Environmental Microbiology

3 Bacterial Metabolism Textbook – Chapters 1 & 2



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The growth of microorganisms demands two things:

1.Energy sources:

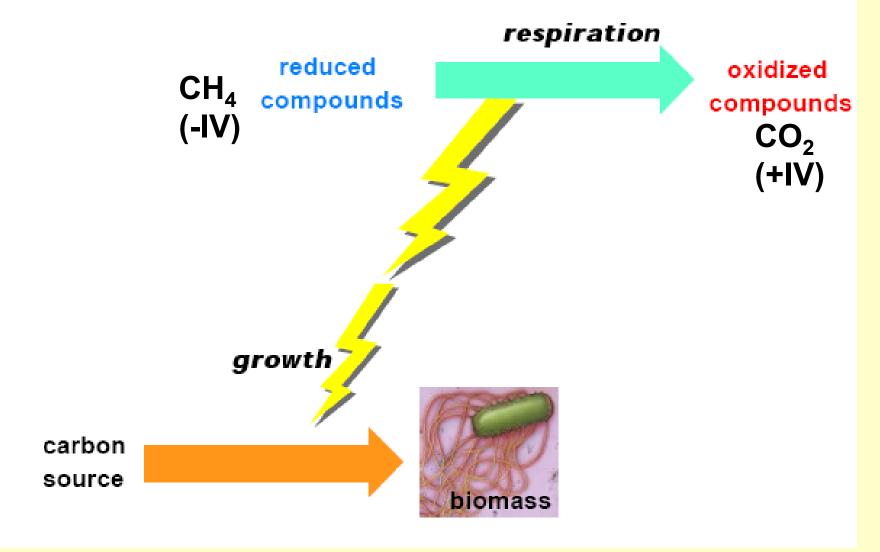
- Solar energy
- Oxidation of organic molecules (stored chemical energy)
- Oxidation of inorganic molecules (storage chemical energy)

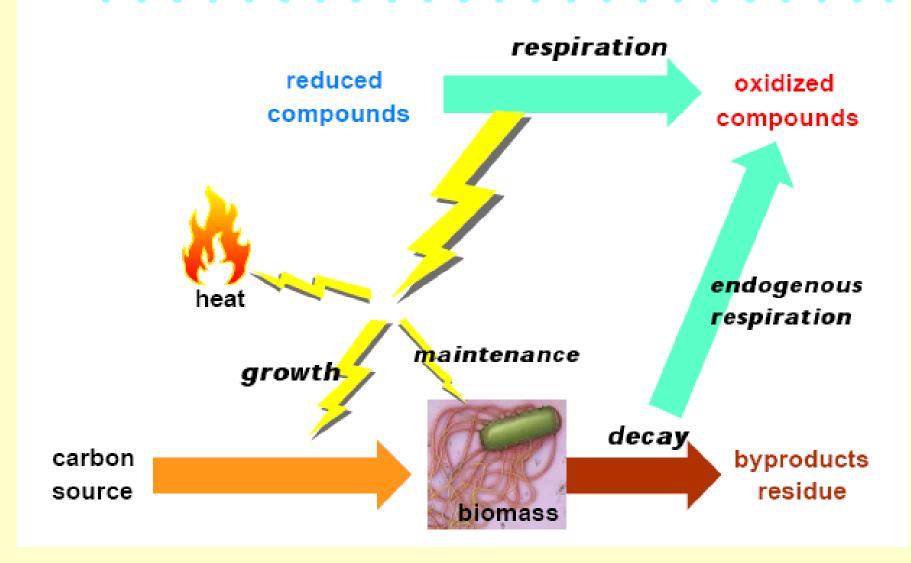
2. Carbon sources for synthesis of cells (with other nutrients)

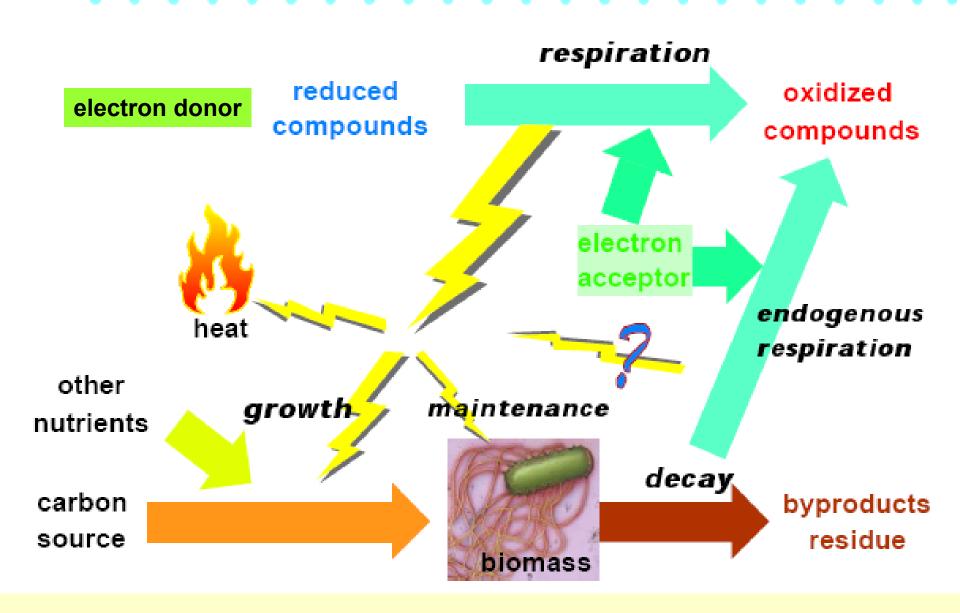
- CO₂ Autotrophic
- Organic molecules Heterotrophic
- All required nutrients (N, P and other inorganic ions)

