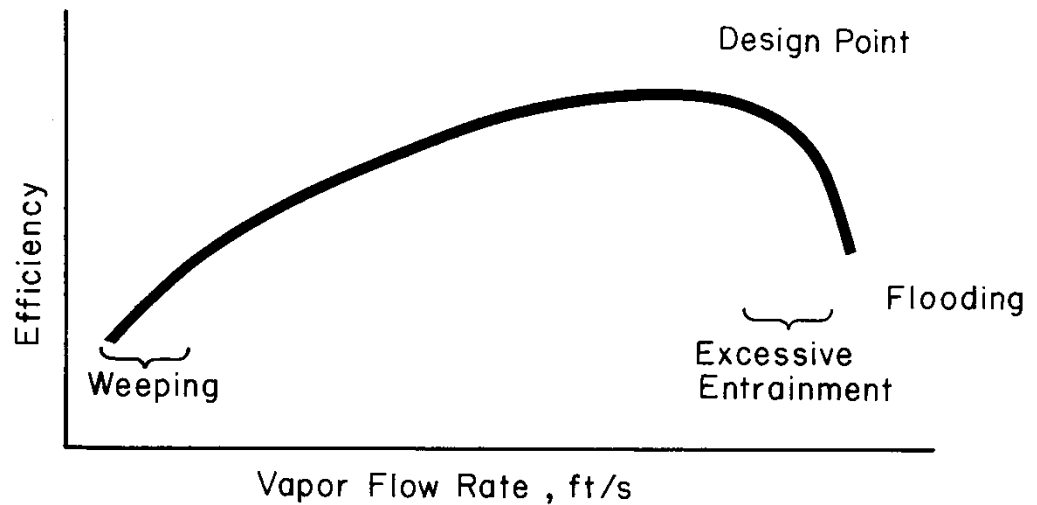


# Distillation Design 3: Review

- Tray operation
  - Entrainment
  - Flooding
  - Turn down ratio
  - Tray efficiency
  - Weeping
  - Weir
  - Downcomer
  - Downcomer flooding (less common than entrainment flooding)
  - Valve, sieve and bubble cap trays
- Column diameter



# Diameter Calculation

$$Dia = \sqrt{\frac{4VRT}{\pi\eta(3600)p(fraction)u_{flood}}}, \text{ ft} \quad \text{Eq. 10-16}$$

V in lbmol/h

T in K

R in  $\frac{\text{atm ft}^3}{\text{K lbmol}}$

p in atm

u in ft/s

$\eta$  is fraction of tray that is active (unitless)

(fraction) is the fraction of flooding (unitless)

$$u_{flood} = C_{sb,f} \left(\frac{\sigma}{20}\right)^{0.2} \sqrt{\frac{\rho_L - \rho_v}{\rho_v}}, \text{ ft/s} \quad \text{Eq. 10-8}$$

