# Advanced Fluid Dynamics

#### Kevin Corcoran

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## Contents

1:	Assignment 1	1
1	Mass conservation and other conservation laws         1.1 Mass conservation in polar coordinates	
2	Momentum equation and vorticity	5
3	Thermal energy equation and hydrostatic equilibrium 3.1 Energy equation	<b>6</b>
	3.2 Hydrostatics	7

## 1: Assignment 1

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## 1 Mass conservation and other conservation laws

### 1.1 Mass conservation in polar coordinates

Question 1: Express the mass conservation equation in 2D polar coordinates

mass conservation

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{u}) = 0.$$

expressed in 2D polar coordinates

$$\frac{\partial \rho}{\partial t} + \frac{1}{r} \frac{\partial (r\rho \vec{u}_r)}{\partial r} + \frac{1}{r} \frac{\partial (\rho \vec{u}_\theta)}{\partial \theta} = 0.$$

where  $\vec{u} = \begin{pmatrix} u_r \\ u_\theta \end{pmatrix}$  is the velocity vector field expressed in polar coordinates.

## Velocity field in polar coordinates

Let  $\beta = \{\vec{v}_r, \vec{v}_\theta\}$  be an orthonormal basis where

$$\vec{v}_r = \begin{pmatrix} \cos \theta \\ \sin \theta \end{pmatrix}, \quad \vec{v}_\theta = \begin{pmatrix} -\sin \theta \\ \cos \theta \end{pmatrix}..$$

Then at each point  $(r, \theta)$  in space the position of a particle can be expressed as

$$\vec{r}(r,\theta) = r\vec{v}_r$$
.

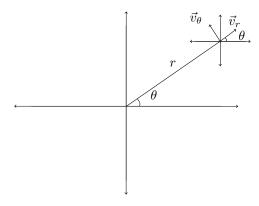


Figure 1: Tangent space? coordinate transform

so a fluid particles velocity can be expressed as

$$\vec{u}(r,\theta) = \frac{\mathrm{d}[r\vec{v}_r]}{\mathrm{d}t} = \frac{\mathrm{d}r}{\mathrm{d}t}\vec{v}_r + r\frac{\partial\vec{v}_r}{\partial\theta}\frac{\mathrm{d}\theta}{\mathrm{d}t}$$
$$= \frac{\mathrm{d}r}{\mathrm{d}t}\vec{v}_r + r\frac{\mathrm{d}\theta}{\mathrm{d}t}\vec{v}_\theta$$
$$= \dot{r}\vec{v}_r + r\dot{\theta}\vec{v}_\theta$$

then in  $\beta$  (polar) coordinates

$$[\vec{u}(r,\theta)]_{\beta} = \begin{pmatrix} \dot{r} \\ r\dot{\theta} \end{pmatrix}.$$

Question 2: If  $\vec{u} = \begin{pmatrix} u_r \\ u_\theta \end{pmatrix} = \begin{pmatrix} u_0 \\ 0 \end{pmatrix}$ , then a fluid particle has speed  $u_0$  pointing in the direction of basis vector  $\vec{v}_r$ .

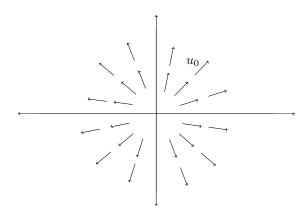


Figure 2: velocity field

Question 3: Solve for  $\rho(r,t)$  with initial condition  $\rho_0(r,t=0) = re^{-\frac{(r-1)^2}{2}}$  and  $\vec{u}_\beta = \begin{pmatrix} u_0 \\ 0 \end{pmatrix}$ .

Mass conservation expressed in polar coordinates, and assuming  $\rho$  doesn't depend on  $\theta$ 

$$\frac{\partial \rho}{\partial t} + \frac{1}{r} \frac{\partial (r \rho \vec{u}_r)}{\partial r} + \frac{1}{r} \frac{\partial (\rho \vec{u}_\theta)}{\partial \theta} = 0.$$

becomes

$$\frac{\partial \rho}{\partial t} + \frac{u_0}{r} \frac{\partial (r\rho)}{\partial r} = 0.$$

if we let  $f(r,t) = r\rho(r,t)$ , then we get

$$\frac{1}{r}\frac{\partial f}{\partial t} + \frac{u_0}{r}\frac{\partial f}{\partial r} = 0$$
$$\frac{\partial f}{\partial t} + u_0\frac{\partial f}{\partial r} = 0$$

considering the parameterization  $f = f(r(s), t(s)) \Rightarrow \frac{\mathrm{d}f}{\mathrm{d}s} = \frac{\mathrm{d}t}{\mathrm{d}s} f_t + \frac{\mathrm{d}r}{\mathrm{d}s} f_r = 0$ , we get the following characteristic equations

