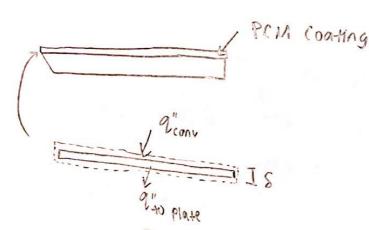
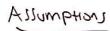
Problem 1



Heat Transfer Rates



- No radiation
- Thin Plate
- no heat generating
- -Ts constant for Plate
- Ts constant for PCM

(b)
$$\dot{E}_{in} - \dot{E}_{out} + \dot{E}_{gen} = \dot{E}_{st}$$

hous transfer rak applied to plate

Problem ?

Assumptions

(a)

$$-\frac{C_{i}}{2}\left(\frac{3a}{3h}\right)^{2}\left(1\right)\left(\frac{3a}{3h^{2}}\right)^{2}$$

- Pr is very small so
$$S<(S_4 \rightarrow U=U_{00})$$

$$-\frac{y}{C_{f}}\left(\frac{\partial y}{\partial y}\right)^{2} \left(\zeta \left(\frac{\partial^{2} y}{\partial y^{2}}\right)^{2}\right) + \left(\frac{\partial^{2} y}{\partial y^{2}}\right)^{2} = \alpha + b\left(\frac{y}{\delta}\right) + \left(\frac{y}{\delta}\right)^{2}$$

$$-\frac{Constant}{S} = \alpha + b\left(\frac{y}{\delta}\right) + \left(\frac{y}{\delta}\right)^{2}$$

$$-\frac{Steady}{S} = 0$$

$$-\frac{S}{S} = \frac{1}{S} + \frac{2C}{S} = \frac{1}{S} + \frac{2C}{S}$$

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$$\frac{T - T_s}{T_{\infty} - T_s} = Z\left(\frac{y}{s}\right) - \left(\frac{y}{s}\right)^2$$

$$b = -2(-1)$$
 $b = -2(-1)$
 $b = 2$

(b) velocity field is constant relative to thermal boundary layer being larger with Small Pr U= U00

$$\frac{d}{dx} \left[\int_{\delta}^{\delta} (T_{\infty} - T) \cup_{\infty} dy \right] = \left[\int_{\delta}^{\delta} \frac{\partial T}{\partial y} \Big|_{y=0} \right]$$

$$T = \left(T_{\infty} - T_{s}\right) \left(2 \left(\frac{y}{s}\right) - \left(\frac{y}{s}\right)^{2}\right) + T_{s}$$

$$\frac{\partial T}{\partial y}\Big|_{y=0} = \left(T_{\infty} - T_{S}\right) \left(\frac{2}{S} - \frac{2}{S} \left(\frac{0}{S}\right)\right) = \left(T_{\infty} - T_{S}\right) \left(\frac{2}{S}\right)$$

$$\frac{d}{dx}\left(\left(\frac{1}{100}-\frac{1}{1}\right)\int_{0}^{\delta}\left(1-\left(2\left(\frac{u}{s}\right)-\left(\frac{u}{s}\right)^{2}\right)V_{M}dy\right)=d\left(\frac{2}{100}-\frac{1}{1}\right)\left(\frac{2}{s}\right)$$

$$\frac{d}{dx}\left(\left(\frac{1}{100}-\frac{1}{1}\right)\int_{0}^{\delta}\left(1-\left(2\left(\frac{u}{s}\right)-\left(\frac{u}{s}\right)^{2}\right)V_{M}dy\right)=d\left(\frac{2}{100}-\frac{1}{1}\right)\left(\frac{2}{s}\right)$$

$$\frac{d}{dx}\left(\left(\frac{1}{100}-\frac{1}{1}\right)\left(\frac{2}{s}\right)+\frac{u^{2}}{3(s)}+\frac{u^{2}}{3(s)}+\frac{u^{2}}{3(s)}\right)=d\left(\frac{2}{s(x)}\right)$$

$$\frac{d}{dx}\left(\frac{1}{100}-\frac{1}{s(x)}+\frac{u^{2}}{3(s)}+\frac{u^{2}}{3(s)}+\frac{u^{2}}{3(s)}\right)=d\left(\frac{2}{s(x)}\right)$$

$$\frac{d}{dx}\left(\frac{1}{100}-\frac{1}{s(x)}+\frac{u^{2}}{3(s)}+\frac{u^{$$

$$\frac{d}{dx} \left[\int_{0}^{8} \left(v_{00} - v \right) v \, dy \right] = v \frac{\partial v}{\partial y} \Big|_{y=0}.$$

