Aerothermodynamic Design Sensitivities for a Reacting Gas Flow Solver on an Unstructured Mesh Using a Discrete Adjoint Formulation

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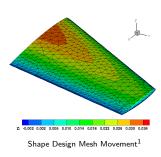
Outline

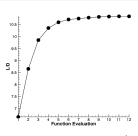
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Introduction - Design





Lift/Drag Objective Function¹

- Exploring design space using high-fidelity CFD is challenging
- zero-order methods (sampling) are prohibitively expensive
- Need to be intelligent about techniques for evaluating sensitivity to design parameters
- Gradient-based optimization much more efficient than sampling, but requires calculating sensitivity derivatives

¹Credit: FUN3D Tutorial Examples.

 \bullet > 100 design variables in OM6 wing shape optimization

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- How do you to compute sensitivity of that many DVs?

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- How do you to compute sensitivity of that many DVs?

Direct differentiation approach - Expensive

- Navier-Stokes equations can be directly differentiated to yield sensitivity derivatives necessary for gradient-based optimization
- Finite difference requires a minimum of one flow solution for each design variable sensitivity
- Prohibitively expensive for large number of design parameters

- ullet > 100 design variables in OM6 wing shape optimization
- How do you to compute sensitivity of that many DVs?

Adjoint approach - More efficient

- Solve adjoint equations in addition to Navier Stokes flow equations to obtain sensitivity derivatives
- One flow and adjoint solution needed for each cost function, regardless of number of design variables
- Considerably more efficient than direct differentiation approach for large number of design parameters

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Introduction - Design

- Adjoint-based design optimization has recieved considerable attention in compressible, perfect gas CFD solvers^{2,3}, but very little in reacting flow solvers
- Difficulty of adjoint approach lies in implementating exact linearizations for 2nd-order flux construction scheme
- Particularly difficult for reacting flows, due to
 - Complexity of linearizing the additional equations for multi-species chemical kinetics
 - Resorting to Automatic Differentiation tools incurs performance overhead that is implementation-specific⁴
 - Serious memory and computational cost concerns when simulating a large number of species

²E. J. Nielsen et al. Computers & Fluids 33.9 (2004), pp. 1131-1155.

³J. E. Peter and R. P. Dwight. Computers & Fluids 39.3 (2010), pp. 373-391.

⁴ J.-D. Müller and P. Cusdin. International Journal for Numerical Methods in Fluids 47.8-9 (2005), pp. 939–945.

Introduction - Improvement to State of the Art

- Current state of the art
 - Attempts made at both continuous⁵ and discrete⁶ adjoint formulations for a compressible reacting flow solver
 - These attempts suffer from quadratic scaling in memory and computational cost with number of species
 - Recent scheme at Barcelona Supercomputing Center⁷ is promising, but only for incompressible reacting flows
- Proposed improvement to the state of the art
 - New decoupled scheme for both hypersonic flow solver and adjoint solver that is robust for high-speed flows in chemical non-equilibrium
 - New scheme significantly improves scaling in computational cost and memory with number of species

⁵S. R. Copeland, F. Palacios, and J. J. Alonso. *52nd Aerospace Sciences Meeting*. American Institute of Aeronautics and Astronautics, 2014.

⁶B. Lockwood et al. 49th AIAA Aerospace Sciences Meeting including the New Horizons Forum and Aerospace Exposition. American Institute of Aeronautics and Astronautics, 2011.

⁷M. K. Esfahani and G. Houzeaux. 57th AIAA/ASCE/AHS/ASC Structures, Structural Dynamics, and Materials Conference. American Institute of Aeronautics and Astronautics, 2016.

Introduction - Decoupled Approach

- Reacting gas simulations require solving a large number of conservation equations
- Memory concerns
 - Size of Jacobians scales quadratically with number species in gas mixture
 - Solving system of equations in a tightly-coupled fashion can be limited by memory constraints
- Cost concerns
 - Cost of solving the linear system scales quadratically with number of species in gas mixture
- Efficiently solving adjoint problem is a primary motivator
 - Solving adjoint system particularly costly if linear solver is slow
 - ullet Can be necessary to store jacobian twice o large memory overhead

Introduction - Decoupled Approach

- Loosely-coupled solvers have become popular in the combustion community⁸
 - Decouple species conservation equations from meanflow equations, and solve two smaller systems

$$\begin{pmatrix}
\square & \square & \dots & \square \\
\square & \square & \dots & \vdots \\
\vdots & \vdots & \ddots & \vdots \\
\square & \dots & \dots & \square
\end{pmatrix}
\rightarrow
\begin{pmatrix}
\square & \dots & \square \\
\vdots & \ddots & \vdots \\
\square & \dots & \square
\end{pmatrix}$$
and
$$\begin{pmatrix}
\square & \square & \dots & \square \\
\square & \square & \dots & \vdots \\
\vdots & \vdots & \ddots & \vdots \\
\square & \dots & \square
\end{pmatrix}$$

$$(4+ns)\times(4+ns)$$

$$ns\times ns$$

 Candler, et al.⁹ originally derived this for Steger-Warming scheme, this work extends to Roe FDS scheme

⁸V. Sankaran and M. Olsen. 16th AIAA Computational Fluid Dynamics Conference. 2003.

