

# PyCHAM (v1.3.3): a Python box model for simulating aerosol chambers

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**Abstract.** Box models of aerosol chambers simulate multi-phase processes to reproduce chamber observations. Comparison of chamber measurements with model estimates allows improvement of process understanding that can be transferred to ambient atmosphere simulations, thereby enabling evaluation of how chamber insights impact the real-world atmosphere. However, there is not yet an open-source modelling software designed for ease of use for chamber scientists. To fulfil this requirement PyCHAM (CHemistry with Aerosol Microphysics in Python) has been produced and is described and verified here. PyCHAM provides the basis for transferring improved process understanding from chamber measurements to regional and global simulations involving aerosol. In this model description paper we present governing equations, verification, and assessment of sensitivities to model inputs. The PyCHAM software is built for desktop computers, with releases available at <https://github.com/simonom/PyCHAM>.

10 *Copyright statement.* TEXT

## 1 Introduction

For the mixture of gases and particles (aerosol) that comprise atmospheres our paucity of understanding presents serious societal issues. Forecasts of climate change and air quality underpin international and national legislation (e.g. UNFCCC, 2018; UK Government, 2020; European Commission Environment, 2020) that demands major economic and political restructuring (MIT Science and Policy of Global Change, 2020) in addition to driving ethical incentives to change behaviour. Whilst our understanding is sufficient to target emission decreases for certain pollutants, uncertainty around the extent of decrease and type of emission remains considerable (Heal et al., 2012; Johnson et al., 2018; Tong et al., 2019). To improve the efficiency of emission targets requires improved understanding of the gas- and condensed-phase processes determining atmospheric abundance of trace constituents. This is the aim of aerosol chambers, which have the advantage of controlling physicochemical conditions to isolate and observe select processes (Schwantes et al., 2017; Charan et al., 2019).

Many major advances in atmospheric modeling have arisen from chamber observations. For example, the partitioning of vapours to particles developed in Odum et al. (1996) and applied in Meng et al. (e.g. 1997) and the gas-phase chemistry of ozone as part of the Master Chemical Mechanism (MCM) developed in Jenkin et al. (1997) and applied in Ying and Li (e.g. 2011). Such advances can be incorporated into improved chamber models (e.g. Charan et al., 2019), aiding the design of experiments to interrogate further processes and systems (e.g. Riva et al., 2020). As chamber use has multiplied, so too have chamber models, with many now published (Naumann, 2003; Pierce et al., 2008; Lowe et al., 2009; Roldin et al., 2014; Sunol et al., 2018; Topping et al., 2018; Charan et al., 2019; Roldin et al., 2019). To our knowledge, however, these have not prioritised accessibility and/or usability. Consequently, chamber research groups without access or ready application of a model are limited in the design, interpretation and advancement of both chamber experiments and their contribution to models. To address this limitation, the EUROCHAMP2020 (Oliveri, 2018) research project and National Centre for Atmospheric Science have developed PyCHAM (CHemistry with Aerosol Microphysics in Python), a zero-dimensional aerosol chamber box model. The model software along with the figures (and required inputs) from this paper are available open-source here: <https://github.com/simonom/PyCHAM>.

In this paper the processes represented in PyCHAM are described, along with details of software application. Where relevant, equations are presented and output from PyCHAM verified. In the following two sections the objectives, rationale and structure of the software are explained.

## 2 Purpose and Scientific Basis

Consistent with the criteria set by the EUROCHAMP2020 research project (Oliveri, 2018), PyCHAM is open source, user-friendly and representative of the latest scientific understanding. Python is the chosen language for two key reasons: code can be transferred between computers without the limitation of requiring a certain compiler (thereby improving ease of use), and the relatively versatile parsing capability which allows the user to readily vary model inputs. To ascertain the access, usability and basic functionality of the software, PyCHAM has been reviewed in O'Meara et al. (2020). Whilst the O'Meara et al. (2020) article provides only a very brief description of PyCHAM, the objective of the current paper is a detailed description coupled with introductory analysis.

Aerosol chambers (interchangeably called smog chambers), defined as those used for interrogating gas- and particle-phase processes, provide a method for isolating specific processes of interest without the convoluting effects present in the ambient atmosphere. Ultimately the goal of the chamber is to improve understanding and quantitative constraint on the evolution of the physicochemical properties of the gas- and particle-phase (Schwantes et al., 2017; Charan et al., 2019; Hidy, 2019). The aim of EUROCHAMP2020 was to advance application of chambers by tackling various weaknesses; consequently, the publications (Oliveri, 2018) resulting from the project provide a thorough introduction to chamber capabilities and operations. A chamber experiment begins with a container (walls are made of a range of materials, but frequently of fluorinated ethylene-propene film (FEP Teflon)), followed by one of two approaches to inlet components: batch mode whereby set volumes of gas or particle are injected at specific times, or in flow mode with a constant influx of gas or particle (Jaoui et al., 2014). The model variables

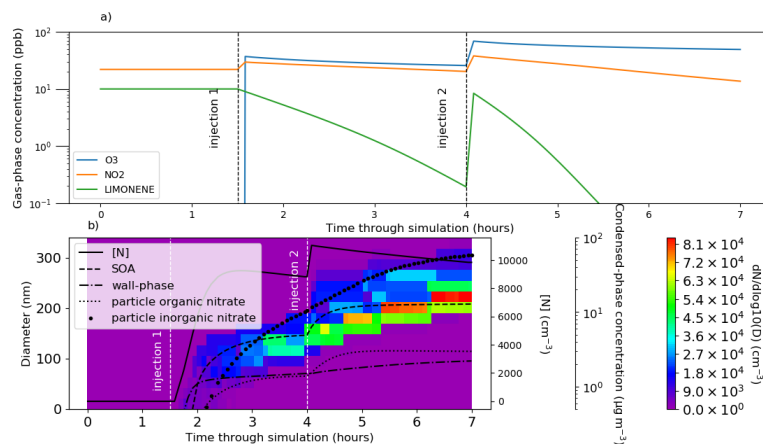
input file for PyCHAM allows users to setup simulations for both modes along with several other specifications representing the majority of aerosol chamber experiments: with or without seed particles (for absence of seed particles nucleation can be simulated); variable temperature, pressure and relative humidity; for lit experiments, either natural light intensity (for open roof chambers) or known actinic flux (for chambers with bulbs) that can be turned on and off at set times. A full list of the model variables is given in Appendix A.

Two previous models act as platforms on which PyCHAM developed: the Microphysical Aerosol Numerical model Incorporating Chemistry (MANIC) (Lowe et al., 2009) and PyBox (Topping et al., 2018), with the former guiding multi-phase processes and the latter guiding python parsing and automatic generation of chemical reaction modules. With the combination of these two pillars, PyCHAM provides a very flexible tool for aerosol chamber scientists whilst representing the latest understanding of key chamber processes: gas-phase photochemistry, gas-particle and gas-wall partitioning, coagulation, nucleation and particle deposition to walls. Consequently its full list of applications is numerous and will certainly grow as chamber experiments evolve, however, key examples include designing chamber experiments, testing and developing gas-phase chemistry mechanisms, quantifying particle and wall partitioning parameters, testing and developing nucleation models and interrogating the effects of processes on secondary organic aerosol (SOA) evolution.

The processes included in PyCHAM may also be represented in large-scale (regional and global) atmospheric models and it is intended that once a process has been successfully modelled by PyCHAM it can be transferred, possibly via parameterisation, to a large-scale model for evaluation, similar to the modelling advances mentioned in the introduction. When interrogating the simulation of a given process it is necessary that convoluting processes are either negligible or verified such that uncertainty around their effects is not compromising. This paper presents verification (through comparison with established models) that the individual process models in the base version of PyCHAM are accurate.

Whilst the majority of this paper is dedicated to studying the process models in PyCHAM in isolation, it is worthwhile illustrating its ability to couple gas-phase chemistry, gas-particle and gas-wall partitioning, particle deposition to walls, coagulation and nucleation in a relatively complex case. Therefore, a simulation has been designed around the role of nitrate radical ( $\text{NO}_3$ ) oxidation of limonene in SOA evolution. Such an experiment has implications for indoor air quality, particularly at night time when the photolysis of  $\text{NO}_3$  ceases (Waring and Wells, 2015), therefore lights were turned off for this simulation. Accurate results can constrain the exposure of individuals to harmful aerosol (Carslaw and Shaw, 2019). Following a similar approach to the experiment of Fry et al. (2011), the effect of  $\text{NO}_3$  in the presence of ozone ( $\text{O}_3$ ) can be replicated through introduction of  $\text{O}_3$  and nitrogen dioxide ( $\text{NO}_2$ ) into the chamber whilst removing the effect of the hydroxyl radical ( $\text{OH}$ ) through addition of excess carbon monoxide. At sufficient concentrations, this mixture causes particle nucleation (Fry et al., 2011), which we simulate here through the nucleation parameterisation described below.  $\text{O}_3$ ,  $\text{NO}_2$  and limonene are injected again later but with the addition of seed aerosol for reproduction of indoor environments with substantial existing particulate matter.

Simulation results in Fig. 1 show the time-profile of gas-phase concentrations of reactant components and mass concentrations of grouped components in the particle and wall phase. The contribution of  $\text{NO}_3$  oxidation of limonene to SOA is indicated by the particle organic nitrate curve. The particle inorganic nitrate curve represents the contribution of dinitrogen pentoxide