$$\frac{T_s = M \frac{\partial U}{\partial y}|_{y=0}}{2J} = \frac{T_s}{M} = \frac{\partial U}{\partial y}|_{y=0}$$

$$\frac{U_s}{M} = \frac{U_s}{M} = \frac{U_s}{$$

$$\frac{\partial}{\partial x} \left[\int_{0}^{8} \left(V_{00} - U \right) U dy \right] = 0.02289 U_{00}^{2} \left(\frac{V_{00} 8}{20} \right)^{-1/4} = 0.0228 U_{0}^{2} \left(\frac{V_{00} 8}{20} \right)^{-1/4}$$

$$U = U_{00} \left(\frac{U}{8} \right)^{1/7}$$

$$\frac{d}{dx} \left[\int_{0}^{8} U_{\infty} U - U^{2} dy \right] = \frac{d}{dx} \left[\int_{0}^{8} U_{\infty}^{2} \left(\frac{y}{8} \right)^{1/7} - U_{\infty}^{2} \left(\frac{y}{8} \right)^{2/7} \right]$$

$$= 0.0228 U_{\infty}^{2} \left(\frac{U_{\infty} S}{S} \right)^{-1/4}$$

$$\frac{d}{dx}\left(\frac{1}{8}\left(\frac{1}{8}\right)^{1/2}\left(y\right)^{8/2}-\frac{1}{9}\left(\frac{1}{8}\right)^{2/2}\left(y\right)^{9/2}\right)\Big|_{8}^{8}=0.0228\left(\frac{\sqrt{6}8}{3}\right)^{-1/4}$$

$$\frac{d}{dx}\left(\frac{7}{5}\left(\frac{1}{5}\right)^{1/7}(5)^{8/7} - \frac{7}{4}\left(\frac{1}{6}\right)^{2/7}(5)^{4/7}\right) = \frac{\partial}{\partial x}\left(\frac{7}{8}5 - \frac{7}{4}5\right) = \frac{\partial}{\partial x}\left(\frac{7}{72}5\right)$$

$$\frac{\partial x}{\partial s} = (0.0228) \left(\frac{72}{12}\right) \left(\frac{70}{100}\right)^{-1/4} s^{-1/4} \rightarrow \int_{0.0228}^{\infty} \left(\frac{12}{12}\right) \left(\frac{70}{100}\right)^{-1/4} s^{-1/4}$$

$$\int_0^{\delta} \delta^{1/4} d\delta = \int_0^{\infty} 0.0228 \left(\frac{72}{7}\right) \left(\frac{U_p}{2}\right)^{1/4} dx$$

$$\frac{4}{5} \int_{-\infty}^{5/4} = 0.0228 \left(\frac{72}{7}\right) \left(\frac{10}{7}\right)^{1/4} \times \rightarrow \int_{-\infty}^{5} = \left(\frac{5}{7}\right) \left(\frac{10}{7}\right)^{1/4} \left(\frac{10}{7}\right)^{1/4} \left(\frac{10}{7}\right)^{1/4} \left(\frac{10}{7}\right)^{1/4} \times \left(\frac{10}{7}\right)^{1/4} \left(\frac{10}{7}\right)^{1/4} \times \left(\frac{10}{7}\right)^{1/4} \left(\frac{10}{7}\right)^{1/4} \times \left(\frac{10}{7}$$

$$S = 0.3747 \left(\frac{U_{00}}{2} \right)^{-1/5} \times 4/5$$

d ((= 0 - T) udy = d = 0 $T = (T_s - T_w) \left(1 - \left(\frac{y}{s}\right)^{1/7}\right) + T_{co}$ $\frac{\partial}{\partial x} \left[\int_{0}^{S_{+}} \left(T_{00} - \left(T_{S} - T_{\mu} \right) \left(1 - \left(\frac{y}{S_{+}} \right)^{1/7} \right) - T_{\mu} \right) U dy \right] = \frac{h}{\mathcal{F}_{Cp}} \left(T_{00} - T_{S} \right)$ $\frac{d}{dx}\left[\int_{0}^{\delta_{1}}\left(T_{N}-T_{s}\right)\left(1-\left(\frac{y}{s_{s}}\right)^{1/2}\right)U_{00}\left(\frac{y}{s}\right)^{1/2}dy\right]=\frac{h}{sC_{p}}\left(T_{00}-T_{s}\right)$ $\frac{d}{dx} \left[\int_{0}^{\delta_{+}} \left(\frac{1}{\delta} \right)^{1/7} (y)^{1/7} - \left(\frac{1}{\delta_{+}} \right)^{1/7} \left(\frac{1}{\delta} \right)^{1/7} y^{2} / r dy \right] = \frac{h}{\rho C_{\rho} U_{m}}$ $\frac{\partial}{\partial x} \left[\left(\frac{1}{5} \right)^{1/7} \left(\frac{7}{5} \right) y^{8/7} - \left(\frac{1}{51} \right)^{1/7} \left(\frac{1}{5} \right)^{1/7} \left(\frac{7}{9} \right) y^{9/7} \right] \right|_{S_{+}}^{S_{+}} = \frac{h}{-9 c_{p} U_{pp}}$ $\frac{d}{dx} \left[\frac{7}{8} \frac{(S_{+})^{8/7}}{(S)^{1/7}} - \frac{7}{9} \frac{S_{+}^{8/7}}{8^{1/7}} \right] = \frac{7}{72} \frac{d}{dx} \left(\frac{S_{+}^{8/7}}{8^{1/7}} \right) = \frac{h}{fC_{P}} \frac{1}{V_{00}}$ For turbulent flow S=S+ * Assume $\int_{0}^{\delta_{+}} 1 d \delta_{+} = \int_{0}^{\chi} \frac{72}{7} \frac{h}{4C_{0}(1)} d \chi + \delta_{+} = \frac{72}{7} \frac{h}{9C_{p}U_{po}} \chi$ N78+9Cp Up = hx