⁹G. V. Candler, P. K. Subbareddy, and I. Nompelis. AIAA Journal 51.5 (2013), pp. 1245–1254.

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Introduction - Choice of Code and Implementation



- FUN3D chosen as code to facilitate all research presented, because
 - Excellent infrastructure for adjoint-based design analysis and optimization
 - Robust hypersonic flow solver
 - NASA Langley Research Center supporting me through the Pathways program
- Decision to pursue discrete adjoint, rather than continuous adjoint, due to current FUN3D implementation

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Fully-Coupled Point Implicit Method

- All work presented is for inviscid flows in chemical non-equilibrium, using a one-temperature model, but is extendable to viscous flows.
- Beginning with the semi-discrete form

$$rac{\partial \mathbf{U}}{\partial t} + rac{1}{V} \sum_f (\mathbf{F} \cdot \mathbf{S})^f = \mathbf{W}$$

$$\mathbf{U} = \begin{pmatrix} \rho_{1} \\ \vdots \\ \rho_{ns} \\ \rho u \\ \rho v \\ \rho w \\ \rho E \end{pmatrix}, \quad \mathbf{F} \cdot \mathbf{S} = \begin{pmatrix} \rho_{1} \overline{U} \\ \vdots \\ \rho_{ns} \overline{U} \\ \rho u \overline{U} + p s_{x} \\ \rho u \overline{U} + p s_{y} \\ \rho u \overline{U} + p s_{z} \\ (\rho E + p) \overline{U} \end{pmatrix} S, \quad \mathbf{W} = \begin{pmatrix} \dot{\rho}_{1} \\ \vdots \\ \dot{\rho}_{ns} \\ 0 \\ 0 \\ 0 \\ 0 \end{pmatrix}$$

Fully-Coupled Point Implicit Method

• Using the Roe FDS scheme to compute the inviscid flux at the face, \mathbf{F}^f , and linearizing the system results in

$$\frac{\delta \mathbf{U}^n}{\Delta t} + \frac{1}{V} \sum_{f} \left(\frac{\partial \mathbf{F}^f}{\partial \mathbf{U}^L} \delta \mathbf{U}^L + \frac{\partial \mathbf{F}^f}{\partial \mathbf{U}^R} \delta \mathbf{U}^R \right)^n \mathbf{S}^f - \frac{\partial \mathbf{W}}{\partial \mathbf{U}} \delta \mathbf{U}^n \\
= -\frac{1}{V} \sum_{f} (\mathbf{F}^f \cdot \mathbf{S}^f)^n + \mathbf{W}^n$$

Which can be thought of more simply as

$$\mathbf{A}\mathbf{u} = \mathbf{b}$$

$$\mathbf{A}
ightarrow rac{(4+ns) imes (4+ns)}{\mathsf{Jacobian Block}}$$

$$\mathbf{b}
ightarrow rac{(4+ns) imes 1}{\mathsf{Residual}}$$

Fully-Coupled Point Implicit Method

- Constructing the Jacobian in a fully-coupled fashion results in large, dense block matricies
- Using a stationary iterative method (i.e., Gauss-Seidel, SSOR, etc.), work is dominated by matrix-vector products

$$Cost \rightarrow O((4 + ns)^2)$$

 Leads to onerous quadratic scaling with respect to number of species

- The main idea is to separate the meanflow and species composition equations, adding a new equation for the total mixture density
- Leads to two sets of conserved variables

$$\mathbf{U}' = \begin{pmatrix} \rho \\ \rho u \\ \rho v \\ \rho w \\ \rho E \end{pmatrix} \qquad \hat{\mathbf{U}} = \begin{pmatrix} \rho_1 \\ \vdots \\ \rho_{ns} \end{pmatrix}$$

Meanflow Species Composition

- The fluxes are solved in two sequential steps
 - The mixture fluxes are first solved as

$$\frac{\partial \mathbf{U}'}{\partial t} + \frac{1}{V} \sum_{f} (\mathbf{F}' \cdot \mathbf{S})^{f} = 0$$

Followed by the species fluxes

$$rac{\partial \hat{\mathbf{U}}}{\partial t} + rac{1}{V} \sum_{f} (\hat{\mathbf{F}} \cdot \mathbf{S})^{f} = \hat{\mathbf{W}}$$