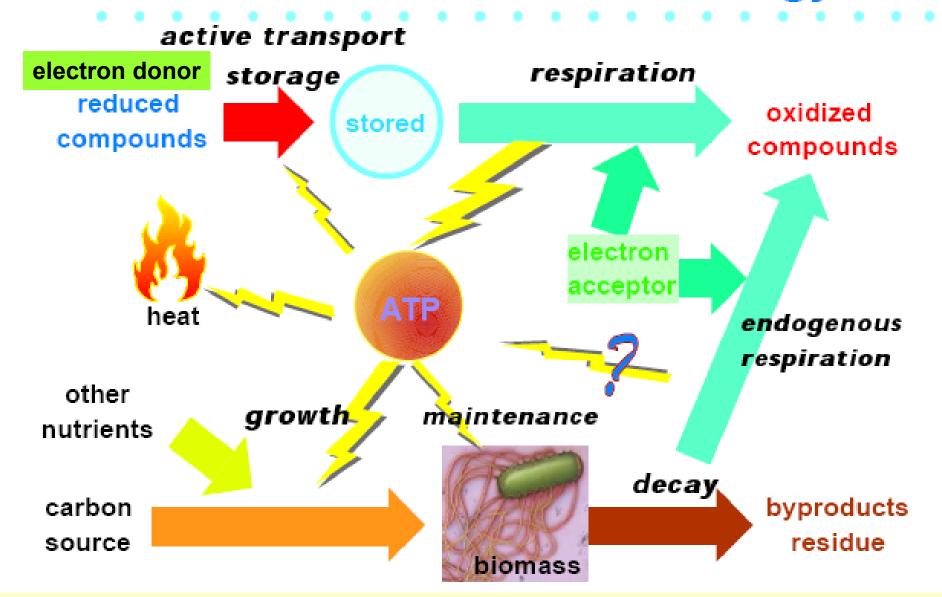
Microbial Metabolism

- energy production
 - oxidation of organic compounds
 - oxidation of inorganic compounds
 - solar energy
- energy consumption
 - synthesis and growth
 - motility
 - active transport
 - maintenance
 - heat









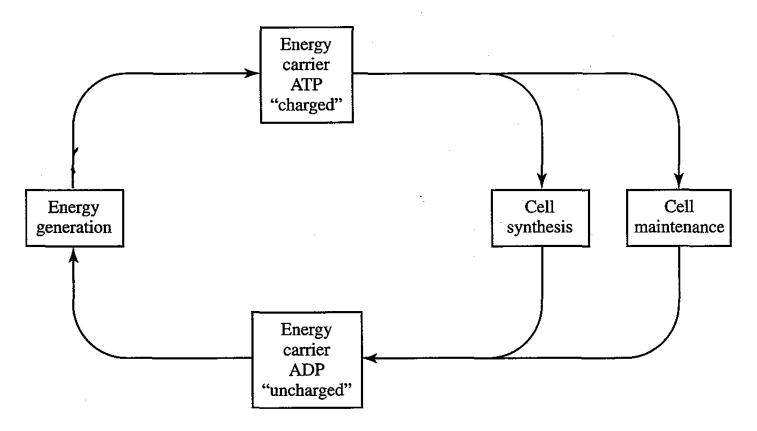


Figure 1.13 Transfer of energy from energy generation to cell synthesis or maintenance via an energy carrier, represented by ATP.

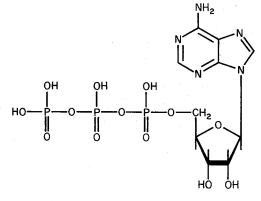
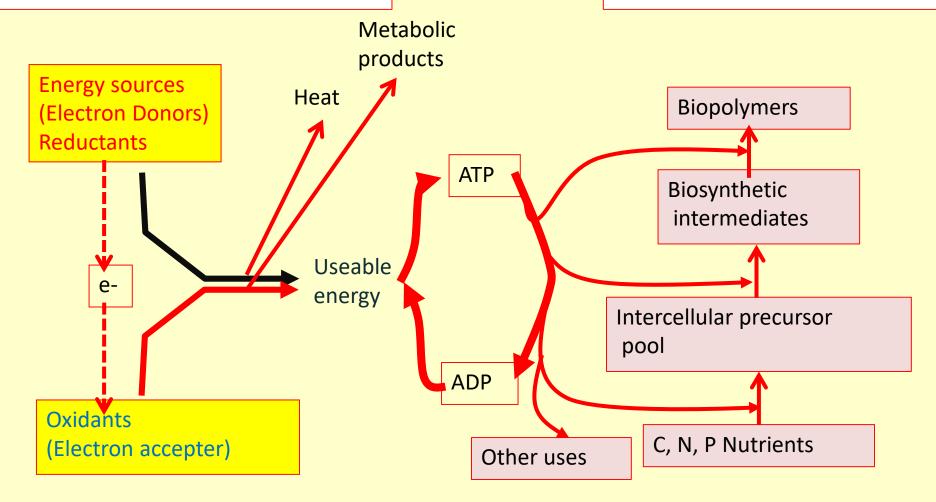


Fig. 7.3 Structure of ATP.

Metabolic Task	Function	Number of Reactions*
Bring nutrients into the cell	To transfer nutrients across the membrane and concentrate them in the cytoplasm	250
Catabolism	To process the major nutrients and produce the 12 precursor metabolites, ATP, and reducing power	406
Biosynthesis	To synthesize all necessary small molecules including building blocks for macromolecules from precursor metabolites	438
Polymerization	To link together building blocks forming macromolecules	482
Assembly	To assemble macromolecules into organelles	7

Catabolism (energy-yielding metabolism)

Anabolism (Biosynthetic metabolism)



Different microbial groups use different ways of energy generation

Catabolic pathways are similar for all bacteria

Oxidation reduction (REDOX) reactions

Catabolism in chemoheterotrophs depends on the oxidation of organic chemicals in the organism's environment. Oxidation remove electrons and reduction adds electrons. Material that are oxidized are called electron donors and those being reduced are called electron accepters. An electron donor (food) and an electron accepter (respiration reductant) must be participated to complete an energy generating reaction.

In the environment, electron donors are organic compounds containing reduced carbons, reduced nitrogen compounds: ammonia, reduced sulfur compound:H₂S, reduced iron such as Fe⁺⁺. There are numerous electron donors in the environment.

The electron acceptor, by comparison, are few including primarily O_2 , nitrate, nitrite, Fe(+3), sulfate, some organic compounds and CO_2 . In recent years, one has found that perchlorate, chromate, selenate, chlorinated organics are capable of participating in biological redox reactions.

Table 2.3 Trophic classification of microorganisms (adapted from Rittmann and McCarty, 2001; Metcalf & Eddy, 2003)

