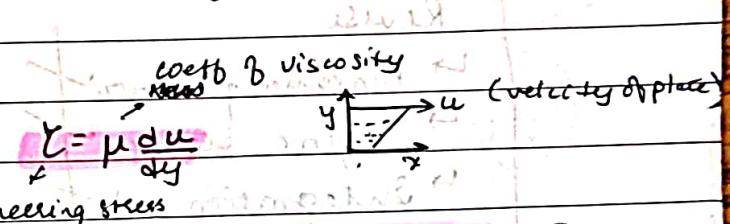


# Fluid Mechanics (8.5f)

- Continuum hypothesis
- Isotropic fluids  $\rightarrow \leftarrow$  same prop from all dir's
- $\lim_{\delta v \rightarrow 0} \frac{\delta m}{\delta v} = \rho \rightarrow$  density  $= \rho = \frac{m}{v}$
- $\lim_{\delta A \rightarrow 0} \frac{\delta F}{\delta A} = P \rightarrow$  pressure
- Compressible fluid :- density can change wrt temp, time, P, etc  
 $\hookrightarrow$  opp  $\rightarrow$  Incompressible ( $\frac{\partial P}{\partial t} = 0$ )
- Viscous :- Normal & Shearing stress exist (stress ~ pressure)  
 Non " " stress exists only
- Newtonian :- Follow Newton's law of viscosity  
 else Non-Newtonian
- Newton's law of viscosity :  $\tau = \mu \frac{du}{dy}$    
 $\tau = 0 \Rightarrow \mu = 0 \Rightarrow$  Ideal fluid       $\mu \text{ const} \Rightarrow$  Newtonian ? Real  
 $\frac{\partial u}{\partial y} = 0 \Rightarrow \mu = \infty \Rightarrow$  Solid       $\mu \text{ depends on } \tau \Rightarrow$  Non-"
- Eulerian Description :- Description of a property with respect to a fixed pt (fluid passes through chosen pt)  
 velocity  $\vec{q} = (u, v, w)$ , Point P = (x, y, z)  
 $u = f(x, y, z, t), v = f(x, y, z, t), w = f(x, y, z, t)$
- Lagrangian Description :- Fluid props. are expressed in terms of initial position (if a point moves along the flow)  
 initial pt P (x<sub>0</sub>, y<sub>0</sub>, z<sub>0</sub>) at t<sub>0</sub>  $\rightarrow u = f(x_0, y_0, z_0, t) \parallel^y v \text{ and } w$
- Lagrangian to Eulerian:  $\phi = \phi(x_0, y_0, z_0, t)$  prop in lag<sup>2</sup>, P(x, y, z) are
  - $x = f_1(x_0, y_0, z_0, t) \parallel^y y \text{ and } z$   
 $\hookrightarrow$  can be solved to get  $x_0 = f_4(x, y, z, t) \parallel^y y_0 + z_0$
  - replace in  $\phi$  to get eulerian  $\phi = \phi'(x, y, z, t) = \phi(f_4, f_5, f_6, t)$

$$\text{Binomial Thm} \rightarrow (1+x)^n = 1 + nx + \frac{(n)(n-1)}{2!}x^2 + \frac{(n)(n-1)(n-2)}{3!}x^3 + \dots$$

Solving:- Eulerian to Lagrangian

- Given  $u(x, y, t)$ ,  $v(x, y, t)$

- Using D operator, get  $x(c_1, c_2, t)$ ,  $y(c_1, c_2, t)$

- $x_0 = x(t_0) \rightarrow$  let  $t_0 = 0$  and find  $c_1(x_0, y_0)$ ,  $c_2(x_0, y_0)$

- Replace in  $x$  &  $y$  to get  $x(x_0, y_0, t)$ ,  $y(x_0, y_0, t)$

- Substitute in  $u(x, y, t)$ ,  $v(x, y, t) \rightarrow$  Lagrangian

- Steady :- properties don't change wrt time :-  $\frac{\partial A}{\partial t} = 0$

- Uniform flow :- velocity doesn't change wrt space  $\frac{\partial q}{\partial r} = 0$   
(mag + dir)

- velocity ( $\vec{q}$ ) =  $\frac{d\vec{r}}{dt} \Rightarrow u = \frac{dx}{dt}, v = \frac{dy}{dt}, w = \frac{dz}{dt}$   
 $\vec{q} = (u, v, w)$   $\vec{r} = (x, y, z)$

- Path line :-  $\frac{dx}{dt} = f, \frac{dy}{dt} = g, \frac{dz}{dt} = h$  [motion of a particle]

- Streamline :-  $\frac{dx}{u} = \frac{dy}{v} = \frac{dz}{w}$  [dir of tangent coincides with vel]  
 $(\vec{q} \times d\vec{r} = 0) \Rightarrow (u, v, w) \times (dx, dy, dz) = 0 \Rightarrow (u dx, v dy, w dz) = 0$   
vel  $\perp$  tangent dir

- Material (spacial or total), local & convection derivative

$$\frac{D}{Dt} = \frac{\partial}{\partial t} + \vec{q} \cdot \vec{\nabla} \Rightarrow \vec{q} \cdot \vec{\nabla} = \vec{q} \frac{\partial}{\partial \vec{r}}$$