• Since the mixture density was determined in the first step, step two actually solves for the species mass fractions

$$\delta \hat{\mathbf{U}}^n = \rho^{n+1} \hat{\mathbf{V}}^{n+1} - \rho^n \hat{\mathbf{V}}^n = \rho^{n+1} \delta \hat{\mathbf{V}}^n + \hat{\mathbf{V}}^n \delta \rho^n$$
$$\hat{\mathbf{V}} = (c_1, \dots, c_{ns})^T, c_s = \rho_s/\rho$$

The Roe FDS scheme species mass fluxes can be rewritten as

$$\hat{\mathbf{F}}_{\rho_s} = c_s \mathbf{F}'_{\rho} + (c_s^L - \tilde{c}_s) \rho^L \lambda^+ + (c_s^R - \tilde{c}_s) \rho^R \lambda^-$$

$$\frac{\partial \hat{\mathbf{F}}_{\rho_s}}{\partial c_s^L} = w \mathbf{F}_{\rho} + (1 - w) \rho^L \lambda^+ - w \rho^R \lambda^-$$

$$\frac{\partial \hat{\mathbf{F}}_{\rho_s}}{\partial c_s^R} = (1 - w) \mathbf{F}_{\rho} + (w - 1) \rho^L \lambda^+ + w \rho^R \lambda^-$$

Jacobian Approximations

Step 1:
$$\frac{\partial \mathbf{F}}{\partial \mathbf{U}'}\Big|_{\hat{\mathbf{V}}} = 5 \times 5 \text{ Roe FDS Jacobian}$$
Step 2:
$$\frac{\partial \mathbf{F}}{\partial \hat{\mathbf{V}}}\Big|_{\hat{\mathbf{U}}'} = \begin{pmatrix} \frac{\partial F_{\rho_1}}{\partial c_1} & 0 \\ & \ddots & \\ 0 & & \frac{\partial F_{\rho_{ns}}}{\partial c_{ns}} \end{pmatrix}$$

Chemical source term linearized via

$$\hat{\mathbf{W}}^{n+1} = \hat{\mathbf{W}}^n + \frac{\partial \hat{\mathbf{W}}}{\partial \mathbf{U}} \Big|_{\mathbf{U}'} \frac{\partial \mathbf{U}}{\partial \hat{\mathbf{V}}}$$
$$\mathbf{C} = \frac{\partial \hat{\mathbf{W}}}{\partial \mathbf{U}} \Big|_{\mathbf{U}'} \frac{\partial \mathbf{U}}{\partial \hat{\mathbf{V}}}$$

• Full system to be solved in step two

$$\rho^{n+1} \frac{\delta \hat{\mathbf{V}}^{n}}{\Delta t} + \frac{1}{V} \sum_{f} (\frac{\partial \hat{\mathbf{F}}^{f}}{\partial \mathbf{V}^{L}} \delta \mathbf{V}^{L} + \frac{\partial \hat{\mathbf{F}}^{f}}{\partial \hat{\mathbf{V}}^{R}} \delta \hat{\mathbf{V}}^{R})^{n,n+1} \mathbf{S}^{f} - \mathbf{C}^{n,n+1} \delta \mathbf{V}^{n}$$

$$= -\frac{1}{V} \sum_{f} (\hat{\mathbf{F}}^{n,n+1} \cdot \mathbf{S})^{f} + \mathbf{W}^{n,n+1} - \hat{\mathbf{V}}^{n} \frac{\delta \rho^{n}}{\Delta t} - R_{\rho}$$

$$R_{\rho} = -\frac{1}{V} \sum_{f} \sum_{s} (\hat{F}^{n,n+1}_{\rho_{s}} \cdot \mathbf{S})$$

• R_{ρ} is included to preserve $\sum_{s} c_{s} = 1$, $\sum_{s} \delta c_{s} = 0$.

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Cost and Memory Savings of the Decoupled Flow Solver

- Most significant savings comes from the source term linearization being purely node-based
 - Convective contributions to block Jacobians are diagonal
 - Source term jacobian is dense block Jacobian
 - In the global system (w/chemistry), all off-diagonal block jacobians are diagonal

$$\begin{pmatrix}
\Box & & & \\
& \ddots & & \\
& & \Box & & \\
& & & \ddots & \\
& & & & \Box
\end{pmatrix}
\begin{pmatrix}
\delta \hat{\mathbf{V}}_1 \\
\vdots \\
\delta \hat{\mathbf{V}}_i \\
\vdots \\
\delta \hat{\mathbf{V}}_{nodes}
\end{pmatrix} = \begin{pmatrix}
\hat{b}_1 \\
\vdots \\
\hat{b}_i \\
\vdots \\
\hat{b}_{nodes}
\end{pmatrix} - \begin{pmatrix}
(\sum_{j=1}^{N_{nb}} [\setminus] \delta \hat{\mathbf{V}}_j)_1 \\
\vdots \\
(\sum_{j=1}^{N_{nb}} [\setminus] \delta \hat{\mathbf{V}}_j)_i \\
\vdots \\
(\sum_{j=1}^{N_{nb}} [\setminus] \delta \hat{\mathbf{V}}_j)_{nodes}
\end{pmatrix}$$

