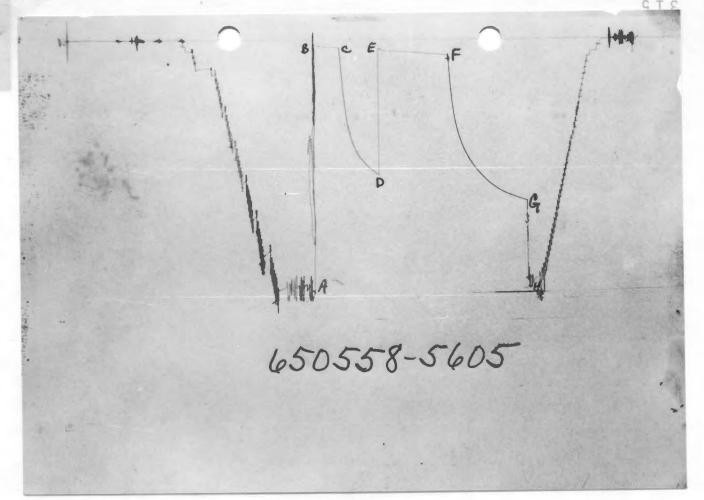


TICKET NO. 65055800 14-APR-83 PRATT

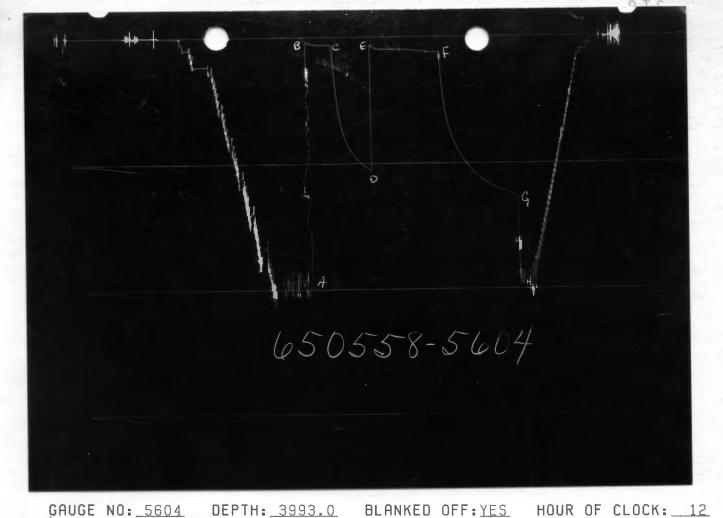
FORMATION TESTING SERVICE REPORT

23-325-14W TEST NO. FIELD AREA WILDCHI 398C. - 3998. BARBER TEXAS ENERGIES, INCORPORATED
LEASE OWNER/COMPANY NAME KANSAS BC/NM



GAUGE NO: 5605 DEPTH: 3958.0 BLANKED OFF: NO HOUR OF CLOCK: 12

ID	DESCRIPTION	DESCRIPTION PRESSURE			TYPE
10	DESCRIT TION	REPORTED CALCULATE	D REPORTED	CALCULATED	1111
A	INITIAL HYDROSTATIC	1914.	4		
B.	INITIAL FIRST FLOW	40.		29.9	F
С	FINAL FIRST FLOW	63.		50.0	
С	INITIAL FIRST CLOSED-IN	63.	1 45.0	44.9	С
D	FINAL FIRST CLOSED-IN	1056.		44.3	
Е	INITIAL SECOND FLOW	66.	9 80.0	80.3	F
F	FINAL SECOND FLOW	124.		00.5	
F	INITIAL SECOND CLOSED-IN	124.		89.8	С
G	FINAL SECOND CLOSED-IN	1262.	7 90.0	09.0	
Н	FINAL HYDROSTATIC	1867.	6		



