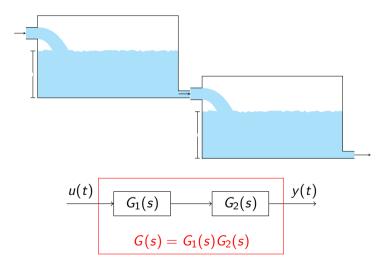
Process Automation Laboratory - PID control

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Second-order models

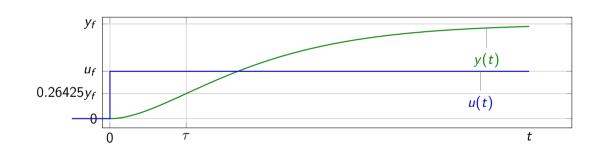
Two first-order models in series



Fitting second-order critically-damped model

Model with two identical time-constants. Assuming model

$$Y(s) = \frac{K}{(s\tau + 1)^2} U(s) \quad \stackrel{U(s) = \frac{u_f}{s}}{\Longrightarrow} \quad y(t) = u_f K \left(1 - \left(1 + \frac{t}{\tau}\right) e^{-\frac{t}{\tau}}\right) u_H(t)$$



$$y_f = \lim_{t \to \infty} y(t) = u_f K \quad \Rightarrow \quad K = \frac{y_f}{u_f}.$$



Feedback control



The PID controller

$$\begin{array}{c|c}
r(t) & e(t) \\
\hline
y(t) & F(s)
\end{array}$$

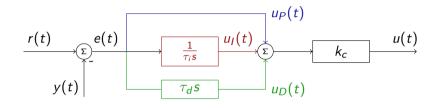
Parallel form (ISA)

$$F(s) = k_c \left(1 + \frac{1}{\tau_i s} + \tau_d s \right)$$

Series form

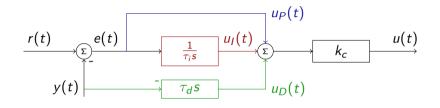
$$F(s) = \mathcal{K}_c \left(rac{ au_I s + 1}{ au_I s}
ight) (au_D s + 1) = \underbrace{rac{\mathcal{K}_c (au_I + au_D)}{ au_I}}_{\mathcal{K}_c} \left(1 + \underbrace{rac{1}{(au_I + au_D)} s}_{ au_I} + \underbrace{rac{ au_I au_D}{ au_I + au_D}}_{ au_d} s
ight)$$

The PID - Parallel form



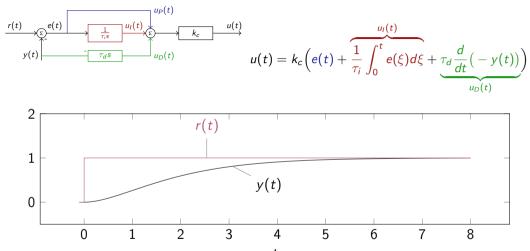
$$u(t) = k_c \left(e(t) + \frac{1}{\tau_i} \int_0^t e(\xi) d\xi + \tau_d \frac{d}{dt} e(t) \right)$$

The PID - Parallel form, modified D-part



$$u(t) = k_c \left(e(t) + \underbrace{\frac{1}{\tau_i} \int_0^t e(\xi) d\xi}_{u_D(t)} + \underbrace{\tau_d \frac{d}{dt} \left(- y(t) \right)}_{u_D(t)} \right)$$

The PID - Parallel form

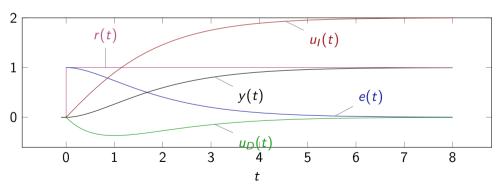


Activity Sketch the error signal e(t), the derivative signal $u_D(t)$ and the integral signal $u_I(t)$ (use $\tau_I = \tau_d = 1$)