Material  
(Lagrangian)  
local  
(Eulerian)

$$\vec{\nabla} = \frac{\partial}{\partial x} \hat{i} + \frac{\partial}{\partial y} \hat{j} + \frac{\partial}{\partial z} \hat{k}$$

Proof:-  $\vec{r} \rightarrow \vec{r} + \delta \vec{r}$   $\vec{a}, \vec{F} \rightarrow$  fluid prop.,  $\vec{q} \rightarrow$  velocity

$$\frac{D \vec{F}}{Dt} = \frac{d \vec{F}}{dt} = \lim_{\delta t \rightarrow 0} \frac{\vec{F}(\vec{r} + \vec{q} \delta t, t + \delta t) - \vec{F}(\vec{r}, t)}{\delta t}$$

$$\left( \vec{q} = \frac{\delta \vec{r}}{\delta t} \Rightarrow \delta \vec{r} = \vec{q} \delta t \right)$$

$$\vec{F}(\vec{r} + \vec{q} \delta t, t + \delta t) \rightarrow \vec{F}(\vec{r}, t) + \vec{F}'$$

$$\vec{F}(\vec{r} + \vec{q} \delta t, t + \delta t) = \vec{F}(\vec{r}, t) + \frac{\partial \vec{F}}{\partial t} \cdot \vec{q} \delta t + \frac{\partial \vec{F}}{\partial \vec{r}} \cdot (\vec{q} \delta t)^2 + \dots$$

(using Taylor)

$$\vec{F}(\vec{x} + \vec{q}\delta t, t + \delta t) = \vec{F}(\vec{x}, t) + \frac{\partial \vec{F}}{\partial t} \vec{q} \delta t + \frac{\partial^2 \vec{F}}{\partial t^2} (\vec{q} \delta t)^2 + \dots$$

(using Taylor expansion)

- Ignore higher terms to get  $\vec{q} \delta t \rightarrow \frac{\partial \vec{F}}{\partial t}$

$$\frac{\partial \vec{F}}{\partial t} = \frac{\partial \vec{F}}{\partial x} \hat{i} + \frac{\partial \vec{F}}{\partial y} \hat{j} + \frac{\partial \vec{F}}{\partial z} \hat{k} = \nabla \vec{F}$$

$$\hookrightarrow \frac{\partial \vec{F}}{\partial x} = \frac{\partial \vec{F}}{\partial x} \cdot \frac{\partial x}{\partial \vec{x}} + \frac{\partial \vec{F}}{\partial y} \cdot \frac{\partial y}{\partial \vec{x}} + \frac{\partial \vec{F}}{\partial z} \cdot \frac{\partial z}{\partial \vec{x}}$$

uniform  
→  $\vec{F}$   
steady

- Steady  $\rightarrow \frac{\partial \vec{F}}{\partial t} = 0$ , Uniform  $\rightarrow \vec{F}$  and  $\vec{q}$

- Bernoulli's theorem:  $P_0 + \rho g h + \frac{1}{2} \rho v^2 = \text{const}$

- Acceleration:  $\frac{D\vec{q}}{Dt}$

- Irrational fluid:  $\text{curl } \vec{q} = \vec{0} \Rightarrow \nabla \times \vec{q} = \vec{0}$

For rotational:  $\vec{\omega} = \text{vorticity} = \text{curl } \vec{q}$

- Normal  $\vec{n} = \vec{\nabla} f$  (Normal of a function)

- If  $\nabla \times \vec{q} = 0$ ,  $\exists$  velocity potential ' $\phi$ '

$$\vec{q} = -\vec{\nabla} \phi$$

- Incompressible:  $\vec{\nabla} \cdot \vec{q} = 0$  or  $\frac{\partial \phi}{\partial t} = 0$

( $\phi$  is harmonic)

- Incompressible & Irrational:  $\vec{\nabla} \cdot \vec{q} = -\vec{\nabla}^2 \phi = 0$

- Conservation of Mass =  $A_1 u_1 = A_2 u_2$  cross-sectional area  
velocity

- E<sup>n</sup> of continuity:  $\frac{\partial \phi}{\partial t} + \vec{\nabla} \cdot (\phi \vec{q}) = 0$

(steady flow)

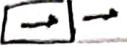
Proof:  $m = \rho v \rightarrow \log m = \log \rho + \log v \Rightarrow \frac{1}{m} \frac{dm}{dt} = \frac{1}{\rho} \frac{d\rho}{dt} + \frac{1}{v} \frac{dv}{dt}$

$$\Rightarrow \frac{1}{\rho} \frac{d\rho}{dt} + \frac{d\phi}{dt} + \vec{\nabla} \cdot (\phi \vec{q}) = 0 \Rightarrow \frac{d\phi}{dt} + \vec{\nabla} \cdot (\phi \vec{q}) = 0$$

using linear growth rate

Proof 1: •  $\delta V \rightarrow$  small vol,  $\delta S \rightarrow$  small SA of  $\delta V$

$$\text{Normal to } \vec{q} \text{ wrt } \delta V = \vec{q} \cdot \hat{n}$$



• Rate of mass flow  $\dot{m} = \int (\vec{q} \cdot \hat{n}) \delta S$

$$M = \int \int (\vec{q} \cdot \hat{n}) \delta S \quad (\text{over total surface})$$

$$\text{From divergence thm} \Rightarrow \oint q dS = \int \nabla \cdot \vec{q} dv \quad \text{where } q = \vec{v} \cdot \hat{n}$$

$$M = \int_v \nabla \cdot (\rho \vec{v}) dv$$

concerned with inner volume, so normal =  $-\hat{n}$

$$M = - \int_v \nabla \cdot (\rho \vec{v}) dv$$

$$M = \frac{d}{dt} \int_v \rho dv \quad \text{acc. to differentiation definition}$$

$$\frac{d}{dt} \int_v \rho dv = - \int_v \nabla \cdot (\rho \vec{v}) dv \Rightarrow \int_v \frac{d\rho}{dt} \left( 2\vec{v} + \nabla \cdot \vec{v} \right) dv = 0$$