PRESSURE TIME TYPE ID DESCRIPTION REPORTED | CALCULATED REPORTED CALCULATED INITIAL HYDROSTATIC 2014 1924.0 INITIAL FIRST FLOW B 41 40.8 30.0 29.9 F FINAL FIRST FLOW C 62 66.0 C INITIAL FIRST CLOSED-IN 66.0 62 C 45.0 44.9 FINAL FIRST CLOSED-IN 1062.3 1066 E INITIAL SECOND FLOW 62.7 62 80.0 80.3 F FINAL SECOND FLOW 123 125.9 INITIAL SECOND CLOSED-IN F 123 125.9 89.8 C 90.0 FINAL SECOND CLOSED-IN 1262.9 1251 G FINAL HYDROSTATIC 1877.4 1952

650558-6144

GAUG	E NO: 6144 DEPTH: 4040.0	BLANK	ED OFF: YE	S HOUR	OF CLOCK	: 12	
ID	DESCRIPTION	PRES	SSURE	TIME REPORTED CALCULATED		TYPE	
A	INITIAL HYDROSTATIC						
В	INITIAL FIRST FLOW			20.0		F	
C	FINAL FIRST FLOW			30.0			
С	INITIAL FIRST CLOSED-IN			45.0		_	
D	FINAL FIRST CLOSED-IN			45.0			
E	INITIAL SECOND FLOW					F	
F	FINAL SECOND FLOW			80.0			
F	INITIAL SECOND CLOSED-IN			90.0		6	
G	FINAL SECOND CLOSED-IN					C	

FINAL HYDROSTATIC

EQUIPMENT & HOLE DATA	TICKET NUMBER: 65055800
FORMATION TESTED: DOUGLAS	
NET PAY (ft):	DATE: 4-10-83 TEST NO: 1
GROSS TESTED FOOTAGE: 18.0	TYPE DOT. OFF BIM CIRODDIE
ALL DEPTHS MEASURED FROM: KELLY BUSHING	TYPE DST: OFF BTM.STRADDLE
CASING PERFS. (ft):	HALLIBURTON CAMP:
HOLE OR CASING SIZE (tn):	PRATT
ELEVATION (ft): 1894	
TOTAL DEPTH (ft):4860.0	TESTER: ROBERT E. MARTIN
PACKER DEPTH(S) (ft): 3974, 3980, 3998	MARTIN COLLINS
FINAL SURFACE CHOKE (tn): 0.250	
BOTTOM HOLE CHOKE (tn): 0.750	WITNESS: SCOTT ALBERG.GEOL.
MUD WEIGHT (16/gal):8.90	
MUD VISCOSITY (sec): 48	DRILLING CONTROCTOR
ESTIMATED HOLE TEMP. (°F):110	DRILLING CONTRACTOR:
ACTUAL HOLE TEMP. (°F): @ ft	VHEATSTATE (RIG# 2)
FLUID PROPERTIES FOR RECOVERED MUD & WATER SOURCE RESISTIVITY CHLORIDES  PIT 0.230 • 40 °F 16000 ppm  TOP 0.350 • 75 °F 16956 ppm  MIDDLE 0.290 • 75 °F 19782 ppm  BOTTOM 0.190 • 75 °F 30521 ppm  - • °F	SAMPLER DATA Pstg AT SURFACE: cu.ft. OF GAS: cc OF OIL: cc OF WATER: cc OF MUD: TOTAL LIQUID cc:  CUSHION DATA TYPE AMOUNT WEIGHT
RECOVERED:  189 FEET OF MUDDY WATER  30 FEET OF MUD  219 FEET - TOTAL RECOVERY	MEASURED FROM TESTER VALVE
REMARKS:	
ELEVATION SHOWN IS AT GROUND LEVEL	1
STYLUS DISENGAGED ON B.T. # 6144.	
IRON PH CALCIUM MAGNES	
TOP NEG 9.5 492 -	MODERATE
MIDDLE NEG 6.85 615 -	LIGHT
BOTTOM NEG 6.5 2458 747	MODERATE