• Matrix-vector products o inner products: $O(ns^2) o O(ns)$

Cost and Memory Savings of the Decoupled Flow Solver

Comparing size of Jacobian systems, using Compressed Row Storage

$$\mathbf{A}_d = \mathsf{Decoupled}$$
 system Jacobians $\mathbf{A} = \mathsf{Fully\text{-}coupled}$ system Jacobians

Relative Memory Cost =
$$\frac{size(\mathbf{A}_d)}{size(\mathbf{A})}$$

= $\lim_{ns \to \infty} \frac{(ns^2 + 5^2)(N_{nodes}) + (ns + 5^2)(N_{nbrs})}{(ns + 4)^2(N_{nodes} + N_{nbrs})}$
= $\frac{N_{nodes}}{N_{nodes} + N_{nbrs}}$

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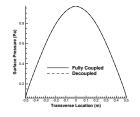
Numerical Results: 2D Cylinder

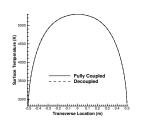


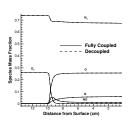
- Fully-coupled and decoupled methods both implemented in the Generic Gas Path of FUN3D
- Tested on 2D cylinder case
 - $V_{\infty}=5000$ m/s, $\rho_{\infty}=0.001$ kg/m³, and $T_{\infty}=200$ K
- Inviscid flow, with 1-Temperature model

Numerical Results: 2D Cylinder

- Verification of implementation
 - 5-species air model: N, N₂, O, O₂, and NO with five reactions

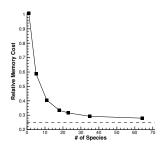


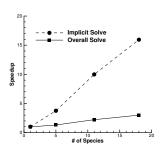




 Surface pressure, surface temperature, and mass fractions on stagnation line agree between decoupled and fully coupled implementations

Numerical Results: 2D Cylinder





- On structured grids $N_{nbrs} \approx 6 N_{nodes}$
 - Half precision off-diagonal $N_{nbrs} = \frac{6N_{nodes}}{2}$

Memory Cost
$$\approx \frac{N_{nodes}}{N_{nodes} + N_{nbrs}} = \frac{N_{nodes}}{N_{nodes} + 6N_{nodes}/2} = \frac{1}{4}$$

• Linear speedup in solver: $\frac{O(ns^2)}{O(ns)} = O(ns)$

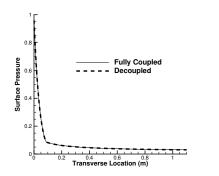
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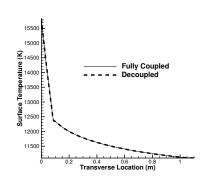
Numerical Results: Axisymmetric Spherically Capped Cone



- Verify that the decoupled scheme is robust at high velocities
 - $V_{\infty} = 15000 \text{ m/s}, \ \rho_{\infty} = 0.001 \text{ kg/m}^3, \ T_{\infty} = 200 \text{ K}.$
 - 11-species air model N, N₂, O, O₂, NO, N⁺, N₂⁺, O⁺, O₂⁺, NO⁺, and electrons, with 22 possible reactions.
 - Inviscid flow, with 1-Temperature model

Numerical Results: Axisymmetric Spherically Capped Cone

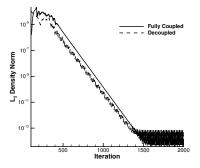


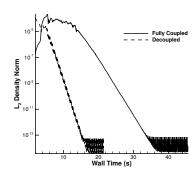


• Surface pressure and surface temperature agree between decoupled and fully coupled implementations

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Numerical Results: Axisymmetric Spherically Capped Cone





- Necessary to scale source term magnitude by $0.001 \le w \le 1$ for the first 500 iterations, due to extreme reaction rates
- Both schemes converge in a similar number of iterations
- Decoupled scheme $\approx 2x$ faster

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 The derivation of the adjoint approach to compute design sensitivities begins with forming the Lagrangian and differentiating with respect to the design variables

$$L(\mathbf{D}, \mathbf{Q}, \mathbf{X}, \mathbf{\Lambda}) = f(\mathbf{D}, \mathbf{Q}, \mathbf{X}) + \mathbf{\Lambda}^T \mathbf{R}(\mathbf{D}, \mathbf{Q}, \mathbf{X})$$