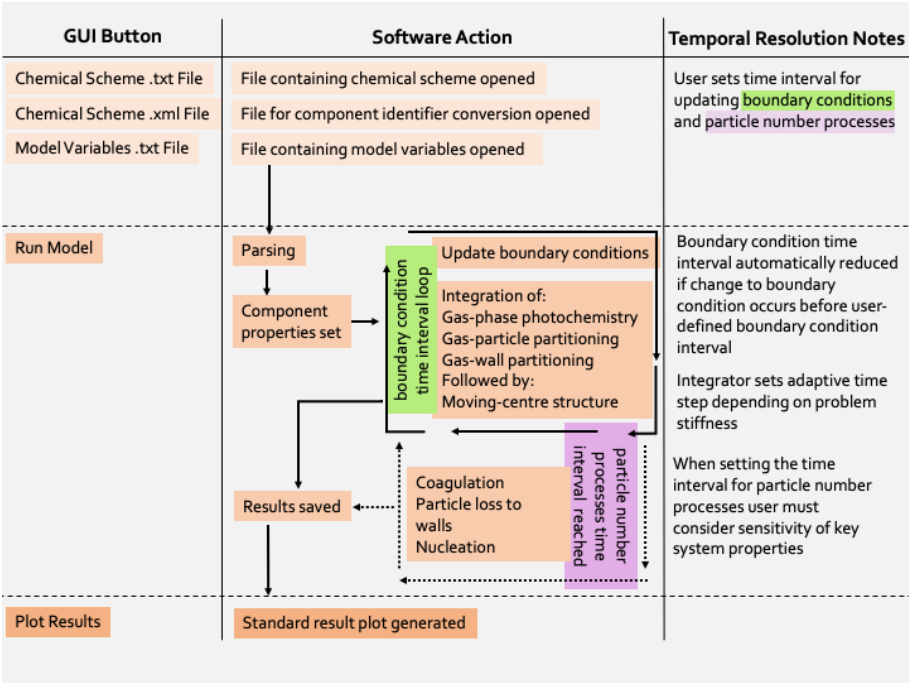
**Figure 1.** Limonene oxidation in the dark with and without seed particles. In a), the gas-phase concentrations of key components and in b), the particle properties. At the start 10 ppb limonene, 22 ppb NO<sub>2</sub> and 500 ppm CO are introduced. At 1.5 hours 38 ppb O<sub>3</sub> and 8 ppb NO<sub>2</sub> are injected (injection 1). At 4 hours a further injection of O<sub>3</sub> (45 ppb), limonene (10 ppb) and NO<sub>2</sub> (19.0) is coincident with an injection of seed aerosol ( $10 \mu\text{g m}^{-3}$  with a mean diameter of  $0.2 \mu\text{m}$ ) (injection 2). In b), the total particle number concentration ([N]) corresponds to the first of the right axes, mass concentrations of: secondary organic aerosol mass concentration (SOA), components condensed to walls (wall-phase) and sum of particle-phase organic components with a nitrate functional group (particle organic nitrate) correspond to the second of the right axes, whilst number size concentrations correspond to the filled contours, colour bar and left axis. Whilst [N] includes seed particles, SOA excludes the seed material and all mass concentrations exclude water.

(N<sub>2</sub>O<sub>5</sub>) and nitric acid (HNO<sub>3</sub>) to the particle phase. Here we simulate the hydrolysis of N<sub>2</sub>O<sub>5</sub> into the aqueous phase of particles and wall by setting its activity coefficient to zero and its accommodation coefficient according to Lowe et al. (2015).

As detailed below, for accurate application of PyCHAM output the partitioning of components to chamber walls is key; without its correct reproduction, comparison against measurements is compromised. However, with correct wall process constraint, simulations such as Fig. 1 can be compared against measurements to verify process understanding. For example, gas-phase organic chemistry research has recently revealed the role of highly oxidised molecules (HOM) (Ehn et al., 2014), with the Peroxy Radical Autoxidation Mechanism (PRAM) simulating their chemistry (Roldin et al., 2019). For the results in Fig. 1, the PRAM scheme has been coupled with that of the Master Chemical Mechanism (MCM) (Jenkin et al., 1997; Saunders et al., 2003). Whilst we do not yet have the measurement ability to quantify the particle- or gas-phase concentrations of individual HOM components, comparison of particulate loading in experiments where HOM is detected provides a useful evaluation tool.

### 3 General Structure

For ease of navigation, PyCHAM has a modular structure with each key physicochemical process assigned an individual module. At the core of PyCHAM lies simultaneous numerical integration of three coupled processes: gas-phase photochemistry,



**Figure 2.** Schematic outlining the steps in the PyCHAM model, as directed by the GUI buttons, with arrows showing the sequence of code. The repeat of model loop time intervals terminates when the end time is reached. The dashed lines indicate the conditional action of modelling the processes affecting particle number (determined by the particle number process time interval).

vapour-particle partitioning and vapour-wall partitioning. The ordinary differential equations (ODEs) for these processes are solved by the backward differentiation formula (which has proven reliability (Jacobson, 2005)) from the CVODE Sundials software (Hindmarsh et al., 2005). We use Assimulo (Andersson et al., 2015), a python wrapper for sundials allowing communication between the solver and Python code. The model structure is outlined in the schematic of Fig. 2, where we introduce the time interval for updating boundary conditions, such as injection of seed particles. The boundary condition time interval is passed to the integrator, which adaptively sets sub-time steps depending on problem stiffness.

Three processes affecting particle number concentration: coagulation, particle loss to walls and nucleation are operator split from the ODEs mentioned above. The size-resolved particle number concentration is a boundary condition for gas-particle partitioning and therefore must be updated outside the ODE solution. Whilst coagulation and particle loss to wall have timescales of minutes to hours (Section 11), nucleation can cause substantial changes within seconds. To be adaptable to varying conditions, operator-split processes are solved over a separate time interval to the ODEs (Fig. 2). Simulation sensitivity to the operator split is investigated in Section 11, including recommendations for its maximum time interval.

In the example model output of Fig. 1 several features of PyCHAM are demonstrated. First, the coupling of gas-phase chemistry and resulting partitioning of vapours with sufficiently low volatility to particles and walls. Nucleation has been simulated prior to the introduction of seed particles with approximate values given for the tuned nucleation parameters described below

such that nucleation begins at the introduction of ozone, has a duration of thirty minutes and produces a peak number concentration similar to that of the seed particle. Finally, coagulation and particle wall loss (the latter using the model of McMurry and Rader (1985)), contribute to the decay in particle number concentration.

The PyCHAM software is initiated with the terminal/command window to generate a graphical user interface (GUI). Via the  
120 GUI, users select three files (Fig. 2) representing: i) the chemical scheme, ii) a file associating the chemical identifiers inside the chemical scheme to their Simplified Molecular Input Line Entry System (SMILE) strings (Weininger, 1988), and iii) a model variables file. A fourth button on the GUI starts the simulation. Unit tests to track the effect of additional development to modules are contained in the software package.

A parsing module interprets the chemical scheme and uses the chemical identifier conversion file to match component identifiers to their SMILE strings. Additionally, modules are automatically created that will calculate time-dependent chemical  
125 reaction rates and track the rate of change of specified components. A gas-phase initiation module sets the starting concentrations of injected components, whilst a particle-phase initiation module establishes any seed particles at experiment start. The integration module is then called, which loops over the boundary condition time interval to update boundary conditions and solve the ODEs for gas-phase photochemistry and partitioning (Fig. 2). Following integration, the moving-centre module is  
130 called to redistribute particles that have changed size sufficiently to cross size bin boundaries. The operator-split processes of particle loss to wall, coagulation and nucleation are the final calculations of a time step if their time interval is met. A saving module stores results for gas, particle and wall concentrations, corresponding time, particle number size distributions (with and without water) and constants such as component molecular weight.

The fifth and final button on the GUI will display and save graphs of the temporal profiles of number size distribution, secondary aerosol mass concentration, total particle number concentration, and the gas-phase concentrations of specified com-  
135 ponents. The programme can be stopped via the terminal when in integration mode, or outside this mode it can be terminated by closing the GUI.

Below we describe and verify the processes described above as coded in PyCHAM. Necessarily each process is treated in isolation, however, Fig. 1 and its associated text exemplify the coupling of mechanisms for a real world application.

## 140 4 Component Properties

The components included in the user-defined chemical scheme are automatically allocated three properties by the PyCHAM software: molecular weight, liquid density and liquid saturation vapour pressure. Molecular weights are estimated by passing SMILE strings to the pybel module of the Open Babel chemical toolbox (O'Boyle et al., 2011). pybel is installed as part of the PyCHAM package and generates unique chemical identifiers for each component based on their SMILE string. For  
145 estimating component densities and liquid-phase saturation vapour pressures, the pybel chemical identifiers are passed to the UManSysProp module (Topping et al., 2016) which is updated on the first run of PyCHAM and at the request of the user (via the model variables file) thereafter (requires internet connection). By default the UManSysProp module applies the liquid density estimation method of Girolami (1994) (recommended by Barley et al. (2013)) and the liquid saturation vapour pressure

estimation method of Nannoolal et al. (2008) (recommended by O’Meara et al. (2014)). Component vapour pressures have a first order effect on partitioning between phases, however estimates for certain components, particularly those with relatively low vapour pressures as these are most difficult to measure experimentally and therefore inform estimation methods, are associated with considerable uncertainty (O’Meara et al., 2014). Consequently, users can also specify the vapour pressures of certain components. Similarly, although the default particle- and wall-phase activity coefficient for all components is one, users may set an alternative value for specific components in the model variables folder.

## 155 5 Gas-phase Chemistry

For a chamber experiment including injection of reactive components, chemical reactions in the gas-phase drive the disequilibria that changes all three phases: gas, particle and wall. As mentioned above, the MCM provides a near-explicit model of gas-phase chemistry for several organic precursors, and developments such as PRAM (Roldin et al., 2019) provide updates to our understanding of atmospheric chemistry. PyCHAM is designed to accommodate such chemical schemes whilst also accepting very simplified or even empty (e.g. for a control simulation comprising only seed particles) chemical equation files. Whilst the software manual details the requirements for input chemical schemes and chemical identifier conversion files, here we describe how PyCHAM deals with chemistry. Equations of the general form:

$$s_{r_1}r_1 + s_{r_2}r_2 \dots = s_{p_1}p_1 + s_{p_2}p_2 \dots \quad (1)$$

where  $s$  represents stoichiometric number,  $r$  reactants and  $p$  products, are expressed as the ODEs:

$$165 \quad \frac{d[r_i]}{dt} = -s_{r_i}k_r\Pi_{j=1}^{j=n}([r_j]^{s_{r_j}}) \quad (2)$$

$$\frac{d[p_i]}{dt} = s_{p_i}k_r\Pi_{j=1}^{j=n}([r_j]^{s_{r_j}}) \quad (3)$$

where  $n$  is the total number of reactants and  $r_j$  is a given reactant for a given reaction.  $k_r$  is the reaction rate coefficient.

For simulations involving gas-phase chemistry, users must therefore provide a reaction(s) of the form in Eq. 1 and an associated reaction rate coefficient inside a chemical scheme file. Naming of chemical components inside the chemical scheme is unrestricted, however, the software must be able to convert names to SMILES (Weininger, 1988). Therefore, users must provide a separate file stating a unique SMILES string for every component (Fig. 2).

Inside the parsing module, reaction rate coefficients, reactant and product identities and their stoichiometric numbers are established from the chemical scheme file. To separate these properties either default formatting may be used, or a variant, so long as the appropriate changes are made inside the model variables file. By default, MCM Kinetic PreProcessor (Sander and Sandu, 2006) formatting is used (Jenkin et al., 1997; Saunders et al., 2003). The MCM is presented via a user-friendly website (Rickard and Young, 2020) and is the recommended source for atmospheric chemistry schemes.

Reaction rate coefficients can be functions of temperature, relative humidity, pressure and concentrations of: third body, nitrogen, oxygen and peroxy radicals. Third body, nitrogen and oxygen concentrations are calculated by the ideal gas law with the user-set temperature and pressure. As in the MCM, the chemical scheme file can include generic reaction rate coefficients (those that have an identifier which is used as the reaction rate coefficient for one or more reactions). Furthermore, the scheme can include a list of peroxy radicals, which is necessary if reaction rate coefficients are to be functions of radical concentrations.