TYPE & SI	YPE & SIZE MEASURING DEVICE:ME		MERLA 2	MERLA 2" TESTER TICKET NO			
TIME	CHOKE S1ZE	SURFACE PRESSURE PSI	GAS RATE MCF	LIQUID RATE BPD	RE	MARKS	
4-10-83					, ,,4		
2347				72	CALLED OUT.	18.	
0025					LEFT CAMP.	,	
0130					ON LOCATION-RIG PU	LLING RIPE.	
0210					STARTED CLOCKS.	. 12	
0245					PICKED UP TOOL.		
0330					TOOL AT THE TABLE.		
0410					TOOL THRU THE TABL	Ε.	
0652					SIDE WALL ANCHOR S	ET - TOOL DID	
					NOT SLIDE.		
0655					INITIAL OPENING -	HAD A STRDNG	
					BLOW OFF BOTTOM OF	THE BUCKET	
					IMMEDIATELY.	(_0)** '' '' '' '' '' ''	
0718					GAS TO THE SURFACE	IN 23 MINUTES	
					UNMEASURABLE.		
0725					INITIAL CLOSED IN PRESSURE.		
0810				11	FINAL OPENING - HAD A STRONG		
					BLOW.		
0820	1/8"	2.0	3.92		GAS TO THE SURFACE	IMMEDIATELY.	
0825	1/8" .	2.0	3.92	-			
0830	19	2.0	3.92		CAUGHT GAS SAMPLE.		
0835	99	1.8	3.528				
0840	11	1.8	3.528				
0845	89	2.0	3.92				
0850	99	2.0	3.92				
0855	99	2.8	4.64			Was a second	
0900	99	4.8	6:24				
0905	44	6.4	7.31		CAUGHT GAS SAMPLE.		
0910	99	7.2	7.82				
0915	11	8.5	8.59			. 1904	
0920	44	8.7	8.70		1.11		
0925	11	8.8	8.77				
0929	11	8.8	8.77			31	
0930					FINAL CLOSED IN PE	RIOD.	
1100					UNSERTED HOOK.		
1235		-			TOOL AT THE TABLE.		
1400		- 1			TOOL LAID DOWN.		

) ( E

TICKET NO: 65055800

CLOCK NO: 6947 HOUR: 12



**GAUGE NO: 5605** 

RE	F	MINUTES	PRESSURE	ΔΡ	<u>t×Δt</u> t+Δt	$\log \frac{t + \Delta t}{\Delta t}$		
			FIRST	FLOW				
В	1	0.0	40.5					
	2	5.0	46.0	5.5		- 1		
	3	10.0	54.3	8.3		1		
	4	15.0	58.5	4.2				
	5	20.0 25.0	59.2 60.4	0.7 1.2				
С	6 7	29.9	63.1	2.7				
		F	IRST CL	.0SED-I	N			
C					•			
С	1	0.0	63.1	246 1	2 5	0.928		
	2 3	4.0 8.0	409.2 634.5	346.1 5 <b>71.4</b>	3.5 6.3	0.674		
	4	12.0	756.4	693.3	8.6	0.543		
	5	16.0	833.6	770.6	10.4	0.458		
	6	20.0	887.2	824.1	12.0	0.397		
	7	24.0	928.9	865.8	13.3	0.352		
	8	28.0	960.7	897.6	14.5	0.316		
	9	32.0	988.4	925.3	15.4	0.287		
	10	36.0	1013.6	950.5	16.3	0.262		
D	11 12	40.0 44.9	1035.1 1056.7	972.0 993.7	17.1 18.0	0.242		
_					10.0			
			SECONE	) FLOW				
Ε	1	0.0	66.9					
	2	10.0	89.4	22.5				
	3	20.0	93.3	3.9				
	4	30.0 <b>40.</b> 0	96.1 99.7	2.9 3.6				
	5 6	50.0	106.5	6.9				
	7	60.0	112.0	5.4				
	8	70.0	117.1	5.1				
F	9	80.3	124.5	7.5		Í		
SECOND CLOSED-IN								
F	1	0.0	124.5					
	2	5.0	538.4	413.9	4.8	1.360		
	3	10.0	715.7	591.1	9.2	1.079		
	4	15.0	819.5	695.0	13.2	0.923		
	5	20.0	893.2	768.7	16.9	0.814		
	6	25.0 30.0	953.6 1000.8	829.0 876.3	20.4 23.6	0.733 0.670		
	7 8	35.0	1043.3	918.7	26.6	0.618		
	9	40.0	1043.3	953.2	29.3	0.575		
	10	45.0	1111.5	986.9	32.0	0.538		
	11	50.0	1139.2	1014.6	34.4	0.506		
	12	55.0	1164.0	1039.5	36.7	0.478		
						•		