D = design variables

f = cost function

 $\mathbf{Q} = \mathsf{flow} \; \mathsf{variables}$

 $\mathbf{R} = \mathsf{flow} \; \mathsf{residual}$

X =computational grid

 $\Lambda = \text{costate variables}$

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$$\frac{\partial L}{\partial \mathbf{D}} = \left\{ \frac{\partial f}{\partial \mathbf{D}} + \left[\frac{\partial \mathbf{X}}{\partial \mathbf{D}} \right]^T \frac{\partial f}{\partial \mathbf{X}} \right\} + \left[\frac{\partial \mathbf{Q}}{\partial \mathbf{D}} \right]^T \left\{ \frac{\partial f}{\partial \mathbf{Q}} + \left[\frac{\partial \mathbf{R}}{\partial \mathbf{Q}} \right]^T \mathbf{\Lambda} \right\}$$

$$+ \left\{ \left[\frac{\partial \mathbf{R}}{\partial \mathbf{D}} \right]^T + \left[\frac{\partial \mathbf{X}}{\partial \mathbf{D}} \right]^T \left[\frac{\partial \mathbf{R}}{\partial \mathbf{X}} \right]^T \right\} \mathbf{\Lambda}$$

 $\mathbf{D} = \mathsf{design} \ \mathsf{variables}$

f = cost function

 $\mathbf{Q} = \text{flow variables}$

 $\mathbf{R} = \text{flow residual}$

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$$+ \left\{ \left[\frac{\partial \mathbf{R}}{\partial \mathbf{D}} \right]^T + \left[\frac{\partial \mathbf{X}}{\partial \mathbf{D}} \right]^T \left[\frac{\partial \mathbf{R}}{\partial \mathbf{X}} \right]^T \right\} \mathbf{\Lambda}$$

D = design variables

f = cost function

 $\mathbf{Q} = \text{flow variables}$

 $\mathbf{R} = \text{flow residual}$

X =computational grid $\Lambda =$ costate variables

- Need to eliminate flow variable dependence on design variables, $\frac{\partial \mathbf{Q}}{\partial \mathbf{D}}$
- Adjoint equation

$$\left[\frac{\partial \mathbf{R}}{\partial \mathbf{Q}}\right]^T \mathbf{\Lambda} = -\frac{\partial f}{\partial \mathbf{Q}}$$

ullet Solve for $oldsymbol{\Lambda}$ and compute sensitivity derivatives

$$\frac{\partial L}{\partial \mathbf{D}} = \left\{ \frac{\partial f}{\partial \mathbf{D}} + \left[\frac{\partial \mathbf{X}}{\partial \mathbf{D}} \right]^T \frac{\partial f}{\partial \mathbf{X}} \right\} + \left\{ \left[\frac{\partial \mathbf{R}}{\partial \mathbf{D}} \right]^T + \left[\frac{\partial \mathbf{X}}{\partial \mathbf{D}} \right]^T \left[\frac{\partial \mathbf{R}}{\partial \mathbf{X}} \right]^T \right\} \mathbf{\Lambda}$$

Fully Coupled Iterative Method

Adjoint problem is a linear system

$$\begin{pmatrix} \frac{\partial \mathbf{R}_{\rho_{i}}}{\partial \rho_{j}}^{T} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho_{j}}^{T} & \frac{\partial \mathbf{R}_{\rho E}}{\partial \rho_{j}}^{T} \\ \frac{\partial \mathbf{R}_{\rho_{i}}}{\partial \rho_{\mathbf{u}}}^{T} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho_{\mathbf{u}}}^{T} & \frac{\partial \mathbf{R}_{\rho E}}{\partial \rho_{\mathbf{u}}}^{T} \\ \frac{\partial \mathbf{R}_{\rho_{i}}}{\partial \rho_{\mathbf{E}}}^{T} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho_{\mathbf{E}}}^{T} & \frac{\partial \mathbf{R}_{\rho E}}{\partial \rho_{\mathbf{E}}}^{T} \end{pmatrix} \begin{pmatrix} \mathbf{\Lambda}_{\rho_{i}} \\ \mathbf{\Lambda}_{\rho \mathbf{u}} \\ \mathbf{\Lambda}_{\rho \mathbf{E}} \end{pmatrix} = - \begin{pmatrix} \frac{\partial f}{\partial \rho_{i}} \\ \frac{\partial f}{\partial \rho_{i}} \\ \frac{\partial f}{\partial \rho_{\mathbf{E}}} \end{pmatrix}$$

 Can be solved with Krylov method (i.e. GMRES), but time marching similar to flow solver shown to be more robust

$$\left(\frac{V}{\Delta t}\mathbf{I} + \frac{\partial \mathbf{R}_1}{\partial \mathbf{Q}}^T\right) \Delta \Lambda = -\frac{\partial f}{\partial \mathbf{Q}} - \frac{\partial \mathbf{R}_2}{\partial \mathbf{Q}}^T \Lambda$$

 Straightforward to formulate, but cost and memory requirements scale quadratically with number of species

