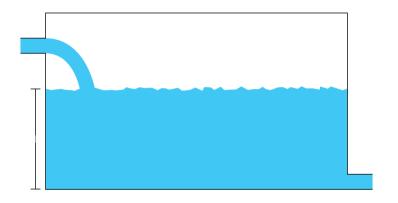
# Process Automation Laboratory - Modeling first-order systems

Kjartan Halvorsen

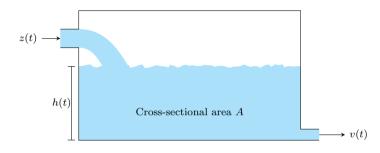
February 14, 2022

# First-order system example: A tank



- 1. What is the state of the system?
- 2. What is the input signal and output signal?

# First-order system example: A tank

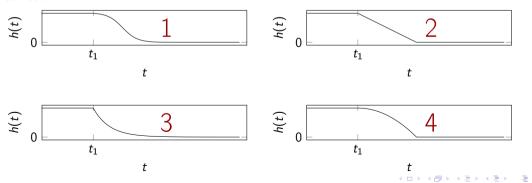


$$\frac{d}{dt}(Ah) = z(t) - x(t) = z(t) - a\sqrt{2gh} \implies \frac{d}{dt}h(t) = -\frac{a\sqrt{2g}}{A}\sqrt{h(t)} + \frac{1}{A}z(t)$$

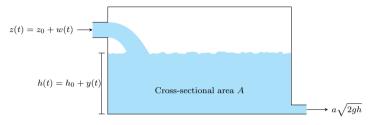
#### Intuition



Individual activity A constant inflow has been present since forever, but at time  $t_1$  the flow in is suddenly shut off. Which of the responses of the water level h(t) below is correct?



### Deviation variables



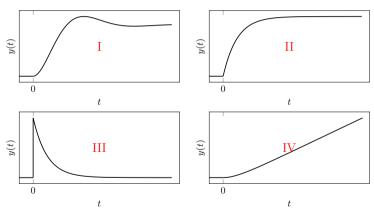
Flow in:  $z(t) = z_0 + w(t)$ . Level of water:  $h(t) = h_0 + y(t)$ . The constants  $h_0$  and  $z_0$  define an *operating point*.

$$\frac{d}{dt}h(t) = -\frac{a\sqrt{2g}}{A}\sqrt{h(t)} + \frac{1}{A}z(t)$$

Individual activity Given  $h_0$  determine the operating point for the inflow,  $z_0$ , such that the system is in equilibrium at the operating point.

### Intuition

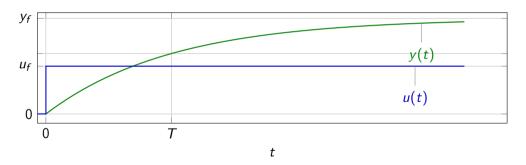
Which change y(t) in the water level corresponds to a step change w(t) in the inflow?



# Fitting a first-order model

Assuming a plant model of first-order with time-constant T

$$Y(s) = \frac{K}{sT+1}U(s) \quad \stackrel{U(s) = \frac{u_f}{s}}{\Longrightarrow} \quad y(t) = u_f K(1 - e^{-\frac{t}{T}})u_H(t)$$

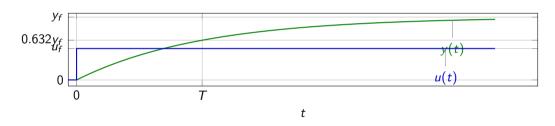


Individual activity Evaluate the response y(t) at the time instant t = T and for  $t \to \infty$ !

### Fitting a first-order model

Assuming a plant model of first-order with time-constant T

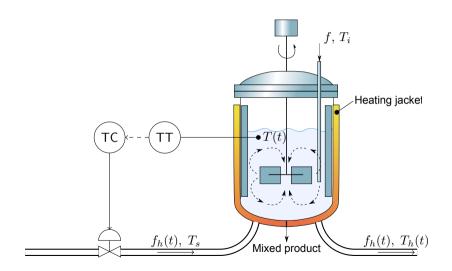
$$Y(s) = \frac{K}{sT+1}U(s) \quad \stackrel{U(s) = \frac{u_f}{s}}{\Longrightarrow} \quad y(t) = u_f K(1 - e^{-\frac{t}{T}})u_H(t)$$



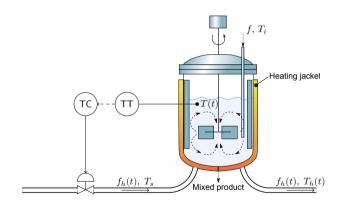
Time-constant: Find the time t = T at which the response has reached 63.2% of its final value

Gain: 
$$y_f = \lim_{t \to \infty} y(t) = Ku_f \quad \Rightarrow \quad K = \frac{y_f}{u_f}$$