(v arbitrary)

# Condition of (incompressibility) & (incompres + irrotational) can be derived from eq<sup>o</sup> of continuity

$\nabla \cdot \vec{F} \rightarrow$  divergence;  $\vec{v} \times \vec{F} \rightarrow$  curl

$$\nabla^2 (\text{Laplacian}) = \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2} + \frac{\partial^2}{\partial z^2} = \nabla \cdot (\nabla \vec{v})$$

$$\nabla^2 \vec{F} = \nabla^2 F_1 \hat{i} + \nabla^2 F_2 \hat{j} \quad (\text{on vector})$$

$$\nabla^2 (\rho v) = (\nabla^2 \rho)v + \rho(\nabla^2 v) + 2(\nabla \rho \cdot \nabla v)$$

Derive  $\frac{D\rho}{Dt}$  using eq<sup>o</sup> of continuity (using Taylor's)

$$\rho_2(x_2, y_2, z_2, t_2) \rightarrow \rho(x_1, y_1, z_1, t_1)$$

$$\rho_2 = \rho_1 + \left( \frac{\partial \rho}{\partial x} \right)_p (x_2 - x_1) + \left( \frac{\partial \rho}{\partial y} \right)_p (y_2 - y_1) + \left( \frac{\partial \rho}{\partial z} \right)_p (z_2 - z_1) + \left( \frac{\partial \rho}{\partial t} \right)_p (t_2 - t_1)$$

(Taylor expansion)

$$\frac{\rho_2 - \rho_1}{t_2 - t_1} \text{ at } t_2 \rightarrow t_1 = \frac{\partial \rho}{\partial t} + \frac{\partial \rho}{\partial x} u + \frac{\partial \rho}{\partial y} v + \frac{\partial \rho}{\partial z} w = \frac{1}{\partial t} \frac{\partial \rho}{\partial t} + \vec{v} \cdot \nabla \rho$$

Kccat

11

Q. Page 14 ?  
Sakshi

Q. Page 11?  
Kalan

Eg. of continuity

in polar coordinates:-

$$30: \frac{\partial f}{\partial r} + \frac{1}{r^2} \frac{\partial}{\partial \theta} (f r^2 q_r) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (f \sin \theta q_\theta) +$$

$$\frac{1}{r \sin \theta} \frac{\partial}{\partial \phi} (f q_\phi) = 0$$

in 3D cylindrical coordinates

$$\frac{\partial f}{\partial r} + \frac{1}{r} \frac{\partial}{\partial r} (f r q_r) + \frac{1}{r} \frac{\partial}{\partial \theta} (f q_\theta) + \frac{\partial}{\partial z} (f q_z) = 0$$

Incompressible :-  $\frac{\partial f}{\partial t} = 0$

Stream fun.  $\psi \rightarrow u = -\frac{\partial \psi}{\partial y}, v = +\frac{\partial \psi}{\partial x}$

$$\text{continuity} \rightarrow d\psi = \frac{\partial \psi}{\partial x} dx + \frac{\partial \psi}{\partial y} dy \Rightarrow [\psi = f + u dx + v dy + c]$$

Relation b/w  $\psi + \phi \rightarrow \nabla^2 \phi = \nabla^2 \psi = 0 \rightarrow$  elliptic PDE

$$\text{Cauchy-Riemann} \leftarrow \left( \frac{\partial \psi}{\partial y}, \frac{\partial \psi}{\partial x} \right) = \left( +\frac{\partial \phi}{\partial x}, -\frac{\partial \phi}{\partial y} \right) = (u, -v)$$

$w = \phi + i\psi = \text{complex potential}$  where  $\phi$  &  $\psi$  are complex conjugates  
↳ Only for incompressible & irrotational

$$q = -\vec{\nabla} \phi \rightarrow (u, v) = \left( -\frac{\partial \phi}{\partial y}, \frac{\partial \phi}{\partial x} \right)$$

Eg. of continuity in Lagrangian  
( $q$  independent of  $t$ )

Conservation of mass

$$\int_{R_0}^{R_1} \delta x \delta y \delta z = \int_R^R \delta x \delta y \delta z \quad \left| \begin{array}{l} dx dy dz = J dx dy dz \\ \text{where } J = \det(x, y, z) \end{array} \right.$$

$$dx dy dz = J dx dy dz$$

$$\text{where } J = \det(x_0, y_0, z_0)$$

$$\int (f_0 - J \varphi) \delta x_0 \delta y_0 \delta z_0 = 0 \Rightarrow f_0 = J \varphi \quad \text{as } x_0, y_0, z_0 \text{ are arbitrary}$$

$$\frac{D\vec{J}}{Dt} = \vec{J} \left( \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} \right)$$

Lagrangian to Euler :- Differentiate wrt t  
 $\vec{J}$  is non zero

Euler to Lagrangian :- Opp. of previous

$\phi$  exist  $\Rightarrow$  irrotational  $\rightarrow$  can be used to prove incomp.  
 $\psi$   $\rightarrow$  rotational or  $\rightarrow$  rotational flow along fixed axis (rotation in 2D)

Streamlines  $\Rightarrow$ ? (only streamlines or with path?)