Decoupled Iterative Method

Rewrite conserved variables similar to decoupled flow solver

$$\begin{pmatrix} \frac{\partial \mathbf{R}_{\rho}}{\partial \rho}^{T} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho}^{T} & \frac{\partial \mathbf{R}_{\rho E}}{\partial \rho}^{T} & \frac{\partial \mathbf{R}_{\rho s}}{\partial \rho}^{T} \\ \frac{\partial \mathbf{R}_{\rho}}{\partial \rho \mathbf{u}}^{T} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho \mathbf{u}}^{T} & \frac{\partial \mathbf{R}_{\rho E}}{\partial \rho \mathbf{u}}^{T} & \frac{\partial \mathbf{R}_{\rho s}}{\partial \rho \mathbf{u}}^{T} \\ \frac{\partial \mathbf{R}_{\rho}}{\partial \rho E}^{T} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho E}^{T} & \frac{\partial \mathbf{R}_{\rho E}}{\partial \rho E}^{T} & \frac{\partial \mathbf{R}_{\rho s}}{\partial \rho E}^{T} \\ \frac{\partial \mathbf{R}_{\rho}}{\partial c_{s}}^{T} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial c_{s}}^{T} & \frac{\partial \mathbf{R}_{\rho E}}{\partial c_{s}}^{T} & \frac{\partial \mathbf{R}_{\rho s}}{\partial c_{s}}^{T} \end{pmatrix} \begin{pmatrix} \Lambda_{\rho} \\ \Lambda_{\rho \mathbf{u}} \\ \Lambda_{\rho E} \\ \Lambda_{c_{s}} \end{pmatrix} = -\begin{pmatrix} \frac{\partial f}{\partial \rho} \\ \frac{\partial f}{\partial \rho \mathbf{u}} \\ \frac{\partial f}{\partial \rho E} \\ \frac{\partial f}{\partial c_{s}} \end{pmatrix}$$

Decoupled Iterative Method

Rewrite conserved variables similar to decoupled flow solver

$$\begin{pmatrix} \frac{\partial \mathbf{R}_{\rho}}{\partial \rho}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho E}}{\partial \rho}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho s}}{\partial \rho}^{\mathsf{T}} \\ \frac{\partial \mathbf{R}_{\rho}}{\partial \rho \mathbf{u}}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho \mathbf{u}}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho E}}{\partial \rho \mathbf{u}}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho s}}{\partial \rho \mathbf{u}}^{\mathsf{T}} \\ \frac{\partial \mathbf{R}_{\rho}}{\partial \rho E}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho E}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho E}}{\partial \rho E}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho s}}{\partial \rho E}^{\mathsf{T}} \\ \frac{\partial \mathbf{R}_{\rho}}{\partial c_{s}}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial c_{s}}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho E}}{\partial c_{s}}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho s}}{\partial c_{s}}^{\mathsf{T}} \end{pmatrix} = - \begin{pmatrix} \frac{\partial f}{\partial \rho} \\ \frac{\partial f}{\partial \rho} \\ \frac{\partial f}{\partial \rho \mathbf{u}} \\ \end{pmatrix}$$

- Recognize that there is an analogue to the species mass equation decoupling used in the flow solver
- Linear system can be decomposed as block jacobi scheme

Decoupled Iterative Method

• Separate into two systems and solve as block jacobi scheme

$$\left(\frac{V}{\Delta t}\mathbf{I} + \frac{\partial \mathbf{R}_{\rho_{s}}}{\partial c_{s}}^{\mathsf{T}}\right) \Delta \Lambda_{c_{s}} = -\frac{\partial f}{\partial c_{s}} - \frac{\partial \mathbf{R}_{\rho_{s}}}{\partial c_{s}}^{\mathsf{T}} \Lambda_{c_{s}} - \frac{\partial \mathbf{R}_{\rho_{s}}}{\partial \rho}^{\mathsf{T}} \Lambda_{\rho} - \frac{\partial \mathbf{R}_{\rho_{s}}}{\partial \rho \mathbf{u}}^{\mathsf{T}} \Lambda_{\rho \mathbf{u}} - \frac{\partial \mathbf{R}_{\rho_{s}}}{\partial \rho \mathcal{E}}^{\mathsf{T}} \Lambda_{\rho \mathcal{E}}$$