Photochemistry is controlled through stating light on/off times inside the model variables file. The treatment of photochemistry is determined by the user and depends on the chemical scheme employed. In the case of the MCM scheme and natural sunlight, the scattering model based on Hayman (1997) and described in Saunders et al. (2003) is invoked by stating the relevant spatial and temporal coordinates in the model variables file. For artificial lights, users must provide a file stating the wavelength-dependent actinic flux (as described in the manual). The model then calls on either the absorption cross-section and quantum yield estimates of MCM v3.3.1 or of a user-defined file.

Users can also specify the components they wish to be tracked during a simulation. PyCHAM automatically generates a module that calculates and records the rate of change of the gas-phase concentration of the given component as a function of individual gas-phase reactions and partitioning. This function is essential for ensuring individual processes affecting a component are being accurately modelled and for trouble-shooting.

## 5.1 Verification

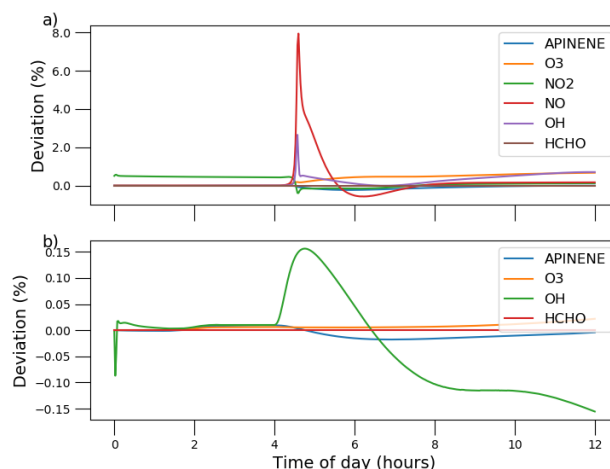
To verify the photochemistry section of PyCHAM, gas-particle partitioning and gas-wall partitioning were turned off, leaving only gas-phase chemistry to be solved. Here we compare against AtChem2 (Sommariva et al., 2018) as a model benchmark, with both using MCM chemical schemes. Fig. 3 shows the deviation with experiment time for two standard aerosol chamber characterisation experiments:  $\alpha$ -pinene ozonolysis in the presence (plot a) and absence (plot b) of NO<sub>x</sub>. To test both the dark and lit scenarios, the simulation is for an environmental chamber with an open roof, starting at midnight and finishing at midday. Initial concentrations of  $\alpha$ -pinene and O<sub>3</sub> were equal at 21.1 ppb for both experiments, whilst for NO<sub>x</sub> the initial concentration was 9.8 ppb in Fig. 3a and 0 ppb in Fig. 3b. Latitude was set to 51.51, longitude to 0.13 (London, UK) and the date to 1<sup>st</sup> July. The deviation between PyCHAM and AtChem2 was calculated using:

$$\sigma_{i,t} = \left( \frac{s_{i,t} - b_{i,t}}{\vee(b_i)} \right) 100, \quad (4)$$

where  $\sigma_{i,t}$  is the percentage deviation (%) for component  $i$  at time  $t$ ,  $s$  is the PyCHAM result,  $b$  is the AtChem2 result.  $\vee(b_i)$  is the AtChem2 maximum for a given component during the simulation which is the chosen scaling factor for deviations as it means any difference between model estimates is referenced against a reasonable value for that component (in contrast scaling by  $b_{i,t}$  when  $b_{i,t} \ll \vee(b_i)$  may introduce a very large percentage deviation for a relatively very small difference between model estimates).

Whilst Fig. 3 indicates that PyCHAM performs well for components with both relatively short (e.g. OH) and long (e.g.  $\alpha$ -pinene) lifetimes, it is necessary to ascertain that agreement is gained through the correct mechanism. Users of PyCHAM



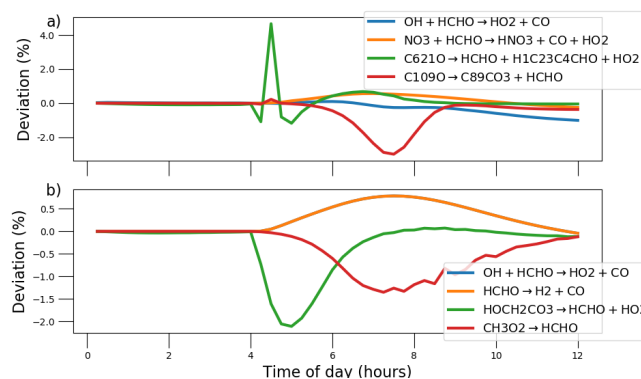


**Figure 3.** Gas-phase photochemistry verified; simulations of photochemistry in an aerosol chamber exposed to natural light, where deviation is defined in Eq. 4.  $\alpha$ -pinene ozonolysis is simulated in both plots, with  $\alpha$ -pinene and O3 given the same initial concentrations of 21.1 ppb, and initial NO<sub>x</sub> concentration in a) 9.8 ppb and in b) 0 ppb. For both simulations, the environmental chamber is transparent and exposed to daylight without cloud interference, with dawn at approximately 4:00 hours. The particle-phase and vapour losses to walls are turned off in PyCHAM to be consistent with the AtChem2 model.

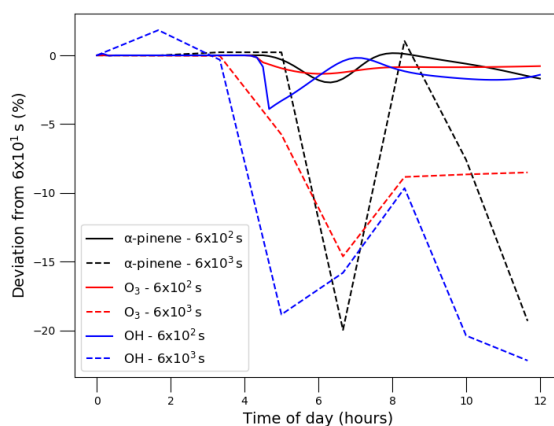
and AtChem2 can specify components that have rates of change tracked. In Fig. 4 we use this to compare the reaction rates for formaldehyde for the same  $\alpha$ -pinene ozonolysis simulations used for Fig. 3. The deviations were again calculated using Eq. 4, but with concentrations replaced by gas-phase concentration rate of change due to a given reaction. Of the loss and production reactions for formaldehyde the two of each with greatest deviation are shown in Fig. 4. The low deviation values in Fig. 4 demonstrate that PyCHAM indeed integrates gas-phase photochemistry correctly.

## 5.2 Photochemical Sensitivity to Temporal Resolution

For minimising the time required for simulation, users can increase the boundary condition time interval (Fig. 2). For discontinuous changes to the simulation, such as the start of component injections, PyCHAM automatically adapts the boundary condition time interval to coincide with the change. However, for continually changing conditions such as continuous injection of components or changing natural light intensity, the boundary condition time interval is determined by the user input. Therefore, increases in time interval can cause loss of temporal detail. The user must balance the need for reduced time for simulation against loss of accuracy in simulated gas-phase concentrations. To illustrate and quantify the issue, the same scenario described above for Fig. 3 is used (i.e., gas-phase chemistry only simulation with increasing natural sunlight intensity). Now we compare PyCHAM low temporal resolution (boundary condition time intervals of  $6 \times 10^2$  and  $6 \times 10^3$  s) results with a PyCHAM high resolution result (time interval of  $6 \times 10^1$  s), with the latter taking the place of AtChem2 inputs to Eq. 4, allowing deviation from the high resolution case to be calculated. Fig. 5 shows the loss of accuracy rising to 20 % for the lowest resolution case for both



**Figure 4.** Deviation of PyCHAM simulated rate of change of formaldehyde (HCHO) from AtChem2 simulations for the MCM reactions given in the legends. Where the definition for deviation is given by Eq. 4. Both plots are results for the  $\alpha$ -pinene ozonolysis reaction described in the main text for Fig. 3, with a) in the presence of NO<sub>x</sub> and b) in the absence of NO<sub>x</sub>.



**Figure 5.** Illustrating the effect of boundary condition time interval resolution in PyCHAM on gas-phase concentrations of  $\alpha$ -pinene, O<sub>3</sub> and OH for the  $\alpha$ -pinene ozonolysis in presence of NO<sub>x</sub> experiment described above for Fig. 3. Time intervals were set to  $6 \times 10^2$  and  $6 \times 10^3$  s as shown in the legend, and the deviation is that from results for a time interval of  $6 \times 10^1$  s.

225 short- and long-lived components. Simulation time for the  $6 \times 10^3$  s resolution was 52 s using a 2.5 GHz Intel Core i5 processor, with factor increases of 7 and 53 for  $6 \times 10^2$  and  $6 \times 10^2$  s resolutions, respectively. Users are advised to conduct a similar test if their chemical scheme or environmental conditions vary significantly from those here.

## 6 Gas-wall partitioning

The partitioning of gases to the chamber wall is often termed wall loss as the net movement is from the gas phase to the wall (for an initially clean chamber wall). Traditionally this process has been viewed as an inconvenience since chamber results often depend on the concentration of gas- and particle-phases of certain components, whilst the fraction of these components lost to walls is poorly constrained. Several studies have focussed on partitioning to Teflon walls, which are frequently employed (Matsunaga and Ziemann, 2010; Zhang et al., 2015; Zhao et al., 2018), however, the process remains poorly modelled across the wide range of chamber materials, relative humidities, gas-phase loading, component volatilities and activity coefficients present in chamber experiments (e.g. Day et al., 2017; Stefenelli et al., 2018). It is therefore preferable to allow the user to fit vapour losses to walls through the tuning of two wall loss parameters, one primarily determining equilibrium, called the effective wall mass concentration ( $C_w$ ), and one determining rate of partitioning, the mass transfer coefficient ( $k_w$ ). These influence gas-wall partitioning through an equation of the same framework as gas-particle partitioning (which is described below and in Zaveri et al. (2008)):

$$\frac{dC_{i,g}}{dt} = -k_w(C_{i,g} - \frac{C_{i,w}}{C_w} p_i^0 \gamma_i), \quad (5)$$

$$\frac{dC_{i,w}}{dt} = k_w(C_{i,g} - \frac{C_{i,w}}{C_w} p_i^0 \gamma_i), \quad (6)$$

where  $p_i^0$  is the liquid (sub-cooled if necessary) saturation vapour pressure of component  $i$  and  $\gamma_i$  is its activity coefficient on the wall. Following the conclusions of Matsunaga and Ziemann (2010) and Zhang et al. (2015),  $k_w$  represents factors such as gas- and wall-phase diffusion, turbulence, accommodation coefficient and the chamber surface area to volume ratio, whilst  $C_w$  reflects the adsorbing and/or absorbing properties of the wall, including effects of relative humidity, surface area, diffusivity and porosity. We recommend the iterative fitting of  $k_w$  and  $C_w$  to observations through minimising observation-model residuals.  $C_w$  in PyCHAM is independent of condensates to the wall, which is consistent with the findings of Matsunaga and Ziemann (2010) and Zhang et al. (2015).