Momentum Operation?  $P = \lim_{\delta s \rightarrow 0} \frac{\delta F}{\delta s} \rightarrow$  Force Surface

Kinetic Euler Eq<sup>n</sup> :- 
$$\frac{D\vec{q}}{Dt} = \vec{F} - \frac{1}{\rho} \vec{\nabla} P$$

$\vec{F} \rightarrow$  external force/mass  
 $P \rightarrow$  internal pressure

Proof:- consider incompressible fluid  $\rightarrow \rho$  constant

External Force  $= \int \vec{F} \rho dV \rightarrow \textcircled{1}$

Force due to pressure  $= - \int \rho (\vec{P} \cdot \hat{n}) dA \rightarrow \textcircled{2}$

$$\textcircled{1} + \textcircled{2} = \frac{dP}{dt} = - \int \vec{\nabla} P dV \quad (\text{using Gauss Divergence})$$

$$\frac{dP}{dt} = 1/\rho^2 \quad P = \int \vec{q} \rho dV$$

$$\int \frac{\partial \vec{q}}{\partial t} dV = \int (\vec{F} \rho - \vec{\nabla} P) dV \quad (\checkmark \text{ arbitrary})$$

After walls

Bernoulli's Eq<sup>n</sup> of a 1D inviscid, incompressible, irrotational flow in a conservative force field

Pre:- irrotation  $\Rightarrow \vec{q} = -\vec{\nabla} \phi$ ,  $\vec{F}$  is conservative  $\Rightarrow \vec{F} = \vec{\nabla} V$ , scalar field

Proof:- Consider Euler's Eq<sup>n</sup>  $\Rightarrow \frac{D\vec{q}}{Dt} = \vec{F} - \frac{1}{\rho} \vec{\nabla} P$  |  $F_B = C(X, Y, Z)$

Resolve along x axis  $\Rightarrow \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = X - \frac{1}{\rho} \frac{\partial P}{\partial x}$

Now  $\frac{\partial u}{\partial y} = -\frac{\partial \phi}{\partial x} = \frac{\partial v}{\partial x} \Rightarrow \frac{\partial v}{\partial y} = \frac{\partial w}{\partial x} + \frac{\partial u}{\partial z} = \frac{\partial w}{\partial y}$

$\Rightarrow \frac{\partial u}{\partial t} \frac{\partial (-\partial \phi)}{\partial x} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = X - \frac{1}{\rho} \frac{\partial P}{\partial x}$  |  $\textcircled{1}$

| for y axis |  $\frac{\partial}{\partial t} \left( \frac{-\partial \phi}{\partial x} \right) + \frac{1}{2} \frac{\partial}{\partial x} (u^2 + v^2 + w^2) = X - \frac{1}{\rho} \frac{\partial P}{\partial x}$

(2) (3)

1. Streamlines :-  $d\psi = 0 \Rightarrow \psi(x, y, t) = c_1, -\phi(x, y, t) = c_2$

→ Continuation :- ①  $dx + ② dy + ③ dz$

$$\Rightarrow \text{mass} - \cancel{\frac{\partial}{\partial t}} d\left(\frac{\partial \phi}{\partial t}\right) + \frac{1}{2} d\left(\underbrace{u^2 + v^2 + w^2}_{q^2}\right) = \cancel{\frac{\partial}{\partial x}} dx + \cancel{\frac{\partial}{\partial y}} dy + \cancel{\frac{\partial}{\partial z}} dz - \frac{1}{\rho} dP$$

⇒  ~~$\frac{\partial \phi}{\partial t}$~~  Integrate on both sides

$$\boxed{\frac{-\partial \phi}{\partial t} + \frac{1}{2} q^2 = -v - \int \frac{\partial dP}{\rho}} \rightarrow \text{Bernoulli's / Pressure Eq?}$$

complex potential:  $w(z) = w(x, y) = \phi(x, y) + i\psi(x, y)$

Derive C-R eqn from complex potential.

$$\frac{\partial \psi}{\partial x} = \cancel{i} \frac{\partial \psi}{\partial y} \rightarrow \text{for CR} / \cancel{i} \frac{\partial \phi}{\partial y} \quad w' = \frac{\partial w}{\partial z} = \frac{\partial \phi}{\partial x} + i \frac{\partial \psi}{\partial x} \quad \frac{\partial \phi}{\partial x} = \phi(x+iy) \\ w' = i \frac{\partial w}{\partial y} = \cancel{i} \frac{\partial w}{\partial y} = \cancel{i} \frac{\partial \phi}{\partial y} + i^2 \frac{\partial \psi}{\partial y} = \frac{\partial \phi}{\partial y} + i \frac{\partial \psi}{\partial y} = \phi(x+iy)$$

$$w'(x+iy) = \left[ \frac{\partial \phi}{\partial x} = \frac{\partial \phi}{\partial r} + i \frac{\partial \phi}{\partial \theta} \right] = \left[ i \frac{\partial \phi}{\partial y} = i \frac{\partial \phi}{\partial r} + i^2 \frac{\partial \phi}{\partial \theta} \right] \rightarrow \text{some to get CR}$$