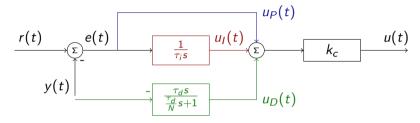
The PID - Parallel form, solution

The PID - Parallel form, solution

$$u(t) = k_c \left(e(t) + \underbrace{\frac{1}{\tau_i} \int_0^t e(\xi) d\xi}_{u_D(t)} + \underbrace{\tau_d \frac{d}{dt} (-y(t))}_{u_D(t)} \right)$$



The PID - practical form



The parameter N is chosen to limit the influence of noisy measurements. Typically,

PID tuning

Method by Smith & Corripio using table by Ziegler-Nichols

Given process model (fitted to response of the system)

$$G(s) = K \frac{\mathrm{e}^{-s\theta}}{\tau s + 1}$$

and PID controller

$$F(s) = k_c \left(1 + \frac{1}{\tau_i s} + \tau_d s \right)$$

Choose the PID parameters according to the following table (Ziegler-Nichols, 1943)

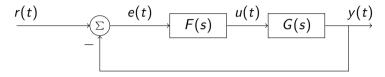
Controller	k _c	$ au_{i}$	$ au_{d}$
Р	$\frac{ au}{ heta K}$		
PI	$rac{0.9 au}{ heta K}$	$\frac{\theta}{0.3}$	
PID	$rac{1.2 au}{ heta K}$	2θ	$\frac{\theta}{2}$

Gives good control for



Analytical PID tuning

Analytical PID tuning



Activity Solve for F(s) in the closed-loop transfer function

$$G_c(s) = \frac{G(s)F(s)}{1 + G(s)F(s)}$$

Analytical PID tuning - Solution

Analytical PID tuning - Solution

Solving for F(s) in the closed-loop transfer function $G_c(s) = \frac{G(s)F(s)}{1+G(s)F(s)}$

$$egin{aligned} ig(1+G(s)F(s)ig)G_c(s)&=G(s)F(s)\ G_c(s)&=ig(1-G_c(s)ig)G(s)F(s)\ F(s)&=rac{G_c(s)}{G(s)}\ 1-G_c(s) \end{aligned}$$

Analytic PID tuning - first-order with delay



Given model $G(s)=Krac{\mathrm{e}^{-s heta}}{ au s+1}$ of the process and desired closed-loop transfer function $G_c(s)=rac{\mathrm{e}^{-s heta}}{ au_c s+1}$

Activity Show that the controller becomes

$$F(s) = rac{1}{K} \left(rac{ au s + 1}{ au_c s + 1 - \mathrm{e}^{-s heta}}
ight) pprox rac{1}{K} \left(rac{ au s + 1}{ au_c s}
ight) = \underbrace{rac{ au}{K au_c}}_{k_c} \left(1 + \underbrace{rac{1}{ au_i s}}_{ au_i} s
ight).$$

Which is a PI-controller with $k_c = \frac{\tau}{K\tau_c}$ and $\tau_i = \tau$.

SIMC-PID tuning rule

[SIMC stands for SIMple Control or Skogestad Internal Model Control]

$$\begin{array}{ccc}
r(t) & \xrightarrow{\Sigma} & \xrightarrow{e(t)} & F(s) & \xrightarrow{u(t)} & G(s) & \xrightarrow{y(t)} \\
& & & & & & & \\
\end{array}$$

Given model of the process and desired closed-loop system

$$G(s) = Krac{\mathrm{e}^{-s heta}}{(au_1 s + 1)(au_2 s + 1)}, \quad au_1 \geq au_2; \qquad G_c(s) = rac{\mathrm{e}^{-s heta}}{ au_c s + 1}.$$

Good robustness is obtained with PID controller

$$F(s) = K_c \left(\frac{\tau_I s + 1}{\tau_I s}\right) (\tau_d s + 1) = \frac{K_c (\tau_I + \tau_d)}{\tau_I} \left(1 + \frac{1}{(\tau_I + \tau_D)s} + \frac{\tau_I \tau_D}{\tau_I + \tau_D} s\right)$$

with

$$K_c = \frac{\tau_1}{K(\tau_c + \theta)}, \qquad \tau_I = \min\{\tau_1, 4(\tau_c + \theta)\}, \qquad \tau_d = \tau_2$$