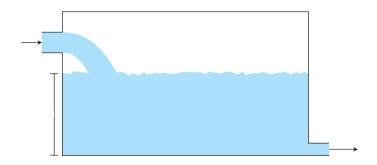
Process Automation Laboratory - Modeling first-order systems

Kjartan Halvorsen

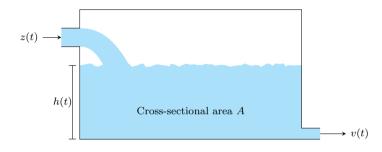
2020-08-17

First-order system example: A tank



- 1. What is the state of the system?
- 2. What is the input signal and output signal?

First-order system example: A tank



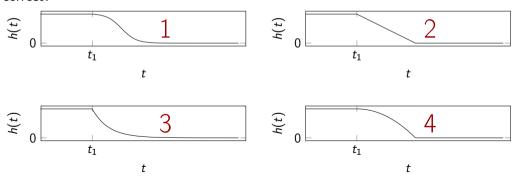
$$\frac{d}{dt}(Ah) = z(t) - x(t) = z(t) - a\sqrt{2gh} \Rightarrow$$

$$\frac{d}{dt}h(t) = -\frac{a\sqrt{2g}}{A}\sqrt{h(t)} + \frac{1}{A}z(t)$$

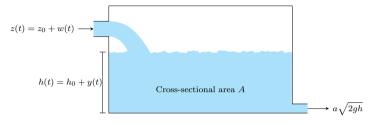
Intuition



Individual activity A constant inflow has been present since forever, but at time t_1 the flow in is suddenly shut off. Which of the responses of the water level h(t) below is correct?



Deviation variables



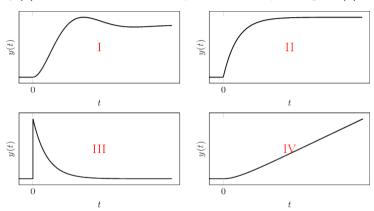
Flow in: $z(t) = z_0 + w(t)$. Level of water: $h(t) = h_0 + y(t)$. The constants h_0 and z_0 define an *operating point*.

$$\frac{d}{dt}h(t) = -\frac{a\sqrt{2g}}{A}\sqrt{h(t)} + \frac{1}{A}z(t)$$

Individual activity Given h_0 determine the operating point for the inflow, z_0 , such that the system is in equilibrium at the operating point.

Intuition

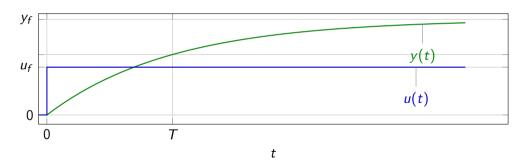
Which change y(t) in the water level corresponds to a step change w(t) in the inflow?



Fitting a first-order model

Assuming a plant model of first-order with time-constant T

$$Y(s) = \frac{K}{sT+1}U(s) \quad \stackrel{U(s) = \frac{u_f}{s}}{\Longrightarrow} \quad y(t) = u_f K(1 - e^{-\frac{t}{T}})u_H(t)$$

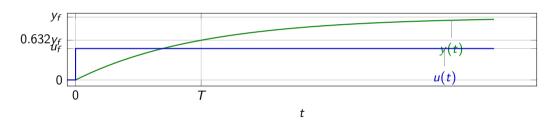


Individual activity Evaluate the response y(t) at the time instant t = T!

Fitting a first-order model

Assuming a plant model of first-order with time-constant T

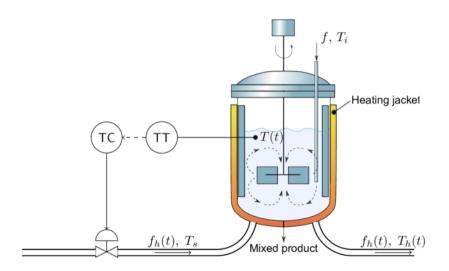
$$Y(s) = \frac{K}{sT+1}U(s) \quad \stackrel{U(s) = \frac{u_f}{s}}{\Longrightarrow} \quad y(t) = u_f K(1 - e^{-\frac{t}{T}})u_H(t)$$



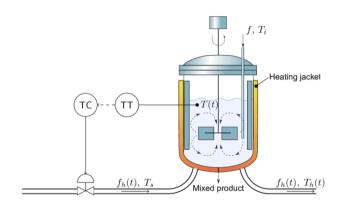
Time-constant: Find the time t = T at which the response has reached 63.2% of its final value