CR in Polar form ( $z = re^{i\theta}$ )

$$w(z) = f(z) = f(re^{i\theta}) = \phi + i\psi \quad (\phi = \phi(r, \theta), \psi = \psi(r, \theta))$$

$$\frac{\partial \psi}{\partial r} = \cancel{i} \frac{\partial \psi}{\partial \theta} e^{i\theta} / \cancel{i} = \cancel{i} \frac{\partial \psi}{\partial \theta}$$

$$\frac{\partial \phi}{\partial r} + i \frac{\partial \psi}{\partial r} = f'(re^{i\theta}) e^{i\theta}, \quad \frac{\partial \phi}{\partial \theta} + i \frac{\partial \psi}{\partial \theta} = f'(re^{i\theta}) rie^{i\theta}$$

$$\text{Equate } f'(re^{i\theta}) e^{i\theta} \quad \boxed{\frac{\partial \phi}{\partial r} = \frac{1}{r} \frac{\partial \phi}{\partial \theta}, \quad \frac{\partial \phi}{\partial \theta} = -r \frac{\partial \psi}{\partial r}} \rightarrow \text{CR}$$

$$w = \phi + i\psi, \quad z = x + iy$$

$$\frac{dw}{dz} = \frac{dw}{dx} \cdot \cancel{\frac{dx}{dz}}^{-1} = \frac{\partial \phi}{\partial x} + i \frac{\partial \psi}{\partial x} = -u + iv$$

$$|\frac{dw}{dz}| = \sqrt{u^2 + v^2} = |\vec{q}| \rightarrow \text{magnitude of velocity from complex potential}$$

left:- Bernoulli, cylindrical or  $\vec{v}$  in other coordinate systems

Residual part

## Sources & Sink

- Strength of source: - Source at origin, mass of fluid/time coming out of origin ('m') → flow across the source =  $2\pi m$  by strength of sink. (Sink is source with  $-m$  strength)
- No source/sink  $\approx$  streamlines don't intersect  $\Rightarrow \psi = \text{const}$   $\forall t > 0$
- with source/sink   $\approx$  streamlines intersect at only source/sink
- $q_r = -\frac{\partial \phi}{\partial r} = -\frac{1}{r} \frac{\partial \psi}{\partial \theta}$  (using complex CR in polar)  $\rightarrow$  ①  
↳ radial velocity
- $2\pi r q_{r,\infty} = 2\pi m \Rightarrow \boxed{q_r = \frac{m}{r}}$   $\rightarrow$  ②,  $q_\theta = 0$
- Using ① & ②  $\rightarrow \psi(r, \theta) = -m\theta$  streamlines from source  
 $\rightarrow \phi(r, \theta) = -m \log r$   $\rightarrow$  ③ along  $r$  const.  
 ↳  $\theta = \text{const}$  (at  $r$  const) ( $r$  measured from center)  
 ↳ equi-velocity potential at concentric circles
- $\boxed{w = \phi + i\psi = -m \log z}$   $\rightarrow$  source at origin  
 $w = -m \log(z - z')$   $\rightarrow$  " " " "  $z'$   $\left. \begin{array}{l} \\ \\ \\ \\ \end{array} \right\} z = re^{i\theta}$
- $w = m \log z \rightarrow$  sink at origin  
 $w = -m \log(z - z') \rightarrow$  " " " "

Volume flow rate per unit area across circle of radius  $r$

$$N = \int_0^{2\pi} \vec{q} \cdot \hat{n} ds = \int_0^{2\pi} (q_r, q_\theta) \cdot \hat{n} ds = \int_0^{2\pi} q_r r d\theta = 2\pi m = m$$

Doublet :- Source + Sink

- $\phi$  at doublet origin in doublet  $\rightarrow$  source  $\rightarrow \rho(r, \theta)$   
 sink  $\rightarrow \phi(r + \delta r, \theta + \delta \theta)$

$$\phi(r, \theta) = -m \log r + m \log(r + \delta r) = m \log\left(1 + \frac{\delta r}{r}\right)$$

$$\boxed{\phi(r, \theta) = -m \frac{\delta r}{r}} + \text{higher powers}$$

Chegg

Strength of doublet  $\mu = m \delta s \cos \theta$  ( $\delta s = a + b r$ )

$$\phi(r, \theta) = \frac{\mu \cos \theta}{r}$$

$$\text{Proof :- } \phi(r, \theta) = \frac{m \delta r}{r} = \frac{m \cdot \delta s \cos \theta}{r} = \frac{\mu \cos \theta}{r}$$

$$\psi(r, \theta) = -\frac{\mu \sin \theta}{r}$$

$$\text{Proof:- } \phi(r, \theta) \propto \frac{1}{r} \frac{\partial \psi}{\partial \theta} = \frac{\partial \phi}{\partial r} = -\mu \cos \theta$$

$$\psi = -\frac{\mu \sin \theta}{r} \quad [\text{as } \frac{\partial \phi}{\partial \theta} \text{ is zero} \Rightarrow \frac{\partial \psi}{\partial r} = 0]$$

$$w = \frac{\mu}{r} e^{i\theta} = \frac{\mu}{z}$$

Doublet located at  $(a, z_1, b) \rightarrow w = \frac{\mu}{z - z_1}$   
makes angle  $\alpha$

$$w = \frac{\mu}{r e^{i(\theta-\alpha)}} = \frac{\mu e^{i\alpha}}{r e^{i\theta}} = \frac{\mu e^{i\alpha}}{z}$$