# Diameter Calculation

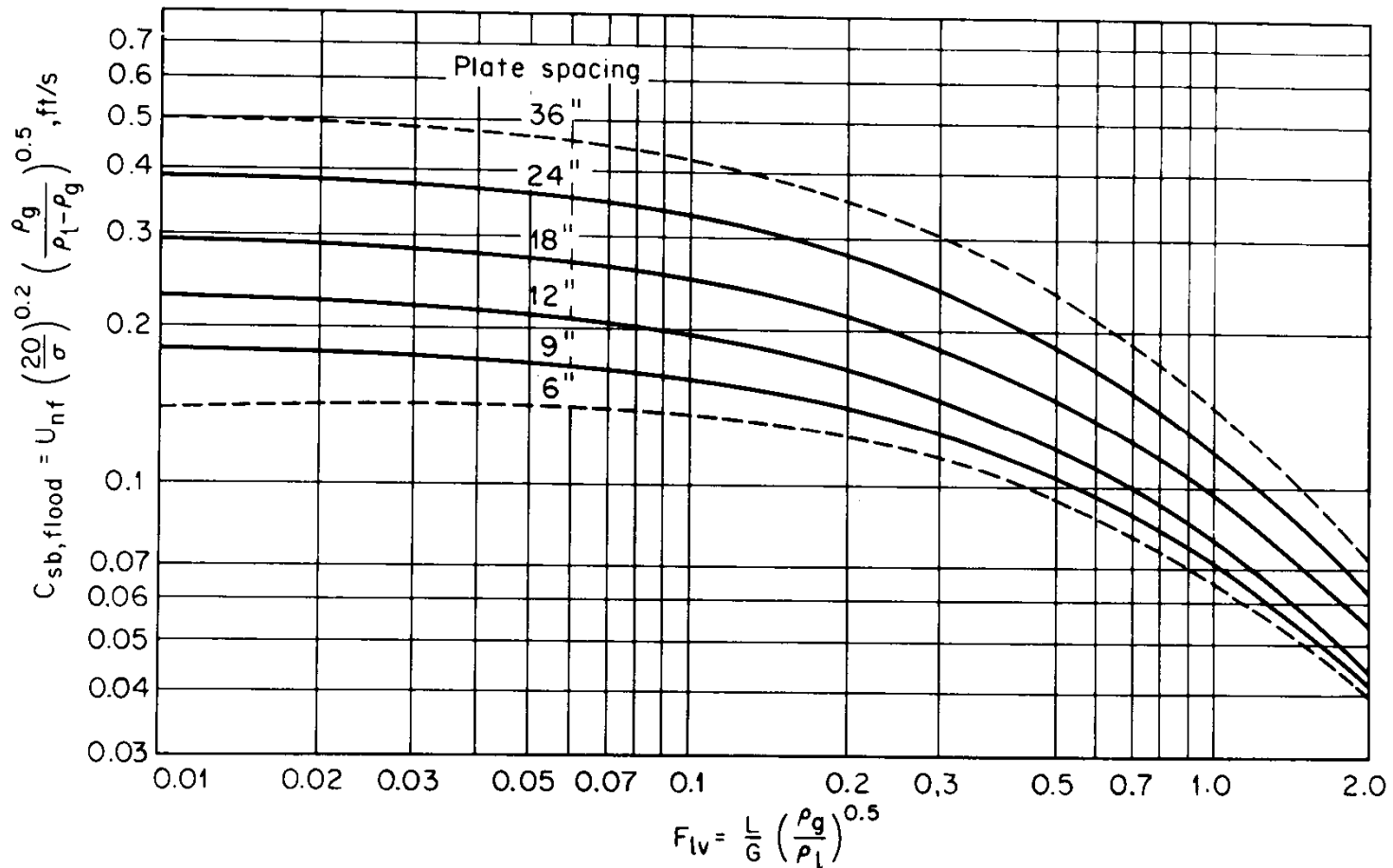


Figure 10-16 Capacity factor for flooding of sieve trays from Fair and Matthews (1958).

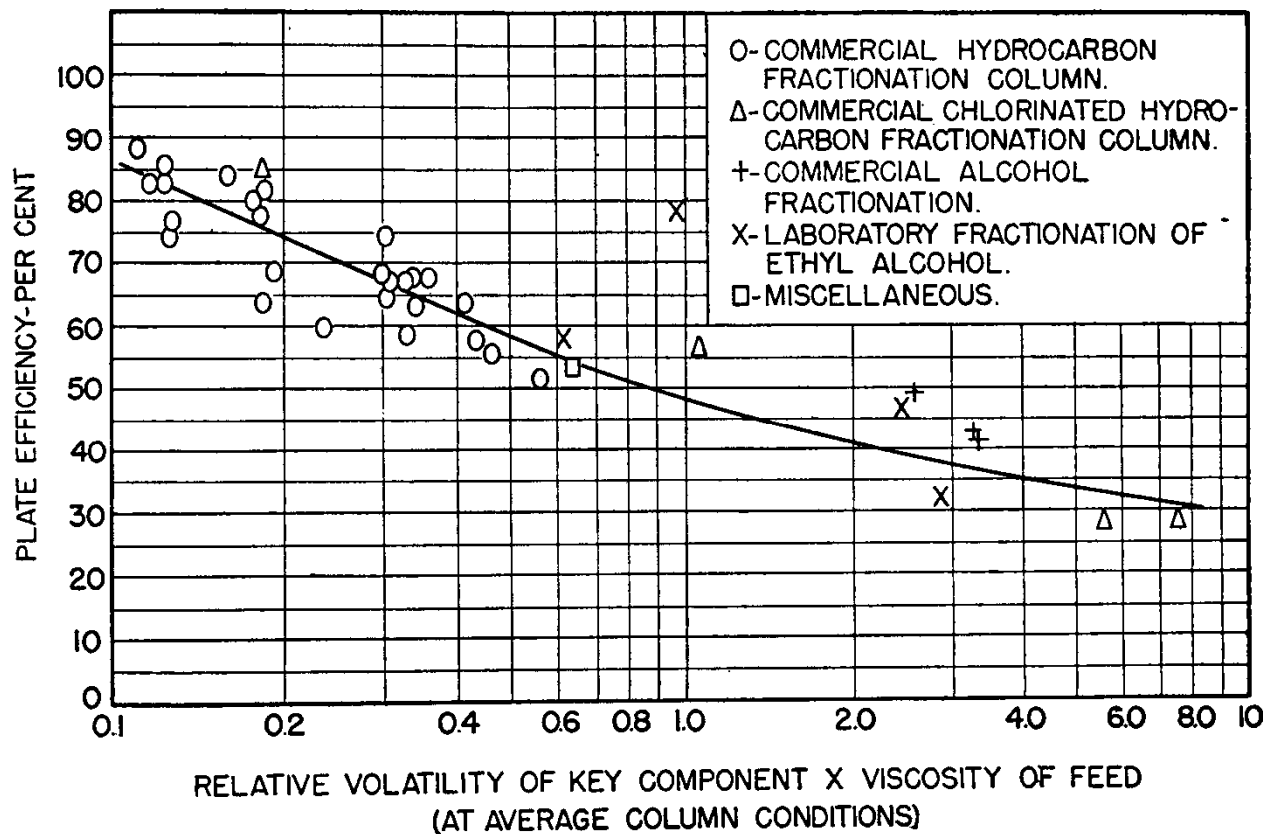
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# Overall Efficiency