A major distinction between the gas partitioning to particles and walls is the much greater size of the wall, where size is represented by surface area or volume depending on whether adsorption or absorption is the main partitioning mechanism, respectively. It could be argued that the effective wall mass concentration is massive compared to the concentration of wall-phase components, making the Raoult (mole fraction, ( $\frac{C_{i,w}}{C_w}$ )) term in Eq. 5 redundant. Following this argument, the gas-wall partitioning equation becomes:

$$\frac{dC_{i,g}}{dt} = -k_w(C_{i,g} - \frac{p_i^0 \gamma_i}{C_w}). \quad (7)$$

However, this approach is unphysical as it removes the dynamic property of partitioning, instead, the  $\frac{p_i^0 \gamma_i}{C_w}$  term implies a fixed concentration of wall-phase component in the gas-phase just above the wall and introduces several issues. First, it implies that components with higher volatility and activity coefficient have a greater concentration on the wall, which is unrealistic.

Second, the fixed wall concentration allows for loss of mass conservation for components with  $C_{i,g} < \frac{p_i^0 \gamma_i}{C_w}$  since components may evaporate from the wall despite having no presence there. Conversely, components with  $C_{i,g} > \frac{p_i^0 \gamma_i}{C_w}$  may undergo an unrealistic degree of condensation to the wall because the evaporation of their wall-phase is unaccounted for.

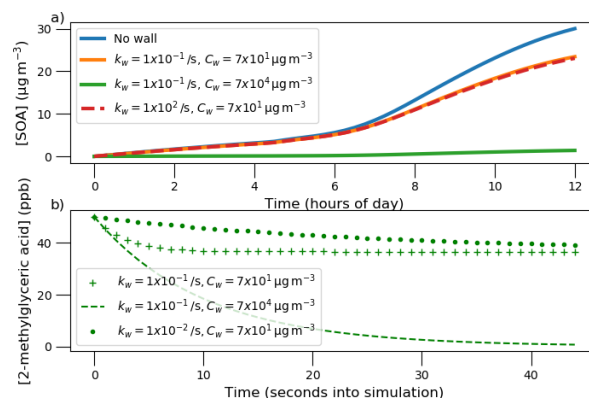
## 6.1 Tuning gas-wall partitioning parameters

Next we illustrate the sensitivity to  $k_w$  and  $C_w$  in Eq. 5. The same simulation setup described above for Fig. 3 was used though with  $\alpha$ -pinene replaced by isoprene with a concentration at experiment start of 63.4 ppb. Seed particles comprised of ammonium sulphate with mean diameter 0.5  $\mu\text{m}$  and number concentration  $6 \times 10^2 \text{ cm}^{-3}$  were introduced at experiment start. Pure component liquid saturation vapour pressures were estimated by the Nannoolal et al. (2008) method and activity coefficients for all components were assumed one. To begin, both  $k_w$  and  $C_w$  were set sufficiently low to effectively turn off gas-wall partitioning. Second,  $C_w$  was set equal to the mass concentration of seed particle ( $70 \mu\text{g m}^{-3}$ ) and  $k_w$  raised to  $1 \times 10^{-1} \text{ s}^{-1}$  at which a notable decrease in [SOA] was observed. Third,  $k_w$  was held whilst  $C_w$  was raised three orders of magnitude greater than the seed mass concentration. Fourth,  $C_w$  was held at  $70 \mu\text{g m}^{-3}$  and  $k_w$  was raised by three orders of magnitude. The effect on SOA mass concentration is given in Fig. 6 and demonstrates that at sufficiently large values of  $C_w$ , SOA production can be effectively suppressed through competitive uptake of vapours to chamber walls. However, for a given  $C_w$ , there is a limit on suppression of SOA formation due to  $k_w$  increase as it affects only the rate of partitioning with walls rather than the condensable fraction.

To guide constraint for wall loss parameters, we follow the example of Matsunaga and Ziemann (2010), with a control experiment comprising a single semi-volatile component introduced to the chamber at the start of the simulation at 50 ppb. We chose 2-methylglyceric acid which has an estimated particle mass concentration saturation vapour pressure ( $C^*$ ) of  $1.15 \times 10^2 \mu\text{g m}^{-3}$  at 298.15 K (the simulation temperature) and is an observed oxidation product of isoprene (Surratt et al., 2006). No other components or particles are introduced. With regards to designing a control experiment for tuning  $C_w$  and  $k_w$ , the results shown in Fig. 6b demonstrate that a component with a  $C^*$  close to the  $C_w$  has large sensitivity to the  $C_w$  value, thereby allowing greatest ease of tuning. Note, that this sensitivity can be altered through varying chamber temperature (and therefore the  $C^*$  of a component), or through varying component. Furthermore, to discern the effect of  $k_w$  a component with substantial partitioning to walls is required. When quantifying  $k_w$  it is worthwhile considering the required precision, because as Fig. 6a demonstrates, above a certain value, no further effect on SOA concentration results.

## 7 Gas-particle partitioning and sectional approach

PyCHAM simulations, like chamber experiments, are possible with and without seed particles. For seed particle experiments, the user defines number size distribution and composition inside the model variables input file. Furthermore, because PyCHAM uses size bins to discretise particles, users can state the number of size bins, lower and upper bin bounds and whether to spread size bins linearly or logarithmically in radius space.

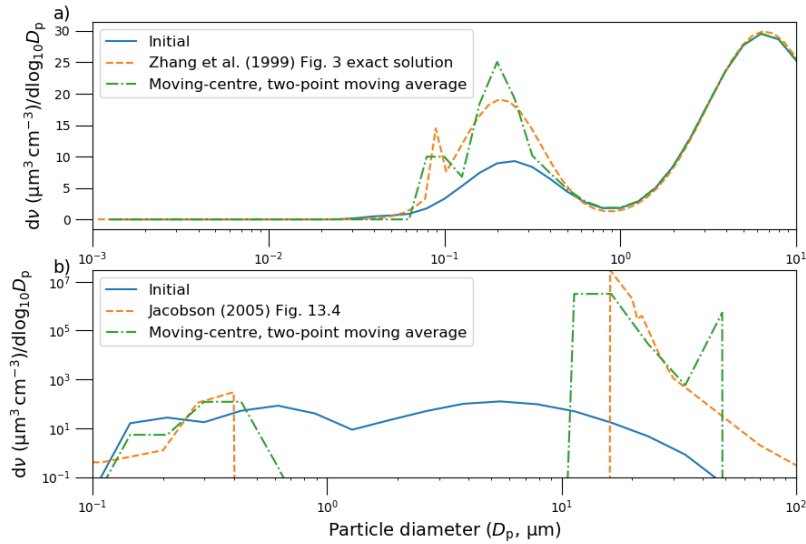


**Figure 6.** In a) sensitivity of SOA mass concentration on the gas-wall partitioning parameters  $k_w$  and  $C_w$  from Eq. 5. Seed particles with a concentration of approximately  $70 \mu\text{g m}^{-3}$  were present at the start of the experiment. Initial concentrations of ozone, isoprene and  $\text{NO}_2$  were set to 21.1, 63.4 and 9.8 ppb, respectively. With regards to photolysis rates, the simulation made the same considerations as in Fig. 3, where natural sunlight drove reactions after dawn at approximately 4:00 am. In b), the same sensitivity is assessed, but for a control experiment where only a single organic component is present.

Particles can grow or shrink as a direct consequence of three processes modelled by PyCHAM: gas-particle partitioning, coagulation and nucleation. Whilst coagulation and nucleation are discussed below, readers are referred to Zaveri et al. (2008) for a thorough explanation of gas-particle partitioning. The transition regime correction factor required for the partitioning estimation in PyCHAM is from Fuchs and Sutugin (1971). Furthermore, the unit test `test_kimt_calc` is available to check that the Kelvin and Raoult effects of the PyCHAM partitioning equation are accurate (e.g. through comparison with Fig. 16.1 of Jacobson (2005)).

In this section we focus on redistribution of particles between size bins following a change in size due predominately to gas-particle partitioning. PyCHAM does this using the moving-centre structure (Jacobson, 2005). The moving-centre approach has the advantage of minimal numerical diffusion and the ability to accommodate populations of particles of varying modes (e.g. a nucleation event in the presence of pre-existing particles). However, it suffers from loss of accuracy due to averaging of particles originally from different size bins that have grown, shrunk or coagulated to a given size bin (Zhang et al., 1999). In contrast the full-moving structure does not average particles of different size bin together, and can therefore exactly model certain chamber scenarios, one of which we use below to verify the moving-centre approach against. Full-moving is not used in PyCHAM, however, as it lacks the general applicability of moving-centre, since it cannot account for additions to the particle population after experiment start (such as through injection of seed or nucleation).

To maintain stability in numerical solutions and improve model accuracy, a condition inside the moving-centre module of PyCHAM iteratively reduces the boundary condition time interval if particles in a size bin change volume sufficiently to be allocated to a size bin beyond the adjacent one, or if particles have an unrealistic negative volume (possibly due to evaporation).



**Figure 7.** In a), replication of Fig.3 of Zhang et al. (1999) where a constant influx of sulphuric acid condenses to seed particles with the shown initial volume-size distribution, with final results shown after 12 hours. In b), replication of Fig. 13.8 of Jacobson (2005), where an initial distribution of particles are subject to a relative humidity of 100.002 % at minute intervals for 9 minutes, with results shown after 10 minutes.

Here we assess the moving-centre method through analysis of output during two periods of relatively substantial (and therefore testing) condensational growth and compare to benchmark simulations. The simulations also illustrate two further means of component influx to chambers using PyCHAM in addition to the simulations above where components were introduced with an initial pulse. In the first case a constant flux of sulphuric acid is added to a chamber with seed aerosol typical of hazy conditions following the benchmark simulation of Zhang et al. (1999). For consistency with the benchmark, gas and particle partitioning to walls was turned off and sulphuric acid was assumed to be non-volatile. The analysis section of Zhang et al. (1999) notes that to resolve the growth of smallest particles in this scenario, spatial resolution must be at least 100 size bins, therefore we use this value and set the solution time interval to 90 s for a total 12 hour simulation.

The exact solution to this condensational growth problem is given by the full-moving structure in Fig. 7a) (taken from Fig. 3 of Zhang et al. (1999)). When PyCHAM is compared against the exact solution, the tri-modal distribution is present with mean values at the correct particle size though with some disagreement in the peak height and spread. The degree of agreement is significantly better than for the 13 size bin moving-centre simulation presented in Zhang et al. (1999) and indicates that PyCHAM is operating as intended. Our results in Fig. 7a are a two-point moving average which is often necessary for the moving-centre structure because its requirement that all particles in a size bin be transferred to the adjacent bin means that some bins will intermittently have zero particles.