Doublet at  $z_1$  & makes angle  $\alpha \Rightarrow w = \frac{\mu e^{i\alpha}}{z - z_1}$   
Multiple doublets  $\rightarrow w = \sum w_i$

$$\log z = \frac{1}{2} \log(z^2 + y^2) + i \tan^{-1}\left(\frac{y}{x}\right)$$

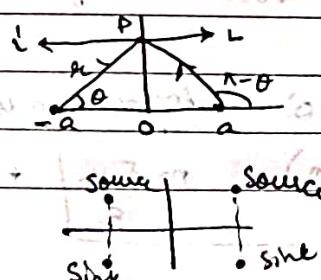
(Q) Pg 431 ? How to draw streamlines from ~~from~~ potential

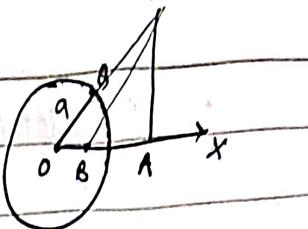
Image :- wrt a surface, flow across it is 0 i.e.  
there are equivalent source-sink systems on  
either side of surface.

Image wet line :-

$$q/r = \frac{m}{r} \cos \theta + \frac{m}{r} \cos(\pi - \theta) = 0$$

$$\frac{m}{r} \cos \theta + \frac{m}{r} \cos(\pi - \theta) = 0$$





### Image wrt circular surface :-

A → source

B → img " , O → img sink

A + sink

B → img " , O → " source

$$|OA| = f \quad |OB| = -a$$

$$|OB| |OA| = a^2 \Rightarrow |OB| = \frac{a^2}{f}$$

N, B source

Take sources at A, B only

$$w = f(z) = -m \log(z-f) = -m \log\left(\frac{z-a^2}{f}\right)$$

- Open 2 & apply log formula, Take  $\phi$  as real part
- take  $\frac{\partial \phi}{\partial r}|_{r=a}$  to get  $\frac{m}{a}$ , hence we need a sink at origin
- go at a

### Milne - Thompson Theorem:-

let  $f(z)$  is complex potential & if no singularities of flow

& within  $|z|=a$ , then the flow crosses out cylinder  $|z|=a$

ii  $w = f(z) + \bar{F}\left(\frac{a^2}{z}\right)$  for  $|z|>a$

Consider source at A which is  $f$  away from  $(0,0)$

w =  $-m \log(z-f)$   $\bar{w} = -m(\log z - f) = -m \log(z-f)$

Apply Milne Thompson to get

new w =  $f w + \bar{w}\left(\frac{a^2}{z}\right)$   
 $= -m \log(z-f) - m \log\left(\frac{z-a^2}{f}\right) + m \log z +$

show  $\frac{\partial \phi}{\partial r}|_{r=a} = 0$   $\rightarrow$  Image wrt circular surface

Potential line  $\rightarrow \phi = \text{constant}$   $\rightarrow \frac{\partial \phi}{\partial r} = 0$

Q:- Pg 36:- last part ( $\pi$ -x wala)

Q:-

Blasius Thm :-

• steady, irrotational & incompressible  
 • No external force  $\rightarrow w=f(z)$

• Force on a fixed cylinder  $(x, y)$

$$F = x\hat{i} + y\hat{j} = \frac{1}{2} i^2 \int \left( \frac{dw}{dz} \right)^2 dz$$

• Drag or friction couple of moment =  $Re\left(-\frac{1}{2} i^2 f^2 \left(\frac{dw}{dz}\right)^2 dz\right)$

Circulation  $\rightarrow$  flow around closed curve

$$\Gamma = \oint_C \vec{q} \cdot d\vec{l} = \oint_C (u dx + v dy + w dz)$$

$\Gamma \rightarrow$  circulation,  $C \rightarrow$  curve

• Kelvin Circulation theorem

- ↪ external forces  $\rightarrow$  conservative  $\wedge$  derivable by single valued potential function  $\rightarrow$  same on curve
- ↪ density  $\rightarrow$   $f \#$  of pressure only
- $\Rightarrow$  circulation in any closed circuit moving with the fluid is constant at all time

Proof :-  $\frac{d\Gamma}{dt} = \oint_C \frac{d}{dt} (\vec{q} \cdot d\vec{l}) = \oint_C \frac{d\vec{q}}{dt} \cdot d\vec{l} + \vec{q} \cdot \frac{d}{dt} d\vec{l}$

Applying Euler

$$= \oint_C \left( \vec{F} - \frac{1}{\rho} \nabla P \right) d\vec{l} + \vec{q} \cdot d\vec{q} = 0 \quad (\text{all singleton values})$$

• Flow around a cylinder

$$\Psi(z, y) = Vz - Uy + \frac{1}{2} w(r^2 - y^2) + C, \quad \text{where } z = x + iy$$

Proof :- fluid  $\rightarrow \infty$  mass  $\rightarrow$  reservoir

At  $\theta = 0$   $\vec{q} = 0 \Rightarrow u, v = 0 \Rightarrow \frac{\partial \Psi}{\partial r} = 0, \frac{\partial \Psi}{\partial \theta} = 0 \Rightarrow \Psi \text{ const}$   $w \uparrow$   $P \uparrow$   $u-wy$   $P \downarrow$   $ds$  time = t

$$\frac{dx}{ds} = \cos \theta, \quad \frac{dy}{ds} = \sin \theta$$

$$\text{normal velocity at } P = (u - wy) \cos(90 - \theta) + (v + wz) \cos(\theta - 180)$$

= " component of velocity of fluid

$$\sin \theta$$

$$-\cos \theta$$

$$= -\frac{\partial \Psi}{\partial s} \quad \rightarrow \text{integrate}$$

...

