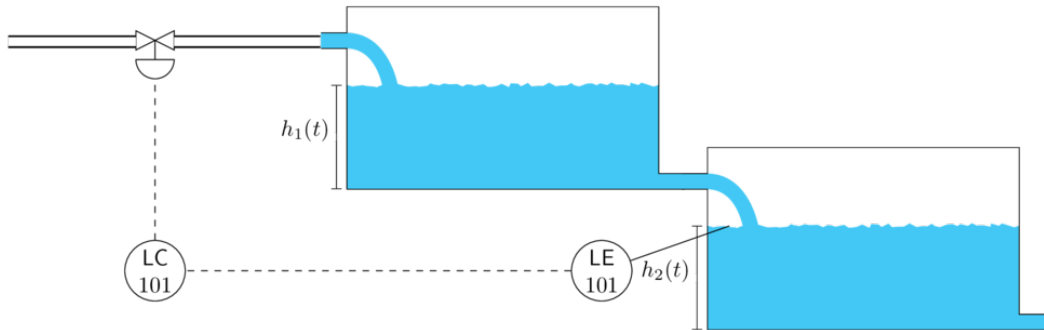


# Control Engineering Laboratory - Cascade control and feed forward

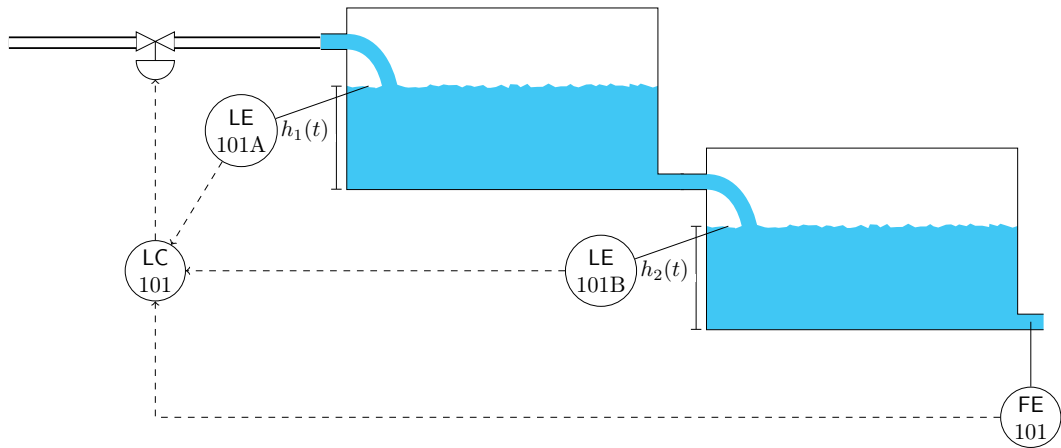
Kjartan Halvorsen

2020-09-28

## The two-tank model with one level sensor

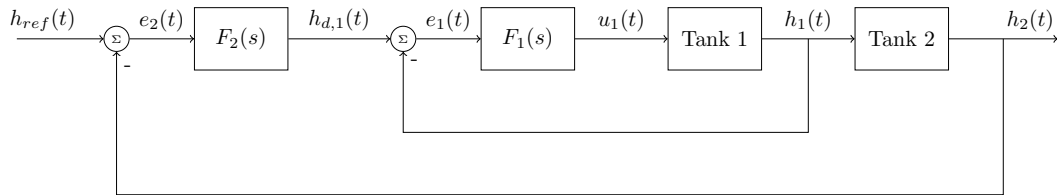


## The two-tank model with two level sensors and one flow sensor

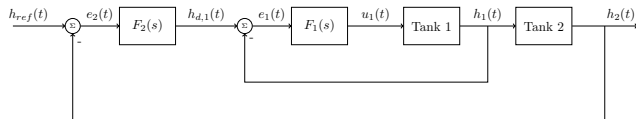


Key idea: We can improve the control using more information

## Cascade control



## Designing the inner loop



Have model  $G_1(s) = \frac{K_1}{s\tau_1+1} = \frac{51}{51s+1}$ . PI controller

$$F_1(s) = k_c \left( 1 + \frac{1}{\tau_i s} \right) = k_c \frac{\tau_i s + 1}{\tau_i s}$$

Characteristic equation

$$s(s\tau_1 + 1) + k_c \frac{K}{\tau_i} (s\tau_i + 1) = 0$$

Choose  $\tau_i$  and  $k_c$  to place the poles at any desired location in the LHP.

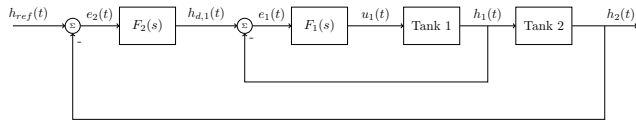
## Exercise

Have characteristic equation

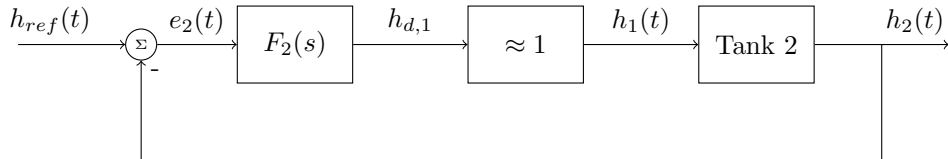
$$s(s\tau_1 + 1) + k_c \frac{K}{\tau_i} (s\tau_i + 1) = 0$$

Choose  $\tau_i = \tau_1$ , and then determine  $k_c$  which gives a pole in  $s = -\frac{4}{\tau_1}$ .