Another case of relatively intense vapour-particle partitioning is provided by the example of cloud condensation nuclei experiencing varying degrees of water vapour supersaturation. Chamber experiments may involve injections of a component at specific times and the model variables input file can take such a scenario as input. Making use of this function we reproduce the benchmark simulation of Jacobson (2005) (Fig. 13.8) where relative humidity is increased to 100.002 % every minute (including at simulation start) for nine minutes, with results analysed after ten minutes. Seed particles are assumed non-volatile and wall interactions are turned off. Parameters such as temperature and the degree of dissociation, molecular weight and density of the seed particle are not disclosed by the reference simulation, therefore we set these as: 318.15 K, 1.0, 200 g mol<sup>-1</sup> and 1 g cm<sup>-3</sup>, respectively. The comparison between the Jacobson (2005) result in Fig. 7b and PyCHAM certainly shows agreement in the main feature of this simulation, which is the initially larger particles out competing smaller particles for water condensation to grow to water droplet size ( $D_p > 10 \mu\text{m}$ ). The PyCHAM result gives reasonable agreement considering that key parameters (such as seed component dissociation) may vary between simulations and taken together with Fig. 7a verifies the operation of gas-particle partitioning and the moving-centre structure.

## 8 Coagulation

Equations of coagulation kernels for Brownian diffusion, convective Brownian diffusion enhancement, gravitational collection, turbulent inertial motion, turbulent shear and Van der Waals collision were taken from Jacobson (2005). The unit test test\_coag produces a plot of coagulation kernels that can be compared to Fig. 15.7 of Jacobson (2005) to verify its accuracy. Once the coagulation kernel for each pair of particle size bins ( $\beta$ ) has been found, the combinations of size bins (denoted  $j$  and  $z$ ) whose coagulation produces a particle of size bin  $k$  are identified:

$$Vb_{l,k} \leq (V_{j,t-h} + V_{z,t-h}) < Vb_{u,k}, \quad (8)$$

where  $V$  is particle volume,  $Vb_{l,k}$  and  $Vb_{u,k}$  are the lower and upper volume bounds of the size bin and  $h$  is the time step for coagulation to occur over. The semiimplicit coagulation equation from Jacobson (2005) is then used to estimate the new number concentration per size bin ( $N$  (#cm<sup>-3</sup>)):

$$N_{k,t} = \frac{N_{k,t-h} + \frac{1}{2}h \sum_{j=1}^{j_{max}} \beta_{z,j} N_{z,t} N_{j,t-h}}{1 + h \sum_{j=1}^{\infty} \beta_{k,j} N_{j,t-h}}, \quad (9)$$

where  $j_{max}$  is the largest size bin that can undergo coagulation to produce a particle in size bin  $k$ . This equation is not mass-conserving. However, mass transfer between size bins is estimated using the number fraction of particles coagulating. For example, for a size bin  $k$ , the gain in molecular concentration of component  $i$  due to coagulation between size bins  $j$  and  $z$  (according to Eq. 8 and Eq. 9) is:

$$\Delta C_{i,k} = \frac{h(\frac{1}{2}\beta_{z,j} N_{z,t} N_{j,t-h} + \frac{1}{2}\beta_{j,z} N_{j,t} N_{z,t-h})}{N_{j,t-h}} C_{i,j,t-h}, \quad (10)$$

350 and the loss of molecular concentration from size bin  $k$  due to coagulation is:

$$\Delta C_{i,k} = - \left( 1 - \frac{1}{1 + h \sum_{j=1}^{\infty} \beta_{k,j} N_{j,t-h}} \right) C_{i,k,t-h}, \quad (11)$$

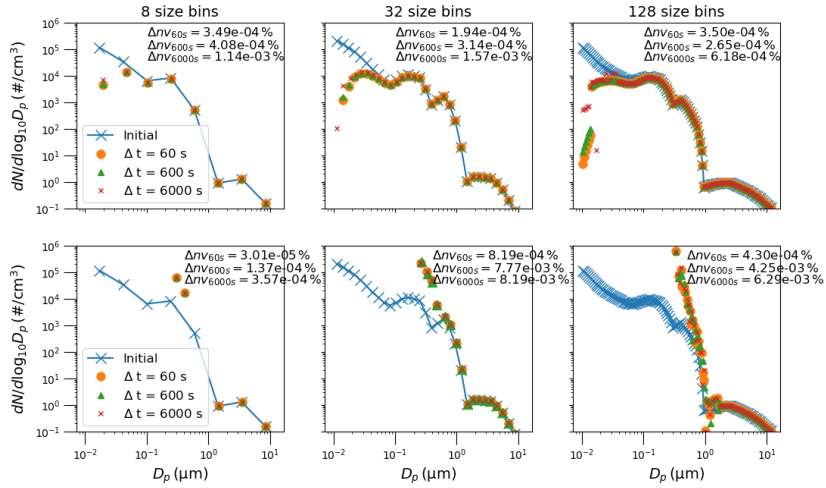
Eqs. 9- 11 show that coagulation directly influences the particle number- and mass-size distributions. We now assess the sensitivity of the number size distribution and mass conservation to the resolution of the operator-split time interval, and spatial resolution. A relatively complex initial distribution with four number modes is taken from ambient observations at Claremont, California on August 27, 1987 (Jacobson, 2005) and assumed to comprise non-volatile material. Results are presented for a six hour simulation in Fig. 8 where particle wall loss was turned off to allow clearer assessment of the coagulation sensitivity. In the top row of Fig. 8 no gas-phase chemistry was allowed, whilst in the bottom row, a single chemical reaction with reaction rate  $5.6 \times 10^{-17} \text{ molec}^{-1} \text{ s}^{-1}$  between  $\alpha$ -pinene and O<sub>3</sub> (both with initial concentrations 100 ppb) was modelled to produce a single low volatility product with saturation vapour pressure of  $1 \times 10^{-10} \text{ Pa}$ , whilst gas-wall partitioning was turned off. For the chemistry case, approximately  $500 \mu\text{g m}^{-3}$  of secondary material was formed, compared to  $90 \mu\text{g m}^{-3}$  of seed material. Columns in Fig. 8 are distinguished by the size bin resolution as presented in the column titles, and within each plot temporal resolution is varied.

The inset text of Fig. 8 ( $\Delta n_v$ ) gives the fractional change in non-volatile material from the start to end (six hours) of the simulation for the three temporal resolutions. It is clear that the coagulation equations introduce negligible error to mass conservation. Two features are present in the top row (no chemistry) of Fig. 8: first, that in terms of number concentration, coagulation overwhelmingly affects the number concentration of smaller particles - note that such particles are sufficiently small in volume that they may coagulate with a larger particle without causing it to grow a size bin; second, that only for the smallest particles (below a diameter of  $3 \times 10^{-2} \mu\text{m}$  in this case) is a sensitivity to temporal resolution clear across all size bin resolutions. For the no chemistry case there is demonstrable coupling of spatial and temporal resolution, with an increase in the former indicating greater sensitivity to the latter. However, all the resolution considerations above become redundant when we consider the case with gas-particle partitioning (bottom row of Fig. 8). In this instance, the effect of partitioning dominates the change in number-size distribution and no sensitivity of coagulation to spatial or temporal resolution is discernible. We recommend users consider these examples in addition to the nature of their simulation and objective when deciding whether temporal or spatial resolution will significantly impact results.

## 375 9 Particle deposition to walls

As with gas-wall partitioning, the loss of particles to chamber walls can significantly invalidate chamber results if unaccounted for and has been detailed in previous publications (Crump and Seinfeld, 1981; McMurry and Rader, 1985; Nah et al., 2017; Wang et al., 2018). During control experiments the deposition rate of particles to walls can be inferred through observations of the rate of decay of particles of varying size (with coagulation accounted for) (Charan et al., 2019). Several studies have published results from such experiments (McMurry and Rader, 1985; Wang et al., 2018), including a relatively large dataset





**Figure 8.** Sensitivity of the coagulation process to changes in operator-split temporal resolution (given in the legend) and spatial resolution (given in column titles). In the top row no chemistry occurred whilst in the bottom row a semi-volatile species was produced, as detailed in the main text. Results are for the end of a simulated six hour experiment. The  $\Delta nv_{\text{temporal resolution}}$  value given in the inset text is the percentage change in total non-volatile particle-phase material from the start to finish of the experiment, demonstrating mass conservation in the model.

from the EUROCHAMP2020 project (Oliveri, 2018). Comparison of inferred wall loss rates indicate that relatively small and larger particles have higher loss rates due diffusion and settling (Crump and Seinfeld, 1981), respectively, however the absolute values and size-dependent gradient of the loss rates vary significantly between control experiments. Even for a given chamber, significant variations appear with changes to relative humidity, disturbance to walls due to air conditioning, and, for teflon chambers, with time since the chamber walls experienced frictional force to create electrostatic charge (Wang et al., 2018).  
 385 Currently no method is available to measure the required inputs that a particle deposition model would need to satisfactorily reproduce observations across all chambers and conditions, therefore in PyCHAM users have three options to estimate particle wall deposition. Here we describe the options and provide examples of their use.

Users select wall loss treatment with the McMurry\_flag option in the model variables input file. The default (if left empty) is no loss of particles to wall, which can be used for estimating wall loss corrected values such as aerosol yield. If set to 1,  
 390 the model of McMurry and Rader (1985) is used, which is based on the particle deposition model of Crump and Seinfeld (1981) but with electrostatic effects. Studies have found the Crump and Seinfeld (1981) and McMurry and Rader (1985) approach to reproduce measured particle wall losses well (Chen et al., 1992; Kim et al., 2001). Selecting McMurry and Rader (1985) requires the user to also input the chamber surface area, the average charge per particle and the average electric field  
 395 inside the chamber, where the latter two may be set to zero for nullifying electrostatic effects. With the test\_wallloss module

users can confirm that PyCHAM accurately reproduces Fig. 2 of McMurry and Rader (1985), as shown here in Fig. 9, which demonstrates the effect of changing the charge number per particle.

If user sets the McMurry\_flag option to 0 then a customised particle deposition rate dependence on particle size is available. This option allows application of known or best estimate deposition rates ( $\beta$ ) to the model, as recommended by Wang et al. (2018). Four further inputs are required for this option: the particle diameter at which the inflection in deposition rates occurs ( $D_{p,flec}$ ) (where the inflection point marks a change in dependence of deposition rate with particle size), the rate of particle deposition to wall at the inflection point ( $\beta_{flec}$ ), and the gradients of the deposition rate with respect to particle diameter before ( $\nabla_{pre}$ ) and after the inflection ( $\nabla_{pro}$ ), where a linear dependence in log-log space is assumed, consistent with observations (Charan et al., 2019). The equations for deposition rate in this instance are given in Eq. 12, and example dependencies of rate with particle size provided by Fig. 9.