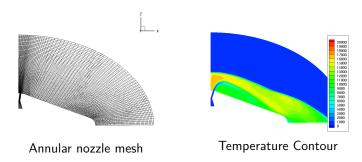
$$\begin{bmatrix} \frac{V}{\Delta t} \mathbf{I} + \begin{pmatrix} \frac{\partial \mathbf{R}_{\rho}}{\partial \rho}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho}}{\partial \rho \mathbf{u}}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho}}{\partial \rho \mathbf{E}}^{\mathsf{T}} \\ \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho \mathbf{u}}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho \mathbf{E}}^{\mathsf{T}} \end{pmatrix} \begin{pmatrix} \Delta \Lambda_{\rho} \\ \Delta \Lambda_{\rho \mathbf{u}} \end{pmatrix} = \\ - \begin{pmatrix} \frac{\partial \mathbf{f}}{\partial \rho} \\ \frac{\partial \mathbf{f}}{\partial \rho \mathbf{u}} \end{pmatrix} - \begin{pmatrix} \frac{\partial \mathbf{R}_{\rho}}{\partial \rho}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho} \mathbf{E}}{\partial \rho \mathbf{E}}^{\mathsf{T}} \\ \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho \mathbf{u}}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho}}{\partial \rho \mathbf{E}}^{\mathsf{T}} \\ \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho \mathbf{u}}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho \mathbf{u}}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho \mathbf{E}}^{\mathsf{T}} \end{pmatrix} \begin{pmatrix} \Lambda_{\rho} \\ \Lambda_{\rho \mathbf{u}} \end{pmatrix} - \begin{pmatrix} \frac{\partial \mathbf{R}_{\rho}}{\partial c_{s}}^{\mathsf{T}} \\ \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial c_{s}}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho \mathbf{u}}^{\mathsf{T}} & \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial \rho \mathbf{E}}^{\mathsf{T}} \end{pmatrix} \begin{pmatrix} \Lambda_{\rho} \\ \Lambda_{\rho \mathbf{u}} \end{pmatrix} - \begin{pmatrix} \frac{\partial \mathbf{R}_{\rho}}{\partial c_{s}}^{\mathsf{T}} \\ \frac{\partial \mathbf{R}_{\rho \mathbf{u}}}{\partial c_{s}}^{\mathsf{T}} \end{pmatrix} \Lambda_{c_{s}}$$

Outline

- Introduction
- 2 Flow Solver
 - Fully-Coupled Method
 - Decoupled Method
- Cost and Memory Savings
 - Cost and Memory Savings of the Decoupled Flow Solver
 - Numerical Results: 2D Cylinder
 - Numerical Results: Axisymmetric Spherically Capped Cone
- 4 Adjoint Solver
 - Derivation of Discrete Adjoint Formulation
 - Fully Coupled Iterative Method
 - Decoupled Iterative Method
- Design Problem
- 6 Concluding Remarks

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Design Problem: Hypersonic Retro Propulsion Vehicle



- Apply adjoint to design Reaction Control System (RCS) jet system to shape shock interaction to maintain maximum drag at minimum surface temperature
- This annular nozzle configuration has been shown to have a steady solution for inviscid flow

Design Problem: Parameterization

Design sensitivities given by

$$\frac{\partial L}{\partial \mathbf{D}} = \left\{ \frac{\partial f}{\partial \mathbf{D}} + \left[\frac{\partial \mathbf{X}}{\partial \mathbf{D}} \right]^T \frac{\partial f}{\partial \mathbf{X}} \right\} + \left\{ \left[\frac{\partial \mathbf{R}}{\partial \mathbf{D}} \right]^T + \left[\frac{\partial \mathbf{X}}{\partial \mathbf{D}} \right]^T \left[\frac{\partial \mathbf{R}}{\partial \mathbf{X}} \right]^T \right\} \mathbf{\Lambda}$$

- Define cost functions => *f*
 - Total vehicle drag (with and without jet thrust contribution)
 - Total vehicle surface temperature (in lieu of heating, since these are inviscid simulations)
- Define design parameters => D
 - Plenum pressure
 - Plenum temperature
 - Jet placement and geometry
- Define mesh parameters => X
 - Custom grid generation utility
 - Faciliate all grid dependencies by wrapping in complex variables

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Design Problem: Grid Generation and Governing Equations

- Grid generation tool provides straightforward way to get mesh sensitivities
 - All parameters can be perturbed by a complex source term, and jacobian calculated via frechet derivatives
 - Structured mesh generation is fast and robust
 - Easy to convert to unstructured grid accepted by FUN3D
- Propose to limit research to inviscid flow, due to large jump in complexity going to full Navier-Stokes
 - Decoupled approach changes very little with addition of viscous terms
 - Viscous terms considerably more exhausting to implement
 - Grid generation process significantly more complicated
 - Scope of research is to demonstrate the new decoupled formulation for flow and adjoint solvers

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Concluding Remarks - Summary of work

Completed work

- Derivation of decoupled method for Roe FDS in adjoint and flow solver
- Implementation/verification of decoupled scheme in flow solver
- Exact linearization of 2nd-order Roe FDS scheme and chemical source term for both fully coupled and decoupled methods
- Implementation of fully coupled adjoint scheme for inviscid flow

Proposed work

- Implementation of decoupled adjoint scheme
- Optimization of Hypersonic Retro Propulsion configuration using fully coupled and decoupled schemes for inviscid flow and adjoint solvers