perthermopalities	Thermophile CIVIII	Energy source			Carbon source ¹
Electron donor			Electron acceptor	Typical products ²	andonoso ismis sis
Trophic group	Microbial group	Type of e donor	0.250.+H+	of the following of the first o	
Chemotroph	a Ver de la		etion (to use O		
Organotroph	Aerobic heterotrophs	Organic	O_2	CO ₂ , H ₂ O	Organic
leterotophs	Denitrifiers	Organic	NO_3 , NO_2	N_2 , CO_2 , H_2O	Organic
	Fermenting organisms	Organic	Organic	Organic:VFAs ³	Organic
	Iron reducers	Organic	Fe (III)	Fe (II)	Organic
	Sulfate reducers	Acetate	SO_4^{2-}	H_2S	Acetate
	Methanogens (acetoclastic)	Acetate	acetate	CH ₄	Acetate
Lithotroph	Nitrifiers: AOB ⁴	NH ₄ ⁺	O ₂ requirements	NO ₂	CO_2
analmagnoonal	Nitrifiers: NOB ⁵	NO_2^-	O_2	NO ₃	CO_2
	Anammox ⁶ bacteria	$N\hat{H_4}^+$	NO_2^-	N_2	CO ₂
	Denitrifiers	H_2	NO_3 , NO_2	N_2 , H_2O	CO_2
	Denitrifiers	S	NO_3^-, NO_2^-	N ₂ , SO ₄ ²⁻ ,H ₂ O	CO_2
	Iron oxidizers	Fe (II)	O_2	Fe (III)	CO_2
	Sulphate reducers	H_2	SO_4^{2-}	H ₂ S, H ₂ O	CO ₂
	Sulphate oxidizers	$H_2S, S^0, S_2O_3^{2-}$	O_2	SO_4^{2-}	CO_2
	Aerobic hydrogenotrophs	H_2	O_2	H_2O	CO_2
	Methanogens (hydrogenotrophic)	generally ₂ H d are psychroph	CO ₂	CH ₄	CO ₂
Phototroph					
utotrophs	Algae, plants	H ₂ O	CO_2	O ₂	CO_2
	Photosynthetic bacteria	H_2S	CO_2	S (0)	CO_2

¹Carbon source: organic for heterotrophs and inorganic (CO₂) for autotrophs; mixotrophs can use both. ² Typical products: CO₂ and H₂O are products of catalysis (energy generation) by many micro-organisms. ³ VFAs: volatile fatty acids (typically acetate, propionate, butyrate).

⁴ AOB: ammonia oxidizing bacteria. ⁵ NOB: nitrite oxidizing bacteria. ⁶ Anammox: anaerobic ammonia oxidizing bacteria.

II. THE MAJOR MODES OF NUTRITION – ORGANISMS CLASSIFIED ACCORDING TO THEIR:

A. CARBON SOURCE

- autotrophs organisms (microbes) w. CO₂ as 1° carbon source.
- heterotrophs organisms using organic carbon compounds as primary carbon source.

B. ENERGY SOURCE

- phototrophs organisms that use solar energy.
- chemotrophs organisms that oxidize/burn chemical compounds as their energy source.

C. ELECTRON SOURCE

- lithotrophs organisms that get their electrons from inorganic compounds.
- organotrophs organisms that get their electrons from organic compounds.

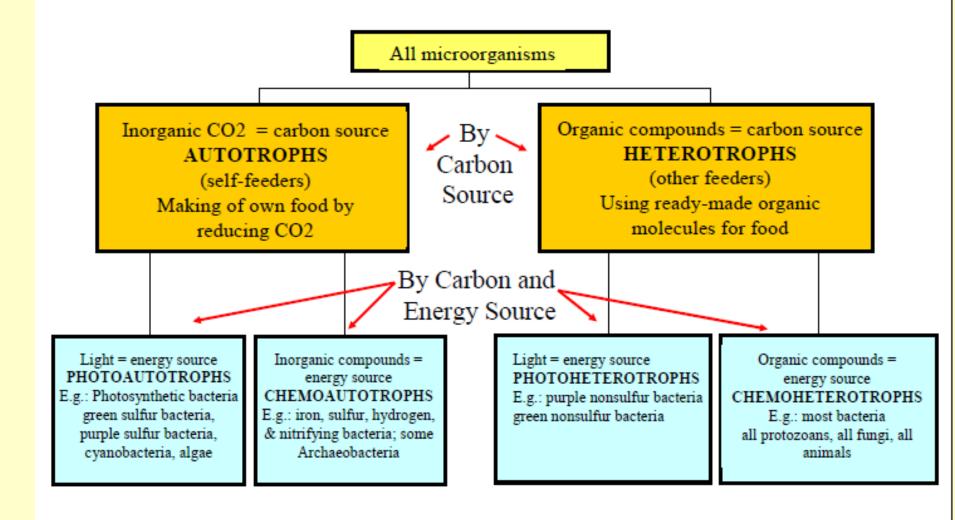
TABLE 7.4 II. THE MAJOR MODES OF NUTRITION -ORGANISMS CLASSIFIED ACCORDING TO THEIR: A. Carbon Source B. Energy Source

Nutritional Categories of Microbes by Carbon and Energy Source Carbon Energy Category Example Source Source Autotroph CO_2 Nonliving Environment Photoautotroph CO2 (Sunlight) Photosynthetic organisms, such as algae, plants, cyanobacteria Chemoautctroph CO2 Simple inorganic Only certain chemicals bacteria, such as methanogens, vent bacteria Heterotroph Other Organisms Organic or Sunlight Photoheterotroph (Sunlight) Nonsulfur Organic bacteria Chemoheterotroph Organic Metabolic Protozoa, fungi, conversion of many bacteria, the nutrients animals from other organisms Saprobe Organic Metabolizing Fungi, bacteria the organic (decomposers) matter of dead organisms Parasite Organic Utilizing the Various parasites tissues, fluids and pathogens; can be bacteria. of a live host fungi, protozoa. animals

 Table 1.6
 Metals as electron acceptors for anaerobic respiration.

Reaction	Microorganism	Reference
$2 \text{ Fe}^{3+} + \text{H}_2 \leftrightarrow 2 \text{ Fe}^{2+} + 2 \text{ H}^+$	Geobacter metallireducens Pelobacter carbinolicus	Lovley and Lonergan (1990) Lovley et al. (1995)
$Mn^{4+} + H_2 \leftrightarrow Mn^{2+} + 2 H^+$	Geobacter metallireducens mixed culture	Lovley (1991) Langenhoff et al. (1997)
$2 \operatorname{Cr}^{6+} + 3 \operatorname{H}_2 \leftrightarrow 2 \operatorname{Cr}^{3+} + 6 \operatorname{H}^+$	Desulfovibrio vulgaris Bacillus strain QC1-2	Lovley and Phillips (1994) Campos et al. (1995)
$Se^{6+} + H_2 \leftrightarrow Se^{4+} + 2 H^+$	Thauera selenatis strains SES-1; SES-3	Macy et al. (1993)
$Se^{6+} + 3 H_2 \leftrightarrow Se^0 + 6 H^+$		Oremland et al. (1989)
$Te^{4+} + 2 H_2 \leftrightarrow Te^0 + 4 H^+$	Schizosaccharomyces pombe	Smith (1974)
$Pb^{2+} + H_2 \leftrightarrow Pb^0 + 2 H^+$	Pseudomonas maltophila	Lovley (1995)
$As^{5+} + H_2 \leftrightarrow As^{3+} + 2 H^+$	Geospirillum arsenophilus	Ahmann et al. (1994)
$Hg^{2+} + H_2 \leftrightarrow Hg^0 + 2 H^+$	Escherichia coli Thiobacillus ferrooxidans	Robinson and Tuovinen (1984)
$U^{6+} + H_2 \leftrightarrow U^{4+} + 2 H^+$	Shewanella putrefaciens	Lovley et al. (1991)