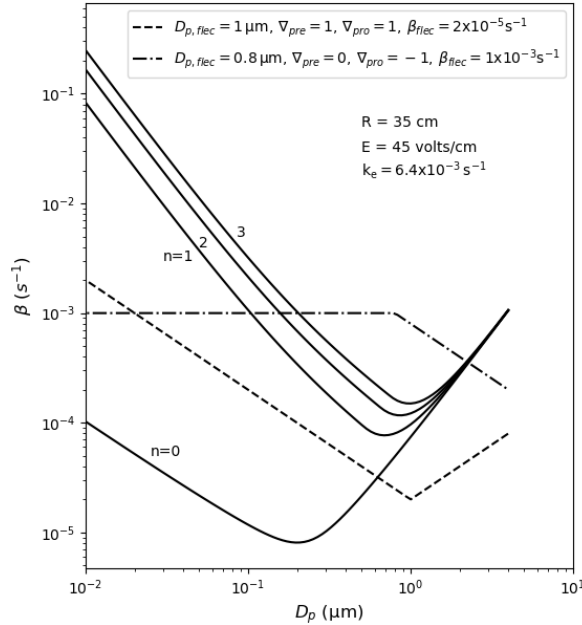
$$\begin{aligned}
 D_p < D_{p,flec} \\
 \log_{10}(\beta(D_p)) &= \log_{10}(D_{p,flec}) - \log_{10}(D_p)\nabla_{pre} + \beta_{flec} \\
 D_p &\geq D_{p,flec} \\
 \log_{10}(\beta(D_p)) &= \log_{10}(D_p) - \log_{10}(D_{p,flec})\nabla_{pro} + \beta_{flec}
 \end{aligned} \tag{12}$$

## 10 Nucleation

The simulation of nucleation to produce newly-formed suspended particles is an area of ongoing research (e.g. Kurten et al., 2018; Li et al., 2020). Important advances in observing the nucleation process continue (Jiang et al., 2011; Dada et al., 2020). The review of Semeniuk and Dastoor (2018) highlights the uncertainty around nucleation modelling, particularly in the presence of organic components. In light of the continuing developments to nucleation modelling and the requirement of PyCHAM to be generally applicable, users are able to provide parameters to a Gompertz function for cumulative new particle number, allowing them to fit to observed number size distributions:

$$P_1(t) = \text{nuc}_{v1} (\exp(\text{nuc}_{v2} (\exp(-t/\text{nuc}_{v3})))) \tag{13}$$

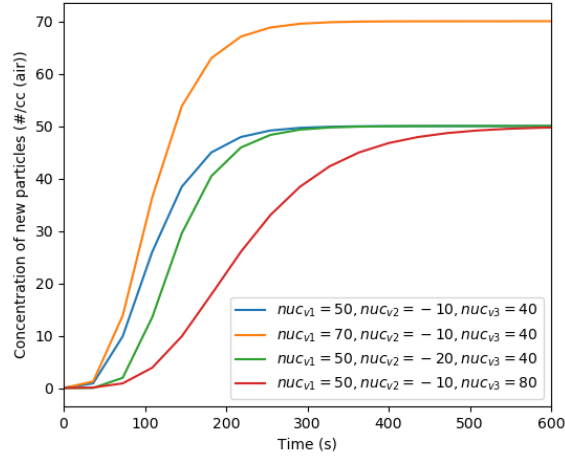
where  $P_1$  is the number concentration of new particles after time  $t$  that enter the smallest size bin, and  $\text{nuc}_{vn}$  are the user-defined parameters. The resulting function forms an asymmetrical sigmoidal curve with time, whilst the parameters allow the amplitude ( $\text{nuc}_{v1}$ ), onset ( $\text{nuc}_{v2}$ ), and duration ( $\text{nuc}_{v3}$ ) of the curve to be adjusted, as shown in Fig. 10. The Gompertz function provides a sigmoidal form with faster increase in new particle number prior to peak rate of production than after (Fig. 10). This form is provided as our testing has indicated it gives better fits to number size distribution than a symmetrical sigmoidal function.



**Figure 9.** Example dependencies of the particle deposition to wall rate using the model of McMurry and Rader (1985) in the solid lines, where the charge per particle is given by  $n$  and other inputs given by inset text ( $R$  is spherical-equivalent chamber radius,  $E$  is the average electric field in the chamber and  $k_e$  is the coefficient of eddy diffusion). The dashed lines demonstrate the the observation-based deposition rate utility of PyCHAM given in Eq. 12, with inputs at the top of the plot.

To obtain the nucleation parameters that most accurately fit measurements, number size distribution measurements provide  
425 a relatively detailed indicator of fit, whilst total particle number concentration is less informative and therefore less able to provide constraint.

Although it is accepted that clusters of molecules are responsible for forming the nucleus of a particle (Seinfeld and Pandis, 2006), the shape and spherical-equivalent radius of these is uncertain. Inside the model variables file the radius of newly nucleated particles is set by the user. Using the volume equation for the cluster's assumed spherical shape and the molar  
430 volume of the component assumed responsible for nucleation (also set by the user), the molar concentration of nucleating component required is calculated and added to the smallest size bin of the particle phase whilst subtracted from the vapour phase. The average radius of the particles in this size bin is then calculated by dividing the total volume of molecules by the number of particles (including those present prior to nucleation). With the Kelvin effect estimated to be relatively large at typical nucleation cluster sizes, the model is very sensitive to the input radius of new particles and the volatility of the  
435 nucleating component. Above a certain vapour pressure (dependent on particle size and the propensity of other components to



**Figure 10.** Effect of varying the nucleation parameters on simulated particle number concentration when considering only nucleation.

condense), the nucleating component will undergo net evaporation during the gas-particle partitioning solution, and possibly invoke the moving-centre structure to reduce the integration time step toward zero seconds (as explained in Section 7).

## 11 Sensitivity to Temporal and Spatial Resolution

The operator-split processes of coagulation, particle loss to walls and nucleation all affect the number, mass and volume size distributions of particles. Whilst the temporal and spatial resolution used for these processes can be decreased to decrease the time required for simulation, it can also introduce inaccuracies to results. Although it is beyond the scope of this paper to assess temporal resolution sensitivity across all possible PyCHAM parameter space, in this section we compare the divergence of outputs from simulations with decreasing temporal and spatial resolution against a high resolution reference for extremes of the relevant parameter space: seeded experiments with no gas-particle partitioning and both seeded and nucleation experiments with relatively great condensational growth of particles. Results here determine the recommended temporal and spatial resolution, provide a useful illustration of sensitivity and may help users perform sensitivity tests for their individual model inputs.

For the no partitioning simulations, the effect of resolution on particle number size distribution and total number concentration is considered, whilst for the partitioning simulations, concentration of secondary material is also relevant. To allow comparison of low resolution simulations with the high simulation reference, output from the former is interpolated to the resolution of the latter. Divergence between the low and high resolution simulations is represented by a single absolute percentage

deviation ( $\sigma$ ). For number size distribution, divergence is averaged over size bins containing particles and time steps, with  $Y$  of the former and  $Z$  of the latter:

$$\sigma = \frac{\sum_{t_i=1}^{t_i=Z} \sum_{k=1}^{k=Y} \frac{|(n_{t_i,k} - \bar{n}_{t_i,k})|}{\vee(n_{t_i,k}, \bar{n}_{t_i,k})}}{ZY} 100, \quad (14)$$

455 where  $n_{t_i,k}$  is the particle number concentration at time step  $t_i$  in size bin  $k$  from a lower resolution simulation and  $\bar{n}_{t_i,k}$  is the output from the reference maximum resolution simulation. Where the two agree exactly the contribution to  $\sigma$  is zero, and where one output is zero and the other is greater,  $\sigma$  is at a maximum of 100. The term  $\vee(n_{t_i,k}, \bar{n}_{t_i,k})$  means the greater of  $n_{t_i,k}$  and  $\bar{n}_{t_i,k}$  is used as denominator. Where the outputs from the two resolutions are similar this choice of denominator makes negligible difference, however, where one is much greater than the other it limits the divergence to a helpful (for interpretation) 460 maximum of 100.

For total number concentration and total secondary material concentration, divergence is calculated as the percentage deviation averaged over time steps:

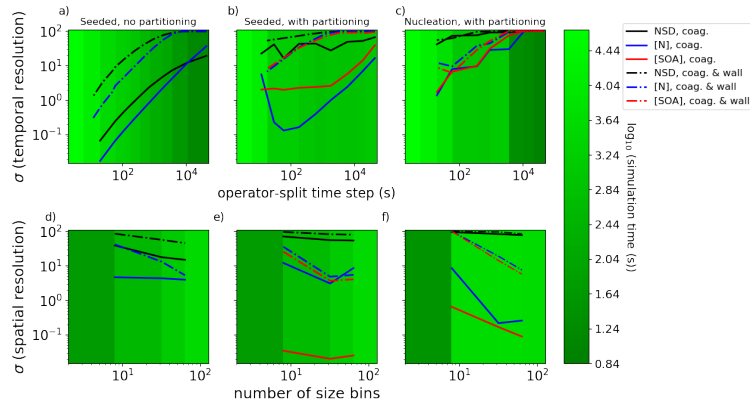
$$\sigma = \frac{\sum_{t_i=1}^{t_i=Z} \frac{|(N_{t_i} - \bar{N}_{t_i})|}{\vee(N_{t_i}, \bar{N}_{t_i})}}{Z} 100, \quad (15)$$

where  $N$  represents either total number concentration or total secondary material concentration.

465 For simulations assessing sensitivity to temporal resolution, 128 logarithmically spaced size bins are used, for which Fig. 8 indicates no limitation to accuracy due to spatial resolution. For seeded simulations, we use the same initial number size distribution as in Fig. 8, as this gives a relatively broad range of particle sizes, which is necessary to fully appreciate the size-dependent effects of the operator-split processes. All simulations were run for 24 hours and the reference simulation had an operator-split time step of 6 s.

470 Results for temporal resolution sensitivity are shown across three plots. The first, given in Fig. 11a) represents the no partitioning case, with sensitivity assessed for two setups: only coagulation, and both coagulation and wall loss turned on. Coagulation proceeds as described in Section 8, whilst wall loss is described in Section 9, with the following inputs to recreate a size-dependent wall loss profile similar to  $n=3$  in Fig. 9:  $D_{p,flec} = 1.0 \mu\text{m}$ ,  $\beta_{flec} = 1.0 \times 10^{-4} \text{ s}^{-1}$ ,  $\nabla_{pre} = \nabla_{pro} = 1.5$ . Consequently, the particle loss to wall is relatively great and the sensitivity results are conservative. Fig. 11a) indicates that 475 under this scenario, particle loss to walls considerably increases sensitivity to temporal resolution, with average deviations of 10 % for both total particle number concentration and number size distribution occurring at resolutions around two orders of magnitude finer than for coagulation alone.