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Concluding Remarks

- Design problem provides good testbed for a truly unique hypersonic application
 - Parameterization is well defined
 - Non-linearity of design space is a concern
 - Optimal steady solution exists?
- Decoupling the species equations yield impressive benefits at minimal cost in robustness
 - 2 times faster and 1/3 required memory for both 2D Cylinder and Sphere-Cone 11-species cases
 - Convergence issues at very high velocities can be offset by scaling source term as solution progresses
- Decoupled adjoint approach is a significant improvement to the state of the art
 - Preliminary testing has shown that memory overhead in adjoint is significantly reduced with decoupled scheme
 - Can expect speedup in adjoint solve similar to flow solve

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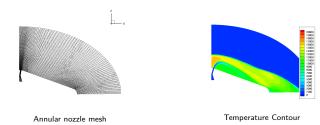
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Design Problem: Hypersonic Retro Propulsion Vehicle



- Benefits of using RCS jet shape shock interaction to maintain maximum drag at minimum surface temperature
 - Lower total mass: Jet propellent mass is less than equivalent TPS material required
 - Lower surface temperature: Jet stream "shrouds" surface in cooler pocket
 - Higher total drag: Jet could propel combustable gas (i.e. methane) to ignite in shock layer and increase drag

 For the Roe flux difference splitting scheme, the species mass fluxes are given by

$$F_{\rho_s} = \frac{\rho_s^L \mathbf{U}^L + \rho_s^R \mathbf{U}^R}{2} - \frac{\tilde{c}_s(\lambda_1 dv_1 + \lambda_2 dv_2) + \lambda_3 dv_{3_s}}{2}$$

$$dv_1 = \frac{p^R - p^L + \tilde{\rho}\tilde{a}(\mathbf{U}^R - \mathbf{U}^L)}{\tilde{a}^2}$$

$$dv_2 = \frac{p^R - p^L - \tilde{\rho}\tilde{a}(\mathbf{U}^R - \mathbf{U}^L)}{\tilde{a}^2}$$

$$dv_{3_s} = \frac{\tilde{a}^2(\rho_s^R - \rho_s^L) - \tilde{c}_s(p^R - p^L)}{\tilde{a}^2}$$

$$\lambda_1 = \mid \tilde{\mathbf{U}} + \tilde{a} \mid, \quad \lambda_2 = \mid \tilde{\mathbf{U}} - \tilde{a} \mid, \quad \lambda_3 = \mid \tilde{\mathbf{U}} \mid$$

• The notation signifies a Roe-averaged quantity

$$\tilde{\mathbf{U}} = wU^{L} + (1 - w)\mathbf{U}^{R}$$

$$w = \frac{\tilde{\rho}}{\tilde{\rho} + \rho^{R}}$$

$$\tilde{\rho} = \sqrt{\rho^{R} \rho^{L}}$$

The species mass fluxes must sum to the total mass flux

$$F_{\rho} = \sum_{s} F_{\rho_s} = \frac{\rho^L \mathbf{U}^L + \rho^R \mathbf{U}^R}{2} - \frac{\tilde{c}_s(\lambda_1 dv_1 + \lambda_2 dv_2) + \lambda_3 dv_3}{2}$$
$$dv_3 = \frac{\tilde{a}^2(\rho^R - \rho^L) - (\rho^R - \rho^L)}{\tilde{a}^2}$$

• Substituting back into species mass flux equation

$$F_{\rho_s} = \tilde{c}_s F_{\rho} + \frac{(c_s^L - \tilde{c}_s)\rho^L(\mathbf{U}^L + \mid \tilde{\mathbf{U}}\mid)}{2} + \frac{(c_s^R - \tilde{c}_s)\rho^R(\mathbf{U}^R - \mid \tilde{\mathbf{U}}\mid)}{2}$$

 This can be simplified to yield a form similar to that derived by Candler, et. al for the Steger-Warming scheme

$$F_{\rho_s} = \tilde{c}_s F_{\rho} + (c_s^L - \tilde{c}_s) \rho^L \lambda^+ + (c_s^R - \tilde{c}_s) \rho^R \lambda^-$$
$$\lambda^+ = \frac{\mathbf{U}^L + |\tilde{\mathbf{U}}|}{2}, \quad \lambda^- = \frac{\mathbf{U}^R - |\tilde{\mathbf{U}}|}{2}$$

• Differentiating with respect to the mass fraction, c_s , the left and right state contributions are

$$\frac{\partial F_{\rho_s}}{\partial c_s^L} = wF_{\rho} + (1 - w)\rho^L \lambda^+ - w\rho^R \lambda^-$$

$$\frac{\partial F_{\rho_s}}{\partial c_s^R} = (1 - w)F_{\rho} + (w - 1)\rho^L \lambda^+ + w\rho^R \lambda^-$$

Again, where w is the Roe-averaged density weighting

$$w = \frac{\tilde{\rho}}{\tilde{\rho} + \rho^R}, \quad \tilde{\rho} = \sqrt{\rho^R \rho^L}$$