The Main Nutritional Types – a Summary



Energy produced from an oxidization reduction chemical reaction

Acetate and Oxygen (Aerobic Oxidation of Acetate)

Donor:
$$\frac{1}{8} \text{ CH}_3 \text{COO}^- + \frac{3}{8} \text{ H}_2 \text{O} = \frac{1}{8} \text{ CO}_2 + \frac{1}{8} \text{ HCO}_3^- + \text{H}^+ + \text{e}^- - 27.40$$

Acceptor:
$$\frac{1}{4} O_2 + H^+ + e^- = \frac{1}{2} H_2 O$$
 - 78.72

Net:
$$\frac{1}{8} \text{ CH}_3 \text{COO}^- + \frac{1}{4} \text{ O}_2 = \frac{1}{8} \text{ CO}_2 + \frac{1}{8} \text{ HCO}_3^- + \frac{1}{8} \text{ H}_2 \text{O}$$

Acetate and Carbon Dioxide (Methanogenesis of Acetate)

Donor:
$$\frac{1}{8} \text{ CH}_3 \text{COO}^- + \frac{3}{8} \text{ H}_2 \text{O} = \frac{1}{8} \text{ CO}_2 + \frac{1}{8} \text{ HCO}_3^- + \text{H}^+ + \text{e}^- - 27.40$$

Acceptor:
$$\frac{1}{8} \text{CO}_2 + \text{H}^+ + \text{e}^- = \frac{1}{8} \text{CH}_4 + \frac{1}{4} \text{H}_2 \text{O}$$
 23.53

Net:
$$\frac{1}{8} \text{ CH}_3 \text{COO}^- + \frac{1}{8} \text{ H}_2 \text{O} = \frac{1}{8} \text{ CH}_4 + \frac{1}{8} \text{ HCO}_3^ \boxed{-3.87}$$

Glucose and Carbon Dioxide (Methanogenesis from Glucose)

Donor:
$$\frac{1}{24} C_6 H_{12} O_6 + \frac{1}{4} H_2 O = \frac{1}{4} C O_2 + H^+ + e^- - 41.35$$

Acceptor:
$$\frac{1}{8} \text{CO}_2 + \text{H}^+ + \text{e}^- = \frac{1}{8} \text{CH}_4 + \frac{1}{4} \text{H}_2 \text{O}$$
 23.53

Net:
$$\frac{1}{24} C_6 H_{12} O_6 = \frac{1}{8} C H_4 + \frac{1}{8} C O_2$$

-17.82

Hydrogen and Oxygen (Aerobic Oxidation of Hydrogen)

Donor:
$$\frac{1}{2} H_2 = H^+ + e^- - 39.87$$

Acceptor:
$$\frac{1}{4} O_2 + H^+ + e^- = \frac{1}{2} H_2 O$$
 - 78.72

Net:
$$\frac{1}{2} H_2 + \frac{1}{4} O_2 = \frac{1}{2} H_2 O$$
 -118.59

Aerobic oxidation of ammonia $\Delta G^0 \text{ Kj / e- eq}$ Acceptor $0.25 \text{ O}_2 + \text{H}^+ + \text{e}^- = 0.5 \text{ H}_2\text{O}$ - 78.72Donor $0.125 \text{ NH}_4^+ + 0.375 \text{ H}_2\text{O} = 0.125 \text{ NO}_3^- + 1.25 \text{ H}^+ + \text{e}^-$ + 35.11Re: $0.125 \text{ NH}_4^+ + 0.25 \text{ O}_2 = 0.125 \text{ H}_2\text{O} + 0.125 \text{ NO}_3^- + 0.25 \text{ H}^+$ - 43.61

5 Anaerobic sulfate reduction with ammonia

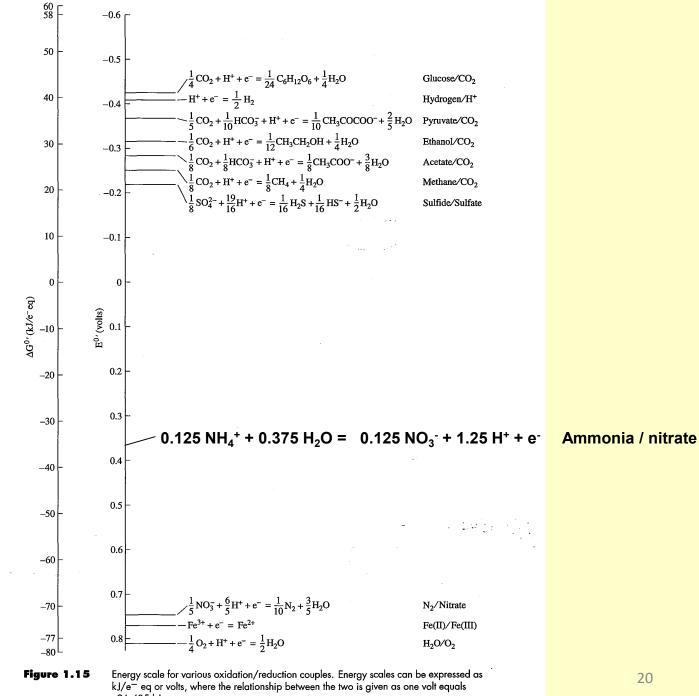
 ΔG^0 Kj / e- eq

Acceptor $0.125 \text{ SO}_4^{=} + 1.188 \text{ H}^+ + \text{e}^- = 0.062 \text{ HS}^- + 0.062 \text{H}_2\text{S} + 0.5 \text{ H}_2\text{O}$ 20.85

Donor $0.125 \text{ NH}_4^+ + 0.375 \text{ H}_2\text{O} = 0.125 \text{ NO}_3^- + 1.25 \text{ H}^+ + \text{e}^-$ 35.11

Re: $0.125 \text{ NH}_4^+ + 0.125 \text{ SO}_4^= = 0.125 \text{ H}_2\text{O} + 0.0625 \text{ H}_2\text{S} + 0.0625 \text{HS}^- + 0.0625 \text{ H}^+$

Redox reaction with positive free energy production is thermodynamically impossible. Anaerobic degradation of ammonia using $SO_4^=$ as acceptor is not possible



-96.485 kJ.