Nux = hx

 $Nu_{x} = \frac{7}{72} \frac{P(P)}{R} \frac{U_{0}}{S} \cdot \frac{V}{I} S_{+}$ ASSUM: $S = S_{+} \rightarrow S_{+} = 0.3747 \left(\frac{U_{0}}{S}\right)^{-1/5} \times ^{4/5}$ $Nu_{x} = \frac{7}{72} Pr \frac{U_{0}}{S} \left(0.3747\right) \left(\frac{U_{0}}{S}\right)^{-1/5} \times ^{4/5}$ $Nu_{x} = \left(\frac{7}{72}\right) \left(0.3747\right) Re^{4/5} Pr = 0.03642 Re_{x}^{4/5} Pr$

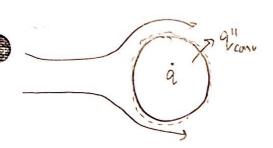
$$\overline{f} = \frac{1}{b-a} \int_{a}^{b} f(x) dx$$

$$Nu_{x} = \int_{0}^{x} Nu_{x} dx \left(\frac{1}{x}\right) = 0.03642 P_{x} \left(\frac{u_{x0}}{2}\right)^{4/5} \int_{0}^{x} u^{4/5} du \frac{1}{x}$$

$$= 0.03642 P_{x} \left(\frac{u_{x0}}{2}\right)^{4/5} \frac{5}{9} \frac{x}{x}$$

$$= 0.02023 Re_{x}^{4/5} P_{x}$$

Problem 4



$$\dot{q} = \dot{q}''_{conv}$$
 $TTDL$

$$\dot{q} = \frac{\dot{E}^2}{R_w}$$
 $q''_{conv} = \bar{h} (T_w - T_w)$

$$\frac{E^{2}}{Rw} = \overline{h} \left(T_{w} - T_{w} \right) TIDL$$

$$\overline{h} = \frac{E^{2}}{Rw} \left(T_{w} - T_{w} \right) TIDL$$

$$V_{W} = \frac{1}{k} = 0.0296 R e_{p} P_{r}^{1/3}$$

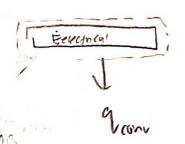
$$V_{W} = \frac{1}{k} = 0.0296 (U_{\infty})^{4/5} D^{4/5} D^{4/5} R(y)^{4/3}$$

$$= \frac{1}{k} = \frac{1}{k} = 0.0296 (U_{\infty})^{4/5} D^{4/5} R(y)^{4/3}$$

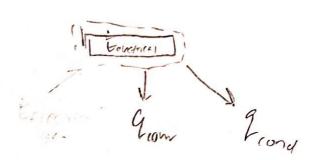
$$= \frac{1}{k} = \frac{1}{k} = 0.0296 (U_{\infty})^{4/5} D^{4/5} R(y)^{4/3}$$

$$= \frac{1}{k} = \frac{1}{k} = 0.0296 R_{\infty} (T_{\omega} - T_{\omega}) R(y)^{4/5} D^{4/5} D^{$$

Casel







Since Tw= constant, the energy leaving both systems

Tronv, = Tronvz

Equation = quan

EIN-East + Egen = Est Electrical = 9 conv + 9 conv

E electrical, 1 = E electrical 2 - 9 cond

In Case 2 W/ 10ss es, the instrument will held to
Supply energy that isn't lost to the fluid. This causes
the system to predict a higher heat transfer
than expected. This would cause an over prediction

In Up