DEPTH: 3958.0		-		GHI	JGE NO:	5605					
SECOND CLOSED-IN - CONTINUED  13 60.0 1184.9 1060.3 38.9 0.453  14 65.0 1202.4 1077.8 40.9 0.431  15 70.0 1216.6 1092.0 42.8 0.411  16 75.0 1229.4 1104.9 44.6 0.393  17 80.0 1241.8 1117.3 46.4 0.376  18 85.0 1254.3 1129.8 48.0 0.361	# ! IIEE IM • 3USX II										
13     60.0     1184.9     1060.3     38.9     0.453       14     65.0     1202.4     1077.8     40.9     0.431       15     70.0     1216.6     1092.0     42.8     0.411       16     75.0     1229.4     1104.9     44.6     0.393       17     80.0     1241.8     1117.3     46.4     0.376       18     85.0     1254.3     1129.8     48.0     0.361	RE	F	MINI	JTES	PRESSURE	ΔР	<u>t×∆t</u> t+∆t	log <mark>t+Δt</mark>			
14     65.0     1202.4     1077.8     40.9     0.431       15     70.0     1216.6     1092.0     42.8     0.411       16     75.0     1229.4     1104.9     44.6     0.393       17     80.0     1241.8     1117.3     46.4     0.376       18     85.0     1254.3     1129.8     48.0     0.361	SECOND CLOSED-IN - CONTINUED										
15     70.0     1216.6     1092.0     42.8     0.411       16     75.0     1229.4     1104.9     44.6     0.393       17     80.0     1241.8     1117.3     46.4     0.376       18     85.0     1254.3     1129.8     48.0     0.361		13		60.0	1184.9	1060.3	38.9	0.453			
16     75.0     1229.4     1104.9     44.6     0.393       17     80.0     1241.8     1117.3     46.4     0.376       18     85.0     1254.3     1129.8     48.0     0.361		14		65.0	1202.4	1077.8	40.9	0.431			
17 80.0 1241.8 1117.3 46.4 0.376 18 85.0 1254.3 1129.8 48.0 0.361		15									
18 85.0 1254.3 1129.8 48.0 0.361											
U 19 89.8 1262.7 1138.1 49.5 0.348	c										
	U	19		89.8	1262.7	1138.1	49.5	0.348			

REMARKS:



GAUGE NO: 5604

	u u r	NU: 3	UU4 n			/	414	VICES
RE	F	MINUTES	PRESSURE	ΔP	<u>t×∆</u> t+∆	<u>.t</u> .t	$\log \frac{t + \Delta t}{\Delta t}$	R
			FIRST	FLOW				
В	1	0.0	40.8					
	2	5.0	52.7	11.9				
	3	10.0	58.5	5.9				
	4	15.0	61.3	2.8				_
	5	20.0	61.3	0.0				G
С	6 7	25.0 29.9	63.0 66.0	1.7 3.0				
		F	IRST CL	.OSED-I	N			
C	1	0.0	66.0					
٦	5	4.0	414.3	348.3		3.5	0.931	
	3	8.0	638.9	572.8		6.3	0.675	
	4	12.0	758.4	692.4		8.6	0.542	
	5	16.0	834.0	768.0	1	0.4	0.457	
	6	20.0	889.1	823.0		2.0	0.397	
	7	24.0	930.2	864.1		3.3	0.352	
	8	28.0	964.4	898.4		4.5		
	9 10	32.0 36.0	992.4 1017.6	926.4 951.5		5.5 6.3		
	11	40.0	1038.6	972.6		7.1	0.243	
ם	12	44.9	1062.3	996.3		8.0	0.222	
			SECONE	) FLOW				
E	1	0.0	62.7				!	
_	2	10.0	95.3	32.5				
	3	20.0	98.8	3.5				
l	4	30.0	98.8	0.0				<b>   </b>
	5	40.0	101.2	2.5				
	6 7	50.0 60.0	107.4 112.4	6.2 5.0				
	8	70.0	121.1	8.7				
F	9	80.3	125.9	4.7				
		S	ECOND C	LOSED-1	N			
F	1	0.0	125.9					
	2	5.0	534.7	408.8		4.8	1.364	
	3	10.0	709.6	583.7		9.2		
	4	15.0	813.5	687.6		3.2		
	5	20.0	890.0	764.1		6.9		
1	6	25.0	952.2	826.4		0.4		
	7 8	30.0 35.0	1000.1 1046.0	874.2 920.1		3.6 6.6		[ ]
	9	40.0	1080.0	954.1		9.4		<b>   </b>
	10	45.0	∂.9	985.0		1.9		11
	11	50.0	.4	1012.5		4.4		11
1	12	55.0	1.52.8	1037.0	9	6.7	0.478	
								┚┖

RE	F	MINUTES	PRESSURE	ΔP	$\frac{\mathbf{t} \times \Delta \mathbf{t}}{\mathbf{t} + \Delta \mathbf{t}}$	log <u>t÷Δt</u> Δt			
SECOND CLOSED-IN - CONTINUED									
	13	60.0	1183.1	1057.2	38.8	0.453			
	14	65.0	1199.6	1073.7	40.9	0.431			
	15	70.0	1213.9	1088.0	42.8	0.411			
	16	75.0	1227.0	1101.1	44.6	0.393			
	17	80.0	1238.6	1112.7	46.4	0.376			
	18	85.0	1251.8	1126.0	48.0	0.361			
G	19	89.8	1262.9	1137.1	49.5	0.348			

REMARKS:

		_	0.0.	I.O.	LENGTH	DEPTH
π-						
		DRILL PIPE	4.500	3.826	3664.0	
50	D	IMPACT REVERSING SUB	5.750	2.750	1.0	3664.0
, F		DRILL COLLARS	6.250	2.250	280.0	
5 <b> </b>		CROSSOVER	6.250	2.250	1.0	
2	٥	DUAL CIP VALVE	5.000	0.870	6.0	
0	٥	HYDROSPRING TESTER	5.000	0.750	5.0	3956.0
0		AP RUNNING CASE	5.000	3.060	4.0	3958.0
5		JAR	5.000	1.750	5.0	
6	v	VR SAFETY JOINT	5.000	1.000	3.0	
7 📙	0	PRESSURE EQUALIZING CROSSOVER	5.000	2.620	1.0	
		OPEN HOLE PACKER	6.750	1.530	6.0	3974.0
		OPEN HOLE PACKER	6.750	1.530	6.0	3980.0
		FLUSH JOINT ANCHOR	5.000	2.370	9.0	
7	0	PRESSURE EQUALIZING CROSSOVER	5.000	2.620	1.0	
·	_	AP RUNNING CASE	5.000	3.060	4.0	3993.0
		OPEN HOLE PACKER	6.750	1.530	6.0	3998.0
		CROSSOVER	5.000	2.000	1.0	
		FLUSH JOINT ANCHOR	5.000	2.370	30.0	
		CROSSO <b>v</b> ER	5.000	2.000	1.0	
· }}		SIDE WALL ANCHOR	6.750	1.620	5.0	4035.0
	٥	BLANKED-OFF RUNNING CASE	5.000		4.0	4040.0
	Т	OTAL DEPTH				4860.0