20

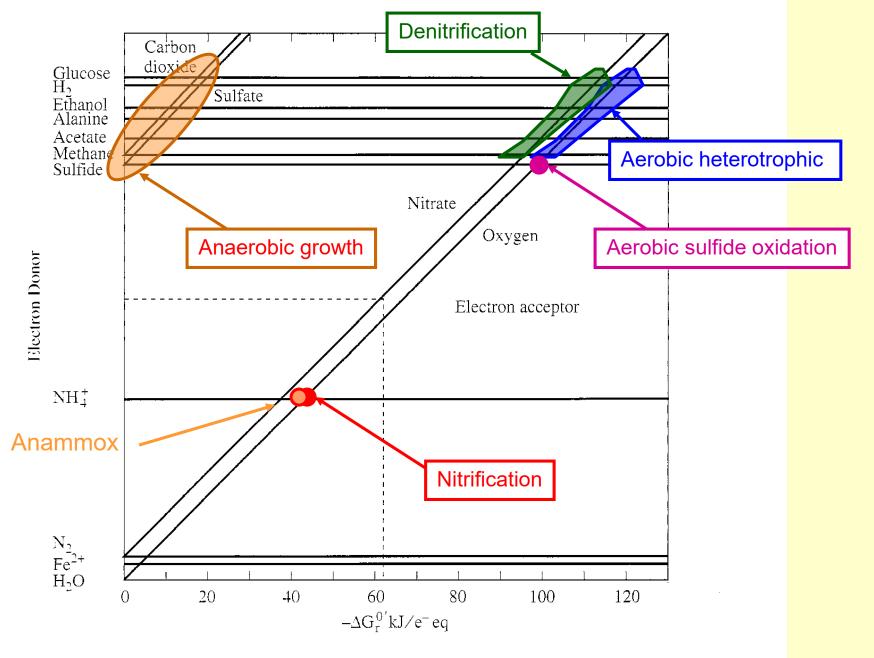
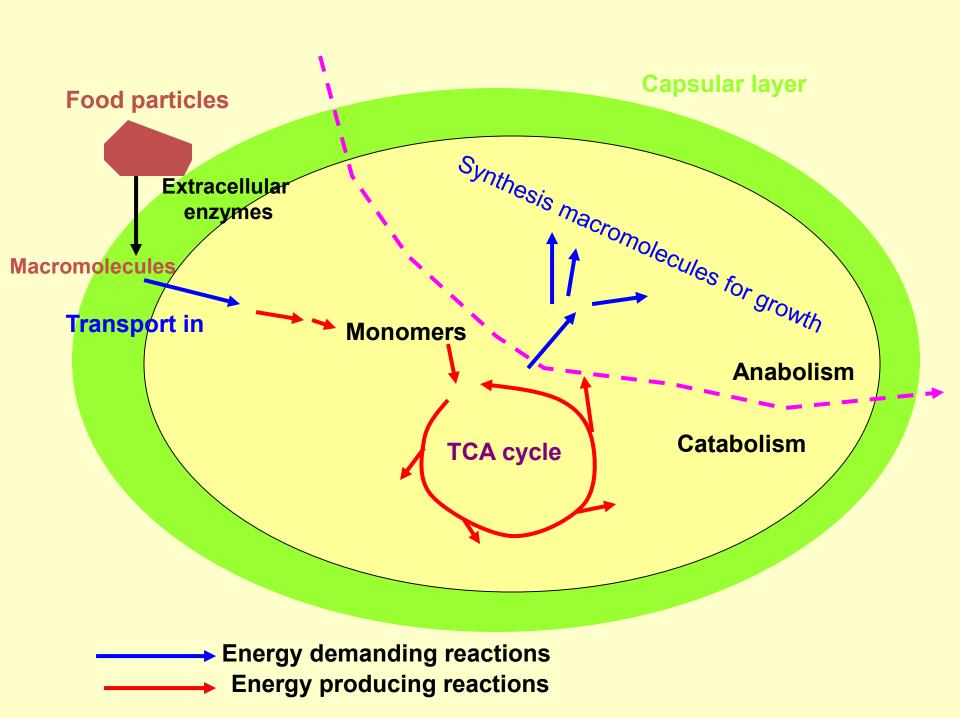
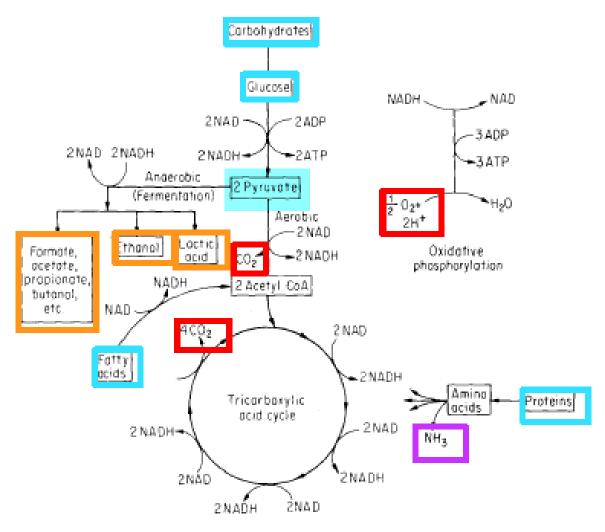


Figure 2.2 Relationship between various electron donors and acceptors and resulting reaction free energy.