## Designing the outer loop

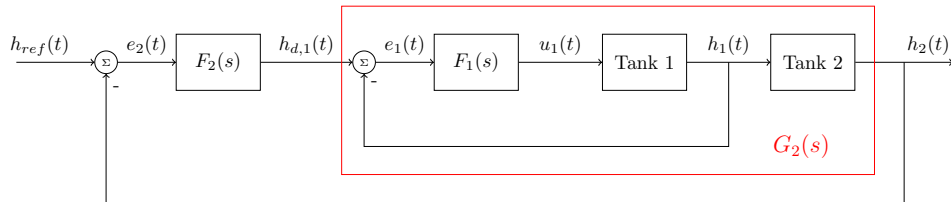


The output of the outer controller  $F_2(s)$  is the desired level in tank 1. If the inner loop is sufficiently fast, we can approximate that the actual level in tank 1 is equal to the desired level.



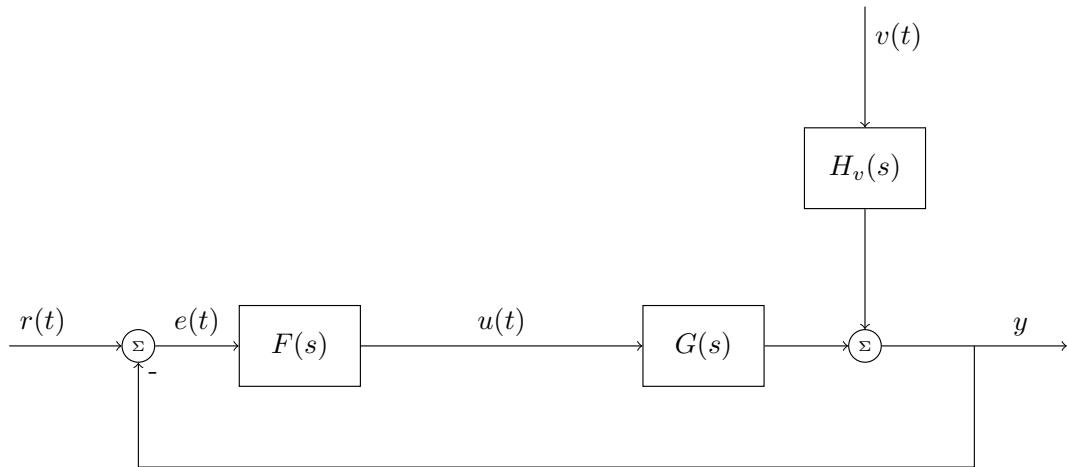
## Designing the outer loop, contd

Alternatively, we can fit a model to the plant and the inner control-loop

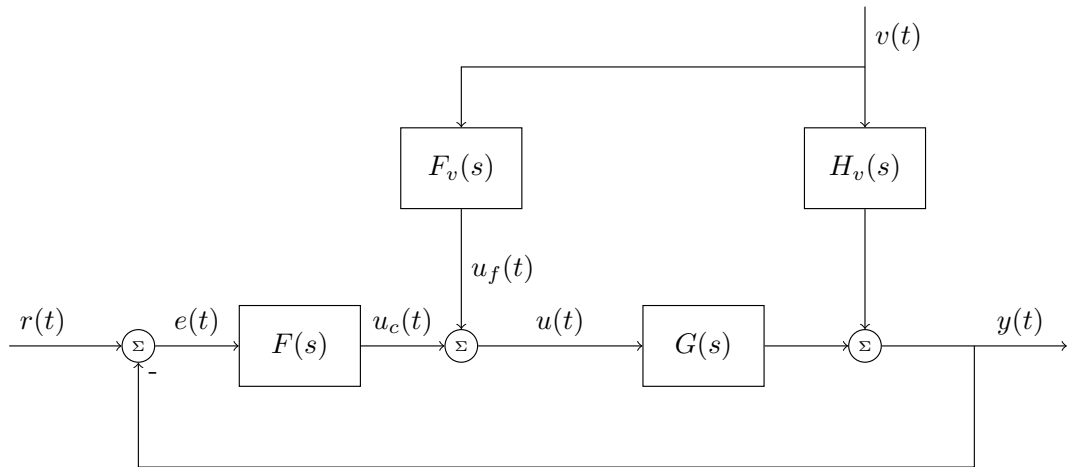




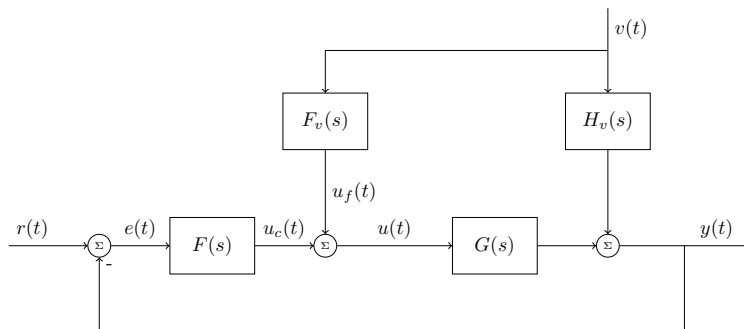
## Feed forward from the disturbance



## Feed forward from the disturbance



## Feed forward from the disturbance



Clearly,

$$Y(s) = H_v(s)V(s) + G(s)(U_c(s) + F_v(s)V(s))$$

Activity: Determine  $F_v(s)$  that eliminates the effect of the disturbance!