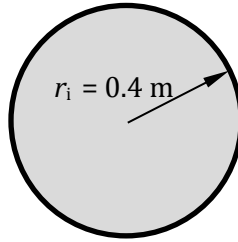


## Homework Set 1

Due date: January 27, 2016 after class

**Problem 1:** An infinitely long cylinder with a thermal conductivity of  $k_i = 5 \text{ W/m}\cdot\text{K}$  and a radius of  $r_i = 0.40 \text{ m}$  generates heat as a function of the radius at a rate of  $\dot{q}_i = 5000[1-r/r_i] \text{ W}\cdot\text{m}^{-3}$ . The temperature at the center of the cylinder,  $r = 0$ , is  $T_{\text{center}} = 500^\circ\text{C}$ . Natural convection is used to remove heat at the outer surface of the cylinder, resulting in a convective heat transfer coefficient of  $h = 8.5 \text{ W/m}^2\cdot\text{K}$ . The system is schematically depicted in Figure 1. Assuming steady-state, negligible contact resistance, one-dimensional radial conduction in the cylinder, constant properties, and negligible radiative heat exchange with the surroundings, determine



**Figure 1.**

- a) The temperature profile as a function of radius.

$$c\rho \frac{\partial T}{\partial t} = \frac{k}{r} \frac{\partial}{\partial r} \left( r \frac{\partial T}{\partial r} \right) + k \frac{\partial^2 T}{\partial z^2} + \frac{1}{r^2} \frac{\partial^2 T}{\partial \phi^2} + \dot{q}$$

$$0 = \frac{k}{r} \frac{\partial}{\partial r} \left( r \frac{\partial T}{\partial r} \right) + \dot{q} \Rightarrow \frac{\partial}{\partial r} \left( r \frac{\partial T}{\partial r} \right) = \frac{-\dot{q}}{k}$$

$$0 = \frac{k}{r} \frac{d}{dr} \left( r \frac{dT}{dr} \right) + \dot{q} \Rightarrow \frac{d}{dr} \left( r \frac{dT}{dr} \right) = \frac{-\dot{q}r}{k} = -\frac{5000r}{k} + 5000 \frac{r^2}{r_i}$$

$$r \frac{dT}{dr} = -\frac{2500r^2}{k} + \frac{5000}{3k} \frac{r^3}{r_i} + C_1$$

$$\text{Heat flux at center: } q_{r=0}'' = 0 \Rightarrow \frac{dT}{dr} \bigg|_{r=0} = 0 \Rightarrow 0 = -\frac{2500(0)^2}{k} + \frac{5000}{3k} \frac{(0)^3}{r_i} + C_1 \Rightarrow C_1 = 0$$

$$\frac{dT}{dr} = -\frac{2500r}{k} + \frac{5000}{3k} \frac{r^2}{r_i} \Rightarrow T = -\frac{1250r^2}{k} + \frac{5000}{9k} \frac{r^3}{r_i} + C_2$$

$$T(r=0) = -\frac{0}{k} + \frac{5000}{9k} \frac{0}{r_i} + C_2 = 500^\circ\text{C}$$

$$T(r) = -\frac{1250r^2}{k} + \frac{5000}{9k} \frac{r^3}{r_i} + 500^\circ\text{C}$$

- b) The heat flux at  $r = 0.2 \text{ m}$  in  $\text{W}\cdot\text{m}^{-2}$ .

$$q_{r=0.2\text{m}}'' = -k \frac{dT}{dr} \bigg|_{r=0.2\text{m}} = 2500r - \frac{5000}{3} \frac{r^2}{r_i} = 333.3 \text{ W}\cdot\text{m}^{-2}$$

c) The temperature at outer surface and outside the boundary layer in °C.

$$T(0.4) = -\frac{1250(0.4\text{m})^2}{k} + \frac{5000(0.4\text{m})^3}{9k} + 500^\circ\text{C} = 477.8^\circ\text{C}$$

$$q''_{r=0.4\text{m}} = -k \frac{\partial T}{\partial r}_{r=0.4\text{m}} = -\frac{2500(0.4\text{m})}{k} + \frac{5000(0.4\text{m})^2}{3k} = 333.3 \text{ W} \cdot \text{m}^{-2} = h[T(r=0.4) - T_\infty]$$

$$q''_{r=0.4\text{m}} = h[T(r=0.4) - T_\infty] \Rightarrow T_\infty = T(r=0.4) - \frac{q''_{r=0.4\text{m}}}{h} = 438.6^\circ\text{C}$$

**Problem 2:** Heat is conducted through a homogeneous wall composed of a material with a temperature-dependent thermal conductivity of  $k = 0.01921 + 0.000137T \text{ W/m} \cdot \text{K}^1$  (where  $T$  is given in °C). The inside convective heat transfer coefficient is  $h = 8.5 \text{ W/m}^2 \cdot \text{K}$ , the outer and inner surface temperatures are  $10^\circ\text{C}$  and  $40^\circ\text{C}$ , respectively, and the wall is 100 mm thick. Assume 1-D heat flow and steady state. Determine the heat flux and inner air temperature. List any other relevant assumptions that are required to solve the problem.

Additional Assumptions:

- No heat generation

Heat transfer across the wall:

$$\dot{E}_{\text{st}}^0 = \dot{E}_{\text{in}} - \dot{E}_{\text{out}} + \dot{E}_{\text{gen}}^0 \Rightarrow \dot{E}_{\text{in}} = \dot{E}_{\text{out}}$$

$$\dot{E}_{\text{in}} = A_s q''_{x=0}, \dot{E}_{\text{out}} = A_s q''_{x=L} \Rightarrow q''_{x=0} = q''_{x=L} = q''$$

$$q'' = -k \frac{dT}{dx} \Rightarrow q'' dx = -k dT \Rightarrow q'' \int_0^L dx = - \int_{T_{s,\text{in}}}^{T_{s,\text{o}}} k dT$$

$$q'' L = - \int_{T_{s,\text{in}}}^{T_{s,\text{o}}} [0.01921 + 0.000137T] dT = \left[ 0.01921T + \frac{0.000137T^2}{2} \right]_{10^\circ\text{C}}^{40^\circ\text{C}}$$

$$q'' = \frac{1}{L} \left[ 0.01921T + \frac{0.000137T^2}{2} \right]_{10^\circ\text{C}}^{40^\circ\text{C}} = \frac{1}{0.1 \text{ m}} \left[ 0.01921(40 - 10) + \frac{0.000137(40^2 - 10^2)}{2} \right]$$

$$q'' = h(T_{\text{in}} - T_{s,\text{in}}) \Rightarrow T_{\text{in}} = \frac{q''}{h} + T_{s,\text{in}} = 40.8^\circ\text{C}$$

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<sup>1</sup>H. Manz, P. Loutzenhiser, T. Frank, P.A. Strachan, R. Bundi, G. Maxwell, Series of experiments for empirical validation of solar gain modeling in building energy simulation codes—Experimental setup, test cell characterization, specifications and uncertainty analysis, *Building and Environment*, Volume 41, Issue 12, Pages 1784-1797