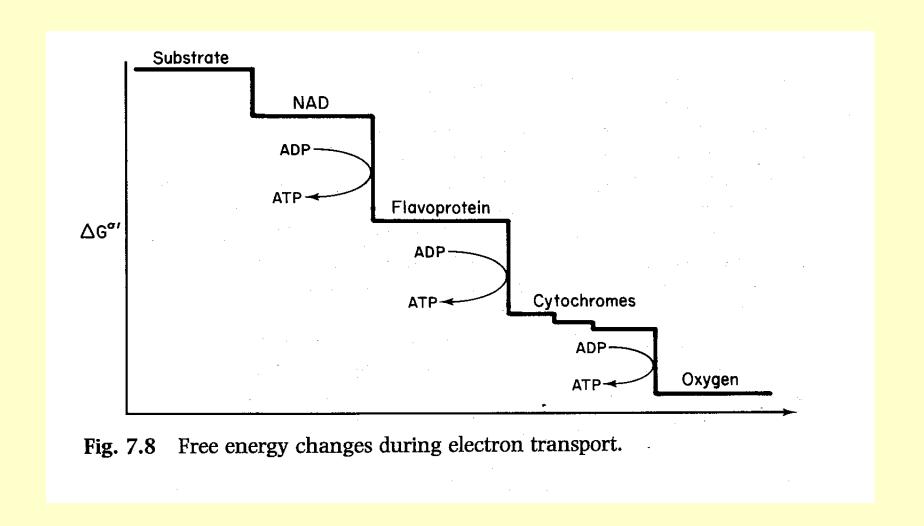
Aerobic Metabolism



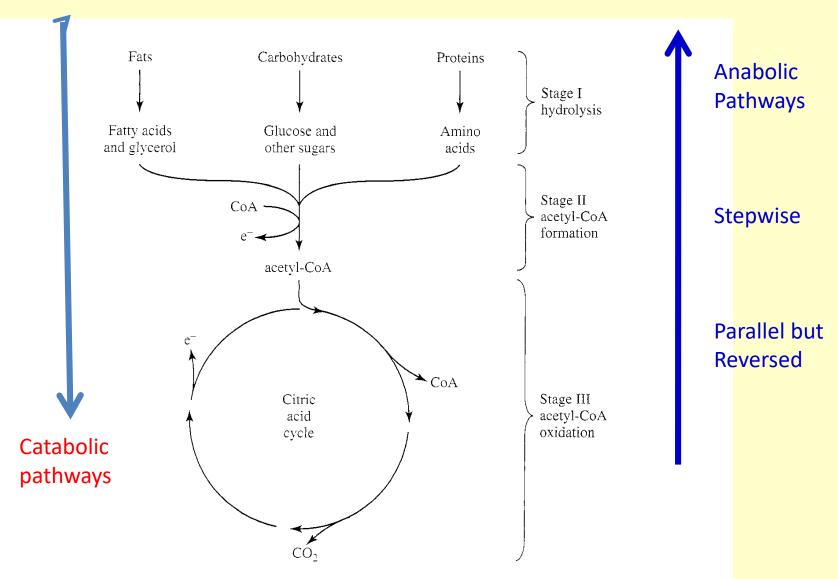
Organic fermentation and oxidation

from Sawyer and McCarty, Chemistry for Environmental Engineers

The catabolic pathways are in step wide manner, so that energy carrier ATP can be synthesized from ADP.



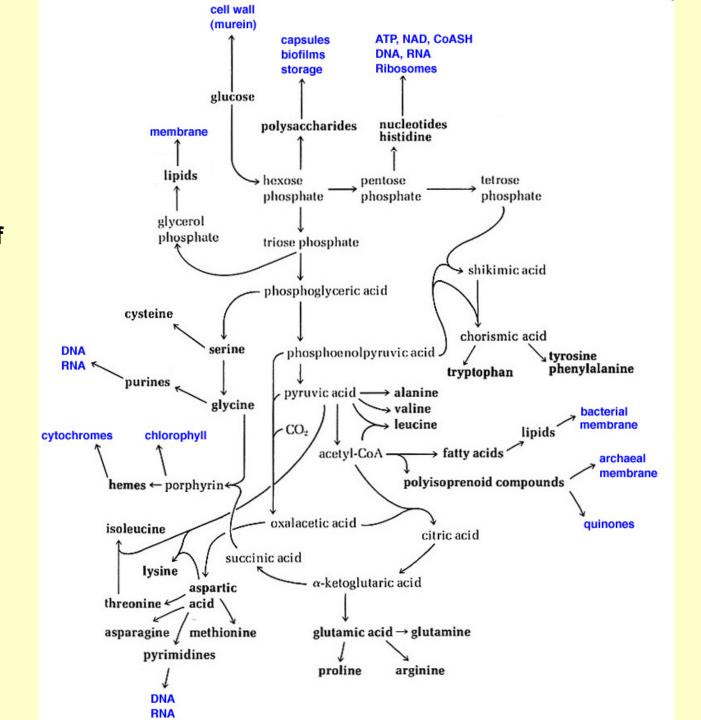
Heterotrophic metabolism pathways – stepwise transformation



The three general stages of catabolism of fats, carbohydrates, and proteins under aerobic conditions.

Reversing the processes gives anabolism.

The main pathways of biosynthesis in procaryotic cells



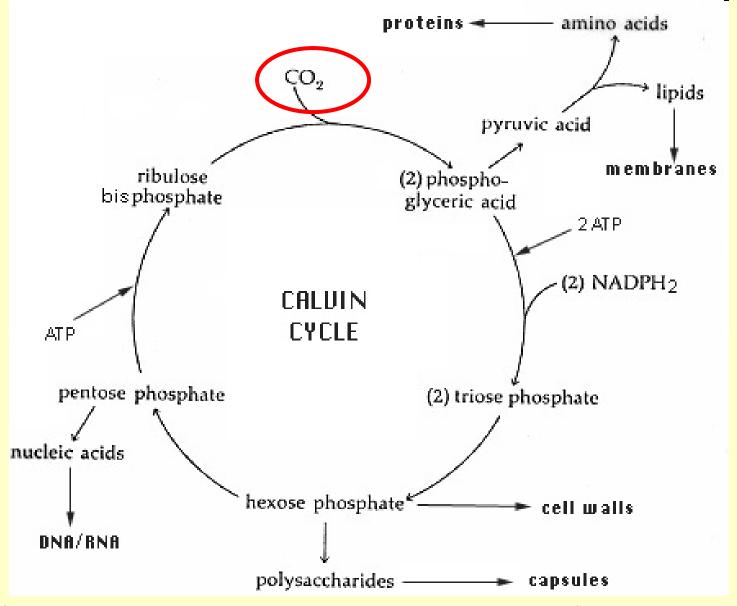
There are also significant difference in energy required for bio-synthesis between heterotrophs and autotrophs

For heterotrophs, the biosynthesis starting point is organic carbons and it takes little energy to elevate to the biomass level:

$$3 \text{ CH}_3 \text{COO}^- + 3 \text{ H}^+ \rightarrow \text{C}_6 \text{H}_{12} \text{O}_6 \quad \Delta \text{G}^{0'} = 335 \text{ kJ}$$
 [1.50]

For autotrophs, the starting point is inorganic CO₂ and it will take significantly higher amount of energy to synthesis biomass:

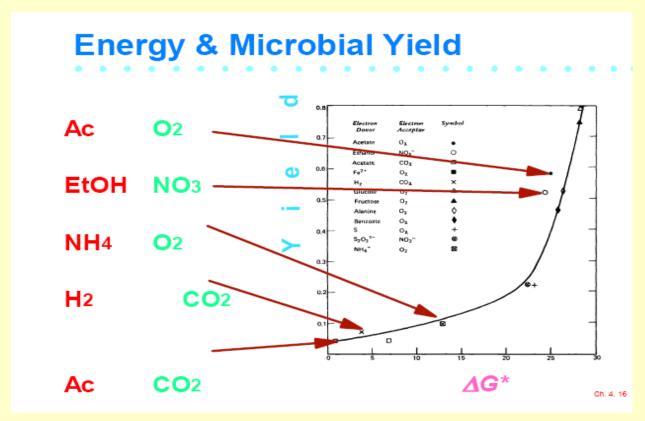
$$6 \text{ CO}_2 + 6 \text{ H}_2\text{O} \rightarrow \text{C}_6\text{H}_{12}\text{O}_6 + 6 \text{ O}_2 \quad \Delta G^{0'} = 2,880 \text{ kJ}$$



The Calvin cycle and its relationship to the synthesis of autotrophic cell materials. The fixation of CO2 to the level of glucose ($C_6H_{12}O_6$) requires 18 ATP and 12 NADPH₂.