- O'Connell correlation (in absence of data based on experience with similar columns)

$$E_o = 0.52782 - 0.27511 \log_{10}(\alpha\mu) + 0.044923 [\log_{10}(\alpha\mu)]^2$$



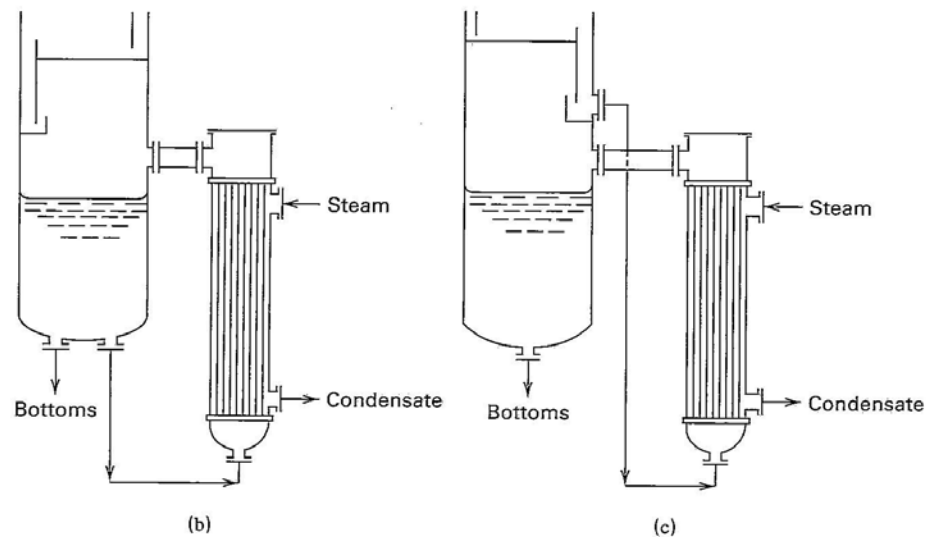
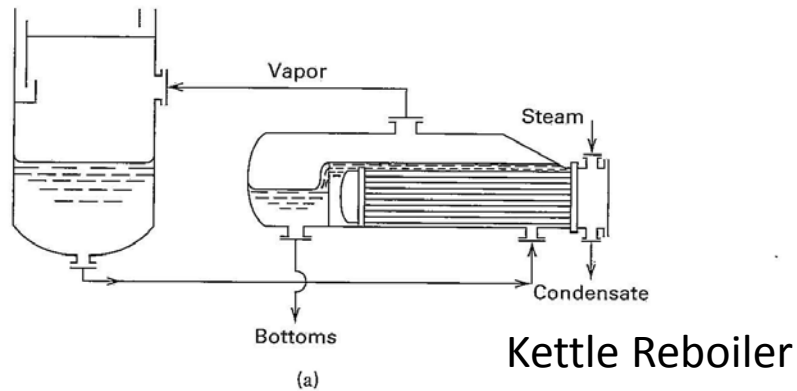
$$E_o = \frac{N_{equil}}{N_{actual}}$$

# Tray Sizing on Simulator

# Tray Efficiency

- Can calculate as part of tray sizing
- Can also estimate from “first principles”
- Possible to include as part of distillation simulation
  - Manual entry of individual tray efficiencies- does not appear to be coupled to efficiency calculation in ChemCAD (under convergence menu)
  - Calculation assuming mass transfer control rather than equilibrium

# Types of Equipment



Thermosyphon Reboilers



# Impact of Pressure

- Vapor density increases with pressure
- $T$  increases with pressure
- $u_{\text{flood}}$  decreases with pressure
- **Net result:** Column diameter decreases with increasing pressure
- Cost of column actually lower for pressures below 6 bar; modestly higher for pressures up to 20 bar.



# Economic Trade-offs

- Capital costs vs. operating costs