For Fig. 11b), two-methylglyceric acid is introduced at a rate of  $1.0 \times 10^{-2} \text{ ppbs}^{-1}$  and increases sensitivity to temporal resolution compared to Fig. 11a). A resolution of around 60 s is required to attain divergences less than 10 % for total number 480 concentrations and secondary material, whilst for number size distribution, not even the lowest temporal resolution of 12 s can produce average divergence below 10 % when compared against the reference case of 6 s. This reflects the steep gradients in particle size-number space that are generated during intense condensational growth periods (e.g. Fig. 7), since small changes to



**Figure 11.** Sensitivity of number size distribution (NSD), total particle number concentration ([N]) and total concentration of secondary material ([SOA]) to operator-split temporal resolution (a-c) and to spatial resolution (d-f). In plots a), b), d), and e), coagulation (coag.) and particle loss to wall (wall) are probed, whilst in c) nucleation (nuc.) is additionally probed. In a) no gas-particle partitioning is allowed, whilst in b) and c) it is, as two-methylglyceric acid is continuously injected at a rate of  $1.0 \times 10^{-2} \text{ ppbs}^{-1}$ . Also in c) an extremely low volatility organic component is present at simulation start at 1 ppb, and set as the nucleating component. The legend for lines in all plots is given in the upper right. Contours represent the time taken for simulation.

the operator-split time step can vary the size bins that particles concentrate in. This effect is even further pronounced when an extremely low volatility organic component is injected at the simulation start at 1 ppb to act as a nucleating agent and no seed  
485 particles present, with results given in Fig. 11c). We use the nucleation parameters for Eq. 13 of:  $\text{nuc}_{v1} = 1 \times 10^4$ ,  $\text{nuc}_{v2} = -10$  and  $\text{nuc}_{v3} = 100$ , for a relatively rapid nucleation period (lasting only ten minutes) and therefore conservative assessment of sensitivity. Fig. 11c) indicates that although particles do not grow to same size bin as the reference case, the total concentration of number and secondary material diverges from the reference case by around 10 % for an operator-split time step of 60 s. Given the conservative nature of these simulations we therefore recommend a maximum operator-split time step of 60 s.

490 In Fig. 11d-f), the same simulation scenarios are applied as for temporal resolution sensitivity, but now we investigate spatial resolution sensitivity. Using a fixed temporal resolution of 60 s, results show the divergence of 8, 32 and 64 size bins compared against results for 128 size bins (all logarithmically spaced). In Fig. 11d), when coagulation alone is effective, reasonable agreement is seen in total number concentrations across size bin resolutions. However, when wall loss is also considered, the relatively high loss rate of small particles to the wall leads to a strong dependence of divergence on resolution. The number  
495 size distribution divergence is poor across all scenarios, indicating that if this is an important output for users (e.g. when fitting nucleation parameters, comparison against number size distribution is very useful), users should employ 128 size bins. Results for the partitioning cases in Fig. 11e) and f) shows that without wall loss, total number concentration and secondary material concentration gives reasonable agreement of 10 % or less when 8 size bins are used. However, when partitioning is active, 32 size bins is the minimum resolution for divergence of approximately 10 % or less. Consequently, whilst recognising substantial  
500 differences between scenarios and user requirements, we recommend a size bin number of 32.

## 12 Conclusions

The PyCHAM (CHemistry with Aerosol Microphysics in Python) software for aerosol chambers has been described. Its open-source repository is given in Section 1. PyCHAM has been designed for optimal ease of use (from online access to output) whilst observing the latest scientific findings relevant to the full range of aerosol chambers (Section 2). We have provided a  
505 model output for the dark oxidation of limonene to illustrate the coupling of modelled processes: gas-phase chemistry, gas-particle partitioning, gas-wall partitioning, redistribution of particles between size bins, particle loss to wall, coagulation and nucleation (Sections 2 and 3).

The steps to run a simulation using the software's GUI were described in Section 3 and the methods for estimating or setting component properties explained in Section 4. The setting up and solution of gas-phase photochemical reactions is detailed in  
510 Section 5, including comparison against the AtChem2 model (Sommariva et al., 2018) for verification and illustration of the effect of varying the boundary condition time interval on model output for a system subject to varying natural light intensity.

For gas-wall partitioning this paper details (Section 6) a parameterisation that aims to satisfy the breadth of chamber characteristics and recommends a method for tuning to observations. In Section 7, gas-particle partitioning and the moving-centre structure for redistributing particles between size bins was introduced and verified against benchmark simulations.

515 Coagulation was detailed in Section 8 and shown to introduce negligible loss of mass conservation. With Section 9, the three options for treating particle losses to walls were detailed and the resulting deposition rates as a function of particle diameter were exemplified, including verification against the benchmark of McMurry and Rader (1985). Similar to gas-wall partitioning, nucleation in PyCHAM is treated with a parameterisation that aims to optimise model versatility, with examples of parameter effects provided (Section 10).

520 In Section 11 the sensitivity of key outputs to varying operator-split temporal resolution and the size bin number was illustrated and informed our recommendations of a minimum operator-split time interval of 60 s and a minimum of 32 size bins. We also show a high sensitivity of model accuracy to the rate of particle wall loss and note that users could use lower resolutions if wall loss is significantly lower than used in our tests.

Throughout the paper guidance and details on the use of PyCHAM is provided. Furthermore, the applicability of the software  
525 to a wide variety of chamber experiments is a continuous theme, true to the software design.

### *Code and data availability.*

The PyCHAM software, figures in this manuscript, PyCHAM inputs to create figures and code to plot figures is available at:  
<https://github.com/simonom/PyCHAM>

## Appendix A: Model Variable Inputs

530 Below is the table of model variables required for input to PyCHAM accompanied by a description.





Input Name	Description
res_file_name	Name of folder to save results to
total_model_time	Total experiment time to be simulated (s)
bc_time_step	Maximum time interval for ode solver and updating boundary conditions (s). Must be at most the value of op_spl_step. Default is 60 s.
op_spl_step	Time (s) interval for solving operator-split processes over, must be at least as the value of bc_time_step. Default is 60 s. Can be set to more than the total_model_time variable above to prevent operator-split processes occurring.
recording_time_step	Time interval for recording results (s). Must be at least the value of bc_time_step. Defaults is 60 s.
number_size_bins	Number of size bins (excluding wall); to turn off particle considerations set to 0 (which is also the default), likewise set pconc and seed_name variables below off. Must be integer (e.g. 1) not float (e.g. 1.0).
lower_part_size	Radius of smallest size bin boundary (um)
upper_part_size	Radius of largest size bin boundary (um)
space_mode	Set to lin for linear spacing of size bins in radius space, or to log for logarithmic spacing of size bins in radius space, if empty defaults to linear spacing
kgwt	Mass transfer coefficient of vapour-wall partitioning (/s), if left empty defaults to zero
eff_abs_wall_massC	Effective absorbing wall mass concentration (g/m <sup>3</sup> (air)), if left empty defaults to zero
temperature	Air temperature inside the chamber (K). At least one value must be given for the experiment start (times corresponding to temperatures given in tempt variable below). If multiple values, representing temperatures at different times, then separate with a comma. For example, if the temperature at experiment start is 290.0 K and this increases to 300.0 K after 3600.0 s of the experiment, input is 290.0, 300.0.
tempt	Times since start of experiment (s) at which the temperature(s) set by the temperature variable above, are reached. Defaults to 0.0 if left empty as at least the temperature at experiment start needs to be known. If multiple values, representing temperatures at different times, then separate with a comma. For example, if the temperature at experiment start is 290.0 K and this increases to 300.0 K after 3600.0 s of the experiment, input is 0.0, 3600.0.
p_init	Pressure of air inside the chamber (Pa)
rh	Relative Humidity (fraction, 0-1)
lat	Latitude (degrees) for natural light intensity (if applicable, leave empty if not (if experiment is dark set light_status below to 0 for all times))
lon	Longitude (degrees) for natural light intensity (if applicable, leave empty if not (if experiment is dark set light_status below to 0 for all times))
DayOfYear	Day of the year for natural light intensity (if applicable, leave empty if not (if experiment is dark set light_status below to 0 for all times)), must be integer between 1 and 365