$$\begin{cases} \frac{\mathrm{d}t}{\mathrm{d}s} = 1 & \Rightarrow t = s + t_0 \underset{t_0 = 0}{\Rightarrow} t = s \\ \frac{\mathrm{d}r}{\mathrm{d}s} = u_0 & \Rightarrow r = u_0 s + r_0 \\ \frac{\mathrm{d}f}{\mathrm{d}s} = 0 & \Rightarrow f = f_0(r_0, t_0) \end{cases}.$$

putting everything together

$$f(r,t) = f(r_0, t_0 = 0) = (r - u_0 t) \rho_0 (r - r u_0 t, 0).$$

$$\Rightarrow \rho(r,t) = (r - u_0 t) e^{-\frac{1}{2}(r - u_0 t - 1)^2}.$$

Plotting  $\rho(r,t)$  at various snapshots in time, with  $u_0 = 1$ , we see an agreement with Figure 2. The density gets pushed away from the origin, r = 0, at a constant speed  $u_0$ .

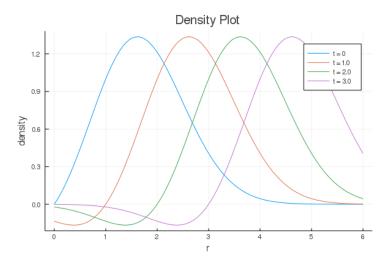


Figure 3

#### 1.2 Other conservation laws

Assuming S is the salt concentration (mass of salt per unit mass of water) in salty water. If salt is conserved, then the equation for the evolution of S is the change in salt concentration w.r.t time equal to the (negative) divergence of salt flux at a point

$$\boxed{\frac{\partial S}{\partial t} + \nabla \cdot (S\vec{u}) = 0}$$

## 2 Momentum equation and vorticity

**Question 1**: Assuming incompressible flow, and constant kinematic viscosity  $\mu$  is constant, show  $\nabla \cdot \Pi = \mu \nabla^2 \vec{u}$ 

Since the flow is incompressible  $\Rightarrow \nabla \cdot \vec{u} = 0$ , then the viscous stress tensor becomes

$$\Pi = (k - \frac{2}{3}\mu)\underbrace{\nabla \cdot \vec{u}}_{=0} I + \mu(\nabla \vec{u} + (\nabla \vec{u})^T) 
= \mu(\nabla \vec{u} + (\nabla \vec{u})^T) 
= \mu \left[ \begin{pmatrix} \frac{\partial u_1}{\partial x_1} & \frac{\partial u_1}{\partial x_2} & \frac{\partial u_1}{\partial x_3} \\ \frac{\partial u_2}{\partial x_1} & \frac{\partial u_2}{\partial x_2} & \frac{\partial u_2}{\partial x_3} \\ \frac{\partial u_3}{\partial x_1} & \frac{\partial u_3}{\partial x_2} & \frac{\partial u_3}{\partial x_3} \end{pmatrix} + \begin{pmatrix} \frac{\partial u_1}{\partial x_1} & \frac{\partial u_2}{\partial x_1} & \frac{\partial u_3}{\partial x_1} \\ \frac{\partial u_1}{\partial x_2} & \frac{\partial u_2}{\partial x_2} & \frac{\partial u_3}{\partial x_2} \\ \frac{\partial u_1}{\partial x_3} & \frac{\partial u_2}{\partial x_3} & \frac{\partial u_3}{\partial x_3} \end{pmatrix} \right] 
\Rightarrow \Pi_{ij} = \mu \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right)$$

Then the,  $i^{\rm th}$  term of the, divergence of  $\Pi$ , for constant kinematic viscosity  $\mu$ 

$$\begin{split} (\nabla \cdot \Pi)_i &= \sum_j = \frac{\partial \Pi_{ji}}{\partial x_j} \\ &= \mu \sum_j \frac{\partial}{\partial x_j} \left( \frac{\partial u_j}{\partial x_i} + \frac{\partial u_i}{\partial x_j} \right) \\ &= \mu \sum_j \frac{\partial}{\partial x_j} \left( \frac{\partial u_j}{\partial x_i} \right) + \frac{\partial^2 u_i}{\partial x_j^2} \\ &= \mu \sum_j \frac{\partial}{\partial x_i} \underbrace{\left( \frac{\partial u_j}{\partial x_j} \right)}_{=\nabla \cdot \vec{u} = 0} + \frac{\partial^2 u_i}{\partial x_j^2} \quad \text{ equality of mixed partials} \\ &= \mu \sum_j \frac{\partial^2 u_i}{\partial x_j^2} \end{split}$$

Therefore,

$$\boxed{\nabla \cdot \Pi = \mu \nabla^2 \vec{u}}$$

**Question 2**: Derive the equation for the evolution of vorticity  $\omega = \nabla \times \vec{u}$  from the momentum equation

