot Group and choose ID Plot Group.
- 2 In the Settings window for ID Plot Group, type Thermal Conductivity H2 in the Label text field.
- 3 Locate the Data section. From the Dataset list, choose Cut Line 2D 1.
- 4 Locate the Legend section. From the Position list, choose Lower right.

Line Graph 1

- I Right-click Thermal Conductivity H2 and choose Line Graph.
- 2 In the Settings window for Line Graph, click Replace Expression in the upper-right corner of the y-Axis Data section. From the menu, choose Component 2 (comp2)> Heat Transfer in Fluids>Material properties>ht.kmean -Mean effective thermal conductivity - W/(m·K).
- 3 Locate the x-Axis Data section. From the Parameter list, choose Expression.
- 4 Click Replace Expression in the upper-right corner of the x-Axis Data section. From the menu, choose Component 2 (comp2)>Heat Transfer in Fluids>Temperature>T -Temperature - K.
- 5 Locate the Coloring and Style section. From the Width list, choose 2.
- **6** Locate the **Legends** section. Select the **Show legends** check box.
- 7 From the Legends list, choose Manual.
- **8** In the table, enter the following settings:

Legends H2

Thermal Conductivity H2

- I In the Model Builder window, click Thermal Conductivity H2.
- 2 In the Settings window for ID Plot Group, locate the Title section.
- **3** From the **Title type** list, choose **None**.