• Motion of cylinder moving with u velocity in x-axis with irrotational flow (as fluid, at rest at  $\alpha$ )

$$w = u \left( \frac{r^2 - a^2}{z} \right) \quad z = re^{i\theta}$$

Proof :-  $\vec{q} = -\vec{\nabla} \phi \Rightarrow \vec{\nabla}^2 \phi = 0$  (irrotational)

$$\frac{\partial^2 \phi}{\partial x^2} + \frac{1}{r} \frac{\partial \phi}{\partial r} + \frac{1}{r^2} \frac{\partial^2 \phi}{\partial \theta^2} = 0$$

• Solution can be of form  $Ae^{in\theta} \cos n\phi$  or  $Bre^{in\theta} \sin n\phi$

• normal velocity of cylinder  $\Rightarrow u_{\text{cylinder}} = -\frac{\partial \phi}{\partial r} \Big|_{r=a}$  (normal velocity of fluid in normal dir)

$$q_r = q_\theta = 0 \Rightarrow -\frac{\partial \phi}{\partial r} = -\frac{1}{r} \frac{\partial \phi}{\partial \theta} = 0, r \rightarrow a$$

$\therefore \phi$  is of form  $Ax \cos \theta + \frac{A_1}{r} \cos \theta, \frac{-\partial \phi}{\partial r} = 0 \Rightarrow A = 0$

$$\frac{-\partial \phi}{\partial r} \Big|_{r=a} = u_a \cos \theta \Rightarrow A_1 = u_a^2 \Rightarrow \phi = \frac{u_a^2}{r} \cos \theta$$

$$\bullet \text{ CL eqn } \frac{\partial \psi}{\partial r} = -\frac{1}{r} \frac{\partial \phi}{\partial \theta} = q_0, \psi = -\frac{u_a^2}{r} \sin \theta \Rightarrow w = \frac{u_a^2}{r^2}$$

$$\frac{1}{r} \frac{\partial \psi}{\partial \theta} = \frac{\partial \phi}{\partial r} = -q_0$$

• Flow past a fixed cylinder in stream

$$w = u(2 + a^2/r^2)$$

Proof:  $\bullet \psi(r, x, y) = Vx + C_1$  ( $y = \text{const}$ , flow only along  $x$  axis,  $w=0$  (fixed))

$$\Rightarrow \phi(r, y) = -Vy + C_2 \quad (\text{using CL})$$

$\bullet w = -u_a^2$  (flow from  $-ve x$  for moving cylinder)

$$\bullet \phi = u_x + \frac{u_a^2 \cos \theta}{r}, \psi = u_y - u_a^2 \sin \theta \rightarrow \text{to make fixed} \Rightarrow w = (2 + \frac{a^2}{r^2})$$

$$\Rightarrow \frac{dw}{dr} = -u + iV \Rightarrow \left| \frac{dw}{dr} \right| = |\vec{q}| = 2|u| \sin \theta \rightarrow \theta = 0, q_{\text{min}} = 0 \\ \theta = \pi/2, q_{\text{max}} = 2|u|$$

• Flow past a cylinder with circulation

$$\alpha = \oint_C \vec{q} \cdot d\vec{s} = q_0 (2\pi r) = -\frac{1}{2} \frac{\partial \phi}{\partial \theta} 2\pi r \Rightarrow \phi = -\alpha \theta \Rightarrow \phi = \frac{\alpha}{2\pi} \log r$$

$$\rightarrow w_{\text{circ}} = \frac{\alpha i}{2\pi} \log 2 \rightarrow w = u\left(2 + \frac{a^2}{r^2}\right) + \frac{\alpha i}{2\pi} \log 2 \quad \text{as } w = \phi + iV$$

$$\frac{dw}{dr} = V/(1/a^2)$$

$$\left| \frac{dw}{dr} \right|_{r=a} = u(1 - e^{-2i\theta}) + \frac{i\alpha}{2\pi a} e^{-i\theta} \Rightarrow |\vec{q}| = |2u \sin \theta + \frac{\alpha}{2\pi a}|$$

$$\text{Stagnation pt} \rightarrow |\vec{q}| = 0 \Rightarrow \left| \frac{\alpha}{4\pi au} \right| \leq 1 \rightarrow \begin{cases} < 1 & \text{2 stagnation pts} \\ > 1 & \text{1 stagnation pt} \end{cases} \quad (\theta = \frac{\pi}{2} \text{ or } \frac{3\pi}{2})$$

## Aerofoil

Incompressible  $\rightarrow$  Aerofoil ~~is a cylinder~~ with ~~has~~ ~~is a~~ ~~type~~ cross-sect.  $\rightarrow$  flow 2D inviscid

