HW #3

For direct methane oxidation in an sore at the anode the net reaction is -

At the anode, $CH_4 + 2H_2O \rightarrow CO_2 + 8H^+ + 8e^-$ Cothode, $O_2 + 4e^- \rightarrow 20^{4-}$

Thus I make of they reacts with 2 moles of 02->2 electrons transferred.

Given, operating temperature, T = 700°C = 973 K Gas pressure, P = 104m = 101325 Pa Gas constant, R = 8.314 3/mole K Farady's constant, F = 96485 c/mol.

change transfer coefficient, & = 0.5

Effective diffusivity of 02, bet = 3.66×10-7 m/s

Ohmie potential, 1 = 3. Rohmic=10x0.1 a.em

= 10x1×10-5 a.m

Total molar concentration from Ideal gas law -Ctotal = P = 101325 FT = 101325 = 12.53 mol/m³

From volume fractions,

O2(18%), CO2 = 0.18 × 12.53 = 2.26 mol/m3 CH4(66%), CCH4 = 0.60 × 12.53 = 7.62 mol/m3 Exchange current density, at cahode, $I_{o}^{c} = 3.8 \times 10^{6} \exp(-\frac{8170}{T}) \times Co_{2}$ $= 3.8 \times 10^{6} \exp(-\frac{8170}{273}) \times 2.26$ $= 3117.86 A/m^{2}$

At anode, $F_6^{\alpha} = 1.3 \times 10^6 \exp\left(-\frac{8427}{T}\right) \times \text{CCHy}$ $= 1.3 \times 10^6 \exp\left(-\frac{8427}{273}\right) \times 7.52$ $= 38768.34 \text{ A/m}^{\circ}$

concentration overpotential,

$$n_{cone} = -\frac{RT}{nF} ln(\frac{cs}{c_b})$$
 Cb = bulk concentration
 $c_s = c_b - \frac{J \cdot S}{nFD}$ $c_s = surface$ concentration

At j = 1.0 A/cm = 10^4 A/m, diffusion layer thickness at cathode / electrolyte interface, 8 = 10 µm = 10×10^6 m cothode: $C_{5.02} = 2.26 - \frac{10^4 \times 10 \times 10^{-6}}{8 \times 96485 \times 3.66 \times 10^{-7}} = 2.20$

 $\eta_{c,cone} = -\frac{8.314 \times 973}{8 \times 96485} \ln \left(\frac{2.20}{2.26} \right) = 0.00179V$ Anode: $c_{s,chy} = 7.52 - \frac{10^4 \times 200 \times 10^{-6}}{8 \times 96485 \times 9.66 \times 10^{-7}} = 7.30$ $\left[c_{a,cone}^{eff} = 9.66 \times 10^{-7} \right]$ $\left[c_{a,cone}^{eff} = 0.00463 \right]$

Activation apotential,
$$\eta_{act} = \frac{RT}{\alpha nF} \sinh^{-1}(\frac{j}{2i_0})$$

At $j = 10^4 A/m^2$.

Anode:
$$\eta_{a,act} = \frac{8.314 \times 973}{0.5 \times 8 \times 96485} \sinh^{-1}(\frac{10^4}{2 \times 38768.34})$$

= 0.06610 V

Assume open-circuit voltage, Eo z 1.1 V

Concentration overpotential at 5 = 2.5 Alem = 2.5 × 104 Alm

Cathode: cs,02 = 2.26 - 2.5 x 10 x 10 x 10-6 8 x 964 85 x 3.66 x 10-7

= 2.18 mol/m3

nc, conc = - RT In(2.18) = 0.00523V

Anode: Cs. CHy = 7.52 - 2.5 × 104 × 200 × 10-6 8 × 96485 × 9.66 × 10-7

= 6.97 mos/m3

na, cone = - RT In(6.97)=0.02337V

Activation overpotentials, at j= 25 Alemander of the said of the s

Cathode: 1/2, act = RT sinh () 210,e)

= 8.314x 273 sinh (2.5x104)

=0.05377 V

Anode: no set = RT sinh (2.5x104)

= 0.01432 V

Ohmic overpotential = J. Rohmic = 2.5×10 ×1×105 = 0.25V Total Overpotential, 7 = 0.00 5 23 + 0.02 337+0.05 377 total + 0.01432+0.25

operating voltage Voperating = Eo- 2 total

=[1.1-0.3467)

Voperating 0.7533V

- > The operating voltage drops from 0.95 V to 0.75 V as current density increases.
 - -> Ohmic loss is the dominant loss at higher current density.