## **EQUATIONS FOR DST LIQUID WELL ANALYSIS**

$$\frac{kh}{u} = \frac{162.6 \text{ QB}}{m}$$

md-ft cp

Indicated Flow Capacity

$$kh = \frac{kh}{\mu} \mu$$

md-ft

Average Effective Permeability

$$k = \frac{kh}{h}$$

mđ

Damage Ratio

$$DR = .183 \frac{P^* - P_f}{m}$$

Theoretical Potential w / Damage Removed

$$Q_1 = Q DR$$

BPD

Approx. Radius of Investigation

$$r_i = 4.63 \sqrt{kt}$$

ft

## **EQUATIONS FOR DST GAS WELL ANALYSIS**

Indicated Flow Capacity

$$kh = \frac{1637 Q_g T}{m}$$

md-ft

Average Effective Permeability

$$k = \frac{kh}{h}$$

md

Skin Factor

$$S = 1.151 \left[ \frac{m(P^*) - m(P_f)}{m} - LOG \frac{kt}{\phi \mu c_f r_w^2} + 3.23 \right] \frac{1}{c_f}$$

Damage Ratio

$$DR = \frac{m(P^*) - m(P_f)}{m(P^*) - m(P_f) - 0.87 \text{ mS}}$$

MCFD

Indicated Flow Rate (Maximum)

$$AOF_1 = \frac{Q_g m(P^*)}{m(P^*) - m(P_f)}$$

Indicated Flow Rate (Minimum)

$$AOF_2 = Q_g \sqrt{\frac{m(P^*)}{m(P^*) - m(P_f)}}$$

MCFD

Approx. Radius of Investigation

$$r_i = 0.032 \sqrt{\frac{kt}{\phi \mu c_t}}$$

ft

## NOMENCLATURE

В	=	Formation Volume Factor (Res Vol / Std Vol)	
Ct	=	System Total Compressibility	(Vol / Vol) / psi
DR	=	Damage Ratio	
h	=	Estimated Net Pay Thickness	Ft
k	=	Permeability	md
m {	=	(Liquid) Slope Extrapolated Pressure Plot	psi/cycle MM psi <sup>2</sup> / cp/cycle
m(P*)	=	Real Gas Potential at P*	MM psi <sup>2</sup> /cp
$m(P_f)$	=	Real Gas Potential at P <sub>f</sub>	MM psi <sup>2</sup> /cp
AOF <sub>1</sub>	=	Maximum Indicated Absolute Open Flow at Test Conditions	MCFD
AOF <sub>2</sub>	=	$\label{thm:minimum indicated} \mbox{ Absolute Open Flow at Test Conditions } \ . \ .$	MCFD
P*	=	Extrapolated Static Pressure	Psig
$P_{f}$	=	Final Flow Pressure	Psig
Q	=	Liquid Production Rate During Test	BPD
$Q_1$	=	Theoretical Liquid Production $\mathbf{w}^{j}$ Damage Removed	BPD
$Q_g$	=	Measured Gas Production Rate	MCFD
r <sub>i</sub>	=	Approximate Radius of Investigation	Ft
r <sub>w</sub>	=	Radius of Well Bore	Ft
S	=	Skin Factor	
t	=	Total Flow Time Previous to Closed-in	Minutes
$\Delta t$	=	Closed-in Time at Data Point	Minutes
Т	=	Temperature Rankine	°R
ф	=	Porosity	_
μ	=	Viscosity of Gas or Liquid	ср
Loa	=	Common Log	