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Input Name	Description
daytime_start	Time of the day (s since midnight) for natural light intensity (if applicable, leave empty if not (if experiment is dark set light_status below to 0 for all times))
act_flux_file	Name of csv file stored in PyCHAM/photofiles containing actinic flux values; use only if artificial lights inside chamber are used during experiment. The file should have a line for each wavelength, with the first number in each line representing the wavelength in nm, and the second number separated from the first by a comma stating the flux (Photons/cm2/nm/s) at that wavelength. No headers should be present in this file. Example of file given by /PyCHAM/photofiles/Example_act_flux and example of the act_flux_path variable is: act_flux_path = Example_act_flux.csv. Note, please include the .csv in the variable name if this is part of the file name. Defaults to empty.
photo_par_file	Name of txt file stored in PyCHAM/photofiles containing the wavelength-dependent absorption cross-sections and quantum yields for photochemistry. If left empty defaults to MCMv3.2, and is only used if act_flux_path variable above is stated. File must be of .txt format with the formatting: J_n_axs wv_m, axs_m J_n_qy wv_M, qy_m J_end where n is the photochemical reaction number, axs represents the absorption cross-section (cm2/molecule), wv is wavelength (nm), _m is the wavelength number, and qy represents quantum yield (fraction). J_end marks the end of the photolysis file. An example is provided in PyCHAM/photofiles/example_inputs.txt. Note, please include the .txt in the file name.
ChamSA	Chamber surface area (m2), used if the Rader and McMurry wall loss of particles option (Rader_flag) is set to 1 below
coag_on	Set to 1 (the default if left empty) for coagulation to be modelled, or set to zero to omit coagulation
nucv1	Nucleation parameterisation value 1
nucv2	Nucleation parameterisation value 2
nucv3	Nucleation parameterisation value 3
nuc_comp	Name of component contributing to nucleation (only one allowed), must correspond to a name in the chemical scheme file. Defaults to empty. If empty, the nucleation module (nuc.py) will not be called.
new_partr	Radius of newly nucleated particles (cm), if empty defaults to 2.0e-7 cm.
inflectDp	The particle diameter (m) at the inflection point of the size-dependent wall deposition rate.
Grad_pre_inflect	Negative log10 of the gradient of particle wall deposition rate against the log10 of particle diameter before inflection (/s). For example, for the rate to decrease by an order of magnitude every order of magnitude increase in particle diameter, set to 1.
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Input Name	Description
Grad_post_inflect	Log10 of the gradient of particle wall deposition rate against the log10 of particle diameter after inflection (/s). For example, for the rate to increase by an order of magnitude for every order of magnitude increase in particle diameter, set to 1.
Rate_at_inflect	Particle deposition rate to wall at the inflection point for size-dependent particle loss to walls (/s)
part_charge_num	Average number of charges per particle, only required if the McMurry and Rader (1985) model for particle deposition to walls is selected
elec_field	Average electric field inside the chamber (g.m/A.s3), only required if the McMurry and Rader (1985) model for particle deposition to walls is selected
McMurry_flag	Set to 0 to use the particle wall loss parameter values given above or 1 to use the McMurry and Rader (1985, doi: 10.1080/02786828508959054) method for particle wall loss, which uses the chamber surface area given by ChamSA above, average number of charges per particle (part_charge_num above) and average electric field inside chamber (elec_field above), defaults to no particle wall loss if empty, similarly -1 turns off particle wall loss
C0	Initial concentrations of any trace gases input at the experiment start (ppb), must correspond to component names in Comp0 variable below. Separate concentrations of multiple components with a comma.
Comp0	Names of trace gases present at experiment start (in the order corresponding to their concentrations in C0). Note, this is case sensitive, with the case matching that in the chemical scheme file. Separate multiple component names with a comma.
Ct	Concentrations of component achieved when injected at some time after experiment start (ppb), if multiple values (representing injection at multiple times), please separate with commas. If multiple components are injected after the start time, then this input should comprise the injected concentrations of components with times separated by commas and components separated by semicolons. E.g., if k ppb of component A injected after m seconds and j ppb of component B injected after n (n>m) seconds, then Ct should be k,0;0,j. The value here is the increase in concentration from the moment before the injection to the moment after (ppb)
Compt	Name of component injected at some time after experiment start. Note, this is case sensitive, with the case matching that in the chemical scheme file. If more than one component, separate with a comma.
injectt	Time(s) at which injections occur (seconds), which corresponds to the concentrations in Ct, if multiple values (representing injection at multiple times), please separate with commas. If multiple components are injected after the start time, then this input should still consist of just one series of times as these will apply to all components. E.g., if k ppb of component A injected after m seconds and j ppb of component B injected after n (n>m) seconds, then this input should be m, n.
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Input Name	Description
const_comp	Name of component with continuous gas-phase concentration inside chamber. Note, this is case sensitive, with the case matching that in the chemical scheme file. Defaults to nothing if left empty. To specifically account for constant influx, see const_infl variable below.
const_infl	Name of component(s) with continuous gas-phase influx to chamber. Note, this is case sensitive, with the case matching that in the chemical scheme file. Defaults to nothing if left empty. For constant gas-phase concentration see const_comp variable above. Should be one dimensional array covering all components. For example, if component A has constant influx of K ppb/s from 0 s to 10 s and component B has constant influx of J ppb/s from 5 s to 20 s, the input is: const_infl = A, B.
const_infl_t	Times during which constant influx of each component given in the const_infl variable occurs, with the rate of their influx given in the Cinfl variable. Should be one dimensional array covering all components. For example, if component A has constant influx of K ppb/s from 0 s to 10 s and component B has constant influx of J ppb/s from 5 s to 20 s, the input is: const_infl_t = 0, 5, 10, 20.
Cinfl	Rate of gas-phase influx of components with constant influx (stated in the const_infl variable above). In units of ppb/s. Defaults to zero if left empty. If multiple components affected, their influx rate should be separated by a semicolon, with a rate given for all times presented in const_infl_t (even if this is constant from the previous time step for a given component). For example, if component A has constant influx of K ppb/s from 0 s to 10 s and component B has constant influx of J ppb/s from 5 s to 20 s, the input is: Cinfl = K, K, 0, 0; 0, J, J, 0.
vol_Comp	Names of components with vapour pressures to be manually assigned in the volP variable below, names must correspond to those in the chemical scheme file and if more than one, separated by commas. Can be left empty, which is the default.
volP	Vapour pressures (Pa) of components with names given in vol_Comp variable above, where one vapour pressure must be stated for each component named in vol_Comp and multiple values should be separated by a comma. Acceptable for inputs to use e for standard notation, such as 1.0e-2 for 0.01 Pa
act_comp	Names of components (corresponding to those the chemical scheme file) with activity coefficients stated in act_user variable below (if multiple names, separate with a comma). Must have same length as act_user.
act_user	Activity coefficients of components with names given in act_comp variable above, if multiple values then separate with a comma. Must have same length as act_comp.
accom_coeff_comp	Names of components (corresponding to names in chemical scheme file) with accommodation coefficients set by the user in the accom_coeff_user variable below, therefore length must equal that of accom_coeff_user. Multiple names must be separated by a comma. For any components not mentioned in accom_coeff_comp, accommodation coefficient defaults to 1.0
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Input Name	Description
accom_coeff_user	Accommodation coefficients (dimensionless) of the components with names given in the accom_coeff_comp variable above, therefore number of accommodation coefficients must equal number of names, with multiple coefficients separated by a comma. Can be a function of radius (m), in which case use the variable name radius, e.g: for NO2 and N2O5 with accommodation coefficients set to 1.0 and 6.09e-08/Rp, respectively, where Rp is radius of particle at a given time (m), the inputs are: accom_coeff_comp = NO2, N2O5 accom_coeff_user = 1.0, 6.09e-08/radius. For any components not mentioned in accom_coeff_comp, accommodation coefficient defaults to 1.0.
pconct	Times (seconds) at which seed particles of number concentration given in pconc variable below are introduced to the chamber. If introduced at multiple times, separate times by a semicolon. For example, for a two size bin simulation with 10 and 5 particles/cc in the first and second size bin respectively introduced at time 0 s, and later at time 120 s seed particles of concentration 6 and 0 particles/cc in the first and second size bin respectively are introduced, input is: pconct = 0; 120 (and the number_size_bins variable above = 2).
pconc	Either total particle concentration, in which case should be a scalar, or particle concentration per size bin, in which case length should equal number of particle size bins (# particles/cc (air)). If an array of numbers, then separate numbers by a comma. If a scalar, the particles will be spread across size bins based on the values in the std and mean_rad variables below. To turn off particle considerations leave empty. If seed aerosol introduced at multiple times during the simulation, separate times using a semicolon. For example, for a two size bin simulation with 10 and 5 particles/cc in the first and second size bin respectively introduced at time 0 s, and later at time 120 s seed particles of concentration 6 and 0 particles/cc in the first and second size bin respectively are introduced, the input is: pconc = 10, 5; 6, 0 (and the number_size_bins variable above = 2).
seed_name	Name of component comprising the seed particles, can either be core for a component not present in the chemical scheme file, a name from this file, or H2O for water, note no quotation marks needed
seed_mw	Molecular weight of seed component (g/mol), if empty defaults to that of ammonium sulphate - 132.14 g/mol
seed_dens	Density of seed material (g/cc), defaults to 1.0 g/cc if left empty
mean_rad	Mean radius of particles (um), defaults to a flag that tells software to estimate mean radius from the particle size bin radius bounds given by lower_part_size and upper_part_size variables above. If more than one size bin the default is the mid-point of each. If the lognormal size distribution is being found (using the std input below), mean_rad should be a scalar representing the mean radius of the lognormal size distribution. If seed particles are introduced at more than one time, then mean_rad for the different times should be separated by a semicolon. For example, if seed particle with a mean_rad of 1.0e-2 um introduced at start and with mean_rad of 1.0e-1 um introduced after 120 s, the input is: mean_rad = 1.0e-2; 1.0e-1 and the pconct input is pconct = 0; 120.

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Input Name	Description
std	Geometric mean standard deviation of seed particle number concentration (dimensionless) when scalar provided in pconc variable above, role explained online in <a href="https://docs.scipy.org/doc/scipy/reference/generated/scipy.stats.lognorm.html">scipy.stats.lognorm</a> page, under pdf method: <a href="https://docs.scipy.org/doc/scipy/reference/generated/scipy.stats.lognorm.html">https://docs.scipy.org/doc/scipy/reference/generated/scipy.stats.lognorm.html</a> . If left empty defaults to 1.1. If seed particles introduced after the experiment start, then separate std for different times using a semicolon. For example, if seed particle with a standard deviation of 1.2 introduced at start and with standard deviation of 1.3 introduced after 120 s, the std input is: std = 1.2; 1.3 and the pconct input is: pconct = 0; 120
core_diss	Core dissociation constant (for seed component) (dimensionless), if empty defaults to 1.0.
light_time	Times (s) for lighting condition, corresponding to the elements of the light_status variable below, if empty defaults to lights off for whole experiment. Use this variable regardless of whether light is natural or artificial (chamber lamps). For example, for a 4 hour experiment, with lights on for first half and lights off for second, use: light_time = 0.0, 7200.0. If light_time doesn't include the experiment start (0.0 s), default is lights off at experiment start.
light_status	Set to 1 for lights on and 0 for lights off, with times given in the light_time variable above, if empty defaults to lights off for whole experiment. Setting to off (0) means that even if variables above that define light intensity are submitted the simulation will be dark. Use this variable for both natural and artificial (chamber lamps) light. The lighting condition for a particular time is recognised when the simulated time meets the time given in light_time. For example, for a 4 hour experiment, with lights on for first half and lights off for second, use: light_status = 1, 0. If status not given for the experiment start (0.0 s), default is lights off at experiment start.
tracked_comp	Name of component(s) to track rate of concentration change (molecules/cc.s); must match name given in chemical scheme, and if multiple components given they must be separated by a comma. Can be left empty and then defaults to tracking no components.
umansysprop_update	Flag to update the UManSysProp module via internet connection: set to 1 to update and 0 to not update. If empty defaults to no update. In the case of no update, the module PyCHAM checks whether an existing UManSysProp module is available and if not tries to update via the internet. If update requested and either no internet or UManSysProp repository page is down, code stops with an error.
chem_scheme_markers	Markers denoting various sections of the user's chemical scheme. If left empty defaults to Kinetic Pre-Processor (KPP) formatting. If filled, must have following elements separated with commas: marker for punctuation at start of reaction lines (just the first element), marker for peroxy radical list starting, punctuation between peroxy radical names, prefix to peroxy radical name, string after peroxy radical name, number of lines taken by peroxy radical list (including the line containing the marker for peroxy radical list starting), punctuation at the end of lines for generic rate coefficients. For example, for the MCM FACSIMILE format: chem_scheme_markers = %, RO2, +, , , 20, ; would be used.

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Input Name	Description
int_tol	Integration tolerances, with absolute tolerance first followed by relative tolerance, if left empty defaults to the maximum required during testing for stable solution: 1.0e-3 for absolute and 1.0e-4 for relative
dil_fac	Volume fraction per second chamber is diluted by, should be just a single number. Defaults to zero if left empty.

Table containing the PyCHAM variable inputs and their associated descriptions.

540 **A1**

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*Disclaimer.* The PyCHAM software is provided under the GNU General Public License v3.0.

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