- Kutta - Joukowski Mapping  $\Rightarrow \tilde{w}_1 = z + a^2$

- Kutta - Joukowski Theorem  $\rightarrow$   $\square$  placed in  $\rightarrow u$  uniform then  $\uparrow$  thrust is  $k g u$  per unit length ( $k$  is circulation around cylinder)

Proof :-  $w_1 = Az + B$  (fixed cylinder in xy plane making  $\alpha$ )

$w_2 = U e^{i\alpha} z^2$  (stream makes  $\alpha$  with cylinder)

$w_3 = \frac{i k}{2\pi} \log z$  (circulation)

$w = w_1 + w_2 + w_3$ , apply Blasius thm

$$x - iy = \frac{-i\alpha}{2} \int_C \frac{(dw)^2}{(az)^2} dz \rightarrow \text{sum of residual at } z=0 \\ = -k g u (\sin \alpha + i \cos \alpha)$$

$$\text{Thrust} = \sqrt{x^2 + y^2} = k g u$$

Joukowski Transformation  $z = \bar{z} + a^2$

$\bullet A \rightarrow A'$ ,  $B \rightarrow B'$  (substitute  $a, -a$  resp.)

$$\bullet |A'Q|B'| = \alpha_1 - \alpha_2 = 2LA PB$$

$$\text{Proof: } z - 2a = (\bar{z} - a)^2 \Rightarrow A'Q e^{i\alpha_1} = (AP e^{i\alpha})^2$$

$$\text{Real part} \Rightarrow A'Q = \frac{AP^2}{OP} e^{i\alpha}, \text{ img} \Rightarrow \alpha_1 = 2\alpha + \theta$$

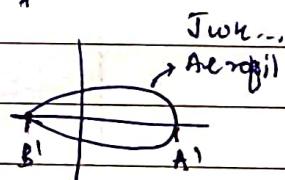
$$\text{Hence } B'Q = \frac{AP^2}{OP}, \alpha_2 = 2\alpha_2 - \theta$$

Also,

$$\boxed{A'Q + B'Q = \frac{AP^2 + BP^2}{OP}} \rightarrow \text{const when } P \text{ lies on any circle}$$

ellipse

when  $P$  lies on original circle  $\rightarrow$  st line  $B'$



$$\bullet \frac{d\bar{z}}{dz} = 0 \text{ at } \pm a$$

$$\text{now } |\vec{q}'| = \left| \frac{dw}{dz} \right| = |\vec{q}| \left| \frac{dz}{d\bar{z}} \right| \rightarrow \text{at } \pm a, \vec{q}' = \infty \text{ unless } \vec{q} = 0$$

Flow around aerofoil (same assumptions as cylinder)

Stagnation pts  $\Rightarrow z = \pm a \Rightarrow \zeta = \pm \frac{a}{2}$

$$\therefore \left( \frac{dw}{dz} \right)_{\text{stagn}}^2 = \frac{(dw/dz)^2}{1 - \frac{a^2}{z^2}} \text{ using } dz = a \sin \theta + \frac{a^2}{2} d\theta$$

$$\therefore w = U e^{i\theta} (z-a) + \frac{Ua^2}{2} e^{-i\theta} + i \kappa \log(z-a)$$

$$\Rightarrow \text{obtain } \frac{dw}{dz} = \frac{Ue^{i\theta}}{z-a} + \frac{iUa^2}{2} e^{-i\theta} + \frac{i\kappa}{z-a}$$

$$\therefore x - iy = \frac{i}{2} \int_C \left( \frac{dw}{dz} \right)^2 dz \quad \text{using sum of residuals}$$

$$= ikU (\sin \theta - i \cos \theta)$$

$$\text{Thrust} = \sqrt{x^2 + y^2} = pkU$$

### Motion of viscous fluid

$\rightarrow$  Tensor :-  $\vec{a} = a_i e_i = a'_i e'_i \Rightarrow \vec{a} \cdot \vec{e}_i = a'_i = a_{ii}$

$$e_i e_j' = \cos(e_i \& e_j') |e_i| |e_j'| = \alpha_{ij}$$

$$a'_i = \alpha_{ij} a_j, \text{ by } a_i = \alpha_{ji} a'_j \rightarrow \text{Tensor representation (orders)}$$

$\rightarrow$  Order 2 transform

$$a'_i b'_j = (\alpha_{ip} a_p)(\beta_{jq} b_q)$$

$$\vec{a} \vec{b} = \begin{bmatrix} a_1 b_1 & a_2 b_2 & a_3 b_3 \\ a_1 b_2 & \dots & \dots \\ a_1 b_3 & \dots & \dots \end{bmatrix}$$

### Stress at a pt in fluid

pt mass fluid  $\Rightarrow$  forces zero, hence take

$\delta s$  with  $\hat{n}$  as normal.  $\therefore$  and SF force and SG moment

$$\tau = \lim_{\delta s \rightarrow 0} \frac{\delta F}{\delta s} \quad (\delta F \text{ is proportional to } \delta s \text{ when } \delta s \text{ is small})$$

depends on  $\hat{n}$  dir, and stress vector itself

$$\tau \propto \beta \rightarrow \propto \hat{n} \text{ dir}$$

$\rightarrow \beta \rightarrow$  direction of  $\tau$  considered