Gain:
$$y_f = \lim_{t \to \infty} y(t) = Ku_f \quad \Rightarrow \quad K = \frac{y_f}{u_f}$$

A Continuous Stirred Tank Reactor



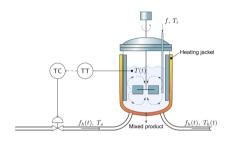
A Continuous Stirred Tank Reactor



Assume:

- constant flow f through the tank reactor
- constant temperatures T_i and T_s
- isothermic reaction (no heat absorbed or generated)

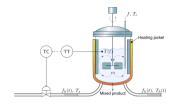
A Continuous Stirred Tank Reactor

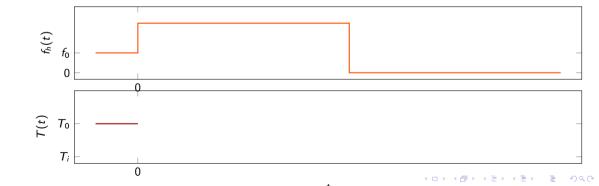


Energy balance:

$$\frac{dT(t)}{dt} = k_1 \big(T_i - T(t)\big) + k_2 \big(T_h(t) - T(t)\big)$$
$$\frac{dT_h(t)}{dt} = k_3 f_h(t) \big(T_s - T_h(t)\big) - k_4 \big(T_h(t) - T(t)\big)$$

Intuition

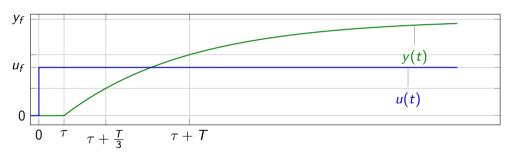




Fitting first-order model with delay

Assuming a plant model of first-order with time constant ${\cal T}$ and delay ${ au}$

$$Y(s) = \frac{Ke^{-s\tau}}{sT+1}U(s) \quad \stackrel{U(s) = \frac{u_f}{s}}{\Longrightarrow} \quad y(t) = u_f K(1 - e^{-\frac{t-\tau}{T}})u_H(t-\tau)$$



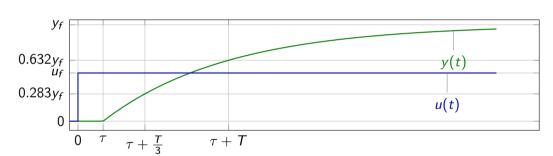
t

Individual activity Evaluate the response y(t) at the two time instants $t = \tau + \frac{T}{3}$ and $t = \tau + T!$

Fitting first-order model with delay

Assuming a plant model of first-order with time constant T and delay au

$$Y(s) = \frac{Ke^{-s\tau}}{sT + 1}U(s) \quad \stackrel{U(s) = \frac{u_f}{s}}{\Longrightarrow} \quad y(t) = u_f K(1 - e^{-\frac{t - \tau}{T}})u_H(t - \tau)$$



t

$$y_f = \lim_{t \to \infty} y(t) = u_f K \quad \Rightarrow \quad K = \frac{y_f}{u_f}.$$

First-order model with delay - example

$$Y(s) = \frac{K e^{-s\tau}}{sT + 1} U(s) \quad \stackrel{U(s) = \frac{u_f}{s}}{\Longrightarrow} \quad y(t) = u_f K \left(1 - e^{-\frac{t - \tau}{T}}\right) u_s(t - \tau)$$

$$y_{f} = 1.6 - 1.5$$

$$0.632y_{f} = 1.0112 - 1$$

$$u_{f} = 0.8 - 1$$

$$0.283y_{f} = 0.4528$$

$$0.5$$

$$0 = 1 \cdot 2 \cdot 3 \cdot 4 \cdot 5 \cdot 6 \cdot 7 \cdot 8 \cdot 9 \cdot 10 \cdot 11$$

$$t_{1} = 1.7 = \tau + \frac{\tau}{3}$$

$$t_{2} = 3.1 = \tau + T$$

$$\begin{cases}
1.7 = \tau + \frac{\tau}{3} \\
3.1 = \tau + T
\end{cases} \Rightarrow \begin{cases}
\tau = 1 \\
T = 2.1
\end{cases}, \quad K = \frac{y_{f}}{u_{f}} = \frac{1.6}{0.8} = 2$$