### A Continuous Stirred Tank Reactor



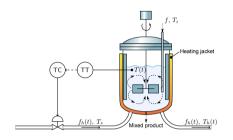
### A Continuous Stirred Tank Reactor



#### Assume:

- 1. Constant flow *f* through the tank reactor
- 2. Constant temperatures  $T_i$  and  $T_s$
- 3. Perfect mixing in the tank reactor
- Perfect mixing in the heating jacket
- 5. Isothermic reaction

### A Continuous Stirred Tank Reactor

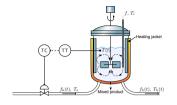


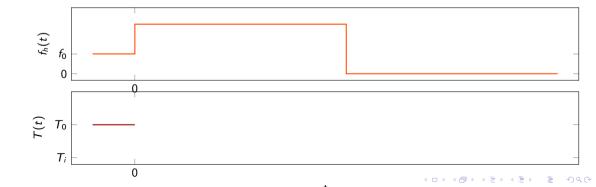
### Energy balance:

$$\frac{dT(t)}{dt} = k_1 (T_i - T(t)) + k_2 (T_h(t) - T(t))$$

$$\frac{dT_h(t)}{dt} = k_3 f_h(t) (T_s - T_h(t)) - k_4 (T_h(t) - T(t))$$

### Intuition

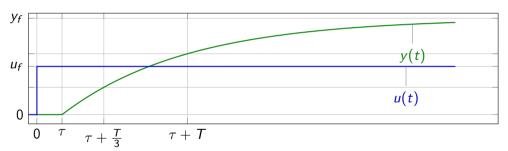




# Fitting first-order model with delay

Assuming a plant model of first-order with time constant  ${\cal T}$  and delay  ${ au}$ 

$$Y(s) = \frac{Ke^{-s\tau}}{sT+1}U(s) \quad \stackrel{U(s) = \frac{u_f}{s}}{\Longrightarrow} \quad y(t) = u_f K(1 - e^{-\frac{t-\tau}{T}})u_H(t-\tau)$$



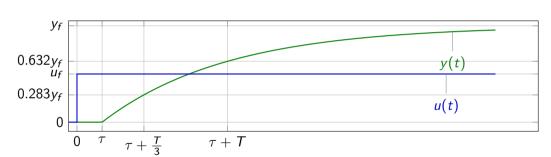
t

Individual activity Evaluate the response y(t) at the two time instants  $t = \tau + \frac{T}{3}$  and  $t = \tau + T!$ 

### Fitting first-order model with delay

Assuming a plant model of first-order with time constant T and delay au

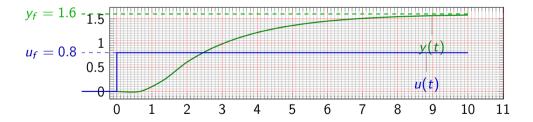
$$Y(s) = \frac{Ke^{-s\tau}}{sT + 1}U(s) \quad \stackrel{U(s) = \frac{u_f}{s}}{\Longrightarrow} \quad y(t) = u_f K(1 - e^{-\frac{t - \tau}{T}})u_H(t - \tau)$$



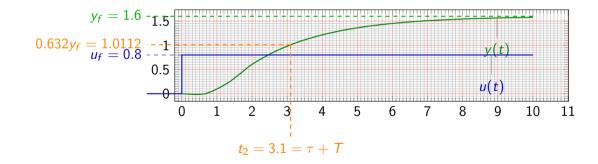
t

$$y_f = \lim_{t \to \infty} y(t) = u_f K \quad \Rightarrow \quad K = \frac{y_f}{u_f}.$$

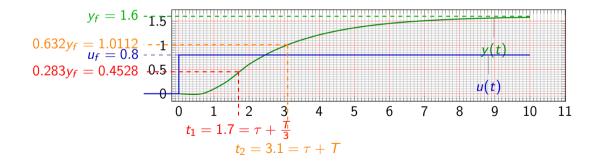
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$$y_{f} = 1.6 \cdot 1.5$$

$$0.632y_{f} = 1.0112 \cdot -1$$

$$u_{f} = 0.8 \cdot 0.5$$

$$0.283y_{f} = 0.4528$$

$$0.5$$

$$0 \cdot 1 \cdot 2 \cdot 3 \cdot 4 \cdot 5 \cdot 6 \cdot 7 \cdot 8 \cdot 9 \cdot 10 \cdot 11$$

$$t_{1} = 1.7 = \tau + \frac{\tau}{3}$$

$$t_{2} = 3.1 = \tau + T$$

$$\begin{cases} 1.7 = \tau + \frac{\tau}{3} \\ 3.1 = \tau + T \end{cases} \Rightarrow \begin{cases} \tau = 1 \\ T = 2.1 \end{cases}, \quad K = \frac{y_{f}}{u_{f}} = \frac{1.6}{0.8} = 2$$

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