Catabolic energy generation: The higher $-\Delta G$ is produced, the more energy is available for growth and maintenance. Aerobic oxidation > anoxic nitrate reduction > anaerobic sulfate reduction > fermentation > anaerobic methane production.

Anabolic energy utilization: The higher the energy level of the carbon source with relation to the biomass, the less energy it takes to synthesis. The autotrophic growth demands the most amount of energy to synthesis biomass.



Cell Yield (Y) for heterotrophy

- Not all of the carbon added as the carbon source is converted to cell biomass
- A fraction is respired as CO₂ during the transformation of the organics to energy (ATP)
- Cell yield coefficient is defined as the amount of biomass produced per unit substrate consumed

Stoichiometry of aerobic bacterial growth

Bacterial Growth: biomass is in both side of the growth equation

substrate + biomass + oxygen + nutrients
$$\longrightarrow$$
 $CO_2 + H_2O + more bacteria + residue$

We can simplify the growth equation by treating biomass as a catalyst

substrate + oxygen + nutrients

$$CO_2 + H_2O + bacteria + residue$$

Bacterial Decay or maintenance:

biomass + oxygen
$$\longrightarrow$$
 CO₂ + H₂O + nutrients+ residue

The concept of Yield:

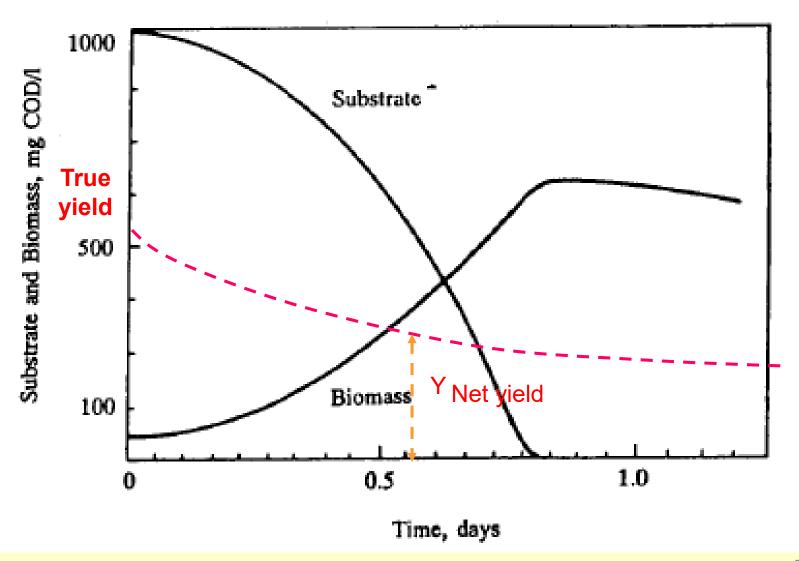
Mathematically, the growth rate of microbial cells is frequently expressed as

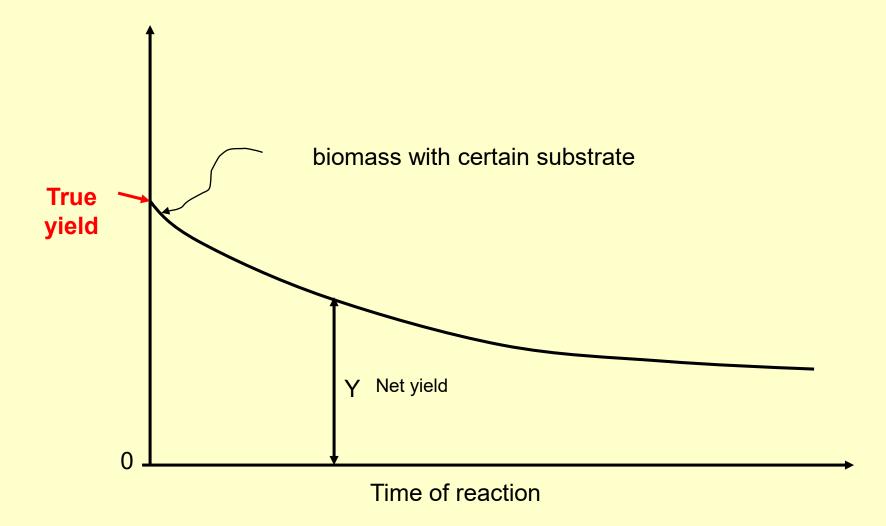
$$\frac{dX_a}{dt} = Y\left(\frac{-dS}{dt}\right) - bX_a$$
 [2.5]

where dX_a/dt represents the net growth rate (M/L³T) of active organism (X_a , M/L³), -dS/dt represents the rate of disappearance (M/L³T) of substrate (S, M/L³), b is the decay rate (T⁻¹) of the organisms, and Y is the true yield of microorganisms (M/M). (A full development of Equation 2.5 and the equations that follow is given in Chapter 3. A short development is used here to support the concept of yield.) The net growth rate is equal the difference between the growth from substrate consumption minus decay due to self (endogenous) respiration or predation. The net yield (Y_n , M/M) can be found by dividing Equation 2.5 by the rate of substrate utilization:

$$Y_n = \frac{dX_a/dt}{-dS/dt} = Y - b\frac{X_a}{-dS/dt}$$
 [2.6]

True Yield is the theoretical biogrowth per unit of substrate consumed without considering decay or maintenance





Cell Yield

Carbon source

Yield coefficient

G of cell per g of chemical

Glucose

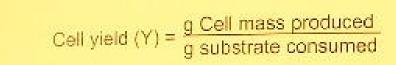
0.4

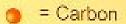
Pentachlorophenol (PCP)

0.05

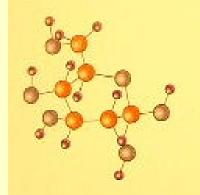
octadecane

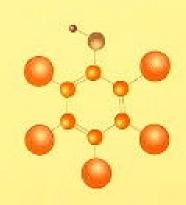
1.49

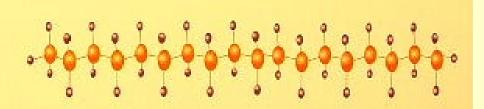




=Hydrogen







Glucose Y = 0.4

Pentachlorophenol Y = 0.05

Biochemical basis of cell yield

- In case of PCP, it is a new chemical that microbes have only encountered since its initial production in 1936
- There is not much chemical energy stored in PCP due to the C-Cl bonds.
- Energy is required to break the C-Cl bonds-energy not available for biomass production.