Assuming density is constant and there is no viscous dissipation  $(\nabla \cdot \Pi = 0)$ , then the momentum equation becomes

$$\rho_0 \frac{D\vec{u}}{Dt} = -\nabla p + \underbrace{\nabla \cdot \Pi}_{=0}.$$

expanding the substantial derivative and multiplying the momentum equation by  $(\nabla \times)$ 

$$\rho_0 \left( \nabla \times \left( \frac{\partial \vec{u}}{\partial t} + \vec{u} \cdot \nabla \vec{u} \right) \right) = \nabla \times (-\nabla p).$$

by continuity

$$\nabla \times \frac{\partial \vec{u}}{\partial t} = \frac{\partial (\nabla \times \vec{u})}{\partial t} = \frac{\partial \omega}{\partial t}.$$

and using the identity

$$(\vec{u}\cdot\nabla)\vec{u} = (\nabla\vec{u})\cdot\vec{u} - \vec{u}\times\underbrace{(\nabla\times\vec{u})}_{=\omega}.$$

we have

$$\rho_0 \left( \frac{\partial \omega}{\partial t} + \underbrace{\nabla \times [(\nabla \vec{u}) \cdot \vec{u} - \vec{u} \times \omega]}_{=0} \right) = -\underbrace{\nabla \times \nabla p}_{=0}.$$

where the curl of grad is zero  $\nabla \times \nabla(\cdot) = 0$ . Dividing by  $\rho_0$ 

$$\frac{\partial \vec{\omega}}{\partial t} - \nabla \times \vec{u} \times \vec{\omega} = 0.$$

using the identity  $\nabla \times (\vec{u} \times \vec{\omega}) = \vec{u}(\underbrace{\nabla \cdot \vec{\omega}}) - \vec{\omega}(\underbrace{\nabla \cdot \vec{u}}) + (\vec{\omega} \cdot \nabla)\vec{u} - (\vec{u} \cdot \nabla)\vec{\omega}$ . Where  $\nabla \cdot \vec{\omega} = 0$  because it is the divergence of curl, and  $\nabla \cdot \vec{u} = 0$  due to the flow

being incompressible. Therefore, the equation for the evolution of vorticity is

$$\frac{\partial \vec{\omega}}{\partial t} + (\vec{u} \cdot \nabla)\vec{\omega} = (\vec{\omega} \cdot \nabla)\vec{u}.$$

or, using the substantial derivative

$$\boxed{\frac{D\vec{\omega}}{Dt} = (\vec{\omega} \cdot \nabla)\vec{u}}.$$

#### Thermal energy equation and hydrostatic equi- $\mathbf{3}$ librium

#### **Energy equation**

Using  $\nabla \cdot \Pi = \mu \nabla^2 \vec{u}$  for incompressible Newtonian fluid, find the expression for viscous heating  $\phi$ 

### 3.2 Hydrostatics

Hydrostatic equilibrium is derived from the momentum equation assuming there is no fluid motion

$$-\nabla p + \rho \vec{g} = 0.$$

**Question 1**: In Cartesian coordinates with  $\vec{g} = -g\vec{e}_z$ , we have

$$-\begin{pmatrix} p_x \\ p_y \\ p_z \end{pmatrix} = \rho \begin{pmatrix} 0 \\ 0 \\ g \end{pmatrix}.$$

**Question 2**: The liquid equation of state implies density is simply a function of temperature

$$\rho = \rho(T)$$
.

and since the liquid is isothermal, temperature is constant  $T=T_0$ . This implies density is constant

$$\rho = \rho_0$$
.

 $p_x = 0$ , and  $p_y = 0$  implies pressure is independent of x and y, so we have

$$p_z = -\rho_0 g$$
 is constant.

integrating with respect to z

$$p(z) = -g\rho_0 z + p_0.$$

since pressure is zero at the surface  $p(H)=0 \Rightarrow p_0=g\rho_0H$ , then pressure increases linearly from z=H to z=0

$$p(z) = -g\rho_0 z + g\rho_0 H$$

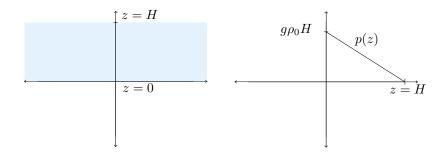


Figure 4: liquidEOS

**Question 3**: For an isothermal perfect gas equation of state, pressure is a function of density only  $p(\rho) = R\rho T_0$ . So the equation for hydrostatic equilibrium in terms of density

$$\rho_z = -\rho \frac{g}{RT_0}.$$

Integrating with respect to z

$$\ln \rho = -\frac{g}{RT_0}z + c.$$

$$\Rightarrow \rho(z) = \rho_0 e^{-\frac{g}{RT_0}z}.$$

Here density decreases exponentially from z=0

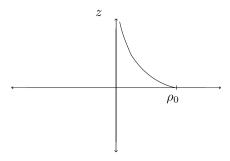


Figure 5: perfectgasEOS

The scaleheight, H, comparing the perfect gas equation of state and Boyles law

$$\frac{p}{\rho} = gmH = RT_0.$$