Biochemical basis of cell yield

- In case of octadecane, it is a component of crude oil that microbes have encountered for millions of years
- Consequently, microbes have had time to evolve efficient enzyme reactions and metabolic pathways to convert it to biomass.
- Octadecane is a highly reduced form of carbon (contains only C-H bonds) and can thus store more energy than compounds that are less reduced or have more oxygen atoms such as carbohydrates (CH₂O)

The COD of a compound is very nearly proportional to its heat of formation, and a crude value of its energy of formation can often be obtained. Thus a rough estimate of the potential energy for the metabolic needs of organism can be made from COD data.

$$C_n H_a O_b N_c + \left(\frac{2n + 0.5a - 1.5c - b}{2}\right) O_2 \rightarrow nCO_2 + cNH_3 + \frac{a - 3c}{2} H_2 O$$
 [2.2]

and

$$COD'/Weight = \frac{(2n+0.5a-1.5c-b)16}{12n+a+16b+14c}$$
 [2.3]

(B) The COD of the organic matter consumed is calculated from the oxidation equation below:

$$8CH_2O + 8O_2 \rightarrow 8CO_2 + 8H_2O$$

$$f_{\text{COD}} = \frac{8O_2}{8\text{CH}_2\text{O}} = \frac{8 \times 32}{8 \times 30} = 1.06 \text{ g COD/g substrate}$$

$$Y'_H = \frac{Y}{f_{COD}} = \frac{0.47 \text{ g VSS/g substrate}}{1.06 \text{ g COD/g substrate}} = 0.44 \text{ g VSS/g COD}$$

(C) The following redox reactions are used to calculate the COD of the biomass generated:

$$C_5H_7NO_2 + 4H_2O \rightarrow 5CO_2 + NH_3 + 20H^+ + 20e^-$$

 $5(4e^- + 4H^+ + O_2 \rightarrow H_2O)$

$$C_5H_7NO_2 + 5O_2 \rightarrow 5CO_2 + NH_3 + 2H_2O$$

$$f_X = \frac{5O_2}{C_5H_2NO_2} = \frac{5 \times 32}{113} = 1.42 \text{ g cell COD/g biomass}$$

Chemical Oxygen Demand (COD)

(D) Benzene
$$C_6H_6 + 7\frac{1}{2}O_2 \longrightarrow 6CO_2 + 3H_2O$$

Th COD =
$$\frac{7\frac{1}{2}*32}{78}$$
 = 3.08 mg COD/mg benzene

Chemical compounds	Theoretical COD Values mg of COD/ mg of compound
Chlorinated organics	0.3 - 1
carbohydrates	1 - 1.2
bacterial cell	1.42
proteins	1.8
short chain carboxylic acids	2
Oil molecules	3
Methane	4

Yield values based on COD are closer together

Organic source	Cell yield g cell per g of compound	Cell yield g cell per g of COD compound
Glucose	0.4	0.40
Pentachlorophenol	0.05	0.15
octadecane	1.45	0.44

Organisms	Yield, g of COD / g of Feed COD
Bacteria with substrate to grow, in	0.6
one day	
Bacteria with much substrate and	0.95
extensive storage, in one hour	
Fish (one year to 0.5 kg)	0.45
Hen	0.32
Pig (to 65 kg)	0.23
Cow (no milk)	0.18
Human (0 to 16 years)	0.01
Human (0 to 70 years)	0.002



The mutation rate for most procaryotic genes is in the neighborhood of 10⁻⁸

http://bioinfo.bact.wisc.edu/themicrobialworld/homepage.html

The Microbial World - a website devoted to microbial sciences

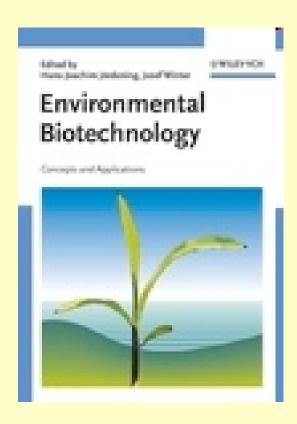
University of Wisconsin – Madison Department of Bacteriology Kenneth Todar

Origin, Evolution and Classification of Microbial Life
Microbes and the Cycles of Elements of Life
Overview of Bacteriology
Structure and Function of Bacterial Cells
Nutrition and Growth of Bacteria
Growth of Bacterial Populations
Life at High Temperatures, by Professor Thomas D. Brock
Control of Microbial Growth
Antimicrobial Agents Used in the Treatment of Infectious Disease
Bacterial Resistance to Antibiotics
Microbial Metabolism
Regulation of Metabolism in Bacteria
Archaea and Bacteria
Lactococcus lactis, Wisconsin's State Microbe
Microbial Interactions with Humans

Introduction to the Microbial World

Effects of Microbes on their Habitat

Chemical and Molecular Composition of Microbial Cells



Environmental Biotechnology: Concepts and Applications
Edited by Hans-Joachim Jördening and Josef Winter
Wiley December 2004

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- 11. Bioreactors (René H. Kleijntjens and Karel Ch. A. M. Luyben)
- 12. In-situ Remediation (T. Held and H. Dörr)
- 13. Composting of Organic Waste (Frank Schuchardt)
- 14. Anaerobic Fermentation of Wet and Semidry Garbage Waste Fractions (Norbert Rilling)
- 15. Landfill Systems, Sanitary Landfilling of Solid Wastes, and Long-term Problems with Leachate (Kai-Uwe Heyer and Rainer Stegmann)
- 16. Sanitary Landfills: Long-term Stability and Environmental Implications (Michael S. Switzenbaum)
- 17. Process Engineering of Biological Waste Gas Purification (Muthumbi Waweru, Veerle Herrygers, Herman Van Langenhove, and Willy Verstraete)
- 18. Commercial Applications of Biological Waste Gas Purification (Derek E. Chitwood and Joseph S. Devinny)
- 19. Perspectives of Wastewater, Waste, Off-gas and Soil Treatment (Claudia Gallert and Josef Winter)

1

Bacterial Metabolism in Wastewater Treatment Systems

Claudia Gallert and Josef Winter

1.1 Introduction

Water that has been used by people and is disposed into a receiving water body with altered physical and/or chemical parameters is defined as wastewater. If only the physical parameters of the water were changed, e.g., resulting in an elevated temperature after use as a coolant, treatment before final disposal into a surface water may require only cooling close to its initial temperature. If the water, however, has been contaminated with soluble or insoluble organic or inorganic material, a combination of mechanical, chemical, and/or biological purification procedures may be required to protect the environment from periodic or permanent pollution or damage. For this reason, legislation in industrialized and in many developing countries has reinforced environmental laws that regulate the maximum allowed residual concentrations of carbon, nitrogen, and phosphorous compounds in purified wastewater, before it is disposed into a river or into any other receiving water body However, enforcement of these laws is not always very strict. Enforcement seems to be related to the economy of the country and thus differs significantly between wealthy industrialized and poor developing countries. In this chapter basic processes for biological treatment of waste or wastewater to eliminate organic and inorganic pollutants are summarized.

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